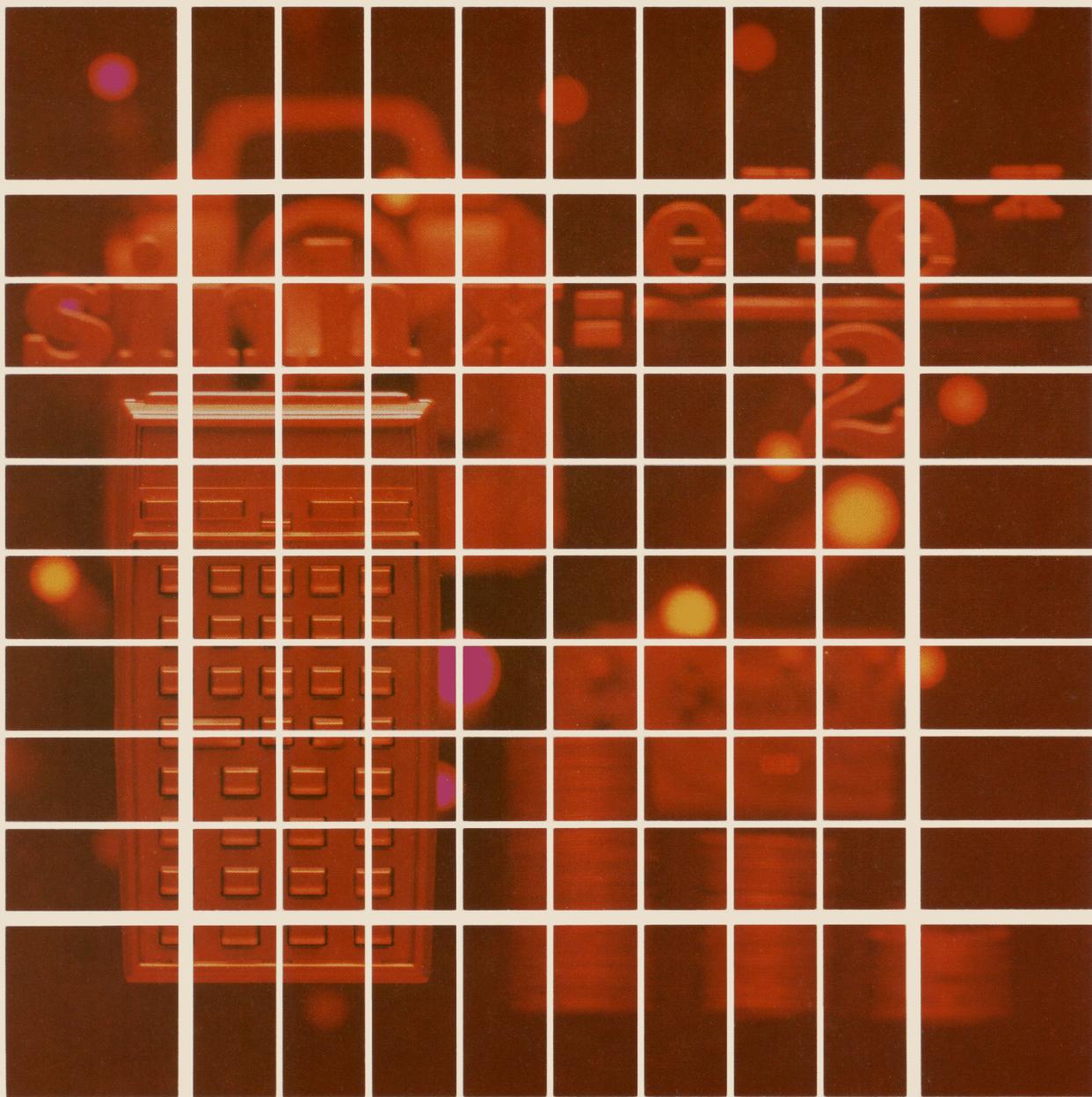


Includes barcode for easy software entry.

HEWLETT-PACKARD

**HP-41**

**USERS' LIBRARY SOLUTIONS**  
**Fluid Dynamics**



## **NOTICE**

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## INTRODUCTION

This HP-41C Solutions book was written to help you get the most from your calculator. The programs were chosen to provide useful calculations for many of the common problems encountered.

They will provide you with immediate capabilities in your everyday calculations and you will find them useful as guides to programming techniques for writing your own customized software. The comments on each program listing describe the approach used to reach the solution and help you follow the programmer's logic as you become an expert on your HP calculator.

### KEYING A PROGRAM INTO THE HP-41C

There are several things that you should keep in mind while you are keying in programs from the program listings provided in this book. The output from the HP 82143A printer provides a convenient way of listing and an easily understood method of keying in programs without showing every keystroke. This type of output is what appears in this handbook. Once you understand the procedure for keying programs in from the printed listings, you will find this method simple and fast. Here is the procedure:

1. At the end of each program listing is a listing of status information required to properly execute that program. Included is the SIZE allocation required. Before you begin keying in the program, press **XEQ ALPHA SIZE ALPHA** and specify the allocation (three digits; e.g., 10 should be specified as 010).

Also included in the status information is the display format and status of flags important to the program. To ensure proper execution, check to see that the display status of the HP-41C is set as specified and check to see that all applicable flags are set or clear as specified.

2. Set the HP-41C to PRGM mode (press the **PRGM** key) and press **■ GTO ◻ ◻** to prepare the calculator for the new program.
3. Begin keying in the program. Following is a list of hints that will help you when you key in your programs from the program listings in this handbook.
  - a. When you see " (quote marks) around a character or group of characters in the program listing, those characters are ALPHA. To key them in, simply press **ALPHA**, key in the characters, then press **ALPHA** again. So "SAMPLE" would be keyed in as **ALPHA "SAMPLE" ALPHA**.
  - b. The diamond in front of each LBL instruction is only a visual aid to help you locate labels in the program listings. When you key in a program, ignore the diamond.
  - c. The printer indication of divide sign is /. When you see / in the program listing, press **+**.
  - d. The printer indication of the multiply sign is ×. When you see × in the program listing, press **×**.
  - e. The † character in the program listing is an indication of the **APPEND** function. When you see †, press **■ APPEND** in ALPHA mode (press **■** and the K key).
  - f. All operations requiring register addresses accept those addresses in these forms:

nn (a two-digit number)

IND nn (INDIRECT: **■**, followed by a two-digit number)

X, Y, Z, T, or L (a STACK address: **◻** followed by X, Y, Z, T, or L)

IND X, Y, Z, T or L (INDIRECT stack: **■ ◻** followed by X, Y, Z, T, or L)

Indirect addresses are specified by pressing **■** and then the indirect address. Stack addresses are specified by pressing **◻** followed by X, Y, Z, T, or L. Indirect stack addresses are specified by pressing **■ ◻** and X, Y, Z, T, or L.

#### Printer Listing

```
01♦LBL "SAM
PLE"
02 "THIS IS
A"
03 "†SAMPLE
"
04 AVIEW
05 6
06 ENTER↑
07 -2
08 /
09 ABS
10 STO IND
L
11 "R3="
12 ARCL 03
13 AVIEW
14 RTN
```

#### Keystrokes

<b>■ LBL</b>	<b>ALPHA</b>	<b>SAMPLE</b>	<b>ALPHA</b>
<b>ALPHA</b>	<b>THIS IS A</b>	<b>ALPHA</b>	
<b>ALPHA</b>	<b>■ APPEND</b>	<b>SAMPLE</b>	
<b>■</b>	<b>AVIEW</b>	<b>ALPHA</b>	
6			
<b>ENTER↑</b>			
<b>2 CHS</b>			
<b>+</b>			
<b>XEQ ALPHA</b>	<b>ABS</b>	<b>ALPHA</b>	
<b>STO ■ ◻</b>	<b>L</b>		
<b>ALPHA</b>	<b>R3= ■ ARCL</b>	<b>03</b>	
<b>■ AVIEW</b>			
<b>ALPHA</b>			
<b>■ RTN</b>			

#### Display

<b>01 LBL<sup>T</sup> SAMPLE</b>
<b>02<sup>T</sup> THIS IS A</b>
<b>03<sup>T</sup> † SAMPLE</b>
<b>04 AVIEW</b>
<b>05 6</b>
<b>06 ENTER ↑</b>
<b>07 -2</b>
<b>08 /</b>
<b>09 ABS</b>
<b>10 STO IND L</b>
<b>11<sup>T</sup> R3=</b>
<b>12 ARCL 03</b>
<b>13 AVIEW</b>
<b>14 RTN</b>

## FLUID DYNAMICS AND HYDRAULICS

1.	CONDUIT FLOW.....	1
	Solves a variety of problems involving viscous conduit flow.	
2.	FLOW WITH A FREE SURFACE.....	10
	Solves flow problems using Manning flow formulae.	
3.	PIPE SLIDE-RULE.....	18
	Given surface coefficient (n) and any three of the following: 1) Flow 2) Slope 3) Pipe diameter 4) Depth %, the fourth is computed. Also computes velocity.	
4.	FORCES AT BENDS AND FITTINGS.....	26
	Solves for force due to a change in velocity of a fluid at a bend or fitting.	
5.	VALVE SIZING.....	32
	Solves Valve Coefficient (Cv) for valves used in Liquid, Gas, Vapor and Steam.	
*6.	PIPE NETWORK ANALYSIS.....	39
	Solves equivalent length of a pipe using the Hazen-Williams equation. This allows for analysis of a water distribution system using the Hardy-Cross method.	
7.	RESTRICTION METERING ORIFICE CALCULATIONS.....	53
	Solves for orifice bore and differential pressure across an orifice with flange taps for gas flow.	
8.	ENERGY EQUATION FOR STEADY FLOW.....	61
	Given any eight of nine terms of the Energy Equation, the ninth is computed.	
9.	COMPRESSIBLE FLOW IN VARIABLE AREA DUCTS.....	67
	Solves the area ratio mach number relationship for isentropic flow of a perfect gas in a variable area duct.	
10.	FLOOD ROUTING AND HYDROGRAPHS.....	75
	Solves for a unit hydrograph or a soil conservation service hydrograph given peak time and flow.	

\* Requires at least one additional memory module.

## CONDUIT FLOW

This program solves for the average velocity, or the pressure drop for viscous, incompressible flow in conduits.

Equations:

$$v^2 = \frac{\Delta P / \rho}{2 \left( f \frac{L}{D} + \frac{K_T}{4} \right)}$$

For laminar flow ( $Re < 2300$ )

$$f = 16/Re.$$

For turbulent flow ( $Re > 2300$ )

$$\frac{1}{\sqrt{f}} = 1.737 \ln \frac{D}{\epsilon} + 2.28 - 1.737 \ln \left( 4.67 \frac{D}{\epsilon Re} \sqrt{f} + 1 \right)$$

is solved by Newton's method.

$$\frac{1}{\sqrt{f_0}} = 1.737 \ln \frac{D}{\epsilon} + 2.28$$

is used as an initial guess in the iteration.

where:  $Re$  is the Reynolds number, defined as  $\rho D v / \mu$ ;

$D$  is the pipe diameter;

$\epsilon$  is the dimension of irregularities in the conduit surface (see table 2);

$f$  is the Fanning friction factor for conduit flow;

$\Delta P$  is the pressure drop along the conduit;

$\rho$  is the density of the fluid;

$\mu$  is the viscosity of the fluid;

$v$  is the kinematic viscosity of the fluid and  $\mu = \rho v$ ;

$L$  is the conduit length;

$v$  is the average fluid velocity;

$K_T$  is the total of the applicable fitting coefficients in table 1.

Table 1  
Fitting Coefficients

Fitting	K
Globe valve, wide open	7.5—10
Angle valve, wide open	3.8
Gate valve, wide open	0.15—0.19
Gate valve, 3/4 open	0.85
Gate valve, 1/2 open	4.4
Gate valve, 1/4 open	20
90° elbow	0.4—0.9
Standard 45° elbow	0.35—0.42
Tee, through side outlet	1.5
Tee, straight through	.4
180° bend	1.6
Entrance to circular pipe	0.25—0.50
Sudden expansion	$(1-A_{up}/A_{dn})^2*$
Acceleration from $v=0$ to $v=v_{\text{entrance}}$	1.0

\* $A_{up}$  is the upstream area and  $A_{dn}$  is the downstream area.

Table 2  
Surface Irregularities

Material	$\epsilon$ (feet)	$\epsilon$ (meters)
Drawn or Smooth Tubing	$5.0 \times 10^{-6}$	$1.5 \times 10^{-6}$
Commercial Steel or Wrought Iron	$1.5 \times 10^{-4}$	$4.6 \times 10^{-5}$
Asphalted Cast Iron	$4.0 \times 10^{-4}$	$1.2 \times 10^{-4}$
Galvanized Iron	$5.0 \times 10^{-4}$	$1.5 \times 10^{-4}$
Cast Iron	$8.3 \times 10^{-4}$	$2.5 \times 10^{-4}$
Wood Stave	$6.0 \times 10^{-4}$ to $3.0 \times 10^{-3}$	$1.8 \times 10^{-4}$ to $9.1 \times 10^{-4}$
Concrete	$1.0 \times 10^{-3}$ to $1.0 \times 10^{-2}$	$3.0 \times 10^{-4}$ to $3.0 \times 10^{-3}$
Riveted Steel	$3.0 \times 10^{-3}$ to $3.0 \times 10^{-2}$	$9.1 \times 10^{-4}$ to $9.1 \times 10^{-3}$

Reference:

Welty, Wicks, Wilson, *Fundamentals of Momentum, Heat and Mass Transfer*, John Wiley and Sons, Inc., 1969.

**Remarks:**

The correlation gives meaningless results in the region  $2300 < Re < 4000$ .

The solution requires an iterative procedure. The time for solution will range from 10 seconds for  $\Delta P$ , to several minutes for  $v$ . The display setting is used to determine when the solution for  $v$  is adequately accurate. Time for solution of  $v$  is roughly proportional to the number or significant digits in the display setting.

If the conduit is not circular, an equivalent diameter may be calculated using the formula below:

$$D_{eq} = 4 \frac{\text{cross sectional area}}{\text{wetted perimeter}}$$

Unitary consistency must be maintained.

**Example:**

A heat exchanger has 20, 3 meter tube passes (60 m of pipe) with 180 degrees bends connecting each pair of tubes (from table 1,  $K_T = 10 \times 1.6$ ). The fluid is water ( $v = 9.3 \times 10^{-7} \text{ m}^2/\text{s}$ ,  $\rho = 10^3 \text{ kg/m}^3$ ). The surface roughness is  $3 \times 10^{-4} \text{ m}$  and the diameter is  $2.54 \times 10^{-2} \text{ m}$ . If the fluid velocity is 3.05 m/s, what is the pressure loss? What is the Reynolds number? What is the Fanning friction factor?

**Keystrokes:**

[XEQ] [ALPHA] SIZE [ALPHA] 015

[///] [ENG] 3

[XEQ] [ALPHA] CONDUIT [ALPHA]

9.3 [EEX] [CHS] 7 [ENTER<sup>↑</sup>]

[EEX] 3 [X] [R/S]

**Display:**

U=?

[EEX] 3 [R/S]

RHO=?

3 [EEX] [CHS] 4 [R/S]

E=?

60 [R/S]

L=?

2.54 [EEX] [CHS] 2 [R/S]

D=?

16 [R/S]

KT=?

3.05 [R/S]

V=?

[R/S]

DP=?

[R/S]

DP=521.9E3

[R/S]

Re=83.30E3

[R/S]

F=10.18E-3

# User Instructions

# Program Listings

<pre> 01♦LBL "CON DUIT" 02 SF 21 03 SF 27 04 "U=?" 05 PROMPT 06 STO 09 07 "RHO=?" 08 PROMPT 09 STO 10 10 ST/ 09 11 "E=?" 12 PROMPT 13 STO 14 14 "L=?" 15 PROMPT 16 STO 03 17 "D=?" 18 PROMPT 19 STO 13 20 "KT=?" 21 PROMPT 22 4 23 / 24 STO 08 25♦LBL C 26 CF 22 27 "V=?" 28 PROMPT 29 SF 00 30 FS? 22 31 CF 00 32 STO 02 33 "DP=?" 34 PROMPT 35 STO 04 36 XEQ 09 37 FS? 00 38 GTO 03 39 RCL 02 40 X†2 41 * 42 RCL 10 43 * 44 STO 04 45 "DP=" 46 GTO 10 47♦LBL 03 48 RND 49 STO 00 </pre>	<p style="text-align: center;">Input</p> <hr/> <p style="text-align: center;">1st V</p> <hr/> <p style="text-align: center;">Calculate ΔP</p> <hr/> <p style="text-align: center;">Iterate to find V using 1st V as guess</p>	<pre> 50 XEQ 08 51 RND 52 RCL 00 53 X&lt;&gt;Y 54 X≠Y? 55 GTO 03 56 "V=?" 57 RCL 02 58 GTO 10 59♦LBL 09 60 RCL 10 61 RCL 13 62 RCL 14 63 / 64 STO 06 65 LN 66 1.737 67 STO 07 68 * 69 2.28 70 + 71 STO 12 72 STO 05 73 FS? 00 74 GTO 07 75♦LBL 08 76 16 77 RCL 02 78 RCL 13 79 * 80 RCL 09 81 / 82 STO 01 83 2300 84 X&lt;=Y? 85 GTO 02 86 RDN 87 / 88 SQRT 89 1/X 90 STO 05 91 GTO 07 92♦LBL 02 93 RCL 12 94 RCL 05 95 - 96 4.67 97 RCL 06 98 * 99 RCL 01 </pre> <hr/> <p style="text-align: right;"><math>\frac{1}{\sqrt{f}}</math></p>
---	---	---

# Program Listings

<pre> 100 / 101 RCL 05 102 * 103 1 104 + 105 STO 11 106 LN 107 RCL 07 108 * 109 - 110 RCL 11 111 1/X 112 CHS 113 1 114 + 115 RCL 07 116 * 117 RCL 05 118 / 119 1 120 + 121 / 122 ST+ 05 123 RCL 05 124 / 125 ABS 126 1 E-3 127 X&lt;=Y? 128 GTO 02 129♦LBL 07 130 RCL 05 131 1/X 132 X↑2 133 RCL 03 134 * 135 RCL 13 136 / 137 RCL 08 138 + 139 2 140 * 141 RCL 04 142 RCL 10 143 / 144 X&lt;&gt;Y 145 FS? 00 146 GTO 00 147 RTN 148♦LBL 00 149 / </pre>	<pre> 150 SORT 151 STO 02 152 RTN 153♦LBL 10 154 ARCL X 155 AVIEW 156 "Re=" 157 ARCL 01 158 AVIEW 159 "F=" 160 RCL 05 161 1/X 162 X↑2 163 ARCL X 164 AVIEW 165 END </pre>	----- Output
--	---	-----------------

## **REGISTERS, STATUS, FLAGS, ASSIGNMENTS**

DATA REGISTERS			STATUS				
00	V	50	SIZE 015 ENG _____ DEG _____	TOT. REG. 52		USER MODE	
	Re			FIX	SCI	ON X OFF _____	
	V			RAD	GRAD		
	L						
05	$\Delta P$		#	FLAGS			
	$1/\sqrt{f}$	55		INIT S/C	SET INDICATES	CLEAR INDICATES	
	$\rho/\epsilon$			00	calculate V	calculate $\Delta P$	
	1.737			22	calculate $\Delta P$	calculate V	
10	$K_T/4$		#	21	S printer enable	printer disable	
	$\mu$			27	S user mode on	user mode off	
	$\rho$	60					
	used						
15	$1/\sqrt{f_0}$		#				
	D						
	$\epsilon$						
		65					
20			#				
		70					
25		75	#				
30		80	#				
35		85	#				
ASSIGNMENTS							
40		90	#	FUNCTION	KEY	FUNCTION	KEY
				change v or			
				$\Delta P$	C		
45		95	#				

**CONDUIT FLOW****PROGRAM REGISTERS NEEDED: 38**

ROW 1 (1 : 2)



ROW 2 (3 : 7)



ROW 3 (7 : 14)



ROW 4 (14 : 20)



ROW 5 (20 : 27)



ROW 6 (27 : 33)



ROW 7 (33 : 41)



ROW 8 (42 : 50)



ROW 9 (50 : 57)



ROW 10 (58 : 66)



ROW 11 (66 : 74)



ROW 12 (74 : 83)



ROW 13 (83 : 93)



ROW 14 (94 : 103)



ROW 15 (104 : 116)



ROW 16 (117 : 126)



ROW 17 (126 : 137)



ROW 18 (138 : 148)



## CONDUIT FLOW

ROW 19 (149 : 157)



ROW 20 (157 : 165)



ROW 21 (165 : 165)



## FLOW WITH A FREE SURFACE

This program solves algebraic manipulations of the following two equations for any of the five variables in each:

Manning flow formula:

$$S = \frac{(nQ)^2}{2.2082 r^{4/3} \times a^2} \quad (1)$$

$$Q = \frac{K}{n} D^{8/3} \times S^{1/2} \quad (2)$$

Where

$S$  = slope of the bottom, dimensionless

$n$  = roughness coefficient

$r$  = hydraulic radius ft.

$Q$  = discharge rate  $\text{ft}^3/\text{sec}$

$a$  = crosssection area  $\text{ft}^2/\text{sec}$

$K$  = discharge factor dimensionless

and

$D$  = hydraulic diameter

References: Civil Engineering Handbook, Leonard Church Urquhart (ed.), McGraw-Hill Book Company, 4th Ed.  
HP-67/HP-97 Users' Library program #00269D.

Example: 1. Find Q for S = .001, N = .013, R = 5/12, and A = 5.0

2. Find K for S = .001, n = .014, Q = 200, and D = 4

Solution:

Keystrokes:

[USER]

[XEQ] [ALPHA] SIZE [ALPHA] 007

[XEQ] [ALPHA] FSFLO [ALPHA]

[A]

.001 [R/S]

.013 [R/S]

[R/S]

5 [ENT] 12 [÷] [R/S]

5 [R/S]

[B]

.001 [R/S]

.014 [R/S]

200 [R/S]

4 [R/S]

[R/S]

Display:

(Set USER mode)

LBL A OR B ?

S ?

N ?

Q ?

R ?

A ?

Q=10.0826

S ?

N ?

Q ?

D ?

K ?

K=2.1962

# User Instructions

STEP	INSTRUCTIONS	INPUT	FUNCTION	DISPLAY
1	Load the program and set USER mode		[USER]	
2	Initialize the program		[XEQ] FSFLO	LBL A OR B ?
3	For Manning Flow formula, press →		[A]	S ?
	and input 4 of the following:	S	[R/S]	N ?
	When prompted for the unknown variable,	N	[R/S]	Q ?
	press [R/S] (make no input). The unknown	Q	[R/S]	R ?
	is then automatically calculated.	R	[R/S]	A ?
		A	[R/S]	S=( )
				-or-
				N=( )
				-or-
				Q=( )
				-or-
				R=( )
				-or-
				A=( )
4	For discharge factor formula, press →		[B]	S ?
	and input 4 of the following:		[R/S]	N ?
	When prompted for the unknown variable,		[R/S]	Q ?
	press [R/S] (make no input). The		[R/S]	D ?
	unknown is then automatically calculated.		[R/S]	K ?
			[R/S]	S=( )
				-or-
				N=( )
				-or-
				Q=( )
				-or-
				D=( )
				-or-
				K=( )

# Program Listings

<pre> 01♦LBL "FSF L0" 02 "LBL A 0 R B?" 03 PROMPT 04♦LBL A 05 1.1 06 STO 00 07 CF 22 08 "S ?" 09 XEQ 11 10 "N ?" 11 XEQ 11 12 "Q ?" 13 XEQ 11 14 "R ?" 15 XEQ 11 16 "A ?" 17 XEQ 11 18 RCL 04 19 4 20 ENTER↑ 21 3 22 / 23 Y↑X 24 2.2082 25 * 26 STO 04 27 GTO IND 06 28♦LBL 01 29 XEQ 16 30 RCL 01 31 * 32 XEQ 15 33 / 34 "S" 35♦LBL 12 36 "I=" 37 ARCL X 38 PROMPT 39♦LBL 11 40 PROMPT 41 STO IND 00 42 RCL 00 43 FC?C 22 44 STO 06 45 ISG 00 46 RTN 47♦LBL 16 </pre>	<p>Equation 1</p> <p>Prompt and store data</p> <p>Calculate S</p> <p>Display routine</p> <p>Input storage routine</p>	<pre> 48 RCL 02 49 RCL 03 50 * 51 X↑2 52 RCL 01 53 / 54 RTN 55♦LBL 15 56 RCL 05 57 X↑2 58 RCL 04 59 * 60 RTN 61♦LBL 02 62 XEQ 15 63 RCL 01 64 * 65 SQRT 66 RCL 03 67 / 68 "N" 69 XEQ 12 70♦LBL 03 71 XEQ 15 72 RCL 01 73 * 74 SQRT 75 RCL 02 76 / 77 "Q" 78 XEQ 12 79♦LBL 05 80 XEQ 16 81 RCL 04 82 / 83 SQRT 84 "A" 85 XEQ 12 86♦LBL 04 87 XEQ 16 88 RCL 05 89 X↑2 90 / 91 2.2082 92 / 93 3 94 ENTER↑ 95 4 96 / 97 Y↑X 98 "R" </pre>	<p>Calculate <math>(NQ)^2 / S</math></p> <p>Calculate denominator</p> <p>Calculate N</p> <p>Calculate Q</p> <p>Calculate A</p> <p>Calculate R</p>
--	---	---	---

# Program Listings

99 XEQ 12		149 RCL 02	Calculate K
100♦LBL B	Equation 2	150 RCL 03	
101 1.1		151 RCL 01	
102 STO 00		152 /	
103 CF 22		153 *	
104 "S?"		154 RCL 04	
105 XEQ 11	Prompt and	155 /	
106 "N?"	store date	156 "K"	
107 XEQ 11		157 XEQ 12	
108 "Q?"		158♦LBL 07	
109 XEQ 11		159 RCL 05	Calculate N
110 "D?"		160 RCL 04	
111 XEQ 11		161 *	
112 "K?"		162 RCL 03	
113 XEQ 11		163 RCL 01	
114 5	adjust pointer	164 /	
115 ST+ 06		165 /	
116 RCL 01		166 "N"	
117 SQRT		167 XEQ 12	
118 STO 01		168♦LBL 09	
119 RCL 04		169 RCL 03	Calculate D
120 8		170 RCL 01	
121 ENTER↑		171 /	
122 3		172 RCL 02	
123 /		173 *	
124 Y↑X	D <sup>8/3</sup>	174 RCL 05	
125 STO 04		175 /	
126 GTO IND		176 3	
06		177 ENTER↑	
127♦LBL 08		178 8	
128 RCL 05		179 /	
129 RCL 02	Calculate Q	180 Y↑X	
130 /		181 "D"	
131 RCL 04		182 XEQ 12	
132 *		183 .END.	
133 RCL 01			
134 *			
135 "Q"			
136 XEQ 12			
137♦LBL 06		90	
138 RCL 03			
139 RCL 05			
140 RCL 02	Calculate S		
141 /			
142 RCL 04			
143 *			
144 /			
145 X↑2			
146 "S"			
147 XEQ 12			
148♦LBL 10		00	

# REGISTERS, STATUS, FLAGS, ASSIGNMENTS

DATA REGISTERS			STATUS				
#	NAME	ADDRESS	SIZE	007	TOT. REG.	053	USER MODE
			ENG	FIX	SCI	ON	x OFF
DEG	X	RAD	GRAD				
00	Pointer S or NS	50					
	n						
	Q						
	2.2082 r <sup>4/3</sup> or D <sup>8/3</sup>						
05	a or k subroutine pointer	55					
10		60					
15		65					
20		70					
25		75					
30		80					
35		85					
ASSIGNMENTS							
40		90	FUNCTION	KEY	FUNCTION	KEY	
45		95					

## FLOW WITH A FREE SURFACE

PROGRAM REGISTERS NEEDED: 47

ROW 1 (1 - 2)



ROW 2 (2 - 5)



ROW 3 (5 - 10)



ROW 4 (10 - 14)



RCW 5 (14 - 17)



ROW 6 (18 - 25)



ROW 7 (26 - 33)



ROW 8 (34 - 41)



ROW 9 (42 - 51)



ROW 10 (52 - 62)



ROW 11 (62 - 71)



ROW 12 (71 - 79)



ROW 13 (80 - 87)



ROW 14 (87 - 93)



ROW 15 (94 - 101)



ROW 16 (101 - 106)



ROW 17 (106 - 110)



ROW 18 (110 - 113)



## FLOW WITH A FREE SURFACE

ROW 19 (114 – 125)



ROW 20 (126 – 136)



ROW 21 (136 – 146)



ROW 22 (147 – 156)



ROW 23 (157 – 166)



ROW 24 (167 – 177)



ROW 25 (178 – 183)



## PIPE SLIDE-RULE

The program computes the unknown, when given the surface coefficient ( $n$ ) and any three of the following: 1) Flow ( $Q$ ); 2) Slope ( $S$ ); 3) Pipe diameter ( $D$ ); 4) Depth % ( $D/d$ ). Also computes Velocity ( $V$ ). When solving for Pipe diameter, the program automatically rounds up to a standard size of 6", 8", 12", 15", 18", 21", 24", etc.--pipe. Depth percentage ( $D/d$ ) is found by Newton's method of iteration. In the case of depth percentages between approximately 82% and 100%, two roots or values are appropriate.

Reference: HP-67/97 Users' Library program #00281D by C. B. Coleman.

Example: Find  $D/d$  and  $V$  given the following:

n = .013	s = .001 (lft/1000ft)*
Q = 850.3 CFS	D = 144 (inches)

Solution:

Keystrokes:

[///] [FIX] 2	Display:
[XEQ] [ALPHA] SIZE [ALPHA] 013	
[XEQ] [ALPHA] PSR [ALPHA] [A]	N ?
.013 [R/S]	S ?
.001 [R/S]	Q ?
850.3 [R/S]	D ?
144 [R/S]	D/d ?
[R/S]	D/d=81.96
[R/S]	(second solution) D/d=100.00
[B]	Q ?
850.3 [R/S]	D ?
144 [R/S]	D/d ?
81.96 [R/S]	V=8.57
etc.	(for second solution V=7.52)

\*Note that slope is given as rise/run, not %. A 30% slope would be entered as .30.

# User Instructions

SIZE: 013				
STEP	INSTRUCTIONS	INPUT	FUNCTION	DISPLAY
1	Load the program.			
2	Initialize		[XEQ] PSR	
3	To solve for S, Q, D or D/d:		[A]	N ?
4	Input the surface coefficient:	n	[R/S]	S ?
5	Input any three of the following:  (ft rise/ft run; Slope not as a percent)	S	[R/S]	Q ?
	Flow (ft <sup>3</sup> /sec)	Q	[R/S]	D ?
	Pipe Diameter (inches)	D	[R/S]	D/d ?
	Depth Percent (%)	D/d	[R/S]	Q=( )
				or S=( )
				or D=( )
				or D/d=( )
	When prompted for the unknown variable,  press [R/S] (make no input). When solving  for D/d, press [R/S] a second time (if no  printer is present) to find the second  solution.			
6	To calculate velocity:		[B]	Q ?
	Input: Flow (ft <sup>3</sup> /sec)	Q	[R/S]	D ?
	Pipe Diameter (inches)	D	[R/S]	D/d ?
	Depth Percent (%)	D/d	[R/S]	V=( )
	Velocity is in ft/sec.			

# Program Listings

```

01♦LBL "PSR
"                                     Initialize
02 SF 21
03 SF 27
04 RAD
05 STOP
06♦LBL B
07 SF 06
08 10
09 STO 04
10 XEQ 05
11 XEQ 02
12 ENTER↑
13 SIN
14 -
15 1/X
16 RCL 10
17 *
18 RCL 11
19 X↑2
20 /
21 1152
22 *
23 "V"
24 GTO 14
25♦LBL A
26 CF 06
27 8
28 STO 04
29 "N"
30 XEQ 00
31 "S"
32 XEQ 00
33♦LBL 05
34 "Q"
35 XEQ 00
36 "D"
37 XEQ 00
38 "D/d"
39 XEQ 00
40 FS?C 06
41 RTN
42 100
43 ST* 09
44 GTO IND
03
45♦LBL 00
46 "F ?"

47 PROMPT
48 STO IND
04
49 RCL 04
50 FC?C 22
51 STO 03
52 ISG 04
53 CLD
54 RTN
55♦LBL 10
56 SF 05
57 XEQ 02
58 XEQ 15
59 "Q"
60 GTO 14
61♦LBL 09
62 1
63 STO 09
64 XEQ 20
65 X↑2
66 100
67 /
68 "S"
69 GTO 14
70♦LBL 11
71 1
72 STO 11
73 XEQ 20
74 .375
75 Y↑X
76 6
77 X<>Y
78 X<=Y?
79 GTO 04
80 8
81 X<>Y
82 X<=Y?
83 GTO 04
84 12
85 X<>Y
86 X<=Y?
87 GTO 04
88 3
89 /
90 .999
91 +
92 INT
93 3

```

Common Input Routine

Solve for Q

Output Q

Solve for S

Output S

Solve for D

Rounding to Standard Size

# Program Listings

94 *	142 X <sup>1/2</sup>
95 X<>Y	143 /
96♦LBL 04	144 3
97 X<>Y	145 1/X
98 "D"	146 Y <sup>1/X</sup>
99 GTO 14	147 RCL 05
100♦LBL 02	148 *
101 RCL 12	149 FS?C 05
102 50	150 RTN
103 /	151 RCL 10
104 1	152 -
105 -	153 STO 00
106 CHS	154 RCL 01
107 ACOS	155 RCL 12
108 ST+ X	156 STO 01
109 STO 12	157 -
110 RTN	158 RCL 02
111♦LBL 12	159 RCL 00
112 PI	160 STO 02
113 STO 12	161 -
114 4	162 /
115 STO 01	163 *
116 CHS	164 CHS
117 STO 02	165 ST+ 12
118♦LBL 15	166 RCL 12
119 RCL 11	167 /
120 8	168 RND
121 ENTER↑	169 X≠0?
122 3	170 GTO 01
123 /	171 ?
124 Y <sup>1/X</sup>	172 RCL 12
125 RCL 09	173 X>Y?
126 SQRT	174 GTO 17
127 *	175 2
128 RCL 08	176 /
129 /	177 COS
130 320	178 1
131 X <sup>1/2</sup>	179 -
132 /	180 2
133 STO 05	181 /
134♦LBL 01	182 CHS
135 RCL 12	183 1 E2
136 ENTER↑	184 *
137 SIN	185 STO 06
138 -	186 .8196
139 5	187 X<>Y
140 Y <sup>1/X</sup>	188 "D/d"
141 RCL 12	189 X<=Y?

# Program Listings

```

190 GTO 14      Output D/d      51
191 FC? 07
192 XEQ 14
193 FS?C 07
194 GTO 14
195 SF 07
196 RCL 12
197 STO 07
198 PI
199 ST+ X      60
200 STO 01
201 CHS
202 STO 02
203 6
204 STO 12
205 GTO 15
206+LBL 20
207 SF 05
208 XEQ 02
209 XEQ 15      70
210 RCL 10
211 /
212 1/X
213 RTN
214+LBL 14
215 "F="      Output Routine
216 ARCL X
217 AVIEW
218 END      80

```

40

90

50

00

# REGISTERS, STATUS, FLAGS, ASSIGNMENTS

DATA REGISTERS			STATUS			
00	used	50	SIZE 013 TOT. REG. 60			USER MODE
	used		ENG FIX SCI			ON X OFF
	used		DEG RAD GRAD			
	subroutine pointer					
05	pointer					
	used	55				
	used					
	used					
10	n					
	S					
	Q	60				
	D					
15	D/d					
20		65				
25		70				
30		75				
35		80				
40		85				
45		90				
ASSIGNMENTS						
40			FUNCTION	KEY	FUNCTION	KEY
			Input for Q, S D or D/d	A		
			Input for V	B		
45						

## PIPE SLIDE RULE

PROGRAM REGISTERS NEEDED: 48

HEWLETT PACKARD  
SOLUTIONS BOOK  
FLUID DYNAMICS/HYDRAULICS

ROW 1 (1 : 5)



ROW 2 (6 : 11)



ROW 3 (12 : 21)



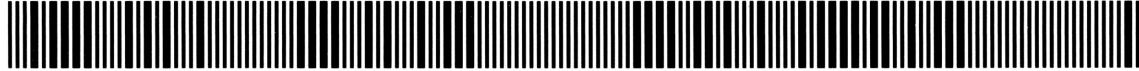
ROW 4 (22 : 29)



ROW 5 (30 : 35)



ROW 6 (35 : 39)



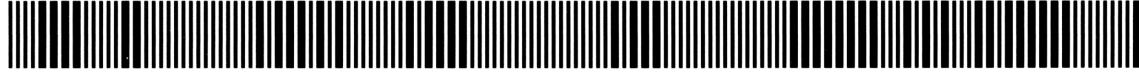
ROW 7 (40 : 46)



ROW 8 (46 : 54)



ROW 9 (55 : 60)



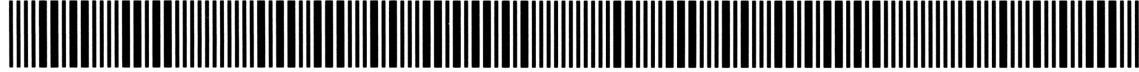
ROW 10 (61 : 68)



ROW 11 (69 : 75)



ROW 12 (76 : 85)



ROW 13 (86 : 94)



ROW 14 (95 : 104)



ROW 15 (105 : 116)



ROW 16 (117 : 128)



ROW 17 (129 : 139)



ROW 18 (140 : 151)



## PIPE SLIDE RULE

HEWLETT PACKARD  
SOLUTIONS BOOK  
FLUID DYNAMICS/HYDRAULICS

ROW 19 (152 : 164)



ROW 20 (165 : 174)



ROW 21 (174 : 184)



ROW 22 (185 : 190)



ROW 23 (190 : 196)



ROW 24 (197 : 206)



ROW 25 (206 : 213)



ROW 26 (214 : 218)



## FORCES AT BENDS AND FITTINGS

When the velocity of a flowing fluid is changed in magnitude or direction, such as at a bend or fitting, a force must act upon the fluid to cause the change. This program considers only the systems where the pipe itself is pressure-tight, but where accelerating forces must be resisted by external means to prevent movement of the piping, increased stress in the pipe walls, or both. The equations are:

$$F_x = \frac{QW}{g} (v_{2x} - v_{1x}), \quad F_y = \frac{QW}{g} (v_{2y} - v_{1y})$$

$$\bar{F} = \vec{F}_x + \vec{F}_y, \quad \bar{R} = -\bar{F},$$

where  $\bar{F}$  = accelerating force on water, lbs

$Q$  = rate of flow,  $\text{ft}^3/\text{sec}$

$W$  = specific weight,  $\text{lbs}/\text{ft}^3$

$g$  = acceleration of gravity,  $\text{ft}/\text{sec}^2$

$v_2$  = velocity leaving fittings,  $\text{ft}/\text{sec}$

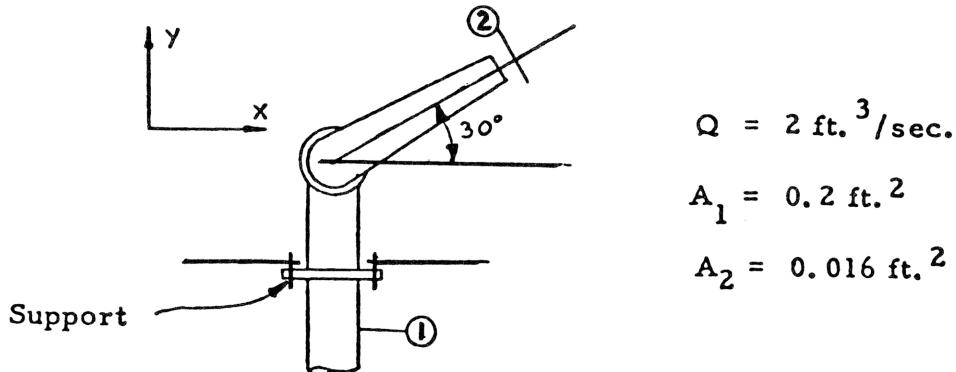
$v_1$  = velocity entering fitting,  $\text{ft}/\text{sec}$

$\bar{R}$  = reaction of water on fitting, lbs

Subscripts:  $x$  for  $x$  direction and  $y$  for  $y$  direction

References: Fluid Mechanics and Hydraulics, by Ronald V. Giles, Schaums Outline Series, McGraw-Hill Book Company, New York, 1962.  
HP-67/HP-97 Users' Library program #00268D

Example:



Find the forces on the water deck gun due to the changes in velocity and direction.

$$V, x_1 = 0$$

$$V, x_2 = V \cos \theta; \theta = 30^\circ, V = \frac{2}{.016} \left( \frac{Q}{A_2} \right).$$

$$V, y_1 = 2/.2 \quad (Q/A_1)$$

$$V, y_2 = V \sin \theta; \theta = 30^\circ, V = \frac{2}{.016} \left( \frac{Q}{A_2} \right).$$

Solution:

Keystrokes:

[XEQ] [ALPHA] SIZE [ALPHA] 002

[XEQ] [ALPHA] FORCE [ALPHA]

62.4 [R/S]

2 [R/S]

0 [R/S]

108.25 [R/S]

10 [R/S]

62.5 [R/S]

[R/S]

[R/S]

[R/S]

Display:

W ?

Q ?

V,X1 ?

V,X2 ?

V,Y1 ?

V,Y2 ?

F,X=419.940.0

F,Y=203.6490.0

F=466.7425.9

R=466.74-154.1

# User Instructions

STEP	INSTRUCTIONS	INPUT	FUNCTION	DISPLAY
1	Load the program			
2	Initialize the program		[XEQ] FORCE	W ?
3	Input: specific weight of fluid  flow rate	W Q	[R/S] [R/S]	Q ? V,X1 ?
	x-component of velocities: entering  leaving	V,X1 V,X2	[R/S] [R/S]	V,X2 ? V,Y1 ?
	y-component of velocities: entering  leaving	V,Y1 V,Y2	[R/S] [R/S]	V,Y1 ? V,Y2 ?
4	Find: x-component of force;  y-component of force;			F,X=( ) <del>4</del> 0.00 F,Y=( ) <del>4</del> 90.0
	net force; and  net reaction.			F=( ) <del>4</del> ( ) R=( ) <del>4</del> ( )

# Program Listings

01♦LBL "FOR		51	
CE"			
02 "W ?"			
03 PROMPT			
04 "Q ?"			
05 PROMPT			
06 *			
07 32.1739	WQ		
08 /	g		
09 STO 00		60	
10 STO 01			
11 "V,X1 ?"			
12 PROMPT			
13 "V,X2 ?"			
14 PROMPT			
15 -			
16 CHS			
17 ST* 00	F <sub>x</sub>		
18 "V,Y1 ?"			
19 PROMPT		70	
20 "V,Y2 ?"			
21 PROMPT			
22 -			
23 CHS			
24 ST* 01	F <sub>y</sub>		
25 0			
26 RCL 00			
27 "F,X"			
28 XEQ 08			
29 90		80	
30 RCL 01			
31 "F,Y"			
32 XEQ 08			
33 RCL 00			
34 R-P			
35 "F"			
36 XEQ 08			
37 RCL 01			
38 CHS			
39 RCL 00			
40 CHS		90	
41 R-P			
42 "R"			
43♦LBL 08	-----		
44 "I=	Display routine		
45 ARCL X			
46 "IΔ"			
47 ARCL Y			
48 PROMPT			
49 RTN			
50 .END.		00	

# REGISTERS, STATUS, FLAGS, ASSIGNMENTS

DATA REGISTERS			STATUS			
#	NAME	#				
			SIZE	TOT. REG.	USER MODE	
			ENG	FIX	SCI	ON OFF
			DEG	RAD	GRAD	
00	QW/g, FX	50				
	QW/g, FY					
05		55				
10		60				
15		65				
20		70				
25		75				
30		80				
35		85				
ASSIGNMENTS						
			FUNCTION	KEY	FUNCTION	KEY
40		90				
45		95				

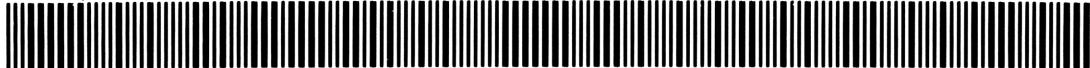
## FORCES AT BENDS AND FITTINGS

PROGRAM REGISTERS NEEDED: 17

ROW 1 (1 - 2)



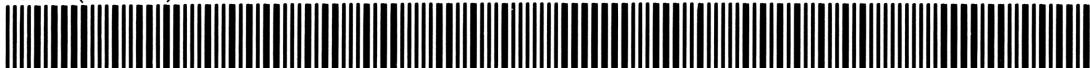
ROW 2 (3 - 7)



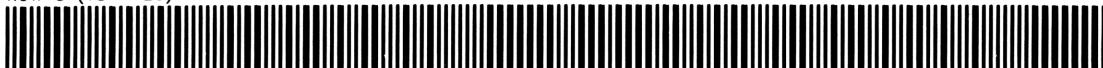
ROW 3 (7 - 13)



ROW 4 (13 - 18)



ROW 5 (18 - 20)



ROW 6 (21 - 28)



ROW 7 (28 - 34)



ROW 8 (35 - 43)



ROW 9 (44 - 50)



ROW 10 (50 - 50)



## VALVE SIZING

This program calculates the valve coefficient Cv.

Valve for Liquid flow:

$$Cv = Q \sqrt{\frac{G}{(P_1 - P_2)}}$$

Valve for Gas flow, if  $P_2 \geq \frac{P_1}{2}$  :

$$Cv = \frac{Q \sqrt{G T_a}}{1360 \sqrt{(P_1 - P_2) P_2}}$$

Valve for Gas flow, if  $P_2 < \frac{P_1}{2}$  :

$$Cv = \frac{Q \sqrt{G T_a}}{1360 (P_1/2)}$$

Valve for Vapor flow, if  $P_2 \geq \frac{P_1}{2}$  :

$$Cv = \frac{Q}{63.4} \sqrt{\frac{V_s}{(P_1 - P_2)}}$$

Valve for Vapor flow, if  $P_2 < \frac{P_1}{2}$  :

$$Cv = \frac{Q}{63.4} \sqrt{\frac{V_s}{(P_1/2)}}$$

Valve for Steam flow, if  $P_2 \geq \frac{P_1}{2}$  :

$$Cv = \frac{Q (1+0.0007 T_s)}{3 \sqrt{(P_1 - P_2) P_2}}$$

Valve for Steam flow, if  $P_2 < \frac{P_1}{2}$  :

$$Cv = \frac{Q (1+0.0007 T_s)}{3 (P_1/2)}$$

References: HP-67/HP-97 Users' Library program #02200D by Paul Crowder.  
 "Process Instruments and Control Handbook" by D. M. Constadine,  
 pub. McGraw-Hill, 1957.

Example: Calculate CV for a gas valve:

Inlet pressure - 135 psig  
Outlet pressure - 115 psig  
Sp. Gr. @ flow - 1.0

Flow temp. - 10°F  
Flow rate - 9000 CFH

Solution:

Keystrokes:

[XEQ] [ALPHA] SIZE [ALPHA] 004  
[XEQ] CV  
[ALPHA] G [ALPHA] [R/S]  
9000 [R/S]  
149.7 [R/S]  
129.7 [R/S]  
1 [R/S]  
10 [R/S]

Display:

L,G,V, OR S ?  
Q ?  
P1 ?  
P2 ?  
G ?  
T ?  
CV = 2.82

# User Instructions

# Program Listings

01♦LBL "CV"		51 XEQ 06	
02 CF 01		52 "VS ?"	
03 "L,G,V, OR S?"		53 PROMPT	
04 PROMPT	Select equation	54 RCL 01	
05 ASTO Y		55 ∕	
06 "L"		56 SQRT	
07 ASTO X		57 *	
08 X=Y?		58 CF 01	
09 GTO 01		59 XEQ 09	
10 "G"		60♦LBL 02	----- Calculate CV for gas
11 ASTO X		61 XEQ 05	
12 X=Y?		62 RCL 00	
13 GTO 02		63 1360	
14 "V"		64 ∕	
15 ASTO X		65 "G ?"	
16 X=Y?		66 PROMPT	
17 GTO 03		67 "T ?"	
18 XEQ 05	Calculate CV for steam	68 PROMPT	
19 "TS ?"		69 460	
20 PROMPT		70 +	
21 .0007		71 *	
22 *		72 SQRT	
23 1		73 *	
24 +		74 XEQ 06	
25 3		75 FS?C 01	
26 ∕		76 GTO 08	
27 RCL 00		77 GTO 10	
28 *		78♦LBL 01	----- Calculate CV for liquid
29 XEQ 06		79 XEQ 05	
30 FS?C 01		80 "G ?"	
31 GTO 08		81 PROMPT	
32♦LBL 10	P <sub>2</sub> > P <sub>1</sub>	82 RCL 01	
33 RCL 01	$\frac{P_2 - P_1}{2}$	83 RCL 02	
34 RCL 02		84 -	
35 *		85 ∕	
36 SQRT		86 SQRT	
37 ∕		87 RCL 00	
38 XEQ 09		88 *	
39♦LBL 08	P <sub>2</sub> < P <sub>1</sub>	89 XEQ 09	----- Prompt and store input
40 RCL 01	$\frac{P_1 - P_2}{2}$	90♦LBL 05	
41 ∕	-----	91 "Q ?"	
42♦LBL 09		92 PROMPT	
43 "CV="	Display	93 STO 00	
44 ARCL X	routine	94 "P1 ?"	
45 PROMPT	-----	95 PROMPT	
46♦LBL 03	Calculate CV for vapor	96 STO 01	
47 XEQ 05		97 "P2 ?"	
48 RCL 00		98 PROMPT	
49 63.4		99 STO 02	
50 ∕		100 RTN	
		101♦LBL 06	-----

# Program Listings

102	STO 03		51	
103	RCL 02	test $P_1, P_2$		
104	RCL 01	$\frac{P_1}{2}$		
105	2			
106	/			
107	X>Y?			
108	GTO 07			
109	RCL 02			
110	ST- 01	$P_2 \geq \frac{P_1}{2}$		
111	RCL 03		60	
112	RTN			
113	LBL 07			
114	STO 01			
115	SF 01			
116	RCL 03	$P_2 < \frac{P_1}{2}$		
117	RTN			
118	.END.			
20			70	
30			80	
40			90	
50			00	

# REGISTERS, STATUS, FLAGS, ASSIGNMENTS

DATA REGISTERS			STATUS			
00	Q	50	SIZE 004 TOT. REG. 035			USER MODE
	P1, P1/2 or P1-P2		ENG	FIX 2	SCI	ON OFF x
	P2		DEG x	RAD	GRAD	
	Used					
05		55	FLAGS			
			#	INIT S/C	SET INDICATES	CLEAR INDICATES
			01	C	P2 < P1/2	P2 ≥ P1/2
10		60				
15		65				
20		70				
25		75				
30		80				
35		85				
ASSIGNMENTS						
40		90	FUNCTION	KEY	FUNCTION	KEY
45		95				

## VALVE SIZING

PROGRAM REGISTERS NEEDED: 32

ROW 1 (1 - 3)



ROW 2 (3 - 6)



ROW 3 (7 - 14)



ROW 4 (14 - 19)



ROW 5 (19 - 27)



ROW 6 (28 - 36)



ROW 7 (37 - 44)



ROW 8 (44 - 51)



ROW 9 (51 - 58)



ROW 10 (58 - 63)



ROW 11 (64 - 69)



ROW 12 (69 - 77)



ROW 13 (77 - 84)



ROW 14 (85 - 92)



ROW 15 (93 - 97)



ROW 16 (98 - 109)



ROW 17 (110 - 118)



## PIPE NETWORK ANALYSIS

(Requires at least one additional memory module)

The first portion of the program computes the equivalent length of a pipe by use of the Hazen-Williams equation. This is a prerequisite to any analysis of a water distribution system by the version of the Hardy-Cross Method used herein which requires that all pipes must be of the same diameter  $d$  (normally  $d=10"$  is used) and roughness  $C$  (normally  $C=100$  is used.)

This portion of the program computes the equivalent length by the equation:

$$L_2 = L_1 \left( \frac{C_2}{C_1} \right)^{1.8519} \cdot \left( \frac{d_2}{d_1} \right)^{4.8707}$$

where the subscript 1 represents the existing pipe and the subscript 2 the equivalent pipe.

The second portion of the program computes corrected flows (4 iterations) using the Hardy-Cross method derived here:

Consider a two pipe loop; flow in one pipe  $Q_1$  and the second pipe  $Q_2$ .

- 1) Head Loss (in one pipe) =  $h = KLQ^n$  where  $K$  is a constant dependent on the diameter, roughness and length of the pipe.

$$K = \left( \frac{1.594}{C} \right)^{1.85} \cdot \frac{L}{D}^{4.87}$$

- 2) Balanced head losses ( $H_1$  and  $-H_2$ ) around loop are equal to 0

$$\Sigma H = H_1 - H_2 = 0$$

- 3) If the assumed flow split  $Q_1$  and  $-Q_2$  are each in error by the same amount  $\Delta Q$

$$\Sigma H = \Sigma K L (Q + \Delta Q)^n = 0$$

- 4) Expanding the polynomial and neglecting all but the first two terms

$$\Sigma H = \Sigma K L Q^n + \Sigma n K L \Delta Q \cdot Q^{n-1} = 0 \text{ whence } \Delta Q = \frac{-\Sigma K L Q^n}{n \Sigma K L Q^{n-1}} = \frac{-\Sigma K L Q^n}{n \Sigma K L Q^n} \bar{Q}$$

- 5) However, since all pipes are of the same size and roughness,  $K$  cancels. Also  $n = 1.85$  ( $=1/0.54$ )

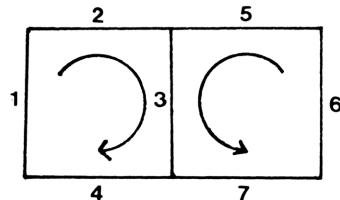
$$\Delta Q = \frac{-\Sigma L Q^{1/0.54}}{\sum \left( \frac{L Q^{1/0.54}}{Q(0.54)} \right)}$$

The third portion of the program enables the computation of the pressure (in psi) at any pipe junction in the distribution system given the starting pressure at a particular pipe junction (normally a point where flow enters the system from a pump or elevated tank). This portion of the program computes the head loss in feet along a particular pipe by the formula

$$h_f = L \left[ \left( \frac{3.5521Q}{C} \right)^{1.8519} \cdot d^{-4.8704} \right]$$

Notes:

1. All pipes must be assumed to carry some flow, no matter how small. No zero flows.
2. The program assumes loops comprise 4 pipes. If a loop contains 3 pipes, enter a zero for 4th pipe number.
3. Prior to running the program, sketch the pipe network and assign pipe numbers and flow directions (clockwise or counterclockwise). Adjacent loops must have opposite flow directions to keep the flow consistant in common pipes.



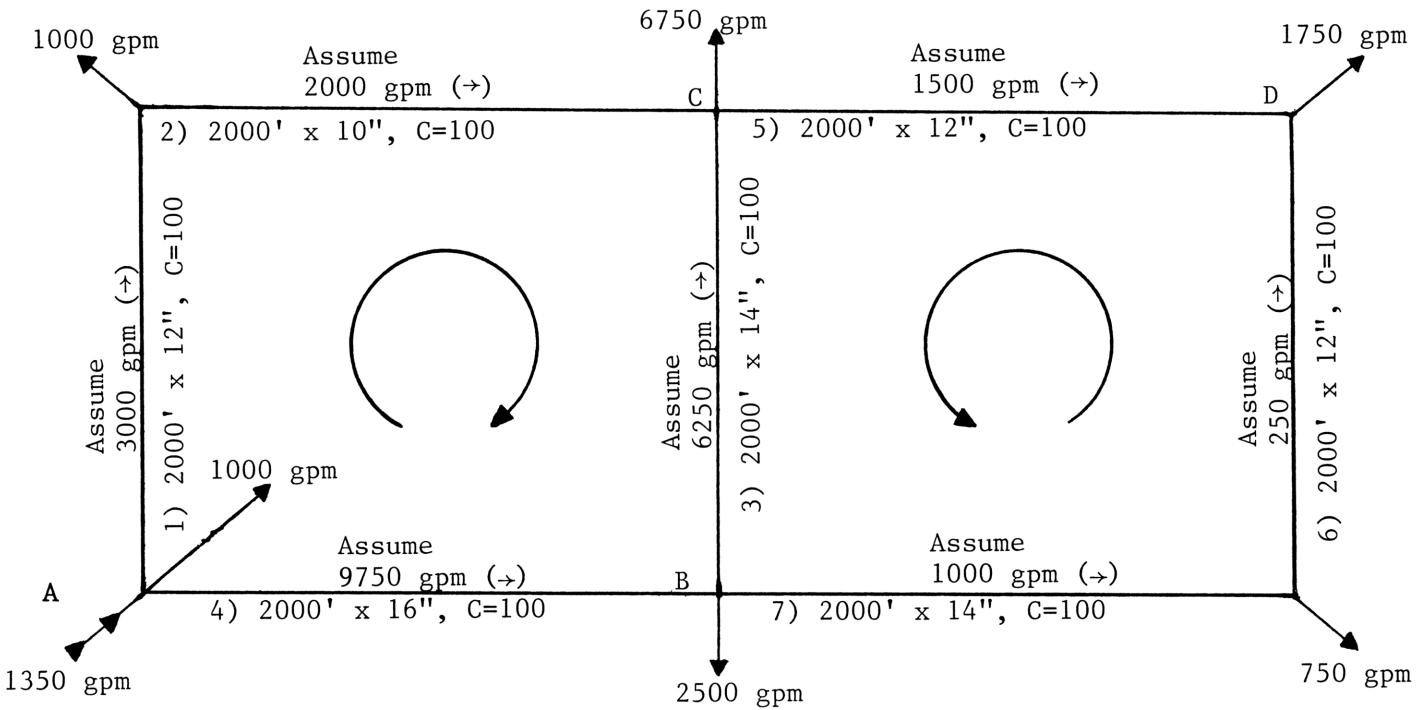
For example, the flow direction in pipe 3 (above) is the same for both loops. Then assign assumed flows in the direction of the arrows positive values and assumed flows opposite the arrows negative values. If the assumed flow in a particular pipe is inadvertently assumed in the wrong direction, the program will automatically correct the sign during the program iterations.

4. SIZE = No. of loops + 2 x No. of pipes + 7.
5. The annunciators in the display show the progress of the calculations (flags 1-4 correspond to iterations 1-4).

Reference: HP-67/HP-97 USERS LIBRARY  
program #02275D by Bernard Golding.

Example:

Compute the correct flows for the network below. Also, find the pressure at point D if the pressure at point A is 100 psi.



Solution:

Keystrokes:

```
[USER]
[XEQ] [ALPHA] SIZE [ALPHA] 023
[XEQ] [ALPHA] NA [ALPHA]
1 [R/S]
2 [R/S]
3 [R/S]
4 [R/S]
[A]
3 [R/S]
5 [R/S]
6 [R/S]
7 [R/S]
```

Display:

```
(Set USER mode)
PIPE NO. ?
PIPE NO. ?
PIPE NO. ?
PIPE NO. ?
A OR B ?
PIPE NO. ?
PIPE NO. ?
PIPE NO. ?
PIPE NO. ?
A OR B ?
```

[B]	NO. OF PIPES ?
7 [R/S]	EQUIV. DIA. ?
10 [R/S]	EQUIV. RUF. ?
100 [R/S]	L,1 ?
2000 [R/S]	d,1 ?
12 [R/S]	C,1 ?
100 [R/S]	Q,1 ?
3000 [R/S]	L,2 ?
2000 [R/S]	d,2 ?
10 [R/S]	C,2 ?
100 [R/S]	Q,2 ?
2000 [R/S]	L,3 ?
2000 [R/S]	d,3 ?
14 [R/S]	C,3 ?
100 [R/S]	Q,3 ?
6250 [CHS] [R/S]	L,4 ?
2000 [R/S]	d,4 ?
16 [R/S]	C,4 ?
100 [R/S]	Q,4 ?
9750 [CHS] [R/S]	L,5 ?
2000 [R/S]	d,5 ?
12 [R/S]	C,5 ?
100 [R/S]	Q,5 ?
1500 [CHS] [R/S]	L,6 ?
2000 [R/S]	d,6 ?
12 [R/S]	C,6 ?
100 [R/S]	Q,6 ?
250 [R/S]	L,7 ?
2000 [R/S]	d,7 ?
14 [R/S]	C,7 ?
100 [R/S]	Q,7 ?
1000 [R/S]	Q,1=3404
[R/S]	Q,2=2404
[R/S]	Q,3=-4134
[R/S]	Q,4=-9346

[R/S]	Q,5=212
[R/S]	Q,6=1962
[R/S]	Q,7=2712
[C]	EQUIV. DIA. ?
10 [R/S]	EQUIV. RUF. ?
100 [R/S]	dP,1=34.55
[R/S]	dP,2=44.09
[R/S]	dP,3=23.37
[R/S]	dP,4=55.24
[R/S]	dP,5=0.20
[R/S]	dP,6=12.45
[R/S]	dP,7=10.71

Since the pressure drops in the direction of the flow (and increases moving upstream), the pressure at point D=100.00 - 55.24 - 23.37 + .20 = 21.59psi.

# User Instructions

STEP	INSTRUCTIONS	INPUT	FUNCTION	SIZE: 007+
				DISPLAY
1	Load the program and set USER mode		[USER]	
2	Initialize the program		[XEQ] NA	PIPE NO. ?
3	Input 4 pipe numbers for each loop.	N	[R/S]	PIPE NO. ?
	Enter a zero for pipe number when there are less than 4 pipes in a loop.	N	[R/S]	PIPE NO. ?
		N	[R/S]	PIPE NO. ?
4	For another pipe loop, press and go to step 3		[A]	PIPE NO. ?
5	When all pipe loops are in, press		[B]	NO. OF PIPES ?
6	Input: the number of pipes;  equivalent diameter;  and equivalent roughness	n  d  C	[R/S]  [R/S]  [R/S]	EQUIV. DIA. ?  EQUIV. RUF. ?  L,1 ?
7	Input: pipe length;  pipe diameter;  pipe roughness;  and assumed flow.	L,x  d,x  C,x  $\pm Q,x$	[R/S]  [R/S]  [R/S]  [R/S]	d,x ?  C,x ?  Q,x ?  L,x+1 ?  or Q,1=C
8	If a mistake is made in putting L,d, or C,  press		[GTO] 03	
	and go to step 7		[R/S]	L,x ?
9	Perform step 7 until the data for all pipes  is input, at which time the program com-  putes corrected flows. If a printer is in  the system, the $\Delta Q$ 's will be printed that  the user may watch convergence.			
10	To see the corrected flows, press		[R/S]	Q,x=( )
11	Repeat step 9 until x=n.			



# Program Listings

<pre> 01♦LBL "NA" 02 FIX 0 03 CF 29 04 CF 01 05 CF 02 06 CF 03 07 CF 04 08 6.3 09 STO 03 10♦LBL A 11 ISG 03 12 RCL 03 13 STO 00 14 .01 15 STO 04 16 0 17 STO IND 03 18♦LBL 01 19 "PIPE NO ?" 20 PROMPT 21 RCL 04 22 * 23 ST+ IND 03 24 .01 25 ST+ 04 26 RCL 04 27 1 E-9 28 X&lt;=Y? 29 GTO 01 30 "A OR B ?" 31 PROMPT 32♦LBL B 33 RCL 03 34 INT 35 STO 03 36 "NO. OF PIPES?" 37 PROMPT 38 STO 06 39 + 40 1 E3 41 / 42 ST+ 03 43 ISG 03 44 1.3 45 STO 01 46 "EQUIV. </pre>	<p>Initialize</p> <p>Set up control registers</p> <p>4th pipe? no</p> <p>Prompt and store data</p>	<pre> DIA. ?" 47 PROMPT 48 STO 02 49 "EQUIV. RUF. ?" 50 PROMPT 51 STO 04 52♦LBL 03 53 "L, " 54 XEQ 04 55 RCL 02 56 "d, " 57 XEQ 04 58 / 59 2.63 60 ENTER† 61 .54 62 / 63 Y↑X 64 * 65 RCL 04 66 "C, " 67 XEQ 04 68 / 69 .54 70 1↑X 71 Y↑X 72 * 73 STO IND 03 74 RCL 06 75 RCL 03 76 + 77 "Q, " 78 XEQ 04 79 STO IND Y 80 ISG 01 81 ISG 03 82 GTO 03 83 .004 84 STO 02 85♦LBL 05 86 CF IND 0 2 87 ISG 02 88 GTO 06 89 RCL 00 90 RCL 06 91 + 92 1 </pre>	<p>Compute equivalent lengths, L and store L's and Q's</p> <p>iteration counter done, display results</p>
---	--	---	---

# Program Listings

93 +		139 SIGN
94 STO 01		140 *
95 1		141 RCL IND
96♦LBL 02		Z
97 "Q,"		142 *
98 ARCL X		143 ST+ 04
99 "I="		144 .54
100 ARCL IND		145 /
01		146 RCL IND
101 PROMPT		Y
102 1		147 /
103 +		148 ABS
104 ISG 01	set annunciator	149 ST+ 03
105 GTO 02		150 GTO 10
106♦LBL 06		151♦LBL 04
107 SF IND 0		152 ARCL 01
2		153 "I?"
108 RCL 00		154 PROMPT
109 6		155 RTN
110 -		156♦LBL 09
111 INT		157 100
112 6		158 ST* 01
113 +		159 RCL 01
114 1 E3		160 INT
115 /		161 ST- 01
116 7		162 X=0?
117 +		163 RTN
118 STO 05	clear E's	164 RCL 04
119♦LBL 07		165 RCL 03
120 0		166 /
121 STO 03	move control	167 FS? 55
122 STO 04	reg. into working	168 PRX
123 RCL IND	control reg.	169 INT
05		170 STO 03
124 STO 01		171 RCL IND
125♦LBL 10		05
126 XEQ 09		172 STO 01
127 RCL 00	compute ΔQ	173♦LBL 11
128 +		174 100
129 ENTER↑		175 ST* 01
130 ENTER↑		176 RCL 01
131 RCL 06		177 INT
132 +		178 ST- 01
133 RCL IND		179 X=0?
X		180 GTO 08
134 ABS		181 RCL 00
135 .54		182 RCL 06
136 1/X		183 +
137 Y↑X		184 +
138 RCL IND		185 RCL 03
Y		186 ST- IND
		Y

# Program Listings

187 GTO 11		234 FIX 2
188+LBL 08		235 ARCL X
189 ISG 05		236 PROMPT
190 GTO 07	do next loop	237 ISG 01
191 GTO 05	iterate	238 GTO 12
192+LBL C	compute pressure	239 .END.
193 "EQUIV. DIA. ?"	drops	
194 PROMPT		
195 STO 02	usually 10	60
196 "EQUIV. RUF. ?"		
197 PROMPT		
198 STO 04	usually 100	
199 1.1		
200 STO 01		
201+LBL 12		
202 RCL 01	pipe no., n	
203 RCL 00		
204 +		70
205 ENTER↑		
206 ENTER↑		
207 RCL 06		
208 +		
209 RCL IND Y	Q <sub>n</sub>	
210 RCL IND Y	L <sub>n</sub>	
211 ABS		
212 3.5521		80
213 *		
214 RCL 04		
215 /		
216 .54		
217 1/X		
218 Y↑X		
219 *		
220 RCL 02		
221 2.63		
222 ENTER↑		
223 .54		90
224 /		
225 CHS		
226 Y↑X		
227 *		
228 .4335		
229 *	Δ pressure	
230 "dP,"		
231 FIX 0		
232 ARCL 01	display	
233 "I="	result	00

# REGISTERS, STATUS, FLAGS, ASSIGNMENTS

DATA REGISTERS			STATUS			
#	NAME	INITIAL VALUE	SIZE		TOT. REG.	USER MODE
			ENG	DEG	SIZE+67	ON X OFF
00	pointer (last control register No.)					
	working control register					
	Equiv. dia./iteration counter					
	used					
	used					
05	control reg. pointer					
	No. of pipes					
	control reg. 1					
	control reg. 2					
	.					
10	.	60				
	L1					
	L2					
	.					
	.					
15	LN	65				
	Q1					
	Q2					
	.					
	.					
20	QN	70				
25		75				
30		80				
35		85				
ASSIGNMENTS						
40		90	FUNCTION	KEY	FUNCTION	KEY
45		95				

## PIPE NETWORK ANALYSIS

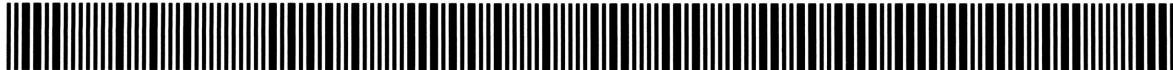
PROGRAM REGISTERS NEEDED: 67

HEWLETT PACKARD  
SOLUTIONS BOOK  
FLUID DYNAMICS/HYDRAULICS

ROW 1 (1 : 5)



ROW 2 (5 : 11)



ROW 3 (12 : 19)



ROW 4 (19 : 23)



ROW 5 (24 : 29)



ROW 6 (30 : 33)



ROW 7 (34 : 36)



ROW 8 (36 : 43)



ROW 9 (43 : 46)



ROW 10 (46 : 49)



ROW 11 (49 : 53)



ROW 12 (53 : 58)



ROW 13 (59 : 66)



ROW 14 (66 : 73)



ROW 15 (73 : 80)



ROW 16 (80 : 86)



ROW 17 (87 : 97)



ROW 18 (97 : 104)



## PIPE NETWORK ANALYSIS

HEWLETT PACKARD  
SOLUTIONS BOOK  
FLUID DYNAMICS/HYDRAULICS

ROW 19 (104 : 114)



ROW 20 (114 : 124)



ROW 21 (125 : 134)



ROW 22 (135 : 143)



ROW 23 (143 : 150)



ROW 24 (151 : 157)



ROW 25 (158 : 167)



ROW 26 (168 : 175)



ROW 27 (176 : 186)



ROW 28 (186 : 193)



ROW 29 (193 : 193)



ROW 30 (194 : 196)



ROW 31 (196 : 204)



ROW 32 (205 : 212)



ROW 33 (212 : 221)



ROW 34 (221 : 228)



ROW 35 (228 : 233)



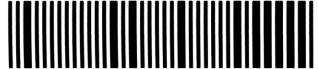
ROW 36 (233 : 239)



**PIPE NETWORK ANALYSIS**

**HEWLETT PACKARD  
SOLUTIONS BOOK  
FLUID DYNAMICS/HYDRAULICS**

ROW 37 (239 : 239)



## RESTRICTION METERING ORIFICE CALCULATIONS

This program solves for orifice bore and for differential pressure across an orifice with flange taps for gas flow.

Equations:

$$C = \frac{Q_{\text{NORM}}}{7727} \sqrt{\frac{T_F G}{P_F}}$$

$$Y_P = 1 - [0.333 + 1.145 (\beta^2 + 0.7\beta^5 + 12\beta^{13})] \frac{\Delta P}{P_F k}$$

$$S_p = \frac{C}{Y_p \sqrt{h}} , \quad h = 27.7 \Delta P$$

$$S_p = .58925\beta^2 + 0.2725\beta^3 - 0.825\beta^4 + 1.75\beta^5$$

$$d = \beta D$$

$$S_f = 0.598\beta^2 + 0.01\beta^3 + 0.00001947\beta^2 (10\beta)^{4.425}$$

$$Y_F = 1 - \left[ \frac{0.41 + 0.35\beta^4}{27.7 P_F k} \right] h_{\text{normF}} \quad h_{\text{normF}} = (C/S_f)^2 / Y_F^2$$

$$h_{\text{max}} = h_{\text{normF}} [Q_{\text{max}} / Q_{\text{normF}}]^2$$

Note: If differential pressure across orifice is too high, the second part of the program will not converge.

References: L. K. Spink, Principles and Practices of Flow Meter Engineering, 9th Ed., page 167, Plimpton Press, 1967.

R. G. Cunningham, Orifice Meters with Supercritical Compressible Flow, pages 625-638, ASTM, July 1951.

HP-67/HP-97 Users' Library program #02448D by Larry Richardson.

Example: An orifice is to be sized to control the flow of nitrogen in a 1.939" ID line to 3330 SCFH. A flow transmitter is to be connected to flange taps for an alarm. The temperature is 100°F (560°R), pressure upstream is 8.3 psig (23 psia) pressure downstream is 4.69 psig ( P=3.61 psi). Meter maximum is to be 4500 SCFH.

$$G = \frac{MW_{\text{nitrogen}}}{MW_{\text{air}}} \approx 28/28.95 \approx 0.967$$

$$K_{\text{nitrogen}} = 1.4$$

Solution:

Keystrokes:

[XEQ] [ALPHA] SIZE [ALPHA] 011	Display:
[XEQ] [ALPHA] ORF [ALPHA]	Q ?
3330 [R/S]	T ?
560 [R/S]	G ?
.967 [R/S]	P ?
23 [R/S]	dP ?
3.61 [R/S]	K ?
1.4 [R/S]	D ?
1.939 [R/S]	d=.585 (" bore)
[R/S]	QMAX ?
4500 [R/S]	HM=209. (" water column)

# User Instructions

# Program Listings

<pre> 01♦LBL "ORF" " 02 "Q ?" 03 PROMPT 04 "T ?" 05 PROMPT 06 "G ?" 07 PROMPT 08 "P ?" 09 PROMPT 10 STO 00 11 / 12 * 13 SQRT 14 X&lt;&gt;Y 15 STO 03 16 * 17 STO 09 18 "dP ?" 19 PROMPT 20 FIX 3 21 STO 01 22 27.7 23 * 24 SQRT 25 ST/ 09 26 "K ?" 27 PROMPT 28 ST* 00 29 "D ?" 30 PROMPT 31 STO 02 32 X↑2 33 7727 34 * 35 ST/ 09 36 .5 37 STO 10 38♦LBL 00 39 1 40 RCL 10 41 13 42 Y↑X 43 12 44 * 45 RCL 10 46 5 47 Y↑X 48 .7 49 * 50 + </pre>	<p>Prompt and store data</p> <p>guess for <math>\beta</math></p> <p>Calculate d</p>	<pre> 51 RCL 10 52 X↑2 53 + 54 1.145 55 * 56 .333 57 + 58 RCL 01 59 * 60 RCL 00 61 / 62 - 63 RCL 09 64 X&lt;&gt;Y 65 / 66 STO 04 67 .5 68 STO 05 69 STO 06 70♦LBL 01 71 RCL 05 72 RCL 05 73 RCL 05 74 1.75 75 * 76 .825 77 - 78 * 79 .2725 80 + 81 * 82 .58925 83 + 84 * 85 * 86 RCL 04 87 - 88 X=0? 89 GTO 03 90 X&lt;0? 91 GTO 04 92 RCL 06 93 ST- 05 94 GTO 05 95♦LBL 04 96 RCL 06 97 ST+ 05 98♦LBL 05 99 RCL 06 100 RCL 02 101 * </pre>	<p><math>Y_p</math></p> <p><math>\beta</math></p> <p>Calculate <math>S_p</math></p> <p><math>S_p = \text{power series}</math></p> <p>iterate</p>
---	---	---	--

# Program Listings

102 RND		153 X↑2	
103 X=0?		154 .598	
104 GTO 03		155 *	
105 2		156 RCL 02	
106 ST/ 06		157 3	
107 GTO 01		158 Y↑X	
108♦LBL 03		159 .01	
109 RCL 10		160 *	
110 RCL 05		161 +	
111 -		162 RCL 02	
112 RCL 02		163 6.425	
113 *		164 Y↑X	
114 RND		165 .51804	
115 X=0?		166 *	
116 GTO 06		167 +	
117 RCL 05		168 RCL 10	s <sub>f</sub>
118 STO 10		169 X<>Y	
119 GTO 00		170 /	
120♦LBL 06		171 X↑2	
121 RCL 05	β	172 STO 10	
122 RCL 02	D	173 STO 07	
123 *	-----	174♦LBL 07	
124 "d="		175 RCL 10	
125 ARCL X	Display	176 1	
126 PROMPT	result	177 RCL 01	
127 FIX 0	-----	178 RCL 07	
128 "QMAX ?"	Calculate h <sub>m</sub>	179 *	
129 PROMPT		180 -	
130 STO 04		181 X↑2	
131 RCL 01		182 /	
132 27.7		183 STO 08	
133 *		184 RCL 07	h <sub>normF</sub>
134 SQRT		185 -	
135 RCL 09		186 RND	
136 *		187 X=0?	
137 STO 10	C	188 GTO 08	
138 RCL 05	β	189 RCL 08	
139 4		190 STO 07	
140 Y↑X		191 GTO 07	
141 .35		192♦LBL 08	
142 *		193 RCL 04	
143 .41		194 RCL 03	Q <sub>max</sub>
144 +		195 /	
145 RCL 00		196 X↑2	
146 /		197 RCL 08	
147 27.7		198 *	
148 /		199 "HM="	-----
149 STO 01	[ ] Y <sub>F</sub>	200 ARCL X	
150 RCL 05		201 PROMPT	Display
151 STO 02		202 .END.	result
152 RCL 02	β		



RESTRICTION METERING  
ORIFICE CALCULATIONS  
PROGRAM REGISTERS NEEDED: 46

ROW 1 (1 - 4)



ROW 2 (4 - 8)



ROW 3 (9 - 18)



ROW 4 (18 - 25)



ROW 5 (26 - 31)



ROW 6 (32 - 39)



ROW 7 (40 - 49)



ROW 8 (50 - 56)



ROW 9 (56 - 67)



ROW 10 (68 - 76)



ROW 11 (76 - 82)



ROW 12 (82 - 90)



ROW 13 (91 - 99)



ROW 14 (100 - 109)



ROW 15 (110 - 120)



ROW 16 (121 - 128)



ROW 17 (128 - 133)



ROW 18 (134 - 143)

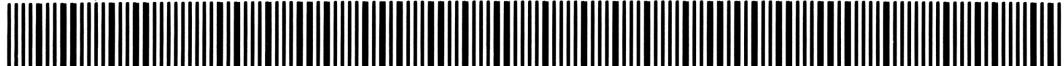


RESTRICTION METERING  
ORIFICE CALCULATIONS

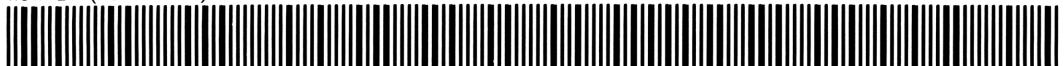
ROW 19 (143 – 152)



ROW 20 (153 – 160)



ROW 21 (161 – 165)



ROW 22 (165 – 177)



ROW 23 (178 – 189)



ROW 24 (190 – 199)



ROW 25 (199 – 202)



## ENERGY EQUATION FOR STEADY FLOW

Given any eight of the nine terms in the equation below, the program calculates the unknown term.

Energy Equation:

$$\frac{P_1}{W} + Z_1 + \frac{V_1^2}{2g} + H_p = \frac{P_2}{W} + Z_2 + \frac{V_2^2}{2g} + H_T + H_L$$

where

$H$  = total dynamic head, ft.

$H_p$  = head added by pump, ft.

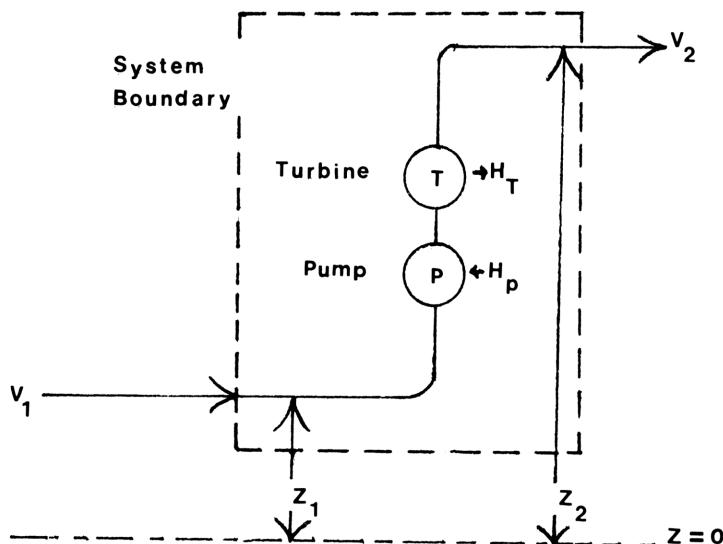
$H_T$  = head extracted by turbine, ft.

$H_L$  = head loss due to friction, ft.

$\frac{V^2}{2g}$  = velocity head, ft.

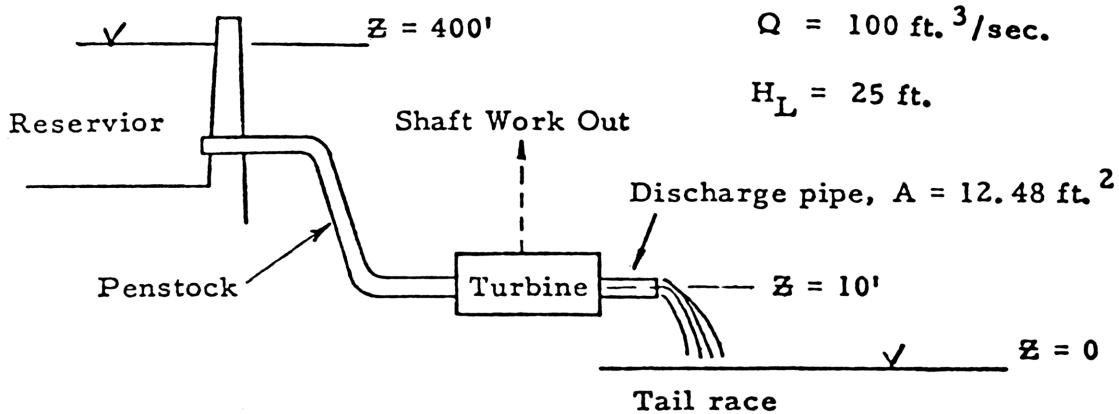
$\frac{P}{W}$  = pressure head, ft.

$Z$  = potential head, ft.



References: HP-67/HP-97 Users' Library program #00267D  
Fluid Mechanics and Hydraulics, by Ronald V. Giles, Schaums Outline Series, McGraw-Hill Book Company, New York, 1962.

Example:



Find the head extracted by the turbine.

Solution:

Keystrokes:

```
[XEQ] [ALPHA] SIZE [ALPHA] 013
[XEQ] [ALPHA] ENRG [ALPHA]
0 [R/S]
400 [R/S]
0 [R/S]
0 [R/S]
0 [R/S]
10 [R/S]
100 [ENT] 12.48 [:] [x2] 64.4 [:] [R/S]
[R/S]
25 [R/S]
```

Display:

```
P1 HEAD ?
Z1 HEAD ?
V1 HEAD ?
HP HEAD ?
P2 HEAD ?
Z2 HEAD ?
V2 HEAD ?
HT HEAD ?
HL HEAD ?
HT HEAD=364.00
```

# User Instructions

STEP	INSTRUCTIONS	INPUT	FUNCTION	DISPLAY
1	Load the program			
2	Initialize the program		[XEQ] ENRG	P1 HEAD ?
3	Input 8 of the following:	P1 HEAD	[R/S]	Z1 HEAD ?
		Z1 HEAD	[R/S]	V1 HEAD ?
		V1 HEAD	[R/S]	HP HEAD ?
		HP HEAD	[R/S]	P2 HEAD ?
		P2 HEAD	[R/S]	Z2 HEAD ?
		Z2 HEAD	[R/S]	V2 HEAD ?
		V2 HEAD	[R/S]	HT HEAD ?
		HT HEAD	[R/S]	HL HEAD ?
		HL HEAD	[R/S]	(xx) HEAD=( )
	When prompted for the unknown variable,			
	press [R/S] (make no input). That			
	quantity is then automatically calculated.			
				SIZE: 013

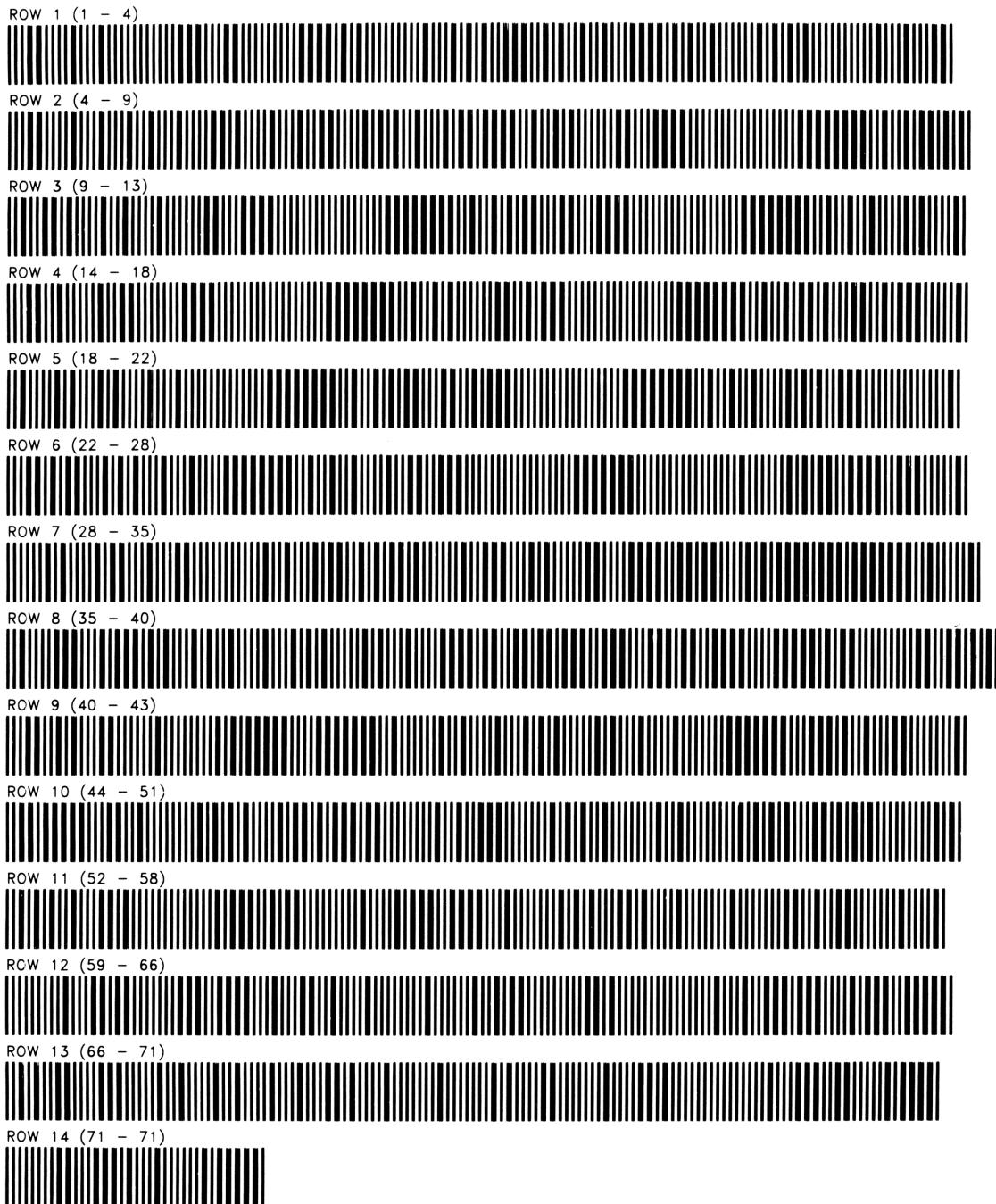
# Program Listings

01♦LBL "ENR		47 CF 01	
G"	Initialize	48 RCL 00	
02 CF 02		49 5	RHS or LHS?
03 SF 01		50 X<=Y?	
04 1.1		51 SF 02	
05 STO 00		52♦LBL 10	
06 CF 22		53 ISG 00	
07 "P1"		54 RTN	
08 XEQ 15		55♦LBL 16	
09 "Z1"	Prompt and	56 5.009	Calculate
10 XEQ 15	store data	57 STO 00	RHS
11 "V1"		58 0	
12 XEQ 15		59♦LBL 17	
13 "HP"		60 RCL IND	
14 XEQ 15		00	
15 "P2"		61 +	
16 XEQ 15		62 ISG 00	
17 "Z2"		63 GTO 17	
18 XEQ 15		64 STO 11	
19 "V2"		65 RTN	
20 XEQ 15		66♦LBL 18	
21 "HT"		67 1.004	Calculate
22 XEQ 15		68 STO 00	LHS
23 "HL"		69 0	
24 XEQ 15		70 GTO 17	
25 XEQ 16		71 .END.	
26 RCL 11	Compute		
27 STO 12	unknown		
28 XEQ 18			
29 RCL 12			
30 FC? 02		80	
31 X<>Y			
32 -			
33 CLA			
34 ARCL 10	Display		
35 "F HEAD=	result		
"			
36 ARCL X			
37 PROMPT			
38♦LBL 15			
39 FS? 01		90	
40 ASTO 10			
41 "F HEAD			
?"			
42 PROMPT			
43 STO IND			
00			
44 FS?C 22			
45 GTO 10			
46 ST- IND			
00	Zero results	00	

# REGISTERS, STATUS, FLAGS, ASSIGNMENTS

DATA REGISTERS			STATUS			
00	pointer	50	SIZE .013 TOT. REG. .038 USER MODE ENG ____ FIX 2 SCI ____ ON ____ OFF X DEG X RAD ____ GRAD ____			
	P1 head					
	Z1 head					
	v1 head					
05	HP head					
	P2 head	55				
	Z2 head					
	V2 head					
10	HT head					
	HL head					
	prompt	60				
	temp. storage					
15	temp. storage					
20		65				
25		70				
30		75				
35		80				
40		85				
45		90				
ASSIGNMENTS						
			FUNCTION	KEY	FUNCTION	KEY
40		95				

ENERGY EQUATION FOR  
STEADY FLOW  
PROGRAM REGISTERS NEEDED: 25



## COMPRESSIBLE FLOW IN VARIABLE AREA DUCTS

This program solves the area ratio mach number relationship for isentropic flow of a perfect gas in a variable area duct. The program will find M given A/A\* or A/A\* given M, or T/To, P/Po or M given any one of these three quantities. The zero subscript refers to stagnation conditions.

Equations:

$$A/A^* = \frac{1}{M} \left( \frac{1 + \frac{k-1}{2} M^2}{\frac{k+1}{2}} \right)^{\frac{k+1}{2(k-1)}}$$

$$P/P_o = \left( 1 + \frac{k-1}{2} M^2 \right)^{\frac{-k}{2(k-1)}}$$

$$T/T_o = \left( 1 + \frac{k-1}{2} M^2 \right)^{-1}$$

where

T = temperature

P = pressure

A = cross-sectional area of ducts at which M occurs

M = Mach number

A\* = throat area of duct

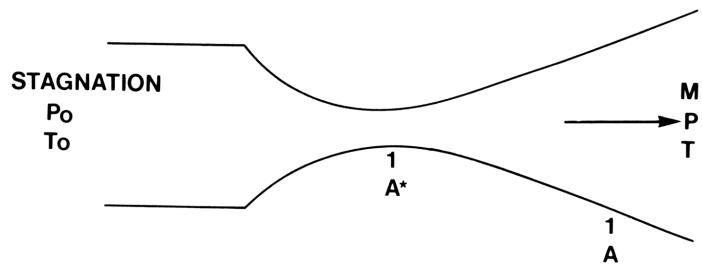
and

$$k = \frac{C_p}{C_n}, \quad C_p = \text{specific heat at constant pressure} \\ C_n = \text{specific heat at constant volume}$$

Notes: The equations apply only to a perfect gas with constant specific heats. An initial guess for M must be supplied for the first equation given above if the area ratio A/A\* is the known quantity. If the guess for M is < 1 then the program converges to a Mach number < 1. If the guess for M is > 1 then the program converges to a solution for M > 1.

References: HP-65 Users' Library program #00780A by Harry Townes.

Example:



For  $K = 1.4$  and  $A/A^* = 1.5$ , find the two possible Mach numbers,  $T/T_o$  and  $P/P_o$ .

Solution:

Keystrokes:

```
[USER]
[XEQ] [ALPHA] SIZE [ALPHA] 009
[XEQ] [ALPHA] COMFLO [ALPHA]
[A]
1.4 [R/S]
1.5 [R/S]
.5 [R/S]
[A]
1.4 [R/S]
1.5 [R/S]
1.5 [R/S]
[B]
1.4 [R/S]
.4303 [R/S]
[R/S]
[B]
1.4 [R/S]
1.8541 [R/S]
[R/S]
```

Display:

```
(Set USER mode)
LBL A OR B ?
K ?
A/A* ?
GUESS FOR M ?
M=0.4303
K ?
A/A* ?
GUESS FOR M ?
M=1.8541
K ?
M ?
T/To=0.9643
P/Po=0.8805
K ?
M ?
T/To=0.5926
P/Po=0.1602
```

# User Instructions

# Program Listings

<pre> 01♦LBL "COM FLO" 02 "LBL A 0 R B ?" 03 PROMPT 04♦LBL A 05 CF 01 06 "K ?" 07 PROMPT 08 1 09 + 10 2 11 / 12 STO 03 13 RCL 03 14 1 15 - 16 STO 04 17 / 18 2 19 / 20 STO 02 21 CF 22 22 "A/A* ?" 23 PROMPT 24 FS? 22 25 SF 01 26 STO 05 27 "GUESS F OR M?" 28 FC? 22 29 "M ?" 30 PROMPT 31 STO 01 32♦LBL 01 33 RCL 01 34 X↑2 35 RCL 04 36 * 37 1 38 + 39 RCL 03 40 / 41 STO 06 42 RCL 02 43 Y↑X 44 STO 07 45 RCL 01 46 / 47 FC? 01 48 GTO 02 </pre>	<p>A/A* vs. M</p> <p>Input made? yes</p> <p>Calculate A/A*</p> <p>A/A*</p>	<pre> 49 RCL 05 50 - 51 STO 08 52 RCL 07 53 CHS 54 RCL 01 55 X↑2 56 / 57 RCL 06 58 RCL 02 59 1 60 - 61 Y↑X 62 + 63 RCL 08 64 X&lt;&gt;Y 65 / 66 ST- 01 67 ABS 68 RCL 01 69 / 70 1 E-3 71 X&lt;=Y? 72 GTO 01 73 RCL 01 74 GTO 09 75♦LBL 02 76 "A/A*" 77 GTO 03 78♦LBL B 79 "K ?" 80 PROMPT 81 STO 00 82 1 83 - 84 ST/ 00 85 2 86 / 87 STO 02 88 CF 22 89 "M ?" 90 PROMPT 91 FS? 22 92 GTO 04 93 "T/Ta ?" 94 PROMPT 95 FS? 22 96 GTO 05 97 "P/Pa ?" 98 PROMPT 99 RCL 00 </pre>	<p>Calculate M iteratively</p> <p>T/To, P/Po, vs. M</p> <p>M input? yes</p>
---	--	--	---

# Program Listings

100 CHS	Calculate M given P/Po	51		
101 1/X				
102 Y↑X				
103 1				
104 -				
105 RCL 02				
106 /				
107 SQRT				
108♦LBL 09		60		
109 "M"				
110♦LBL 03	Display routine			
111 "T="				
112 ARCL X				
113 PROMPT				
114 RTN				
115♦LBL 04				
116 X↑2				
117 *				
118 1				
119 +		70		
120 STO 01	Calculate T/To			
121 1/X				
122 "T/Ta"				
123 XEQ 03				
124 RCL 01				
125 RCL 00				
126 Y↑X				
127 1/X				
128 "P/Pa"				
129 XEQ 03				
130♦LBL 05	Calculate P/Po	80		
131 1/X				
132 1				
133 -				
134 RCL 02				
135 /				
136 SQRT				
137 GTO 09				
138 .END.				
40		90		
50		00		

## **REGISTERS, STATUS, FLAGS, ASSIGNMENTS**

DATA REGISTERS			STATUS			
00	K/(K-1)	50	SIZE	009	TOT. REG.	052
	Used		ENG	FIX 4	SCI	USER MODE
	(K+1)/2(K-1) or (K-1)/2		DEG	X	RAD	ON X OFF
	(K-1)/2					
	(K-L)/2					
05	A/A*	55	FLAGS			
	Used		#	INIT S/C	SET INDICATES	CLEAR INDICATES
	Used		01	C	calculate M	calculate A/A*
	Used		22	C	refer to owner's manual	
10		60				
15		65				
20		70				
25		75				
30		80				
35		85				
40		90	ASSIGNMENTS			
45		95		FUNCTION	KEY	FUNCTION

COMPRESSIBLE FLOW IN VARIABLE  
AREA DUCTS  
PROGRAM REGISTERS NEEDED: 36

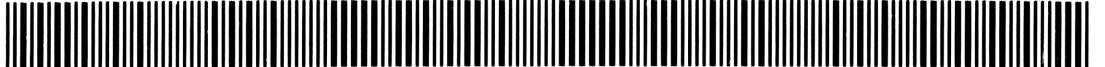
ROW 1 (1 - 2)



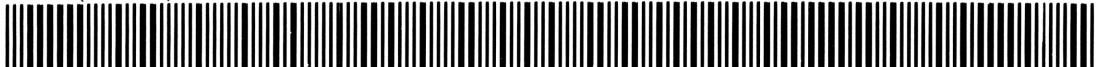
ROW 2 (2 - 4)



ROW 3 (5 - 13)



ROW 4 (14 - 22)



ROW 5 (22 - 27)



ROW 6 (27 - 29)



ROW 7 (29 - 40)



ROW 8 (41 - 51)



ROW 9 (52 - 64)



ROW 10 (65 - 72)



ROW 11 (73 - 78)



ROW 12 (79 - 87)



ROW 13 (88 - 93)



ROW 14 (93 - 97)



ROW 15 (97 - 106)



ROW 16 (107 - 115)



ROW 17 (116 - 123)



ROW 18 (123 - 129)



COMPRESSIBLE FLOW IN VARIABLE  
AREA DUCTS

ROW 19 (130 - 138)



## FLOOD ROUTING AND HYDROGRAPHS

This program calculates either a unit hydrograph or a soil conservation service hydrograph from a given peak time (time of concentration) and peak flow. Any time interval can be selected. The program will also route a given hydrograph through a given dam calculating an outflow hydrograph from given storage conditions and a given outflow structure.

Equations:

### Flood routing

$$I_n + I_{n+1} + \frac{2 S_n}{\Delta t} - O = \frac{2 S_{n+1}}{\Delta t} + O_{n+1}$$

where:

I = inflow;

S = storage;

$\Delta t$  = time interval;

O = outflow;

n = cycle number.

### UNIT HYDROGRAPH

$$y = 1.45x^{1.67}, \quad 0.5 > x > 0$$

$$y = 1.16 + \ln x, \quad 0.9 > x > 0.5$$

$$y = \text{Sin} (e^{x-1} \cdot 90), \quad 1.2 > x > 0.9$$

$$y = 1.93 - .83 x, \quad 1.6 > x > 1.2$$

$$y = 7.49e^{-1.63x}, \quad x > 1.6$$

SCS HYDROGRAPH

$$y = 1.7 x^2, \quad 0.7 > x > 0$$

$$y = 1.06 + .8 \ln x, \quad 1. > x > 0.7$$

$$y = 1.9 - .83x, \quad 1.8 > x > 1.0$$

$$y = 5.7e^{-1.44x}, \quad x > 1.8$$

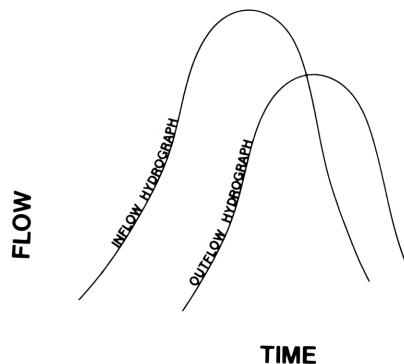
where  $x = \text{time/time of peak}$

and  $y = \text{flow/peak flow}$

Notes: If a subroutine is used to calculate outflow from  $[\frac{2}{\Delta t} S + \text{outflow vs. outflow}]$  it must always produce flows greater than or equal to zero.

- References:
1. HP-67/HP-97 USER'S LIBRARY program #01442D by Lawrence Busack
  2. PENNSYLVANIA STATE UNIVERSITY, Hydrologic and Hydraulic Analysis for Small Watersheds, PENN State University, University Park, PA, 1974.
  3. U.S. Department of Interior, Bureau of Reclamation, Design of Small Dams, GPO, Washington, D.C., 1974.
  4. U.S. Department of Agriculture, Soil Conservation Service, National Engineering Handbook Section 4 - Hydrology, GPO, Washington, D.C., 1972.

Example:



A dam with a sharp crested weir spillway is located on a small stream. The spillway is 100 feet wide and has a discharge coefficient of 3.5. At the elevation of the spillway no water is stored. At an elevation of 2 feet above the spillway 100 acre-feet of water is stored and at an elevation of 4 feet above the spillway 250 acre-feet of water is stored. A flood which reaches a peak flow of 1400 cfs in 2.9 hours flows through the dam. Calculate the inflow hydrograph using the SCS curve and the outflow hydrograph. Use a 1/4 hour time interval.

Solution:

First develop the outflow vs.  $\frac{2S}{\Delta t} + \text{outflow}$  relationship

at 2 feet elevation,

$$\begin{aligned} \text{outflow} &= (3.5) (100) (2)^{3/2} [Q = CLH^{3/2}] \\ &= 989.95 \text{ cfs} \\ \frac{2S}{\Delta t} + \text{outflow} &= \left[ \frac{(2)(100) \text{ AC-FT}}{.25 \text{ HRS}} \right] \left[ \frac{43560 \text{ ft}^3}{\text{AC-FT}} \right] \\ &\quad \times \left[ \frac{1}{3600 \frac{\text{SEC}}{\text{HR}}} \right] + 989.95 \\ &= 10669.95 \text{ cfs} \end{aligned}$$

Then, calculating outflow values at each elevation and  $\frac{2S}{\Delta t} + \text{outflow}$  (as above) for 4 feet and interpolating to find intermediate values, the following table is developed:

<u>ELEVATION</u>	<u>OUTFLOW</u>	<u><math>\frac{2S}{\Delta t} + \text{OUTFLOW}</math></u>
0	0	0
1/2	123.74	2543.74
1	350.00	5190.00
1 1/2	642.99	7902.99
2	989.95	10669.95
2 1/2	1383.50	14693.50
3	1818.65	18758.65
3 1/2	2291.77	22861.77
4	2800.00	27000.00

Using a curve-fitting program to yield an analytical expression for the above table,

$$\text{OUTFLOW} \approx 0.11 \left[ \frac{2S}{\Delta t} + \text{outflow} \right] - 200$$

This equation is programmed in subroutine 09.

The hydrographs (inflow and outflow) are then calculated. The keystrokes which follow reflect a printer in the system.

KEYSTROKES:

DISPLAY:

[USER]

(set USER mode)

[XEQ] [ALPHA] SIZE [ALPHA] 009

[XEQ] [ALPHA] HYDRO [ALPHA]

TIME INTVL. ?

.25 [R/S]

TIME, PEAK Q ?

2.90 [R/S]

PEAK Q ?

1400 [R/S]

A,B, OR C ?

[C]

A OR B ?

[B]

T=0.00

IN=0.00

T=0.25

IN=17.69

OUT=0.00  
•  
•               (increment T)  
•  
T=1.25  
  
IN=442.18  
  
OUT=0.00  
  
T=1.50  
  
IN=636.74  
  
OUT=86.00  
  
etc.  
•  
•               (increment T)  
•

# User Instructions

SIZE: 009

STEP	INSTRUCTIONS	INPUT	FUNCTION	DISPLAY
1	Load the program and set USER mode		[USER]	
2	Initialize the program		[XEQ] HYDRO	TIME INTVL. ?
3	Input: time interval; time of peak flow; and peak flow.	i t_peak Q_peak	[R/S] [R/S] [R/S]	TIME, PEAK Q ? PEAK Q ? A, B, OR C ?
4	To do flood routing, press		[C]	A OR B ?
5	For a unit hydrograph, press		[A]	T=( )
6	find inflow		[R/S]*	IN=( )
7	flood routing only, find outflow		[R/S]*	OUT=( )
8	Increment T and go to step 6		[R/S]*	T=( )
9	For an SCS hydrograph, press		[B]	T=( )
10	Find inflow		[R/S]*	IN=( )
11	flood routing only, find outflow		[R/S]*	OUT=( )
12	Increment T and go to step 10		[R/S]*	T=( )
	NOTE: If an analytical expression is not known for outflow as a function of $\frac{2S}{\Delta t} +$ outflow, outflow may be read from a graph of the function and input manually at step 7 or 11. To do so, change line 112 from XEQ09 to R/S. When the program stops, enter a value for outflow which corresponds to the value for $\frac{2S}{\Delta t} +$ outflow in the display, and press [R/S] to continue.  *These keystrokes are unnecessary if there is a printer in the system.			

# Program Listings

<pre> 01♦LBL "HYD R0" 02 CLRG 03 SF 21 04 CF 02 05 "TIME IN TVL. ?" 06 PROMPT 07 STO 01 08 "TIME, P EAK Q?" 09 PROMPT 10 STO 00 11 "PEAK Q ?" 12 PROMPT 13 STO 04 14 "A,B, OR C ?" 15 PROMPT 16♦LBL A 17 11 18 STO 08 19 GTO 11 20♦LBL B 21 12 22 STO 08 23 GTO 12 24♦LBL C 25 SF 02 26 SF 03 27 "A OR B ?" 28 PROMPT 29♦LBL 10 30 "I=" 31 ARCL X 32 AVIEW 33 RTN 34♦LBL 12 35 RCL 02 36 RCL 00 37 / 38 STO 03 39 .7 40 X&gt;Y? 41 GTO 00 42 X&lt;&gt;Y 43 1 44 X&gt;Y? 45 GTO 01 </pre>	<pre> Initialize -----</pre> <p>Prompt and store data</p> <pre> -----</pre> <p>UNIT hydrograph</p> <p>SCS hydrograph</p> <p>do flood routing</p> <pre> -----</pre> <p>Display routine</p> <pre> -----</pre> <p>SCS hydrograph calculations</p>	<pre> 46 X&lt;&gt;Y 47 1.8 48 X&gt;Y? 49 GTO 02 50 RCL 03 51 1.44 52 * 53 CHS 54 E↑X 55 5.7 56 * 57 GTO 03 58♦LBL 00 59 RCL 03 60 X↑2 61 1.7 62 * 63 GTO 03 64♦LBL 01 65 RCL 03 66 LN 67 .8 68 * 69 1.06 70 + 71 1 72 X&gt;Y? 73 X&lt;&gt;Y 74 GTO 03 75♦LBL 02 76 RCL 03 77 .83 78 * 79 CHS 80 1.9 81 + 82 1 83 X&gt;Y? 84 X&lt;&gt;Y 85♦LBL 03 86 RCL 04 87 * 88 RCL 02 89 "T" 90 XEQ 10 91 RCL 01 92 + 93 STO 02 94 X&lt;&gt;Y 95 "IN" 96 XEQ 10 </pre>	<p>increment time</p>
--	--	--	-----------------------

# Program Listings

97 FC? 02		145 RCL 03
98 GTO IND		146 1.63
08		147 *
99 FS?C 03		148 CHS
100 GTO 13		149 E↑X
101 RCL 05		150 7.49
102 X<>Y		151 *
103 STO 05		152 GTO 03
104 +		153♦LBL 04
105 STO 06		154 RCL 03
106 RCL 07		155 1.67
107 FS?C 01		156 Y↑X
108 RCL 05		157 1.45
109 RCL 06		158 *
110 +		159 GTO 03
111 STO 07		160♦LBL 05
112 XEQ 09	change to STOP for manual input	161 RCL 03
113 2		162 LN
114 *		163 1.16
115 ST- 07		164 +
116 2		165 GTO 03
117 /		166♦LBL 06
118 "OUT"		167 RCL 03
119 XEQ 10		168 1
120 GTO IND		169 -
08		170 E↑X
121♦LBL 13		171 90
122 SF 01		172 *
123 STO 05		173 DEG
124 GTO IND		174 SIN
08		175 GTO 03
125♦LBL 11	UNIT hydrograph calculations	176♦LBL 07
126 RCL 02		177 RCL 03
127 RCL 00		178 .83
128 /		179 *
129 STO 03		180 CHS
130 .5		181 1.93
131 X>Y?		182 +
132 GTO 04		183 GTO 03
133 X<>Y		184♦LBL 09
134 .9		185 .11
135 X>Y?		186 *
136 GTO 05		187 200
137 X<>Y		188 -
138 1.2		189 X<0?
139 X>Y?		190 0
140 GTO 06		191 RTN
141 X<>Y		192 .END.
142 1.6		
143 X>Y?		
144 GTO 07		00

} calculate out-  
flow peculiar  
to the sample  
problem

# REGISTERS, STATUS, FLAGS, ASSIGNMENTS

DATA REGISTERS			STATUS			
00	Time, peak	50	SIZE 009 ENG _____ DEG X	TOT. REG. 59	USER MODE ON <input checked="" type="checkbox"/> OFF _____	
	Time increment			FIX 2	SCI _____	ON <input type="checkbox"/> OFF _____
	Time, total			RAD _____	GRAD _____	
	T/T peak					
	Q peak					
05	Qi	55	FLAGS			
	In+In+1		#	INIT S/C	SET INDICATES	CLEAR INDICATES
	2S/Δt + 0,-0		01	C	1st pass through	
	Pointer		02	C	do flood routing	
			03	C	1st pass through	
10		60				
15		65				
20		70				
25		75				
30		80				
35		85				
ASSIGNMENTS						
40		90	FUNCTION	KEY	FUNCTION	KEY
45		95				

## FLOOD ROUTING AND HYDROGRAPHS

PROGRAM REGISTERS NEEDED: 51

ROW 1 (1 - 4)



ROW 2 (4 - 5)



ROW 3 (5 - 8)



ROW 4 (8 - 11)



ROW 5 (11 - 14)



ROW 6 (14 - 20)



ROW 7 (20 - 27)



ROW 8 (27 - 30)



ROW 9 (31 - 41)



ROW 10 (41 - 49)



ROW 11 (50 - 57)



ROW 12 (57 - 66)



ROW 13 (67 - 74)



ROW 14 (75 - 83)



ROW 15 (84 - 93)



ROW 16 (94 - 99)



ROW 17 (100 - 110)



ROW 18 (111 - 118)



## FLOOD ROUTING AND HYDROGRAPHS

ROW 19 (118 – 125)



ROW 20 (126 – 135)



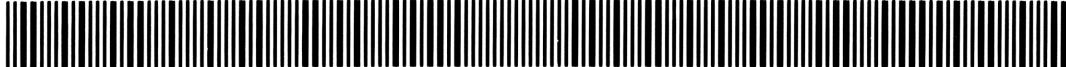
ROW 21 (136 – 142)



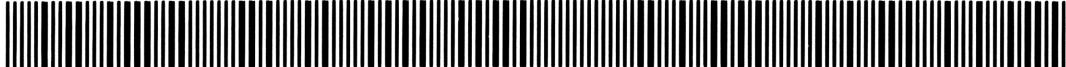
ROW 22 (143 – 150)



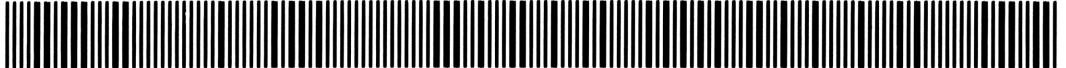
ROW 23 (150 – 157)



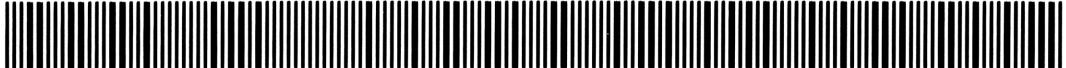
ROW 24 (157 – 163)



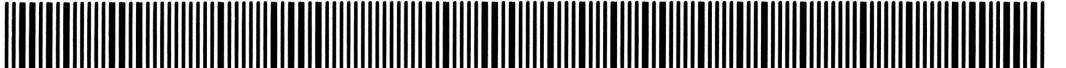
ROW 25 (164 – 174)



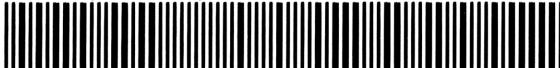
ROW 26 (175 – 181)



ROW 27 (182 – 189)



ROW 28 (190 – 192)



**NOTES**

## **Hewlett-Packard Software**

In terms of power and flexibility, the problem-solving potential of the HP-41 programmable calculator is nearly limitless. And in order to see the practical side of this potential, HP has different types of software to help save you time and programming effort. Every one of our software solutions has been carefully selected to effectively increase your problem-solving potential. Chances are, we already have the solutions you're looking for.

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You can choose from:

<b>Aviation (Pre-Flight Only) 00041-15018</b>	<b>Statistics 00041-15002</b>
<b>Clinical Lab 00041-15024</b>	<b>Stress Analysis 00041-15027</b>
<b>Circuit Analysis 00041-15024</b>	<b>Games 00041-15022</b>
<b>Financial Decisions 00041-15004</b>	<b>Home Management 00041-15023</b>
<b>Mathematics 00041-15003</b>	<b>Machine Design 00041-15020</b>
<b>Structural Analysis 00041-15021</b>	<b>Navigation 00041-15017</b>
<b>Surveying 00041-15005</b>	<b>Real Estate 00041-15016</b>
<b>Securities 00041-15026</b>	<b>Thermal and Transport Science 00041-15019</b>
	<b>Petroleum Fluids 00041-15039</b>

### **Users' Library**

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You can choose from:

<b>Business Stat/Marketing/Sales 00041-90094</b>	<b>Civil Engineering 00041-90089</b>
<b>Home Construction Estimating 00041-90096</b>	<b>Heating, Ventilating &amp; Air Conditioning 00041-90140</b>
<b>Lending, Saving and Leasing 00041-90086</b>	<b>Mechanical Engineering 00041-90090</b>
<b>Real Estate 00041-90136</b>	<b>Solar Engineering 00041-90138</b>
<b>Small Business 00041-90137</b>	<b>Calendars 00041-90145</b>
<b>Geometry 00041-90084</b>	<b>Cardiac/Pulmonary 00041-90097</b>
<b>High-Level Math 00041-90083</b>	<b>Chemistry 00041-90102</b>
<b>Test Statistics 00041-90082</b>	<b>Games 00041-90099</b>
<b>Antennas 00041-90093</b>	<b>Optometry I (General) 00041-90143</b>
<b>Chemical Engineering 00041-90100</b>	<b>Optometry II (Contact Lens) 00041-90144</b>
<b>Control Systems 00041-90092</b>	<b>Physics 00041-90142</b>
<b>Electrical Engineering 00041-90088</b>	<b>Surveying 00041-90141</b>
<b>Fluid Dynamics and Hydraulics 00041-90139</b>	<b>Time Module Solutions 00041-90395</b>
<b>Games II 00041-90443</b>	

\*Some books require additional memory modules to accomodate all programs.

## **FLUID DYNAMICS AND HYDRAULICS**

CONDUIT FLOW  
FLOW WITH A FREE SURFACE  
PIPE SLIDE-RULE  
FORCES AT BENDS AND FITTINGS  
VALVE SIZING  
PIPE NETWORK ANALYSIS  
RESTRICTION METERING ORIFICE CALCULATIONS  
ENERGY EQUATION FOR STEADY FLOW  
COMPRESSIBLE FLOW IN VARIABLE AREA DUCTS  
FLOOD ROUTING AND HYDROGRAPHS

