

Engineering Fundamentals Review

Manual

HP49G

CHOTKEH

Engineering Fundamentals Review

Manual

HP49G

Eit-FE Review Software Package
Version (6.1)

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ABOUT THE MANUAL AND CALCULATOR

This is a two (2) part manual and contains over 900 core engineering fundamental equations all of which are programmed into the Library of HP49G.

Part 1: Is the original reference manual containing over 500 equations, SECTION 1 - 8:

Part 2: Is the quick reference to NCEES HANDBOOK. Most of the 400 core useable and programmable equations are programmed into the calculator. SECTION 9.

HOW TO USE THE CALCULATOR:

When using this software package, ensure that the calculator is in **RPN** and **DEG** mode.

1. The key board:

There are three (3) types of distinctive function keys in HP49G:

- 1.1 The hard keys with their functions showed on the face of the keys. They are activated by pressing the key. Throughout this manual, they are identified by bold letters and underlined, like **ON**, **ENTER**, **NXT**, **SIN**, **TOOL**, **MODE**, etc.
- 1.2 The same hard keys with their colored functions showed at the top of the keys. To activate the function, the corresponding color coded **↶** or **↷** must be pressed prior to the subject key. They are identified by underlined symbols (not bold), like LIB, EVAL, PREV, MATH, MTRW, etc.
- 1.3 The soft keys or screen menu keys. There are six (6), F1-F6, keys located just below the screen. To activate the menu item, press the corresponding F key. The screen menu items (Directories, Sub-directories and Equation's name) are identified with plain capital letters (no bold no underline), like PUMP, PIPE, FLME, EXPR =, THER, etc.

2. Useful keys and their functions:

The user must ensure to use the implied **↶** or **↷** key, as needed. Numbers in parenthesis (next to the following specified keys) represent the calculator key-board's row and column respectively. For more information refer to Chapter 1 of HP catalog.

ALPHA (7,1) Use to turn the calculator to alphabetical mode. If the key pressed twice, the calculator will stay in this mode. Press again when typing is finished. The key may also be pressed and hold during the typing. Then release when typing is over.

ANS (10,5) To recall the previous answer (in **ALG** mode) or last argument (in **RPN** mode).

BASE (9,4) To display the list of binary arithmetic objects.

ABOUT THE MANUAL AND CALCULATOR

- CANCEL (10,1) To cancel the command line.
- CLEAR (4,5) To clear the screen. This symbol is only underlined, means the corresponding \rightarrow key must be pressed first.
- CMD (4,1) To display the last four (4) commands/calculations. Highlight and press OK to copy to stack.
- DEL (5,5) To delete the object on level 1.
- EVAL (4,4) To evaluate an expression, written on level 1.
- ENTER (10,5) To obtain a result, select an option or duplicate the object on level 1 (RPN mode).
- EXPR= This appears on the screen menu, when solving an equation or expression. It is used to calculate the expression. EXPR= is the last symbol on the screen menu. If it does not appear on the first page of the menu, there may be more than six (6) variables in the current equation.
- Press NXT to ensure no variable is missing.
- LASTARG At RPN mode, press ANS or type LASTARG press ENTER.
- LAST MENU To get only one (1) step back and forth between the menus, press \leftarrow and hold, press PREV (XXT).
- LIB (9,3) To get to the Library to use the Library program.
- MODE (2,2) To set the mode like: **RPN/ALGEBRAIC, DEGREE/RADIAN, POLAR/RECTANGULAR, FLAGS, CAS** (Computer Algebra System), etc.
- MTH (4,4) To display the mathematics menu.
- MTRW (4,3) To write a matrix.
- NUM To find the numeric value of the answer/object.
- NUM.SLV (7,2) To get to numeric equation solver application.
- NXEQ To rotate the list of related equations written under one name. The name of these equations are followed by \rightarrow .
- NXT (3,3) To go to the next page of multiple page screen menu.

ABOUT THE MANUAL AND CALCULATOR

| | |
|--------------------|--|
| <u>OFF</u> (10,1) | To turn the calculator off. |
| <u>ON</u> (10,1) | To turn the calculator on. |
| <u>PREV</u> (3,3) | To return back to the previous page of screen menu. |
| <u>SPC</u> (10,4) | To create space between the keyed-in data. |
| <u>STO</u> (3,2) | To store a current object in a variable. |
| SWAP | At RPN mode: press <u>TOOL</u> , F3 (STACK), F2 (SWAP) |
| <u>TOOL</u> (2,3) | To display a menu of commands like: EDIT, VIEW, PURGE, etc. |
| <u>UPDIR</u> (3,1) | To get back to one (1) level higher directory. |
| <u>UNITS</u> (8,4) | To go to units conversion menu. |
| <u>VAR</u> (3,1) | To display the list of variables contained in the current directory. |
| <u>WIN</u> (1,2) | To display plotting parameters and draw the specific plot. |
| <u>Y =</u> (1,1) | To list the equation(s) and data to plot. |
| <u>()</u> (8,5) | Use to identify/enter the value as a complex number. The real and the imaginary part must be separated by " comma " or " SPC ". When writing the expression, use " comma " only. But you may use either of them when entering components of complex numbers inside parenthesis. |
| <u>^</u> (4,3) | The inverted comma as ' '. Use to write an expression or equation (in RPN mode). Also use to specify the equation or variables name. |
| <u>#</u> (9,4) | To specify/enter a binary integer. |
| <u>←</u> (4,5) | To delete the object on level 1 (drop) or to delete the character to the left of cursor. |
| <u>Δ</u> | The symbol of angle, to retrieve, press <u>CHARS</u> (4,2), highlight the symbol, press ECHO <u>ENTER</u> . Or press <u>ALPHA</u> ↵ 6. |

ABOUT THE MANUAL AND CALCULATOR

3. How to identify the name, retrieve, and solve the equation:

- 3.1 In the solution part of every problem, in Problems and Solutions Book, following statement is used to refer to the subject equation, i.e. Hazen Williams (HAZN) equation, in SI system.
" Refer to equation (20) **SI** (FLME/FRICH/HAZN)" (20) is the number of equation in CHOTKEH manual, SI is the SI system, FLME is the main directory for Fluid Mechanic. FRICH is the sub-directory for friction head and HAZN is the name of the equation.
Therefore after getting to LIB, press FLME FRICH HAZN SI.
Now, by knowing what to look for, get to the Library (LIB).
- 3.2 Press **LIB** To get to the Library. You should see the menu on the screen.
- 3.3 Look up for the subject directory on the screen menu. You have to go to the subject directory first. If not found, press **NXT**. When found, press the corresponding F key.
- 3.4 Follow the same instruction for sub-directory(s). In few occasions there are more than three (3) sub-directories prior to equation's name.
- 3.5 Find the **equation/expression** name and press the corresponding soft key. The equations with their names followed by \rightarrow , contain more than one equation. See NXEQ in page 2.
- 3.6 You should see the equation's variables listed on the screen menu and the equation, in whole or in part, at the top of the screen. If there are more than six (6) variables in the equation, press **NXT** to see the rest.
- 3.7 The "EXPR =" symbol is the last on the screen menu. If the equation has more than five (5) variables, press **NXT**.

NOTE: Throughout the CHOTKEH Manual, the equation's **directory/sub-directory** names are shown in parenthesis at the right side of the subject's title.

- 3.8 Enter the variable's value: Key in the value and press the corresponding variable's F key. You should see the variables symbol and its entered value at the top of the screen. If not correct, enter the correct value again. When finished, press \leftarrow and unknown variable's F key. The answer will appear.

The holders of HP49G may also use the solver's screen feature. Press \rightarrow **NUMSLV** **ENTER**. Highlight the variables and input the values. Then highlight the unknown variable and press SOLVE key. If the known variable's value needed to be calculated or unit conversion feature must be used, the user must quit the screen and get back, when the calculation or conversion was performed. This is a time consuming process. Press **ON** (CANCEL) to quit the screen.

ABOUT THE MANUAL AND CALCULATOR

IMPORTANT NOTE: For the equations with complex numbers, which are programmed in the expression form (only in ELECTRICITY SECTION), you will not find the unknown's symbol on the screen. To get the answer, you have to press **EXPR=** (on the screen menu) and then NUM, if necessary.

- 3.9 If you have to retrieve another equation in the same sub-directory, type **OMENU** press **ENTER** and continue as directed above. Otherwise press LIB for other directories.
- 3.10 After you retrieved the equation, if you observed any inconsistency between the variables in the equation and the ones on the screen menu, first ensure that you retrieved the right equation. If the answer is yes, refer to NOTE 3 below.

NOTE 1:

Except for the complex number contained equations/expressions, every equation can be solved for any variable in the equation, if the rest are known.

NOTE 2:

When using CHOTKEH's Library software, stay in HOME directory. If you are using your own created equations, with the units attached to the variables, a new directory must be created and subject equations must be stored in new directory.

To create a new directory, i.e. **AAA**:

Press ' type **AAA**, press PRG (4,2) **MEM DIR CRDIR**

Press VAR, **AAA** will appear on the screen menu. Press the corresponding soft (F) key, the { **HOME AAA** } will appear at the top of the screen, which means that the calculator is in **AAA** directory. Use **AAA** to write your own equations in this directory. To get back to **HOME**, press UPDIR.

NOTE 3:

Do not enter the variable's value accompanied with the unit sign, i.e. for $L=2$ feet, enter 2 not 2_ft. This may happen when using calculator's UNITS conversion feature. The variables' value must all be numeric and consistent. If by error the values are followed by unit signs or the values are represented by an expression, etc., you may get the "**Bad Guess**" error message or may lose the variable's name on the menu. If that happened:

- a. Purge the variable: press ' type **variable's name** press ENTER TOOL F key under PURGE. If did not work:
- b. Press VAR press ALPHA twice type **CLVAR** press ENTER. This process will purge all variables in the current directory.

NOTE 4:

Although enough care has been taken in compiling the contents of this Manual, writing the programs, and problems and solutions, mostly for educational purposes, the preparer assumes no responsibility resulting from any error or omission in this manual, program, or problems and solutions. The contents of this manual and the associated program are subject to change without prior notice.

FREQUENTLY ASKED QUESTIONS, HP49G

1. The screen is too dark/light, how do I adjust it?

Press the ON key and hold. Push the (+) or (-) key to adjust the shade of the screen.

2. How do I set the calculator to, i.e., three (3) decimal point?

Press **MODE** ▼ CHOOS ▼ OK ► key in : 3 OK. To reverse:

Press **MODE** ▼ CHOOS ▲ OK OK.

3. How do I display the clock?

Press **MODE** DISP Scroll down to Clock ↓CHK OK OK

4. How do I turn the calculator's beeper off?

Press **MODE** Scroll down to Beep ↓CHK OK

5. How can I see the entire current equation?

Press the **ALPHA** key and hold, type EQ, release **ALPHA** key, press ENTER. Current equation will appear on the screen.

6. How can I get to the previous Menu?

You may go only one step back to the previous menu. Press ← and hold, press **PREV** (**NXT**).

7. How can I SWAP the objects displayed on Level 1 and Level 2 of the screen?

At RPN mode, press **TOOL**, **F3** (STACK), **F2** (SWAP)

8. Although I am following the directions to solve for a variable, in the retrieved equation, why I am not getting the correct answer?

In the majority of cases, instead of pressing ← and soft key under the subject variable, the user is pressed **EXPR=**. Also check for the units and calculator mode, i.e. Radian vs Degree or Rectangular vs Polar, etc.

9. While using the program, what should I do if I notice the loss of a variable on the menu or getting error message?

Refer to CHOTKEH's Manual, page A-5, NOTES 2 and 3 for answer. Then correct the condition as follows:

- Purge the variable: key in ' type variable's name press **TOOL** PURGE. If did not work:
- Press **ALPHA** twice, type CLVAR press **ENTER**. This process will purge all variables before the directory. If did not work:
- Press **ON F1 F6** keys simultaneously and release. Press soft key under NO. This will re-set the calculator and clears the entire memory. If you have any equation or Directory you want to keep. This is not a right approach.

In this case, to get back to RPN, degree and MTH on the soft menu:

Press **MODE** CHOOS RPN OK ▼ ▼ CHOOS degree OK FLAGS ▲ ▲ ▲ (highlight 117) ↓CHK OK OK

10. Can I erase or change the data in the CHOTKEH program?

CHOTKEH's programs are built in the calculator, you may not erase it by mistake. Also resetting the calculator or removing the batteries shall not affect the program.

11. Am I allowed to use the HP49G in the examination site?

For permissibility, contact the State Board where you are registered to take the examination.

12. How do I obtain technical support for CHOTKEH products?

Upon the receipt of the package, fill out the Registration form and mail/facsimile to CHOTKEH. There is 120 days of free technical support for registered users. Facsimile your questions to (212)942-8105.

Thank you for purchasing CHOTKEH products.

EXAMPLES OF HP49G NUMERIC KEYBOARD CALCULATIONS

The following calculations are separately done in **RPN** and **ALG** modes. To get to these modes: Press **MODE** **CHOOS**, highlight **RPN** or **Algebraic**, press **F6** **F6**

| Reverse Polish Notation (RPN) | Algebraic (ALG) |
|--|---|
| 1. Calculate 13×96 | |
| Key in: 13 SPC 96 × Answer: <u>1248</u> | Key in: 13 × 96 ENTER Answer: <u>1248</u> |
| 2. Calculate $\frac{24}{1.5}$ | |
| Key in: 24 SPC 1.5 ÷ Answer: <u>16</u> | Key in: 24 ÷ 1.5 ENTER Answer: <u>16</u> |
| 3. Calculate $13 \times 96 + 12$ | |
| Key in: 13 SPC 96 × 12 + Answer: <u>1260</u> | Key in: 13 × 96 + 12 ENTER Answer: <u>1260</u> |
| 4. Calculate 2.5^4 | |
| Key in: 2.5 SPC 4 y^x Answer: <u>39.0625</u> | Key in: 2.5 y^x 4 ENTER Answer: <u>39.0625</u> |
| 5. Calculate 3.6^{-4} | |
| Key in: 3.6 SPC 4 +/- y^x Answer: <u>5.9537E-3</u> | Key in: 3.6 y^x 4 +/- ENTER Answer: <u>5.9537E-3</u> |
| 6. Calculate $1/25$ | |
| Key in: 25 1/X Answer: <u>.04</u> | Key in: 1/X 25 ENTER Answer: <u>.04</u> |
| 7. Calculate $\sqrt{75} + \frac{1}{2.5^2}$ | |
| Key in: 75 √x 2.5 x² 1/x + Answer: <u>8.82</u> | Key in: √x 75 + 1 ÷ 2.5 y^x 2 ENTER Answer: <u>8.82</u> |

SAMPLES OF HP49G NUMERIC KEYBOARD CALCULATIONS

| Reverse Polish Notation (RPN) | Algebraic (ALG) |
|--|--|
| <p>8. Calculate $\sqrt{17^3 - 16^{2.5}}$</p> | |
| <p>Key in: 17 SPC 3 y^x 16 SPC 2.5 y^x - √x</p> <p>Answer: <u>62.36</u></p> | <p>Key in: √x () 17 y^x 3 - 16 y^x 2.5</p> <p>ENTER</p> <p>Answer: <u>62.36</u></p> |
| <p>9. Calculate $\sqrt{\frac{13^2 - 16^{1.5}}{(2.5 + 2)^2}}$</p> | |
| <p>Key in: 13 SPC 2 y^x 16 SPC 1.5 y^x -</p> <p>2.5 SPC 2 + 2 y^x + √x</p> <p>Answer: <u>2.28</u></p> | <p>Key in: √x () () 13 y^x 2 - 16 y^x 1.5</p> <p>▶ + () 2.5 + 2 ▶ y^x 2 ENTER</p> <p>Answer: <u>2.28</u></p> |
| <p>10. Given a voltage (210, Δ0) and current (11, Δ15) calculate the complex impedance.</p> | |
| <p><u>At POLAR:</u></p> <p>Key in: () 210 Δ 0 ▶ SPC () 11 Δ 15 +</p> <p>Answer: <u>(19.09, Δ-15)</u></p> | <p><u>At POLAR:</u></p> <p>Key in: () 210 Δ 0 ▶ + () 11 Δ 15</p> <p>ENTER</p> <p>Answer: <u>(19.09, Δ-15)</u></p> |
| <p>11. Calculate the Rectangular and Polar equivalent of two (2) impedances , (15 +4j) and (12, Δ-5) , in parallel. $Z_e = 1/(1/Z_1 + 1/Z_2)$</p> | |
| <p><u>At Rectangular:</u></p> <p>() 15 SPC 4 1/x</p> <p>() 12 Δ 5 +/- 1/x</p> <p>+ 1/x</p> <p>Answer: <u>(6.86, 0.44)</u></p> <p><u>At POLAR</u></p> <p>Answer: <u>(6.87, Δ3.68)</u></p> | <p><u>At Rectangular:</u></p> <p>Key in: 1 + () 1 + () 15 , 4 ▶ +</p> <p>1 + () 12 Δ 5 +/- ENTER</p> <p>Answer: <u>(6.86, 0.44)</u></p> <p><u>At POLAR</u></p> <p>Answer: <u>(6.87, Δ3.68)</u></p> <p>If angle -5 did not work, enter 355 (360-5)</p> |

NOTE: To enter the symbol of angel (Δ): Press **ALPHA** ↵ 6

To get to POLAR (RΔZ) mode, press **MODE**, highlight Coord System, press CHOOS, highlight Polar, press OK OK. When using POLAR, make sure calculator is in DEG mode, unless the given angle is in Radian.

SELECTED BUILT-IN FUNCTIONS

HP49G

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BINARY ARITHMETIC

Example (1): Convert Hexadecimal 56AB to Decimal base.

Press \leftarrow MTH BASE HEX. May also press \rightarrow BASE HEX

Press \leftarrow # 56 ALPHA ALPHA A B ENTER

Press DEC

Answer: # 22187d

Example (2): Display the same in Octal base

Press OCT

Answer : # 53253o

Example (3): Display the same in Binary base

Press BIN

Answer: # 101011010101011b

Example (4): Divide the above answer by 10101b

At RPN mode: Press \leftarrow # 10101 \div

At ALG mode: Press \div \leftarrow # 10101 ENTER

Answer: #10000100000b

COMBINATION

Example: Find combination (arrangement without order) (5,4)

At RPN mode: Press \leftarrow MTH NXT PROB

Type 5 SPC 4, pres COMB

Answer: 5

At ALG mode: Press \leftarrow MTH NXT PROB

Press COMB, type 5, 4 ENTER

Answer: 5

COMPLEX NUMBER

Example: Solve $\frac{(9+4i)+(-4+3i)}{(3+i)}$

At **RPN** mode:

Press: ' () () 9 , 4 ► + () -4 , 3 ► ► ÷ () 3 , 1

Press **EVAL**

Answer: (2.2,1.6) or 2.2+1.6i

At **ALG** mode:

Press: () () 9 , 4 ► + () -4 , 3 ► ► ÷ () 3 , 1

Press **ENTER**

Answer: (2.2,1.6) or 2.2+1.6i

DETERMINANT

Example: Solve

$$\begin{vmatrix} 1 & -1 & 4 \\ 2 & 11 & -3 \\ 6 & -7 & 10 \end{vmatrix}$$

At **RPN** mode:

Press **↵** **MTH** **MATRX** **NORM** **NXT**. You should see **DET** on the screen Menu.

Press **↵** **MTRW** **F5** (If necessary to make the **GO** with right arrow active.)

Key in 1 **SPC** -1 **SPC** 4 **ENTER** ▼ **↵** ◀

Key in 2 **SPC** 11 **SPC** -3 **ENTER**

Key in 6 **SPC** -7 **SPC** 10 **ENTER** **ENTER**

Press **DET**

Answer: -193

ELECTRIC CIRCUITS

Example: For (10, Δ 0) volt and (2, Δ 30) amps: calculate the impedance.

At **RPN**, **DEG**, and **POLAR** mode:

Press: ' () 10 , **ALPHA** ► 6 0 ► ÷ () 2 , **ALPHA** ► 6 30 **EVAL**:

Answer: (5 , Δ -30)

At **RPN**, **DEG**, and **RECT** mode:

Answer: (4.33, -2.5)

EXPRESSION

Example: Solve: $2^{(1.1 \times 1.6)} + \text{LOG}22 + 1^{2.5} \sqrt{7} * \text{SIN}50$

At **RPN** and **DEG** mode: Press:

' 2 y^x () 1.1 \times 1.6 \blacktriangleright + \blacktriangleright LOG (22) \blacktriangleright + \blacktriangleright \sqrt{x} 2.5 \rightarrow , 7 \blacktriangleright \times SIN 50

Press **EVAL**

Answer: 6.3978

At **ALG** and **DEG** mode: Press:

2 y^x () 1.1 \times 1.6 \blacktriangleright + \blacktriangleright LOG (22) \blacktriangleright + \blacktriangleright \sqrt{x} 2.5 \rightarrow , 7 \blacktriangleright \times SIN 50

Press **ENTER**

Answer: 6.3978

FACTORIAL

Example: Solve 5!

At **RPN** mode: Press: \blacktriangleleft **MTH** **NXT** **PROB** 5 !

Answer: 120

At **ALG** mode: Press: \blacktriangleleft **MTH** **NXT** **PROB** 5 ! **ENTER**

Answer: 120

LINEAR (SIMULTANEOUS) EQUATIONS

Example: Solve $2x + 4y + z = 9$ for x, y, z

$$-x - 3y - z = -8$$

$$3x - y + z = -2$$

At **RPN** mode: Press \blacktriangleleft **MTRW**

Key in 9 **SPC** -8 **SPC** -2 **ENTER** **ENTER**

Press \blacktriangleleft **MTRW** F5 (If necessary to make the GO with right arrow active.)

Key in 2 **SPC** 4 **SPC** 1 **ENTER** \blacktriangledown \blacktriangleright \blacktriangleleft

Key in -1 **SPC** -3 **SPC** -1 **ENTER**

Key in 3 **SPC** -1 **SPC** 1 **ENTER** **ENTER**

Press \div

Answer: $x = -1, y = 2, z = 3$

PERMUTATION

Example: Find Permutation (arrangement with order) (5,4)

At RPN mode: Press \leftarrow MTH NXT PROB

Type 5 SPC 4, press PERM

Answer: 120

At ALG mode: Press \leftarrow MTH NXT PROB

press PERM, type 5, 4 ENTER

Answer: 120

PLOTTING

Example: Plot x^2-2x-3 and find the roots. Calculator must be in ALG mode:

Press: \leftarrow Y= (F1) CLEAR ADD, key in x^2-2x-3 ENTER

Press: ERASE DRAW. The curve will appear

Press FCN ROOT, read the first root:

Answer: Root = -1

Press NXT \times to locate the cursor. Move the cursor to the right close to intersection with x axis. Press ROOT, read the second root:

Answer: Root = 3

Press ON ON

QUADRATIC/POLYNOMIAL EQUATIONS

Example 1: Solve $2x^2+5x-12=0$ (Quadratic Equation)

Press \rightarrow NUMSLV \blacktriangledown \blacktriangledown OK, key in: [2 SPC 5 SPC -12] OK SOLVE ENTER

Answer: 1.5,-4

Example 2: Solve $x^2-9=0$ (Quadratic Equation)

Press \rightarrow NUMSLV \blacktriangledown \blacktriangledown OK, key in: [1 SPC 0 SPC -9] OK SOLVE ENTER

Answer: -3, 3

Example 2: Solve $3x^3-1.5x^2-12x+6=0$ (Polynomial Equation)

Press \rightarrow NUMSLV \blacktriangledown \blacktriangledown OK

Key in: [3 SPC -1.5 SPC -12 SPC 6] OK SOLVE ENTER

Answer: .5, -2, 2

TIME ARITHMETIC

To set the time and date: Press \rightarrow TIME, select 3 OK. Move the cursor and choose the options.

Example (1): Determine the date 49 days after 7/9/00

For time arithmetic, calculator must be in RPN, Fixed 6 decimal and M/D/Y mode.

Press \rightarrow TIME, select Tools OK NXT. Key in 7.092000 ENTER

Key in 49 press DATE+

Answer: 08.272000 or 8/27/00

Example (2): Calculate number of days between 7/9/00 and 8/27/00

Press \rightarrow TIME, select Tools OK NXT. Key in 7.092000 ENTER

Key in 8.272000 press DDAYS

Answer: 49 days

UNIT CONVERSION

For unit conversion application, calculator must be in RPN mode.

Following is the UNITS catalog menu which converts to built-in units.

Press \rightarrow UNITS to reach to the menu:

TOOLS LENG AREA VOL TIME SPEED press NXT

MASS FORCE ENRG POWR PRESS TEMP press NXT

ELEC ANGL LIGHT RAD VISC

Example (1): Find equivalent of 8 gallon in cubic feet.

Press \rightarrow UNITS VOL NXT 8 gal PREV

Press \leftarrow ft³

Answer: 1.069 ft³

Example (2): Calculate 1.5 yards + 2.5 feet + 3 inches.

Press \rightarrow UNITS LENG 1.5 yd 2.5 ft 3 in

Press + +

Answer (1): 87_in

Press \leftarrow ft

Answer (2): 7.25_ft

Press \leftarrow yd

Answer (3): 2.42_yd

START UP

EIT-FE SOLVED PROBLEMS

HP49G

Before practicing, please read pages A-1 through A-5 of CHOTKEH's Manual

GENERAL NOTE: The entire program is stored in the calculator's library, therefore, first, get to the library by pressing \rightarrow LIB. Calculator in **RPN** mode (No **ALG** on top of screen)

1- The repayment of a \$100,000 loan during a 30 year period based on equal end-of-the-year installments, at an interest rate of 15% requires annual payments which is most nearly:

- (A) \$ 4,000
- (B) 13,800
- (C) 15,230
- (D) 17,500
- (E) 20,800

Solution:

This is an Engineering Economic (ENEC) problem. Refer to page 3-4 for Mortgage.

The ID NAME for installment is equation (30) **INSTL** (ENEC/MORT):

Select LIB, Press ENEC NXT MORT INSTL. Enter values for variables:

Enter .15 for **I**; 30 for **n**; 100000 for **LOAN**

Press \leftarrow INSTL

Answer: INSTL = 15230 (C)

2- A 2" diameter shaft is subject to a torque equal to 10,000 in-lbf. The shearing stress due to torsion is nearly:

- (A) 0 psi
- (B) 6370 psi
- (C) 7650 psi
- (D) 12770 psi
- (E) 15900 psi

Solution:

This is a Mechanics of Material (MEMA) problem. Refer to page 7-1 for stress in the shaft.

The ID NAME for Sheer Stress, in a solid round shaft, is equation (11) **SOLID** (MEMA/SHAFT/SHEAR):

Select LIB, Press NXT MEMA SHAFT SHEAR SOLID

Enter 10000 for **T**; 1 for **r**

Press \leftarrow τ

Answer: τ = 6366 psi (B)

GENERAL NOTE: The entire program is stored in the calculator's library, therefore, first, get to the library by pressing \rightarrow LIB. Calculator in **RPN** mode (No **ALG** on top of screen)

3- If the interest rate is 12% compounded monthly, the effective rate per annum is most nearly:

- (A) 12.00%
- (B) 12.12%
- (C) 12.34%
- (D) 12.68%
- (E) 12.96%

Solution:

This is an Engineering Economic (ENEC) problem. Refer to page 3-3 for Interest. The ID NAME for Effective Interest Rate is equation (27) **EFFEC** (ENEC/INTER)

Select LIB, Press ENEC INTER EFFEC

Enter .12 for I; 12 for m

Press \leftarrow iEF

Answer: iEF = .1268 (D)

4- What is the maximum efficiency of a Carnot cycle operating between temperatures of 980 oF and 500 oF

- (A) 33%
- (B) 50%
- (C) 67%
- (D) 75%
- (E) 100%

Solution:

This is a Thermodynamics (THER) problem. Refer to page 8-2 for efficiency equations.

The ID NAME for Carnot Efficiency, with the given temperatures, is equation (15) **TEMP** (THER/EFFI/CARN)

Select LIB, Press NXT THER EFFI CARN TEMP. Enter values for variables.

Key in ' 980+460 EVAL=1440, enter for Th; ' 500+460 EVAL=960 enetr for Tl

Press \leftarrow η

Answer: η = .333 or 33% (A)

GENERAL NOTE: The entire program is stored in the calculator's library, therefore, first, get to the library by pressing \rightarrow LIB. Calculator in **RPN** mode (No **ALG** on top of screen)

5- Evaluate the following determinant:

$$y = \begin{vmatrix} 3 & 1 & -1 \\ 4 & -2 & 0 \\ 2 & 1 & 4 \end{vmatrix}$$

The answer is more nearly:

- (A) 33
- (B) 121
- (C) -48
- (D) 77
- (F) -11

Solution:

This is a built-in function and shall be calculated as follows:

Press \leftarrow MTRW F5 (If necessary to make the "GO" with the right arrow active.

Key in 3 SPC 1 SPC -1 ENTER ∇ \rightarrow \blacktriangleleft

Key in 4 SPC -2 SPC 0 ENTER

Key in 2 SPC 1 SPC 4 ENTER ENTER

Press \leftarrow MTH MATRX NORM NXT DET Answer: -48 (C)

6- What input horsepower required for a pump with 80% efficiency, inlet pressure of 10 psia, outlet pressure of 20 psig, and a flow of 5 cfs of water? Assume sea level condition.

- (A) 2.90 hp
- (B) 10.40 hp
- (C) 14.00 hp
- (D) 25.00 hp
- (E) 40.00 hp

Solution:

This is a Fluid Mechanics (FLME) problem with specific equations in English and SI Systems.

Refer to FLUID MECHANIC SECTION, page 4-6 for pumps.

The ID NAME for **hp**, with the flow in cfs in English system, is equation (71) **CFS (FLME/PUMP/HP'ENG)**:

Select LIB, Press FLME NXT PUMP HP ENG CFS. Enter the values

Press ' \leftarrow () 20+14.7-10 \blacktriangleright *144/62.4 EVAL = 57, enter for **hA**; 5 for **cfs**; 62.4 for **ρ** , and .8 for **η**

Press \leftarrow hp Answer: hp=40.4 (E)

GENERAL NOTE: The entire program is stored in the calculator's library, therefore, first, get to the library by pressing \rightarrow LIB. Calculator in RPN mode (No ALG on top of screen)

7- An industrial plant draws an average current of 600 amp. daily from a 3 phase, 440 volt, 60 HZ line, at a power factor of .75 lagging. If a condenser improved the power factor to .92 lagging, the new value of average daily current will be most nearly :

- (A) 450 amp.
- (B) 475 amp.
- (C) 490 amp.
- (D) 550 amp.
- (E) 650 amp.

Solution:

This is an Electricity (ELEC) problem. Refer to gage 2-5 for power equations.

The ID NAME for three phase effective Power is equation (51) 3ϕ (ELEC/POWR/EFEC):

Select LIB, Press ELEC NXT POWR EFEC 3ϕ . Enter values.

Enter 440 for V; 600 for I; .75 for PF; Press \leftarrow P

With the calculated power under old power factor; enter .92 for PF (new power factor)

Press \leftarrow I

Answer: I=489 (C)

8- Oil flows through a 6" diameter pipe at a rate of 150 gpm. Its viscosity is 0.001 pound-second per square foot, and its specific gravity is 0.8. Under these conditions, the Reynolds Number NR is most nearly:

- (A) 1320
- (B) 2000
- (C) 3300
- (D) 9900
- (E) 12400

Solution:

This is a Fluid Mechanics (FLME) problem with specific equations in English and SI Systems.

Refer to FLUID MECHANIC SECTION, page 4-5 for pipes. Calculate the velocity first.

The ID NAME for velocity, flow in **gpm** in English system, is equation (60) **GPM** (FLME/PIPE/VELO/ENG):

Select LIB, Press FLME NXT PIPE VELO ENG GPM. Enter the values for variables.

Enter 150 for **gpm**; .5 for **D**; Press \leftarrow V v=1.7 fps (the value for v is stored in the calculator)

The ID NAME for Reynolds Number, with absolute viscosity, is equation (75) **ABSO** (FLME/REYN)

Select LIB, Press FLME NXT REYN ABSO. Enter the values.

Press ' 62.4x.8 EVAL= 49.92 for ρ ; .001 for μ ; 32.2 for g (values for **D** & v are stored before)

Press \leftarrow NRe

Answer NRe=1319 (A)

GENERAL NOTE: The entire program is stored in the calculator's library, therefore, first, get to the library by pressing \rightarrow LIB. Calculator in **RPN** mode (No **ALG** on top of screen)

9- A steel shaft 30" long an 2" in diameter is subjected to a torque equal to 60,000 in-lbf. If G is assumed to be 12EE6 psi, the angular rotation, in degree, at the end of the shaft is most near to:

- (A) .7
- (B) .11
- (C) .56
- (D) 5.70
- (E) 45.00

Solution:

This is a Mechanics of Material (MEMA) problem. Refer to page 7-1 for angle of twist in the shaft. The ID NAME for Angle of Twist, in solid bar is equation (06) **SOLID** (MEMA/SHAFT/ANGL)

Select LIB, Press NXT MEMA SHAFT ANGLE SOLID

Enter 60000 for T; 30 for L; 12E6 for G; 1 for r

Press \leftarrow Ω

Answer: $\Omega = 5.47$ (D)

10- Air is compressed in a frictionless manner with no transfer of heat from a condition of 70 oF and 14.7 psia to 1000 psia. What is the resulting air temperature in degree Fahrenheit?

- (A) 70
- (B) 234
- (C) 990
- (D) 1310
- (E) 10340

Solution:

This is a Gas Properties (GASP) problem. Refer to page 5-3 for isentropic process.

The ID NAME for temperature, with the given pressure, is equation (27) **$\Delta T/P$** (GASP/ISENT)

Select LIB, Press GASP ISENT $\Delta T/P$. Enter the values for variables.

Key in ' 70+460 EVAL = 530, enter for T1, 1000 for p2; 14.7 for p1; and 1.4 for k (assumed)

Press \leftarrow T2

Answer: T2=1769.7 oR

Select UNITS NXT TEMP oR \leftarrow oF

Answer: T2=1310 oF (D)

GENERAL NOTE: The entire program is stored in the calculator's library, therefore, first, get to the library by pressing \rightarrow **LIB**. Calculator in **RPN** mode (No **ALG** on top of screen)

11- Water flows through a 2' diameter drain pipe to a level such that a 60 degree arc at the top of the pipe is not wetted.

The hydraulic radius, in feet, is most nearly:

- (A) 0.50
- (B) 0.58
- (C) 0.67
- (D) 1.00
- (E) 2.00

Solution:

This is a Mathematics (MATH) problem. Refer to page 6-1 for hydraulic radius.

The ID **NAME** for Hydraulic Radius, with the given angle, is equation (10) **ANGL** (MATH/HYD.R)

Select **LIB**, Press MATH HYD.R ANGL

Enter 1 for r; 360-60=300 for Ω

Press \leftarrow HR

Answer: **HR = .58 (B)**

12- Ten pounds of helium at a constant pressure of 20 psia are heated for two hours at a constant rate of 100 btu/hr. The helium volume is allowed to increase in a frictionless manner from 700 cubic feet to 1000 cubic feet. How much work is done?

- (A) 0 ft-lb/hr
- (B) 550 Btu
- (C) 1110 Btu
- (D) 43,200 ft-lb/hr
- (E) 86,400 ft-lb/hr

Solution:

This is a Gas Properties (GASP) problem. Refer to page 5-1 for constant pressure process.

The ID **NAME** for the Work Done is equation (07) **W** (GASP/PRESS).

Select **LIB**, Press GASP PRESS **NXT** W. Enter the values for variables.

Key in ' 20x144 **Eval** =2880, enter for **p1**; 1000 for **v2**; 700 for **v1**

Press \leftarrow W

W = 864000 lb-ft

To convert the answer to Btu:

Select **UNITS NXT** ENRG ft*lb \leftarrow BTU

Answer: **W = 1110 btu (C)**

DYNAMICS

DESCRIPTION

FORMULA

NAME

BANKING ANGLE: (DYNA/BANK)

ENGLISH System: (DYNA/BANK/ENG)

| | | |
|-------------------------------|--|--------------|
| (01) For motion impeding down | $\Omega = \text{ATAN}\left(\frac{.0668 * \text{mph}^2}{r}\right) + \text{ATAN}\mu$ | <i>DOWN</i> |
| (02) For motion impeding up | $\Omega = \text{ATAN}\left(\frac{.0668 * \text{mph}^2}{r}\right) - \text{ATAN}\mu$ | <i>UP</i> |
| (03) Ideal | $\Omega = \text{ATAN}\left(\frac{.0668 * \text{mph}^2}{r}\right)$ | <i>IDEAL</i> |
| (04) Height of outside edge | $h = RW * \text{Sin}\Omega$ | <i>HIGHT</i> |

SI Units: (DYNA/BANK/SI)

| | | |
|-------------------------------|---|--------------|
| (05) For motion impeding down | $\Omega = \text{ATAN}\left(\frac{.00786 * \text{kmh}^2}{r}\right) + \text{ATAN}\mu$ | <i>DOWN</i> |
| (06) For motion impeding up | $\Omega = \text{ATAN}\left(\frac{.00786 * \text{kmh}^2}{r}\right) - \text{ATAN}\mu$ | <i>UP</i> |
| (07) Ideal | $\Omega = \text{ATAN}\left(\frac{.00786 * \text{kmh}^2}{r}\right)$ | <i>IDEAL</i> |
| (08) Height of outside edge | $h = RW * \text{Sin}\Omega$ | <i>HIGHT</i> |

CIRCULAR MOTION, ACCELERATED: (DYNA/CIRM)

Angle subtended: (DYNA/CIRM/ θ)

| | | |
|---|--|------------------|
| (09) With the given α and T | $\theta = \omega_o * t + \frac{1}{2} \alpha * t^2$ | α, T |
| (10) With the given α and ω | $\theta = \frac{\omega^2 - \omega_o^2}{2\alpha}$ | α, ω |
| (11) With the given N | $\theta = 2\pi N$ | <i>N</i> |

Angular acceleration: (DYNA/CIRM/ α)

| | | |
|---|---|-------------|
| (12) With the given α and ω | $\alpha = \frac{\omega - \omega_o}{t}$ | ω, T |
| (13) With the given θ and T | $\alpha = \frac{2(\theta - \omega_o * t)}{t^2}$ | θ, T |

DYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|---|-------------------|
| <u>Angular velocity (DYNA/CIRM/ ω)</u> | | |
| (14) With the given α and T | $\omega = \omega_o + \alpha * t$ | $\alpha . T$ |
| (15) With the given α and θ | $\omega = \sqrt{\omega_o^2 + 2\alpha * \theta}$ | $\alpha . \theta$ |
| (16) With the given RPM | $\omega = \frac{2\pi * RPM}{60}$ | RPM |
| <u>Centrifugal force: (DYNA/CIRM/ FC)</u> | | |
| (17) With the given w and an | $F_c = \frac{w * a_n}{g}$ | W . AN |
| (18) With the given w and v | $F_c = \frac{w * v^2}{g * r}$ | W . V |
| (19) With the given w and ω | $F_c = \frac{w * r * \omega^2}{g}$ | W . ω |
| <u>Linear velocity: (DYNA/CIRM/ V)</u> | | |
| (20) With the given RPM | $v = \frac{2\pi * r * RPM}{60}$ | RPM |
| (21) With the given ω | $v = \omega * r$ | ω |
| <u>Normal acceleration: (DYNA/CIRM/ AN)</u> | | |
| (22) With the given v and r | $a_n = \frac{v^2}{r}$ | V . R |
| (23) With the given ω and r | $a_n = r * \omega^2$ | $\omega . R$ |
| (24) Rotational speed | $RPM = \frac{30}{\pi} (\omega_o + \alpha * t) = RPM_o + \frac{30\alpha * t}{\pi}$ | RPM→ |
| <u>Time: (DYNA/CIRM/ T)</u> | | |
| (25) With the given α and ω | $t = \frac{\omega - \omega_o}{\alpha}$ | $\alpha . \omega$ |
| (26) With the given α and θ | $t = \frac{\sqrt{2\alpha * \theta + \omega_o^2} - \omega_o}{\alpha}$ | $\alpha . \theta$ |
| (27) With the given θ and ω | $t = \frac{2\theta}{\omega + \omega_o}$ | $\theta . \omega$ |

DYNAMICS

DESCRIPTION

FORMULA

NAME

ENERGY: (DYNA/ENRG)

(28) Potential

$$E_p = m \cdot g \cdot h$$

POTEN

Kinetic: (DYNA/ENRG/KINET)

(29) Linear system

$$E_k = \frac{1}{2} m \cdot v^2$$

LINER

(30) Circular system

$$E_k = \frac{1}{2} I \cdot \omega^2$$

CIRCU

LINEAR MOTION (DYNA/LINM)

Acceleration: (DYNA/LINM/ A)

(31) With the given v and t

$$a = \frac{v - v_0}{t}$$

V. T

(32) With the given s and t

$$a = \frac{2(s - s_0) - 2v_0 \cdot t}{t^2}$$

S. T

(33) With the given s and v

$$a = \frac{v^2 - v_0^2}{2(s - s_0)}$$

S. V

Displacement: (DYNA/LINM/ S)

(34) With the given a and t

$$s = s_0 + v_0 \cdot t + \frac{1}{2} a \cdot t^2$$

A. T

(35) With the given a and v

$$s = s_0 + \frac{v^2 - v_0^2}{2a}$$

A. V

(36) With the given t and v

$$s = s_0 + \frac{1}{2} t (v_0 + v)$$

T. V

Initial velocity: (DYNA/LINM/ VO)

(37) With the given a, t, and v

$$v_0 = v - a \cdot t$$

A. T. V

(38) With the given a, s, and t

$$v_0 = \frac{s - s_0}{t} - \frac{1}{2} a \cdot t$$

A. S. T

(39) With the given a, s, and v

$$v_0 = \sqrt{v^2 - 2a(s - s_0)}$$

A. S. V

DYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

Velocity: (DYNA/LINM/ V)

- | | | |
|---|----------------------------------|---------|
| (40) With the given a and t | $v = v_0 + a \cdot t$ | $A . T$ |
| (41) With the given a and s | $v = \sqrt{v_0^2 + 2a(s - s_0)}$ | $A . S$ |
| (42) With the given a , s , and t | $v = \frac{2(s - s_0)}{t} - v_0$ | $S . T$ |

Time: (DYNA/LINM/ T)

- | | | |
|---------------------------------|--|---------|
| (43) With the given a and v | $t = \frac{v - v_0}{a}$ | $A . V$ |
| (44) With the given a and s | $t = \frac{\sqrt{v_0^2 + 2a(s - s_0)} - v_0}{a}$ | $A . S$ |
| (45) With the given s and v | $t = \frac{2(s - s_0)}{v + v_0}$ | $S . V$ |
-

PENDULUM: (DYNA/PEND)

Compound: (DYNA/PEND/COMP)

- | | | |
|------------------------|---|----------|
| (46) Angular frequency | $\omega = \sqrt{\frac{m \cdot g \cdot L}{I}}$ | ω |
| (47) Frequency | $f = \frac{1}{2\pi} \sqrt{\frac{m \cdot g \cdot L}{I}}$ | F |
| (48) Period | $T = 2\pi \sqrt{\frac{I}{m \cdot g \cdot L}}$ | T |

Simple: (DYNA/PEND/SIMP)

- | | | |
|------------------------|---|----------|
| (49) Angular frequency | $\omega = \sqrt{\frac{g}{L}}$ | ω |
| (50) Frequency | $f = \frac{1}{2\pi} \sqrt{\frac{g}{L}}$ | F |
| (51) Period | $T = 2\pi \sqrt{\frac{L}{g}}$ | T |

DYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

PROJECTILE MOTION: (DYNA/PROJ)

Horizontal: (DYNA/PROJ/HORIZ)

| | | |
|------------------------------|-------------------------------|------|
| (52) Altitude above the base | $y = H_h - \frac{1}{2} g t^2$ | ALTI |
|------------------------------|-------------------------------|------|

| | | |
|-----------------|---|------|
| (53) Drop angle | $\Omega = \text{ATAN} \left(\frac{v_o}{H_h} \sqrt{\frac{2H_h}{g}} \right)$ | ANGL |
|-----------------|---|------|

| | | |
|------------------|-----------------------------|------|
| (54) Flight time | $T = \sqrt{\frac{2H_h}{g}}$ | TIME |
|------------------|-----------------------------|------|

| | | |
|--------------------------------------|---------------------------------|------|
| (55) Horizontal displacement (Range) | $R = v_o \sqrt{\frac{2H_h}{g}}$ | RANG |
|--------------------------------------|---------------------------------|------|

Vertical: (DYNA/PROJ/VERTI)

Altitude: (DYNA/PROJ/VERTI/ALTI)

| | | |
|----------------|---|-------|
| (56) At time t | $y = v_o t \sin \Omega - \frac{1}{2} g t^2$ | AT: T |
|----------------|---|-------|

| | | |
|--------------|--------------------------------------|-----|
| (57) Maximum | $H = \frac{v_o^2 \sin^2 \Omega}{2g}$ | MAX |
|--------------|--------------------------------------|-----|

Flight Time: (DYNA/PROJ/VERTI/TIME)

| | | |
|------------|----------------------------------|------|
| (58) Total | $T = \frac{2v_o \sin \Omega}{g}$ | TOTL |
|------------|----------------------------------|------|

| | | |
|--------------------|--|-------|
| (59) At altitude y | $t = \frac{v_o \sin \Omega + \sqrt{v_o^2 \sin^2 \Omega - 2gy}}{g}$ | AT: Y |
|--------------------|--|-------|

Horizontal Displacement: (DYNA/PROJ/VERTI/DISP)

| | | |
|----------------|-------------------------|-------|
| (60) At time t | $x = v_o t \cos \Omega$ | AT: T |
|----------------|-------------------------|-------|

| | | |
|--------------------|--|-------|
| (61) At altitude y | $x = v_o \cos \Omega \frac{v_o \sin \Omega + \sqrt{v_o^2 \sin^2 \Omega - 2gy}}{g}$ | AT: Y |
|--------------------|--|-------|

| | | |
|-------------------|-------------------------------------|------|
| (62) Range, total | $R = \frac{v_o^2 \sin(2\Omega)}{g}$ | RANG |
|-------------------|-------------------------------------|------|

DYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

Velocity: (DYNA/PROJ/VERTI/VELO)

| | | |
|-----------------|---|----|
| (63) Total | $v = \sqrt{v_o^2 - 2g \cdot y}$ | V |
| (64) Horizontal | $v_x = v_o \cdot \cos \Omega$ | VX |
| (65) Vertical | $v_y = v_o \cdot \sin \Omega - g \cdot t$ | VY |

SPRING: (DYNA/SPRIN/MASS)

Angular frequency: (DYNA/SPRIN/MASS/ ω)

| | | |
|-----------------------------|---------------------------------------|------|
| (66) With the given k and w | $\omega = \sqrt{\frac{k \cdot g}{w}}$ | K. W |
| (67) With the given f | $\omega = 2\pi \cdot f$ | F |
| (68) With the given T | $\omega = \frac{2\pi}{T}$ | T |

Frequency: (DYNA/SPRIN/ F)

| | | |
|------------------------------|---|----------|
| (69) With the given k and w | $f = \frac{1}{2\pi} \cdot \sqrt{\frac{k \cdot g}{w}}$ | K. W |
| (70) With the given ω | $f = \frac{\omega}{2\pi}$ | ω |
| (71) With the given T | $f = \frac{1}{T}$ | T |

Period: (DYNA/SPRIN/MASS/ T)

| | | |
|------------------------------|---------------------------------------|----------|
| (72) With the given k and w | $T = 2\pi \sqrt{\frac{w}{k \cdot g}}$ | K. W |
| (73) With the given ω | $T = \frac{2\pi}{\omega}$ | ω |
| (74) With the given T | $T = \frac{1}{f}$ | F |

DYNAMICS

DESCRIPTION

FORMULA

NAME

Torsional: (DYNA/SPRIN/TORS)

(75) Angular frequency

$$\omega = \sqrt{\frac{K}{I}}$$

ω

(76) Frequency

$$f = \frac{1}{2\pi} \sqrt{\frac{K}{I}}$$

f

(77) Period

$$T = 2\pi \sqrt{\frac{I}{K}}$$

T

DYNAMICS EXAMPLES: (DYNA/XMPL)

MOTION ON SLOPE: (DYNA/XMPL/SLOP)

Acceleration: (DYNA/XMPL/SLOP/ACCEL)

(78) (a) Moving uphill

$$a = \left(\frac{F}{W} - \sin\beta - \mu \cos\beta \right) g$$

UPHIL

(79) (b) Moving downhill

$$a = \left(\frac{F}{W} + \sin\beta - \mu \cos\beta \right) g$$

DNHIL

(80) (c) Moving horizontally

$$a = \left(\frac{F}{W} - \mu \right) g$$

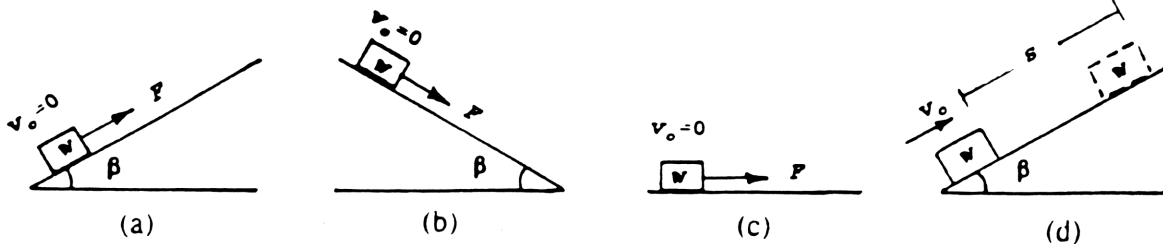
HORIZ

Displacement: (DYNA/XMPL/SLOP/DISP)

(81) (d) Moving uphill

$$s = \frac{v_o^2}{2g(\sin\beta + \mu \cos\beta)}$$

UPHIL



DYNAMICS

DESCRIPTION

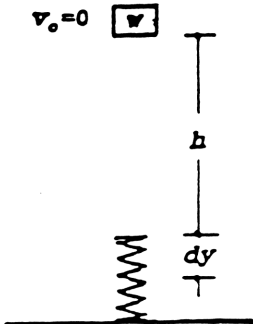
FORMULA

NAME

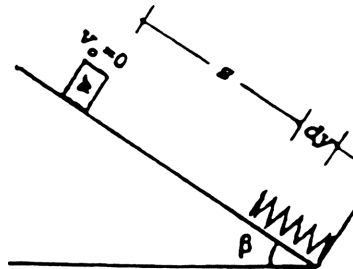
SPRING DEFLECTION, WORK: (DYNA/XMPL/SPRIN)

Deflection when an object hits over the spring: (DYNA/XMPL/SPRIN/DFLEC)

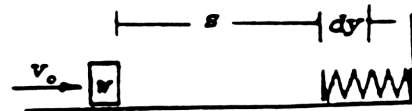
| | | |
|--------------------------|---|-------|
| (82) (e) Free drop | $dy = \frac{w + \sqrt{w^2 + 2k \cdot w \cdot h}}{k}$ | DROP |
| (83) (f) Downhill | $dy = \frac{w(\sin\beta - \mu \cos\beta) + \sqrt{w^2(\sin\beta - \mu \cos\beta)^2 + 2k \cdot w \cdot s(\sin\beta - \mu \cos\beta)}}{k}$ | DNHIL |
| (84) (g) Horizontal move | $dy = \frac{-\mu w + (\mu^2 w^2 - k(2\mu w \cdot s - \frac{w \cdot v_o^2}{g}))^{.5}}{k}$ | HORIZ |



(e)



(f)



(g)

PULLEYS: (DYNA/XMPI/PULY)

| | | |
|--------------------------------|--|-------|
| (85) (h) Acceleration on slope | $a = g \frac{w_1(\cos\beta - \mu \sin\beta) - w_2}{w_1 + w_2}$ | ACCEL |
| (86) (i) Tension on cables | $T = 2w_1 \left(1 - \frac{w_1 - w_2}{w_1 + w_2}\right)$ | TNSN |

DYNAMICS

VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT (ENG, SI)</u> |
|---------------|--|
| <u>a</u> | Linear acceleration; <u>ft/s²</u> , <u>m/s²</u> (1 ft/s ² = 0.3048 m/s ²). |
| <u>an</u> | Normal acceleration; <u>ft/s²</u> , <u>m/s²</u> (1 ft/s ² = 0.3048 m/s ²). |
| <u>dy</u> | Deflection; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>Ek</u> | Kinetic energy; <u>ft-lbf</u> , <u>J</u> (1 ft-lbf = 1.3558 J(N.m)). |
| <u>Ep</u> | Potential energy; <u>ft-lbf</u> , <u>J</u> (1 ft-lbf = 1.3558 J(N.m)). |
| <u>f</u> | Frequency; <u>cps</u> (cycle per second) |
| <u>F</u> | Force; <u>lbf</u> , <u>N</u> (1 lbf = 4.4482 N). |
| <u>Fc</u> | Centrifugal force; <u>lbf</u> , <u>N</u> (1 lbf = 4.4482 N). |
| <u>g</u> | Acceleration of gravity; (<u>g</u> = 32.2 ft/s ² = 9.81 m/s ²). |
| <u>h</u> | Height; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>Hh</u> | Launch base altitude from the target; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>I</u> | Mass moment of inertia; <u>lbm-ft²</u> , <u>Nm-m²</u> (1 lbm-ft ² = 0.04214 kg.m ²). |
| <u>k</u> | Spring constant; <u>lbf/ft</u> , <u>N/m</u> (1 lbf/ft = 14.5939 N/m). |
| <u>kph</u> | Kilometer per hour; (1 kph = 0.62137 mph). |
| <u>l</u> | Length, pendulum; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>m</u> | Mass; <u>lbm</u> , <u>kg</u> (1 lbm = 0.4536 kg). |
| <u>mph</u> | Mile per hour; (1 mph = 1.609344 kph). |
| <u>N</u> | Number of rotations; <u>None</u> . |
| <u>R</u> | Maximum projectile range on horizontal plane; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m) |
| <u>r</u> | Radius; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>RPM</u> | Revolution per minute. |
| <u>RPMo</u> | Initial revolution, per minute. |
| <u>RW</u> | Road's width; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>s</u> | Linear displacement; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>T</u> | Total flight time; <u>sec.</u> : Period; <u>spc.</u> : Tension; <u>lbf</u> , <u>N</u> (1 lbf = 4.4482 N). |
| <u>t</u> | Time; <u>sec.</u> |
| <u>Th</u> | Flight time; <u>sec.</u> |
| <u>v</u> | Velocity; <u>ft/s</u> , <u>m/s</u> (1 ft/s = 0.3048 m/s). |
| <u>vx</u> | Horizontal velocity; <u>fps</u> , <u>m/s</u> (1 ft/s = 0.3048 m/s). |
| <u>vy</u> | Vertical velocity; <u>fps</u> , <u>m/s</u> (1 ft/s = 0.3048 m/s). |
| <u>w</u> | Weight; <u>lb</u> , <u>kg</u> (1 lb = 0.4536 kg). |
| <u>x</u> | Projectile's horizontal displacement; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>xh</u> | Horizontal displacement; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>y</u> | Projectile altitude above the base; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>yh</u> | Altitude above the base; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |

DYNAMICS

VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT</u> |
|---------------|--|
| α | Angular acceleration; <u>rad/s</u> . |
| β | Angle with horizontal plane; <u>deg</u> . |
| μ | Coefficient of friction; <u>decimal</u> . |
| Ω | Banking, Launch, or Drop angle; <u>deg</u> . |
| ω | Angular velocity; <u>rad/s</u> . |
| ω_o | Initial angular velocity; <u>rad/s</u> . |
| θ | Angle subtended; <u>rad</u> . |

ELECTRICITY

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

BATTERIES IN PARALLEL: (ELEC/BATT)

| | | |
|---------------------------------|---|-------|
| (01) Current through battery #1 | $I_1 = \frac{V_1 - V_2 + I * R_2}{R_1 + R_2}$ | I_1 |
| (02) Current through battery #2 | $I_2 = \frac{V_2 - V_1 + I * R_1}{R_1 + R_2}$ | I_2 |

CAPACITORS: (ELEC/CAPAC)

Equivalent Capacitance: (ELEC/CAPAC/EQUIV)

| | | |
|---|---|--------------|
| (03) Parallel, 2 or 3 <u>Series: (ELEC/CAPAC/EQUIV/SERI)</u> | $C_o = C_1 + C_2 + C_3$ | PARA |
| (04) Two in Series | $C_o = \frac{C_1 * C_2}{C_1 + C_2}$ | TWO |
| (05) Three in Series | $C_o = \frac{C_1 * C_2 * C_3}{C_1 * C_2 + C_1 * C_3 + C_2 * C_3}$ | THREE |

Capacitance Reactance: (ELEC/CAPAC/REAC)

| | | |
|--------------------------|--------------------------------|--------------------------------|
| (06) With f and C | $X_c = \frac{1}{2\pi * f * C}$ | F . C |
| (07) With V and I | $X_c = \frac{V}{I}$ | V . I |
| (08) With ω and C | $X_c = \frac{1}{\omega * C}$ | ω . C |

| | | |
|----------------------------------|---|--------------|
| (09) Coulomb Law (ELEC) | $F = \frac{q_1 * q_2}{4\pi * \epsilon * r^2}$ | CULMB |
|----------------------------------|---|--------------|

IMPEDANCE: (ELEC/IMPED)

| | | |
|----------------|-------------------|------------|
| (10) Magnitude | $Z = \frac{V}{I}$ | MAG |
|----------------|-------------------|------------|

ELECTRICITY

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|--|-------------|
| <u>Magnitude: R, L, and C in Parallel (ELEC/IMPED/PARA)</u> | | |
| (11) With R and C | $Z = \frac{R * X_c}{\sqrt{R^2 + X_c^2}}$ | R . C |
| (12) With R and L | $Z = \frac{R * X_L}{\sqrt{R^2 + X_L^2}}$ | R . L |
| (13) With L and C | $Z = \frac{X_L * X_c}{X_L - X_c}$ | L . C |
| (14) With R , L, and C | $Z = \frac{R * X_L * X_c}{\sqrt{X_L^2 * X_c^2 + R^2 (X_L - X_c)^2}}$ | R . L . C |
| <u>Magnitude of R, L, and C in Series (ELEC/IMPED/SERI)</u> | | |
| (15) With R and C | $Z = \sqrt{R^2 + X_c^2}$ | R . C |
| (16) With R and L | $Z = \sqrt{R^2 + X_L^2}$ | R . L |
| (17) With C and L | $Z = X_L - X_c$ | C . L |
| (18) With R , L, and C | $Z = \sqrt{R^2 + (X_L - X_c)^2}$ | R . L . C |

INDUCTORS: (ELEC/INDUC)

Equivalent Inductance: (ELEC/INDUC/EQUIV)

Parallel: (ELEC/INDUC/EQUIV/PARA)

| | | |
|-----------------------------|---|-------|
| (19) Two in Parallel | $L_o = \frac{L_1 * L_2}{L_1 + L_2}$ | TWO |
| (20) Three in Parallel | $L_o = \frac{L_1 * L_2 * L_3}{L_1 * L_2 + L_1 * L_3 + L_2 * L_3}$ | THREE |
| (21) Two or three in Series | $L_o = L_1 + L_2 + L_3$ | SERI |

Inductive Reactance: (ELEC/INDUC/REAC)

| | | |
|-------------------|----------------------|------------|
| (22) With f and L | $X_L = 2\pi * f * L$ | F . L |
| (23) With V and I | $X_L = \frac{V}{I}$ | V . I |
| (24) With w and L | $X_L = L * \omega$ | \omega . L |

ELECTRICITY

DESCRIPTION

FORMULA

NAME

KIRCHOFF'S LAW: (ELEC/KIRC)

Two (2) MESH network: (ELEC/KIRC/2LOOP)

The format of the equations resulted from applying the Kirchoff's Law, are as follow:

$$\begin{cases} A_1 I_1 + B_1 I_2 = C_1 \\ A_2 I_1 + B_2 I_2 = C_2 \end{cases}$$

(25) Current in MESH #1

$$I_1 = \text{EXPR} = \frac{C_1 B_2 - B_1 C_2}{A_1 B_2 - A_2 B_1} \quad I1$$

(26) Current in MESH #2

$$I_2 = \text{EXPR} = \frac{C_1 A_2 - A_1 C_2}{A_2 B_1 - A_1 B_2} \quad I2$$

Three (3) MESH network: (ELEC/KIRC/3LOOP)

The format of the equations, resulted from applying the Kirchoff's Law, are as follow:

$$\begin{cases} A_1 I_1 + B_1 I_2 + C_1 I_3 = D1 \\ A_2 I_1 + B_2 I_2 + C_2 I_3 = D2 \\ A_3 I_1 + B_3 I_2 + C_3 I_3 = D3 \end{cases}$$

Current in MESH #1

$$(27) \quad I_1 = \text{EXPR} = \frac{(C_3 B_2 - C_2 B_3) (C_2 D_1 - C_1 D_2) - (C_2 B_1 - C_1 B_2) (C_3 D_2 - C_2 D_3)}{(C_3 B_2 - C_2 B_3) (C_2 A_1 - C_1 A_2) - (C_2 B_1 - C_1 B_2) (C_3 A_2 - C_2 A_3)} \quad I1$$

Current in MESH #2

$$(28) \quad I_2 = \text{EXPR} = \frac{(A_3 C_2 - A_2 C_3) (A_2 D_1 - A_1 D_2) - (A_2 C_1 - A_1 C_2) (A_3 D_2 - A_2 D_3)}{(A_3 C_2 - A_2 C_3) (A_2 B_1 - A_1 B_2) - (A_2 C_1 - A_1 C_2) (A_3 B_2 - A_2 B_3)} \quad I2$$

Current in MESH #3

$$(29) \quad I_3 = \text{EXPR} = \frac{(A_3 B_2 - A_2 B_3) (A_2 D_1 - A_1 D_2) - (A_2 B_1 - A_1 B_2) (A_3 D_2 - A_2 D_3)}{(A_3 B_2 - A_2 B_3) (A_2 C_1 - A_1 C_2) - (A_2 B_1 - A_1 B_2) (A_3 C_2 - A_2 C_3)} \quad I3$$

MOTORS: (ELEC/MOTR)

Elevators: (ELEC/MOTR/ELEV)

English System: (ELEC/MOTR/ELEV/ENG)

(30) Power in kW

$$kW = \frac{w \times fpm}{44254 \times \eta} \quad KW$$

(31) Power in hp

$$hp = \frac{w \times fpm}{33000 \times \eta} \quad HP$$

ELECTRICITY

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|---|-------------|
| <u>SI System: (ELEC/MOTR/ELEV/SI)</u> | | |
| (32) Power in kW | $kW = \frac{W \times rpm}{6118.33 \times \eta}$ | KW |
| (33) Power in hp | $hp = \frac{W \times rpm}{4562.4 \times \eta}$ | HP |
| <u>Power: (ELEC/MOTR/POWER)</u> | | |
| <u>Single Phase: (ELEC/MOTR/POWER/ 1ϕ)</u> | | |
| (34) Power in kW | $kW = \frac{V \times I \times PF \times \eta_M}{1000}$ | KW |
| (35) Power in hp | $hp = \frac{V \times I \times PF \times \eta_M}{745.7}$ | HP |
| <u>Three Phase: (ELEC/MOTR/POWER/ 3ϕ)</u> | | |
| (36) Power in kW | $kW = \frac{\sqrt{3} \times V \times I \times PF \times \eta_M}{1000}$ | KW |
| (37) power in hp | $hp = \frac{\sqrt{3} \times V \times I \times PF \times \eta_M}{745.7}$ | HP |
| <u>Pumps: (ELEC/MOTR/PUMP)</u> | | |
| <u>Horsepower: (ELEC/MOTR/PUMP/HP)</u> | | |
| <u>English System: (ELEC/MOTR/PUMP/HP/ENG)</u> | | |
| (38) Flow in gpm | $hp = \frac{h \times gpm \times SG}{3960 \times \eta}$ | GPM |
| (39) Flow in lbps | $hp = \frac{h \times lbps}{550 \times \eta}$ | LBPS |
| (40) Flow in cfs | $hp = \frac{h \times cfs \times SG}{8.814 \times \eta}$ | CFS |
| <u>SI System: (ELEC/MOTR/PUMP/HP/SI)</u> | | |
| (41) Flow in m3ps | $hp = \frac{h \times m3ps \times SG}{.07615 \times \eta}$ | M3PS |
| (42) Flow in lps | $hp = \frac{h \times lps \times SG}{76.15 \times \eta}$ | LPS |
| (43) Flow in kgps | $hp = \frac{h \times kgps}{76.15 \times \eta}$ | KGPS |
| <u>Speed: (ELEC/MOTR)</u> | | |
| (44) Rotational speed | $RPM = \frac{120 \times f(1-s)}{P}$ | RPM |
| <u>Torque: (ELEC/MOTR/TORQ)</u> | | |
| (45) English System | $T = \frac{5252.1 \times hp}{RPM}$ | ENG |
| (46) SI System | $T = \frac{7120.8 \times hp}{RPM}$ | SI |

ELECTRICITY

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|---|-------------|
| POWER: (ELEC/POWR) | | |
| Apparent: (ELEC/POWR/APAR) | | |
| (47) Single phase | $P_a = V \times I$ | 1 ϕ |
| (48) Three phase | $P_a = \sqrt{3} \times V \times I$ | 3 ϕ |
| Effective: (ELEC/POWR/EFEC) | | |
| (49) Instantaneous | $P_i = V \times I (\cos \phi + \cos(2\omega \cdot t + \phi))$ | INST |
| (50) Average, single phase | $P = V \times I \times PF$ | 1 ϕ |
| (51) Average, three phase | $P = \sqrt{3} \times V \times I \times PF$ | 3 ϕ |
| Reactive: (ELEC/POWR/REAC) | | |
| (52) Average, single phase | $P_r = V \times I \times \sin(\arccos(PF))$ | 1 ϕ |
| (53) Average, three phase | $P_r = \sqrt{3} \times V \times I \times \sin(\arccos(PF))$ | 3 ϕ |
| <hr/> | | |
| POWER FACTOR: (ELEC/PFAC) | | |
| Power Factor Equations: (ELEC/PFAC/EQUA) | | |
| (54) Power Factor with ϕ | $PF = \cos(\phi)$ | ϕ |
| (55) Power Factor with X and R | $PF = \cos(\arctan \frac{X}{R})$ | X, R |
| (56) Power Factor with W and VA | $PF = \frac{kW}{kVA}$ | W, VA |
| (57) Power Factor (Single phase) | $PF = \frac{1000 \times kW}{V \times I}$ | 1 ϕ |
| (58) Power Factor (Three phase) | $PF = \frac{1000 \times kW}{\sqrt{3} \times V \times I}$ | 3 ϕ |
| (59) Power Factor with I1 and I2 | $PF_2 = PF_1 \times \frac{I_1}{I_2}$ | I1, I2 |
| Power Factor Correction: (ELEC/PFAC/COREC) | | |
| (60) System Power Factor | $PF_1 = \frac{R \cdot kW + M \cdot kW}{\sqrt{(M \cdot kW \times \tan(\arccos(M \cdot PF)))^2 + (R \cdot kW + M \cdot kW)^2}}$ | SYSPF |
| (61) Capacitors kVAR | $kVAR = (R \cdot kW + M \cdot kW) \times (\tan(\arccos(PF_1)) - \tan(\arccos(PF_2)))$ | KVAR |
| (62) Capacitors Value, in Farad. | $C = \frac{159.15 \times kVAR}{f \times V^2}$ | FARAD |

ELECTRICITY

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|---|-------------|
| RESISTORS: (ELEC/RESIS) | | |
| Equivalent Resistance: (ELEC/RESIS/EQUIV) | | |
| Parallel: (ELEC/RESIS/EQUIV/PARA) | | |
| (63) Two in parallel | $R_e = \frac{R_1 * R_2}{R_1 + R_2}$ | TWO |
| (64) Three in parallel | $R_e = \frac{R_1 * R_2 * R_3}{R_1 * R_2 + R_1 * R_3 + R_2 * R_3}$ | THREE |
| (65) Series, 2 or 3 | $R_e = R_1 + R_2 + R_3$ | SERI |
| (66) Resistance, general equation | $R = \frac{\rho * L}{A}$ | GNRL |
| (67) Resistance variance with temperature | $R_2 = R_1 (1 + \alpha * dt)$ | ΔT |
| (68) Thermal Coefficient of resistant | $\alpha = \frac{R_2 - R_1}{dt * R_1}$ | ΔT |
| <hr/> | | |
| RESONANCE: (ELEC/RESO) | | |
| (69) Angular velocity | $\omega_r = \sqrt{\frac{1}{L * C}}$ | ANG. V |
| Capacitance: (ELEC/RESO/CAPAC) | | |
| (70) With L and w | $C_x = \frac{1}{L * \omega^2}$ | L. ω |
| (71) With L and f | $C_x = \frac{1}{L (2\pi * f)^2}$ | L. F |
| Frequency: (ELEC/RESO/FREQ) | | |
| (72) With w and R | $f_r = \frac{\omega_r}{2\pi}$ | $\omega. R$ |
| (73) With L and C | $f_r = \frac{1}{2\pi} \sqrt{\frac{1}{L * C}}$ | L. C |
| (74) With f and X | $f_r = f \sqrt{\frac{X_c}{X_L}}$ | F. X |
| Inductance: (ELEC/RESO/INDUC) | | |
| (75) With C and f | $L_x = \frac{1}{C (2\pi * f)^2}$ | C. F |
| (76) With C and w | $L_x = \frac{1}{C * \omega^2}$ | C. ω |

ELECTRICITY

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|--|-------------|
| <u>VOLTAGE DROP: (ELEC/VDRP)</u> | | |
| <u>Line Current: (ELEC/VDRP/CURR)</u> | | |
| (77) Single phase load | $I = \frac{1000 \times kW}{V \times PF}$ | 1 ϕ |
| (78) Three phase load | $I = \frac{1000 \times kW}{\sqrt{3} \times V \times PF}$ | 3 ϕ |
| <u>Voltage drop, across a copper conductors: (ELEC/VDRP/DROP)</u> | | |
| (79) AWG size Conductors: 14 AWG - 1 AWG, 20 amps - 130 amps: | | |
| | $VD = .001 \times L \times I (.1257 e^{(-.2285 \times AWG)} \times PF + (.0552 + .00121 \times AWG) \times \sin(\arccos(PF)))$ | AWG |
| (80) AUGHT size Conductors: 1/0 - 4/0, 150 amps - 230 amps: | | |
| | $VD = .001 \times L \times I (.1512 e^{(-.2169 \times AWT)} \times PF + (.0565 - .0014 \times AWT) \times \sin(\arccos(PF)))$ | AWT |
| (81) KCMIL size Conductors: 250 KCM - 1000 KCM, 255 amps - 545 amps: | | |
| | $VD = .001 \times L \times I (4.322 \times KCM^{-.8} \times PF + .0835 \times KCM^{-.0876} \times \sin(\arccos(PF)))$ | KCM |

ELECTRICITY

VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT (ENG, SI)</u> |
|--|---|
| <u>A</u> | Section area of wire; <u>CM</u> , <u>m²</u> (1 CM = 5.067EE-10 m ²). |
| <u>C</u> | Capacitance, Capacitor value; <u>farad</u> , Charge; <u>Coulomb</u> . |
| <u>Ce</u> | Equivalent Capacitance; <u>farad</u> . |
| <u>cfs</u> | Cubic feet per second (1 cfs = 448.83 gpm = 0.02832 m ³ /s). |
| <u>CM</u> | Circular Mill ($CM = d^2 \times 1.131$, d=diameter of wire in inch). |
| <u>cps</u> | Cycle per second. |
| <u>dt</u> | Temperature difference; <u>oC</u> . |
| <u>F</u> | Force; <u>N</u> (Newton) (1 N = 0.22481 lbf). |
| <u>f</u> | Frequency; <u>cps</u> . |
| <u>fpm</u> | Feet per minute (1 fpm = 0.3048 mpm). |
| <u>gpm</u> | Gallon per minute (1 gpm = 0.002228 cfs = 6.309EE-5 m ³ /s). |
| <u>h</u> | Head; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m). |
| <u>I</u> | Current; <u>Amp</u> . |
| <u>kgps</u> | Kilogram per second (1 kgps = 2.2046 lbps). |
| <u>L</u> | Inductance; <u>henry</u> : Length; <u>ft</u> , <u>m</u> (1 ft = .3048 m). |
| <u>Le</u> | Equivalent Inductance; <u>henry</u> . |
| <u>lbps</u> | Pound per second (1 lbps = .4536 kgps). |
| <u>lps=L/s</u> | Liter per second (1 L/s = 15.85 gpm = 0.035315 cfs). |
| <u>m³ps=m³/s</u> | Cubic meter per second (1 m ³ /s = 15850 gpm = 35.315 cfs). |
| <u>M.KW</u> | Motor/Inductive load; <u>kW</u> . |
| <u>M.PF</u> | Motor/Induction's load Power Factor; <u>None</u> . |
| <u>mpm</u> | Meters per minute. |
| <u>p</u> | Number of poles; <u>none</u> . |
| <u>P</u> | Effective Power; <u>watt</u> . |
| <u>Pa</u> | Apparent Power; <u>volt amp</u> . |
| <u>PF</u> | Power Factor; <u>None</u> . |
| <u>Pi</u> | Instantaneous effective Power; <u>watt</u> . |
| <u>Pr</u> | Reactive Power; <u>var</u> . |
| <u>q</u> | Charge; C (coulomb). |

ELECTRICITY

VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT (ENG, SI)</u> |
|----------------------|---|
| <u>r</u> | Distance; <u>ft, m</u> (1 ft = .3048 m). |
| <u>R</u> | Resistance; <u>ohm</u> . |
| <u>R.KW</u> | Resistive load; <u>kW</u> . |
| <u>Ro</u> | Original resistance (at 20 Oc); <u>ohm</u> . |
| <u>RPM</u> | Revolution Per Minute. |
| <u>S</u> | Slip; <u>decimal</u> . |
| <u>SG</u> | Specific Gravity; <u>None</u> . |
| <u>T</u> | Period of cycle; <u>spc</u> : Torque; <u>ft-lbf, N-m</u> (1 ft-lbf = 1.3558 N.m = .13826 kg.m). |
| <u>t</u> | Temperature; <u>oC</u> : Time; <u>sec</u> . |
| <u>V</u> | Voltage; <u>volt</u> |
| <u>VD</u> | Voltage Drop; <u>volt</u> |
| <u>w</u> | Weight; <u>lbf, kg</u> (1 lbf = .4536 kg). |
| <u>X</u> | Reactance; <u>ohm</u> . |
| <u>Xc</u> | Capacitive reactance; <u>ohm</u> . |
| <u>XL</u> | Inductive reactance; <u>ohm</u> . |
| <u>Z</u> | Impedance; <u>ohm</u> |
| <u>α</u> | Thermal coefficient of resistance; <u>1/oC</u> . |
| <u>ε</u> | Permittivity; <u>C2/N-m2</u> . |
| <u>η</u> | Efficiency; <u>decimal</u> . |
| <u>η_M</u> | Motor's efficiency; <u>decimal</u> . |
| <u>ω</u> | Angular velocity; <u>rad/sec. or deg./sec</u> . |
| <u>φ</u> | Phase angle; <u>deg</u> . |
| <u>ρ</u> | Resistivity; <u>ohm-CM/ft, ohm.m</u> (1 ohm-CM/ft = 1.66243E-9 ohm.m). |

ENGINEERING ECONOMICS

ANNUAL COST, EQUIVALENT UNIFORM: (ENEC/ANNU)

- (01) With Sinking Fund depreciation, SF
$$A = \frac{i(P-L)(1+i)^n}{(1+i)^n - 1} + L \cdot i + AE$$
 SF
- (02) With SF & uniform gradient, G
$$A = \frac{i(P-L)(1+i)^n}{(1+i)^n - 1} + L \cdot i + AE + G(A/G, i, n)$$
 SF+G
- (03) With Straight Line depreciation, SL
$$A = \frac{P-L}{n} + \frac{i}{2 \cdot n} (n+1)(P-L) + L \cdot i + AE$$
 SL
- (04) Equalized Annual Cost/Income (For up to five (5) years, same interest rate.)

$$A_{eq} = \frac{i(1+i)^n}{(1+i)^n - 1} (A_1(1+i)^{-1} + A_2(1+i)^{-2} + A_3(1+i)^{-3} + A_4(1+i)^{-4} + A_5(1+i)^{-5})$$
 AEQ
-

BONDS: (ENEC/BOND)

- (05) Present Worth
$$PW = BSV(1+R)^{-n} + \frac{i \cdot BFV}{2} \frac{(1+R)^n - 1}{R(1+R)^n}$$
 PW
- (06) Rate of Return (approximate)
$$ROR = \frac{\frac{BSV - PV}{n} + i \cdot BFV}{\frac{BSV + PW}{2}}$$
 ROR
-

CAPITALIZED COST: (ENEC/CAPIT)

- (07) With no periodical replacement
$$CC = P + \frac{A}{i}$$
 N. REP
- With periodical replacement/cost: (ENEC/CAPIT/W.REP)
- (08) With in-kind periodical replacement
$$CC = P + \frac{P-L}{(1+i)^n - 1} + \frac{A}{i}$$
 KIND
- (09) With other periodical cost
$$CC = P + \frac{PC}{(1+i)^n - 1} + \frac{A}{i}$$
 OTHER

ENGINEERING ECONOMICS

COMPOUND FACTORS/VALUES: (ENEC/FACTR)

| | | |
|--|--|-----------|
| (10) Future to Annual/Annual to Future | $A = \frac{f}{(1+f)^n - 1} * F$ | AF |
| (11) Gradient to Annual/Annual to Gradient | $A = \left(\frac{1}{f} - \frac{n}{(1+f)^n - 1} \right) * G$ | AG |
| (12) Present to Annual/Annual to Present | $A = \frac{f(1+f)^n}{(1+f)^n - 1} * P$ | AP |
| (13) Present to Future/Future to Present | $F = (1+f)^n * P$ | FP |
| (14) Gradient to Present/Present to Gradient | $P = \left(\frac{(1+f)^n - 1}{f^2(1+f)^n} - \frac{n}{f(1+f)^n} \right) * G$ | PG |

DEPRECIATION: (ENEC/DEPRI)

Double Declining Balance: (ENEC/DEPRI/DDB)

| | | |
|---|---|--------------|
| (15) For the xth year | $D_x = \frac{2P}{n} \left(1 - \frac{2}{n}\right)^{(x-1)}$ | DX |
| (16) Book value after x year(s) | $BV_x = P \left(1 - \frac{2}{n}\right)^x$ | BVX |
| (17) After Tax Depreciation Recovery (ATDR) | $ATDR = TAX.R \left(\frac{2P}{n \left(1 - \frac{2}{n}\right)} \frac{\left(\frac{(1+f)n}{n-2}\right)^n - 1}{\left(\frac{(1+f)n}{n-2}\right)^n \left(\frac{(1+f)n}{n-2} - 1\right)} \right)$ | RECOV |

Sinking Fund: (ENEC/DEPRI/SF)

| | | |
|---------------------------------|--|------------|
| (18) For the xth year | $D_x = (P-L) \frac{f}{(1+f)^n - 1} (1+f)^{(x-1)}$ | DX |
| (19) Book value after x year(s) | $BV_x = P - (P-L) \frac{f}{(1+f)^n - 1} \frac{(1+f)^x - 1}{f}$ | BVX |

ENGINEERING ECONOMICS

DEPRECIATION: (ENEC/DEPRI)

Straight line: (ENEC/DEPRI/SL)

(20) For the xth year
$$D_x = \frac{P-L}{n} \quad \mathbf{DX}$$

(21) Book value after x year(s)
$$BV_x = \frac{(P-L)(n-x)}{n} + L \quad \mathbf{BVX}$$

(22) After Tax Depreciation Recovery (ATDR)
$$\mathbf{ATDR} = \mathbf{TAX} \cdot \mathbf{R} \frac{P-L}{n} \frac{(1+i)^n - 1}{i(1+i)^n} \quad \mathbf{RECOV}$$

Sum Of the Years' Digits: (ENEC/DEPRI/SOYD)

(23) For the xth year
$$D_x = \frac{2(P-L)(n-x+1)}{n(n+1)} \quad \mathbf{DX}$$

(24) Book value after x year(s)
$$BV_x = P - 2(P-L) \left(n - \frac{x-1}{2} \right) \frac{x}{n(n+1)} \quad \mathbf{BVX}$$

(25) After Tax Depreciation Recovery (ATDR)

$$\mathbf{ATDR} = \mathbf{TAX} \cdot \mathbf{R} \left(\frac{2n}{n(n+1)} \frac{(1+i)^n - 1}{i(1+i)^n} - \frac{2}{n(n+1)} \left(\frac{(1+i)^n - 1}{i^2(1+i)^n} - \frac{n}{i(1+i)^n} \right) \right) \quad \mathbf{RECOV}$$

INTEREST RATE, COMPOUNDED/INFLATION: (ENEC/INTER)

(26) Continuous (yield)
$$i_{CO} = e^{i \cdot y} - 1 \quad \mathbf{YIELD}$$

(27) Effective
$$i_{EF} = \left(1 + \frac{i}{m} \right)^m - 1 \quad \mathbf{EFFECT}$$

(28) Equivalent
$$i_{EQ} = e^{\left(\frac{\ln(1+i)}{m} \right)} - 1 \quad \mathbf{EQUIV}$$

(29) Interest and Inflation combined
$$i_{INF} = i + r(1+i) \quad \mathbf{INFLT}$$

ENGINEERING ECONOMICS

MORTGAGE: (ENEC/MORT)

(30) Installment (Periodical Payment)
$$INSTL = \frac{I(1+I)^n}{(1+I)^n - 1} LOAN$$
 INSTL

(31) Number of payments
$$NP = \frac{-\ln((1-I+LV)/INSTL)}{\ln(1+I)}$$
 NUMB

(32) Balance after xth payment
$$BAL_x = \frac{INSTL}{I} (1 - (1+I)^{(x-n)})$$
 BALAN

Interest Paid: (ENFC/MORT/INTER)

(33) As a part of xth payment
$$I_x = INSTL (1 - (1+I)^{x-1-n})$$
 XTH

(34) Total, after xth payment
$$I_c = INSTL * x - LOAN + \frac{INSTL}{I} (1 - (1+I)^{(x-n)})$$
 TOTAL

Principal Paid: (ENEC/MORT/PRINC)

(35) As a part of xth payment
$$P_x = INSTL (1+I)^{(x-1-n)}$$
 XTH

(36) Total, after xth payment
$$P_c = LOAN - \frac{INSTL}{I} (1 - (1+I)^{(x-n)})$$
 TOTAL

PRESENT WORTH (No depreciation): (ENEC/PW)

Before Tax: (ENEC/PW/B.TAX)

(37) With Uniform Annual Expenses

$$PW = -P + (AR - AE) \frac{(1+i)^n - 1}{i(1+i)^n} + \frac{L}{(1+i)^n}$$
 UNIF

(38) With Uniform Gradient on Annual Expenses

$$PW = -P + (AR - AE - (A/G, i, n) G) \frac{(1+i)^n - 1}{i(1+i)^n} + \frac{L}{(1+i)^n}$$
 GRADI

ENGINEERING ECONOMICS

PRESENT WORTH (No depreciation): (ENEC/PW)

After Tax: (ENEC/PW/A.TAX)

(39) With Uniform Annual Expenses

$$PW = -P + (AR - AE) (1 - TAX.R) \frac{(1+i)^n - 1}{i(1+i)^n} + \frac{L}{(1+i)^n} \quad UNIF$$

(40) With Uniform Gradient on Annual Expenses

$$PW = -P + (AR - AE - (A/G, i, n) G) (1 - TAX.R) \frac{(1+i)^n - 1}{i(1+i)^n} + \frac{L}{(1+i)^n} \quad GRADI$$

Rate Of Return on Investment: (ENEC/ROR)

(41) With salvage value

$$\frac{((1+ROR)^n - 1) AAR}{ROR(1+ROR)^n} + \frac{L}{(1+ROR)^n} = P \quad SAL > 0$$

(42) Without salvage value

$$\frac{((1+ROR)^n - 1) AAR}{ROR(1+ROR)^n} = P \quad SAL = 0$$

ENGINEERING ECONOMICS

VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT</u> |
|---------------|--|
| <u>A</u> | Annuity; amount . |
| <u>AAR</u> | Annual Average Revenue; amount . |
| <u>A1</u> | A2, A3, A4, or A5= Annual expense/income for different years; amount . |
| <u>AE</u> | Annual Uniform Expense; amount . |
| <u>Aeq</u> | Equalized Annual Cost/Income; amount . |
| <u>AI</u> | Annual Income; amount . |
| <u>APR</u> | Annual Percentage Rate; decimal . |
| <u>AR</u> | Annual Revenue; amount . |
| <u>ATDR</u> | After Tax Depreciation Recovery (Present Worth); amount . |
| <u>BFV</u> | Bond's Face Value; amount . |
| <u>BSV</u> | Bond's Sale Value; amount . |
| <u>BVx</u> | Book value at the end of xth year; amount . |
| <u>CC</u> | Capitalized Cost; amount (Initial capital investment to perpetually support project from the interest earned). |
| <u>F</u> | Future Value; amount . |
| <u>G</u> | Uniform Gradient; amount . |
| <u>I</u> | Interest rate per period; APR/12 for monthly payment in case of mortgage; decimal . |
| <u>i=I</u> | Interest rate per period; decimal . ("i" is HP48 designated variable. It should not be used for programming) |
| <u>INSTL</u> | Installment (Payment per period); amount . |
| <u>L</u> | Salvage Value; amount . |
| <u>LOAN</u> | Loan Value; amount . |
| <u>m</u> | Compound number; None . |
| <u>N</u> | $N = 2n$ ($R = ROR/2$); none . (Number of payments for bonds with semi annually interest payment. In case of annual interest payment, $R = ROR$ and $N = n$). |
| <u>n</u> | Number of Payments or Periods; none . |
| <u>P</u> | Present Value; amount . |
| <u>PC</u> | Periodical Uniform Costs; amount . |
| <u>PW</u> | Present Worth; amount . |
| <u>r</u> | Inflation rate per period; decimal . |
| <u>R</u> | $ROR/2$ ($N = 2n$); decimal (Rate for bonds with semi annually interest payment. In case of annual interest payment $R = ROR$ and $N = n$). |
| <u>ROR</u> | Rate of Return; decimal . |
| <u>TAX.R</u> | Tax rate; decimal . |
| <u>x</u> | Period number; none . |
| <u>y</u> | Period; years . |

FLUID MECHANICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

BERNOULLI EQUATIONS: (FLME/BERN)

English System: (FLME/BERN/ENG)

- | | | |
|----------------------------|---|---------------|
| (01) No friction loss | $\frac{P_1}{\rho} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho} + \frac{v_2^2}{2g} + z_2$ | NO. HF |
| (02) With friction loss | $\frac{P_1}{\rho} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho} + \frac{v_2^2}{2g} + z_2 + hf$ | W. HF |
| (03) Friction & minor loss | $\frac{P_1}{\rho} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho} + \frac{v_2^2}{2g} + z_2 + h_f + h_{fIT}$ | HF+ |

SI System: (FLME/BERN/SI)

- | | | |
|----------------------------|---|---------------|
| (04) No friction loss | $\frac{P_1}{\rho \times g} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho \times g} + \frac{v_2^2}{2g} + z_2$ | NO. HF |
| (05) With friction loss | $\frac{P_1}{\rho \times g} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho \times g} + \frac{v_2^2}{2g} + z_2 + hf$ | W. HF |
| (06) Friction & minor loss | $\frac{P_1}{\rho \times g} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho \times g} + \frac{v_2^2}{2g} + z_2 + h_f + h_{fIT}$ | HF+ |
-

CAPILLARITY AND SURFACE TENSION: (FLME/CAPIL)

Capillary rise: (FLME/CAPIL/RISE)

- | | | |
|---------------------|---|------------|
| (07) English System | $h = \frac{4\sigma \cos\beta}{\rho \cdot d}$ | ENG |
| (08) SI System | $h = \frac{0.40788 \cdot \sigma \cdot \cos\beta}{\rho \cdot d}$ | SI |

Surface Tension: (FLME/CAPIL/TENS)

- | | | |
|---|--------------------------------|--------------|
| (09) Surface Tension (General) | $\sigma = \frac{P}{L}$ | GENER |
| (10) Surface Tension (In bulb surrounded by air) | $\sigma = \frac{P \cdot D}{8}$ | AIR |
| (11) Surface Tension (In a droplet or bubble in liquid) | $\sigma = \frac{P \cdot D}{4}$ | LIQID |

FLUID MECHANICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|--|--------------|
| FRICITION FACTOR (MOODY CHART): (FLME/FRIC.F) | | |
| (12) Laminar flow, $NRe < 2000$ | $f = \frac{64}{NRe}$ | LAMI |
| (13) Turbulent flow, $NRe > 4000$ | $\frac{1}{\sqrt{f}} = -2 \text{LOG} \left(\frac{\epsilon D}{3.7} + \frac{2.51}{NRe \sqrt{f}} \right)$ | TURBU |

FRICITION HEAD/LOSS IN PIPE: (FLME/FRIC.H)

Darcy Equations: (FLME/FRIC.H/DARCY)

| | | |
|---|---|--------------|
| (14) General, with the given velocity, in fps | $h_f = \frac{f * L_e * v^2}{2 * g * D}$ | GENER |
|---|---|--------------|

English System: (FLME/FRIC.H/DARCY/ENG)

| | | |
|----------------------------------|--|------------|
| (15) With the given flow, in gpm | $h_f = \frac{f * L_e * gpm^2}{248528 * g * D^5}$ | GPM |
|----------------------------------|--|------------|

| | | |
|----------------------------------|--|------------|
| (16) With the given flow, in cfs | $h_f = \frac{f * L_e * cfs^2}{1.2337 * g * D^5}$ | CFS |
|----------------------------------|--|------------|

SI System: (FLME/FRIC.H/DARCY/SI)

| | | |
|----------------------------------|---|------------|
| (17) With the given flow, in lps | $h_f = \frac{f * L_e * lps^2}{1233700 * g * D^5}$ | LPS |
|----------------------------------|---|------------|

| | | |
|-----------------------------------|---|-------------|
| (18) With the given flow, in m3ps | $h_f = \frac{f * L_e * m3ps^2}{1.2337 * g * D^5}$ | M3PS |
|-----------------------------------|---|-------------|

Hazen-Williams equation (FLME/FRIC.H/HAZN)

| | | |
|---------------------|--|------------|
| (19) English System | $h_f = \frac{3.012 * v^{1.85} * L_e}{C_{HW}^{1.85} * D^{1.165}}$ | ENG |
|---------------------|--|------------|

| | | |
|----------------|--|-----------|
| (20) Si System | $h_f = \frac{6.797 * v^{1.85} * L_e}{C_{HW}^{1.85} * D^{1.165}}$ | SI |
|----------------|--|-----------|

| | | |
|----------------------------------|-------------------------------|--------------|
| (21) Fittings, Valves, Entrances | $h_f = \frac{K * v^2}{2 * g}$ | FITIN |
|----------------------------------|-------------------------------|--------------|

| | | |
|-------------------------------|--|-------------|
| (22) Nozzle, Orifice, Ventury | $h_f = \left(\frac{1}{C_v^2} - 1 \right) \frac{v^2}{2 * g}$ | NOZL |
|-------------------------------|--|-------------|

| | | |
|-------------------------|-----------------------------------|-------------|
| (23) Sudden Contraction | $h_f = \frac{K_c * v_2^2}{2 * g}$ | CONT |
|-------------------------|-----------------------------------|-------------|

Enlargement: (FLME/FRIC.H/NLRG)

| | | |
|--------------|---|-------------|
| (24) Gradual | $h_f = \frac{K_e * (v_1 - v_2)^2}{2 * g}$ | GRAD |
|--------------|---|-------------|

| | | |
|-------------|---|-------------|
| (25) Sudden | $h_f = \left(1 - \left(\frac{D_1}{D_2} \right)^2 \right)^2 \frac{v_1^2}{2 * g}$ | SUDD |
|-------------|---|-------------|

| | | |
|------------------|---|--------------|
| (26) Scaled pipe | $h_f = h_{f_{nev}} \left(\frac{D_{nev}}{D_{scal}} \right)^5$ | SCALE |
|------------------|---|--------------|

FLUID MECHANICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|---|---------------|
| <u>HYDROSTATIC PRESSURE: (FLME/HYD.P)</u> | | |
| <u>English System: (FLME/HYD.P/ENG)</u> | | |
| <u>Horizontal plate: (FLME/HYD.P/ENG/HORIZ)</u> | | |
| (27) Density | $\rho = \frac{P}{h}$ | DENSI |
| (28) Gage pressure | $p = \rho * h$ | PRESS |
| (29) Vertical force | $F = \rho * h * A$ | FORCE |
| <u>Inclined rectangular plate: (FLME/HYD.P/ENG/INCLN)</u> | | |
| <u>Pressure: (FLME/HYD.P/ENG/INCLN/PRESS)</u> | | |
| (30) Gage pressure | $p = \rho * L * \sin \Omega$ | GAGE |
| (31) Gage pressure, average | $p_A = .5 * \rho (L_1 + L_2) \sin \Omega$ | AVER |
| (32) Location of Center of Gravity | $C_G = .5 (L_1 + L_2)$ | CEN. G |
| (33) Location of Center of Pressure | $C_P = \frac{2}{3} (L_1 + L_2 - \frac{L_1 * L_2}{L_1 + L_2})$ | CEN. P |
| (34) Normal force on plane | $F = .5 * \rho (L_1 + L_2) \sin \Omega * A$ | FORCE |
| <u>SI System: (FLME/HYD.P/SI)</u> | | |
| <u>Horizontal plate: (FLME/HYD.P/SI/HORIZ)</u> | | |
| (35) Density | $\rho = \frac{P}{h * g}$ | DENSI |
| (36) Gage pressure | $p = \rho * h * g$ | PRESS |
| (37) Vertical force | $F = \rho * h * g * A$ | FORCE |
| <u>Inclined rectangular plate: (FLME/HYD.P/SI/INCLN)</u> | | |
| <u>Pressure: (FLME/HYD.P/SI/INCLN/PRESS)</u> | | |
| (38) Gage pressure | $p = \rho * L * g * \sin \Omega$ | GAGE |
| (39) Gage pressure, average | $p_A = .5 * \rho * g (L_1 + L_2) \sin \Omega$ | AVER |
| (40) Location of Center of Gravity | $C_G = .5 (L_1 + L_2)$ | CEN. G |
| (41) Location of Center of Pressure | $C_P = \frac{2}{3} (L_1 + L_2 - \frac{L_1 * L_2}{L_1 + L_2})$ | CEN. P |
| (42) Normal force on plane | $F = .5 * \rho * g (L_1 + L_2) \sin \Omega * A$ | FORCE |

FLUID MECHANICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

OPEN CHANNEL: (FLME/CHAN)

| | | |
|-----------|-------------|-------------|
| (43) Flow | $V = v * A$ | <i>FLOW</i> |
|-----------|-------------|-------------|

Roughness Constant: (FLME/CHAN/ROGH)

| | | |
|---------------------|--|------------|
| (44) English System | $n = \frac{1.4859 * HR^{\frac{2}{3}} * SLP^{.5}}{v}$ | <i>ENG</i> |
|---------------------|--|------------|

| | | |
|----------------|---|-----------|
| (45) SI System | $n = \frac{HR^{\frac{2}{3}} * SLP^{.5}}{v}$ | <i>SI</i> |
|----------------|---|-----------|

Velocity: (FLME/CHAN/VELO)

| | | |
|---------------------|--|------------|
| (46) English System | $v = \frac{1.4859 * HR^{\frac{2}{3}} * SLP^{.5}}{n}$ | <i>ENG</i> |
|---------------------|--|------------|

| | | |
|----------------|---|-----------|
| (47) SI System | $v = \frac{HR^{\frac{2}{3}} * SLP^{.5}}{n}$ | <i>SI</i> |
|----------------|---|-----------|

ORIFICE: (FLME/ORIF)

Coefficient: (FLME/ORIF/COEF)

| | | |
|------------------|-------------------------------|-------------|
| (48) Contraction | $C_c = \frac{C_d * v_1}{v_a}$ | <i>CONT</i> |
|------------------|-------------------------------|-------------|

| | | |
|----------------|--|--------------|
| (49) Discharge | $C_d = \frac{4 * V}{\pi * D^2 * \sqrt{2 * g * h}}$ | <i>DISCH</i> |
|----------------|--|--------------|

| | | |
|---------------|-------------------------|-------------|
| (50) Velocity | $C_v = \frac{C_d}{C_c}$ | <i>VELO</i> |
|---------------|-------------------------|-------------|

Discharge Velocity: (FLME/ORIF/VELO)

| | | |
|-------------|------------------------------------|-------------|
| (51) Actual | $v_a = \frac{x}{\sqrt{2 * y / g}}$ | <i>ACTU</i> |
|-------------|------------------------------------|-------------|

| | | |
|------------|--------------------------|--------------|
| (52) Ideal | $v_i = \sqrt{2 * g * h}$ | <i>IDEAL</i> |
|------------|--------------------------|--------------|

Flow quantity: (FLME/ORIF/FLOW)

| | | |
|------------------|--|----------|
| (53) Gage height | $v = \frac{C_d * \pi * D^2}{4} (2 * g * h)^{.5}$ | <i>H</i> |
|------------------|--|----------|

| | | |
|------------------------|---|------------|
| (54) Height difference | $v = \frac{C_d * \pi * D^2}{4} (2 * g * dh (SG_1 - SG_2))^{.5}$ | ΔH |
|------------------------|---|------------|

FLUID MECHANICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|---|--------------|
| <u>PIPE: (FLME/PIPE)</u> | | |
| (55) Area (full flow) | $A = \frac{\pi * D^2}{4}$ | AREA |
| <u>Flow quantity: (FLME/PIPE/FLOW)</u> | | |
| <u>English System: (FLME/PIPE/FLOW/ENG)</u> | | |
| (56) Flow in gpm | $gpm = \frac{v * \pi * D^2}{.00891}$ | GPM |
| (57) Flow in cfs | $cfs = \frac{v * \pi * D^2}{4}$ | CFS |
| <u>SI System: (FLME/PIPE/FLOW/SI)</u> | | |
| (58) Flow in lps | $lps = 785.4 * v * D^2$ | LPS |
| (59) Flow in m3ps | $m3ps = \frac{v * \pi * D^2}{4}$ | M3PS |
| <u>Velocity: (FLME/PIPE/VELO)</u> | | |
| <u>English System: (FLME/PIPE/VELO/ENG)</u> | | |
| (60) Flow in gpm | $v = \frac{.00891 * gpm}{\pi * D^2}$ | GPM |
| (61) Flow in cfs | $v = \frac{4 * cfs}{\pi * D^2}$ | CFS |
| <u>SI System: (FLME/PIPE/VELO/SI)</u> | | |
| (62) Flow in lps | $v = \frac{lps}{785.4 * D^2}$ | LPS |
| (63) Flow in m3ps | $v = \frac{4 * m3ps}{\pi * D^2}$ | M3PS |
| <u>Hydraulic Radius: (FLME/PIPE/HYD.R)</u> | | |
| (64) General | $HR = \frac{\text{Flow Area (FA)}}{\text{Wet Perimeter (WP)}}$ | GENER |
| (65) Central angle given | $HR = \frac{r (.5 * \pi * \Omega - 90 * SIN \Omega)}{\pi * \Omega}$ | ANGL |
| (66) Height of liquid given | $HR = .5 * r - \frac{90 (r-h) * SIN(ACOS(\frac{r-h}{r}))}{\pi * ACOS(\frac{r-h}{r})}$ | HIGHT |

FLUID MECHANICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

PUMP: (FLME/PUMP)

Head added by: (FLME/PUMP/HEAD)

English System: (FLME/PUMP/HEAD/ENG)

| | | |
|------------------|--|------------|
| (67) Flow in gpm | $h_A = \frac{246858 \times hp \times \eta}{gpm \times \rho}$ | <i>GPM</i> |
|------------------|--|------------|

| | | |
|------------------|---|------------|
| (68) Flow in cfs | $h_A = \frac{550 \times hp \times \eta}{cfs \times \rho}$ | <i>CFS</i> |
|------------------|---|------------|

SI System: (FLME/PUMP/HEAD/SI)

| | | |
|------------------|---|------------|
| (69) Flow in lps | $h_A = \frac{76150 \times hp \times \eta}{lps \times \rho}$ | <i>LPS</i> |
|------------------|---|------------|

| | | |
|-------------------|--|-------------|
| (70) Flow in m3ps | $h_A = \frac{76.15 \times hp \times \eta}{m3ps \times \rho}$ | <i>M3PS</i> |
|-------------------|--|-------------|

Horsepower: (FLME/PUMP/HP)

English System: (FLME/PUMP/HP/ENG)

| | | |
|------------------|--|------------|
| (71) Flow in gpm | $hp = \frac{h_A \times gpm \times \rho}{246858 \times \eta}$ | <i>GPM</i> |
|------------------|--|------------|

| | | |
|------------------|---|------------|
| (72) Flow in cfs | $hp = \frac{h_A \times cfs \times \rho}{550 \times \eta}$ | <i>CFS</i> |
|------------------|---|------------|

SI System: (FLME/PUMP/HP/SI)

| | | |
|------------------|---|------------|
| (73) Flow in lps | $hp = \frac{h_A \times lps \times \rho}{76150 \times \eta}$ | <i>LPS</i> |
|------------------|---|------------|

| | | |
|-------------------|--|-------------|
| (74) Flow in m3ps | $hp = \frac{h_A \times m3ps \times \rho}{76.15 \times \eta}$ | <i>M3PS</i> |
|-------------------|--|-------------|

REYNOLDS NUMBER: (FLME/REYN)

| | | |
|------------------------------|--|-------------|
| (75) With Absolute Viscosity | $NR_e = \frac{D \times v \times \rho}{\mu \times g}$ | <i>ABSO</i> |
|------------------------------|--|-------------|

| | | |
|-------------------------------|---------------------------------|--------------|
| (76) With Kinematic Viscosity | $NR_e = \frac{D \times v}{\nu}$ | <i>KINET</i> |
|-------------------------------|---------------------------------|--------------|

SPEED OF SOUND: (FLME/SOUND/ENG)

Gas: (FLME/SOUND/ENG/GAS)

| | | |
|-----------------------------|---|----------------|
| (77) With variables K, R, T | $c_g = \sqrt{k \times g \times R \times T}$ | <i>K. R. T</i> |
|-----------------------------|---|----------------|

| | | |
|----------------------------------|---|--------------------------------|
| (78) With variables K, p, ρ | $c_g = \sqrt{\frac{k \times p \times g}{\rho}}$ | <i>K. P. ρ</i> |
|----------------------------------|---|--------------------------------|

Liquid: (FLME/SOUND/ENG/LIQID)

| | | |
|------------------------|---|-------------|
| (79) With Bulk Modules | $c_l = \sqrt{\frac{BM \times g}{\rho}}$ | <i>BULK</i> |
|------------------------|---|-------------|

| | | |
|--|---|-------------|
| (80) With Coefficient of compressibility | $c_l = \sqrt{\frac{g}{CM \times \rho}}$ | <i>COMP</i> |
|--|---|-------------|

FLUID MECHANICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|------------------------------------|---------------------------|--------------|
| <u>THIN CYLINDER: (FLME/CYLIN)</u> | | |
| (81) Hoop stress | $f = \frac{P \cdot r}{t}$ | STRES |
| (82) Thickness of cylinder | $t = \frac{P \cdot r}{f}$ | THICK |

TURBINE HORSEPOWER: (FLME/TURB/HP)

English System: (FLME/TURB/HP/ENG)

| | | |
|------------------|---|------------|
| (83) Flow in gpm | $hp = \frac{gpm \cdot \rho \cdot h \cdot \eta}{246858}$ | GPM |
|------------------|---|------------|

| | | |
|------------------|--|------------|
| (84) Flow in cfs | $hp = \frac{cfs \cdot \rho \cdot h \cdot \eta}{550}$ | CFS |
|------------------|--|------------|

SI System: (FLME/TURB/HP/SI)

| | | |
|------------------|---|------------|
| (85) Flow in lps | $hp = \frac{h \times lps \times \rho \times \eta}{76150}$ | LPS |
|------------------|---|------------|

| | | |
|-------------------|--|-------------|
| (86) Flow in m3ps | $hp = \frac{h \times m3ps \times \rho \times \eta}{76.15}$ | M3PS |
|-------------------|--|-------------|

VENTURI: (FLME/VENT)

| | | |
|-----------------------------|--|-------------|
| (87) Flow quantity (with h) | $v = \frac{\pi \cdot C_d \cdot D_1^2 \cdot D_2^2}{4} \left(\frac{2g \cdot dh(SG_1 - SG_2)}{D_1^4 - D_2^4} \right)^{.5}$ | HEAD |
|-----------------------------|--|-------------|

| | | |
|-----------------------------|--|--------------|
| (88) Flow quantity (with p) | $v = \frac{\pi \cdot C_d \cdot D_2^2}{4 \left(1 - D_2^4/D_1^4 \right)^{.5}} + \left(2g \left(\frac{P_1 - P_2}{\rho} \right) + z_1 - z_2 \right)^{.5}$ | PRESS |
|-----------------------------|--|--------------|

| | | |
|--------------------|--|---------------|
| (89) Velocity head | $h_v = \frac{v^2 (D_1^4 - D_2^4)}{2g(SG_1 - SG_2) \left(\frac{\pi}{4} C_d \cdot D_1^2 \cdot D_2^2 \right)^2}$ | VEL. H |
|--------------------|--|---------------|

WATER HAMMER: (FLME/HAMR)

| | | |
|------------------------|--|------------------------------|
| (90) Pressure increase | $dp = \frac{\rho \cdot C \cdot dv}{g}$ | ΔP |
|------------------------|--|------------------------------|

| | | |
|------------------------------------|---------------------------|-------------|
| (91) Time for shock wave to travel | $t = \frac{2 \cdot L}{C}$ | TIME |
|------------------------------------|---------------------------|-------------|

FLUID MECHANICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|--|-------------|
| <u>WEIR, RECTANGULAR, SUPPRESSED: (FLME/WEIR)</u> | | |
| <u>Flow quantity: (FLME/WEIR/FLOW)</u> | | |
| (92) English System | $V = 3.33 * b * h^{\frac{2}{3}}$ | ENG |
| (93) SI System | $V = 1.838 * b * h^{\frac{2}{3}}$ | SI |
| <u>Head: (FLME/WEIR/HEAD)</u> | | |
| (94) English System | $h = \left(\frac{V}{3.33 * b} \right)^{\frac{2}{3}}$ | ENG |
| (95) SI System | $h = \left(\frac{V}{1.838 * b} \right)^{\frac{2}{3}}$ | SI |
| (96) Velocity | $v = \frac{V}{b(h+PH)}$ | VELO |

FLUID MECHANICS

VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT (ENG, SI)</u> |
|--|---|
| <u>A</u> | Area; <u>ft²</u> , <u>m²</u> (1 ft ² = .0929 m ² .) |
| <u>b</u> | Weir's width; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m.) |
| <u>BM(E)</u> | Bulk Modules; <u>lbf/ft²</u> . |
| <u>c</u> | Speed of sound; <u>ft/s</u> , <u>m/s</u> (1 ft/s = .3048 m/s, not given, assume: air: 1130 ft/s, 344.4 m/s water: 4880 ft/s, 1487 m/s.) |
| <u>Cc</u> | Contraction Coefficient; <u>None</u> . |
| <u>Cd</u> | Discharge Coefficient; <u>None</u> . |
| <u>cfs=ft³/s</u> | Cubic foot per second (1 cfs = 448.83 gpm = 0.028317 m ³ /s = 28.317 L/s.) |
| <u>cg</u> | Speed of sound in gas; <u>ft/s</u> , <u>m/s</u> (1 ft/s = 0.3048 m/s.) |
| <u>CG</u> | Location of Center of gravity; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m.) |
| <u>C.HW</u> | Hazen-William Coefficient; <u>None</u> (Assumed same value for ENG and SI Systems.) |
| <u>cl</u> | Speed of sound in liquid; <u>ft/s</u> , <u>m/s</u> (1 ft/s = 0.3048 m/s.) |
| <u>CM</u> | Compressibility; <u>ft²/lbf</u> . |
| <u>Cp</u> | Location of Center of pressure; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m.) |
| <u>Cv</u> | Velocity Coefficient; <u>None</u> . |
| <u>D</u> | Diameter; <u>ft</u> , <u>m</u> : Diameter of droplet, bubble; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>d</u> | Depth; <u>ft</u> , <u>m</u> : Diameter; <u>ft</u> , <u>m</u> : Diameter of capillary tube ; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>dh</u> | Height difference; <u>ft</u> , <u>m</u> (1 ft = 0.3048 m.) |
| <u>dp</u> | Pressure difference; <u>lbf/ft²</u> , <u>Pa</u> (1 lbf/ft ² = 47.88 Pa.) |
| <u>dv</u> | Velocity difference; <u>ft/s</u> , <u>m/s</u> (1 ft/s = 0.3048 m/s.) |
| <u>F</u> | Force; <u>lbf</u> , <u>N</u> (1 lbf = 4.4482 N.) |
| <u>f</u> | Friction Factor; <u>None</u> : Hoop stress; <u>lbf/s²</u> , <u>Pa</u> (1 lbf/in ² = 6894.8 Pa.) |
| <u>g</u> | Gravity acceleration; <u>ft/s²</u> , <u>m/s²</u> (g=32.2 ft/s ² , g=9.8067 (9.81) m/s ² .) |
| <u>gpm</u> | Gallon per minute (1 gpm = 0.002228 cfs = 6.309EE-5 m ³ /s = 0.06309 L/s.) |
| <u>hA</u> | Added head; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>hf</u> | Friction head; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>hFIT</u> | Fittings friction head; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>HR</u> | Hydraulic Radius; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>hv</u> | Velocity head; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>K/Ke</u> | Coefficient; <u>None</u> . |
| <u>k</u> | Specific Heat Ratio; <u>None</u> . |
| <u>L</u> | Length; <u>ft</u> , <u>m</u> : Distance; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>Le</u> | Equivalent length; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>lps=L/s</u> | Liter per second (1 L/s = 15.85 gpm = 0.035315 cfs = 1 EE-3 m ³ /s.) |
| <u>m³ps=m³/s</u> | Cubic meter per second (1 m ³ /s = 15850 gpm = 35.315 cfs = 1000 L/s.) |
| <u>n</u> | Manning roughness constant; <u>None</u> (If not given, assume the design values as: copper: 140, plastic: 130, cast iron/concrete/steel: 100. Assumed same value for ENG and SI) |

FLUID MECHANICS

VARIABLES IDENTIFICATION

SYMBOL DESCRIPTION; UNIT (ENG, SI)

| | |
|-------------------|--|
| <u>NRe</u> | Reynold's number; <u>None</u> . |
| <u>P</u> | Pressure; <u>lbf/in²</u> , <u>Pa</u> (1 lbf/in ² = 6894.8 Pa.) |
| <u>p</u> | Pressure; <u>lbf/ft²</u> , <u>Pa</u> (1 lbf/ft ² = 47.88 Pa.) |
| <u>PH</u> | Plate's height; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>r</u> | Radius of pipe; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) : Radius of cylinder; <u>in</u> , <u>m</u> (1 in = .0254 m.) |
| <u>SG</u> | Specific Gravity; <u>None</u> : subscript 1 = heavier, 2 = lighter. |
| <u>SLP</u> | Slope; <u>ft/1000ft</u> . |
| <u>t</u> | Thickness; <u>in</u> . : Time; <u>sec</u> . |
| <u>T</u> | Absolute temperature; <u>oR</u> . |
| <u>V</u> | Flow quantity; <u>ft³/s</u> , <u>m³/s</u> (1 ft ³ /s = .028317 m ³ /s.) |
| <u>v</u> | Velocity; <u>ft/s</u> , <u>m/s</u> (1 ft/s = .3048 m/s.) |
| <u>va</u> | Actual velocity; <u>ft/s</u> , <u>m/s</u> (1 ft/s = .3048 m/s.) |
| <u>vi</u> | Ideal velocity; <u>ft/s</u> , <u>m/s</u> (1 ft/s = .3048 m/s.) |
| <u>x</u> | x coordinate from orifice; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>y</u> | y coordinate from orifice; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>z</u> | Elevation above datum; <u>ft</u> , <u>m</u> (1 ft = .3048 m.) |
| <u>α</u> | Blade's angle with x axis; <u>degree</u> . |
| <u>β</u> | Liquid's angle with the wetted tube wall; <u>degree</u> . |
| <u>ε</u> | Specific roughness; <u>ft</u> (If not given, assume the design values as; copper/plastic: 0.000005, cast iron: 0.0008, steel: 0.0002, concrete: 0.004) |
| <u>η</u> | Efficiency; <u>decimal</u> . |
| <u>μ</u> | Absolute viscosity; <u>lbf-sec/sf</u> . |
| <u>ν</u> | Kinematic viscosity, <u>ft²/sec</u> . |
| <u>Ω</u> | Inclination or central angle; <u>deg</u> . |
| <u>ρ</u> | Density; <u>lb/ft³</u> , <u>kg/m³</u> (If not given for water, assume: 62.4 lb/ft ³ , 1000 kg/m ³ .) |
| <u>σ</u> | Surface tension; <u>lbf/ft</u> , <u>N/m</u> (1 lbf/ft = 14.594 N/m.) |

GAS PROPERTY CHANGE (IDEAL GAS)

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|----------------------------------|-------------|
| <u>CONSTANT PRESSURE: (GASP/PRESS)</u> | | |
| dp=0, Q=dh, c=cp | | |
| (01) Volume change | $v_2 = v_1 \frac{T_2}{T_1}$ | ΔV |
| (02) Temperature change | $T_2 = T_1 \frac{v_2}{v_1}$ | ΔT |
| (03) Enthalpy change | $dh = c_p (T_2 - T_1)$ | ΔH |
| (04) Entropy change | $ds = c_p * \ln \frac{T_2}{T_1}$ | ΔS |
| (05) Internal energy change | $du = c_v (T_2 - T_1)$ | ΔU |
| (06) Heat | $Q = c_p (T_2 - T_1)$ | Q |
| (07) Work | $W = p_1 (v_2 - v_1)$ | W |

CONSTANT TEMPERATURE: (GASP/TEMP)

dT=0, dh=0, du=0, W=Q, n=1

| | | |
|----------------------|-----------------------------|------------|
| (08) Pressure change | $p_2 = p_1 \frac{v_1}{v_2}$ | ΔP |
| (09) Volume change | $v_2 = v_1 \frac{p_1}{p_2}$ | ΔV |

Entropy change: (GASP/TEMP/ ΔS)

| | | |
|---------------------|--|------------|
| (10) English System | $ds = \frac{R}{778} * \ln \frac{v_2}{v_1}$ | ENG |
| (11) SI System | $ds = R * \ln \frac{v_2}{v_1}$ | SI |

Heat: (GASP/TEMP/HEAT)

With P and V: (GASP/TEMP/HEAT/P.V)

| | | |
|---------------------|---|------------|
| (12) English System | $Q = \frac{P_1 * v_1}{778} * \ln \frac{v_2}{v_1}$ | ENG |
| (13) SI System | $Q = P_1 * v_1 * \ln \frac{v_2}{v_1}$ | SI |

GAS PROPERTY CHANGE (IDEAL GAS)

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

CONSTANT TEMPERATURE (continued): (GASP/TEMP)

With R, T, and V: (GASP/TEMP/HEAT/R.T.V)

14) English System

$$Q = \frac{R \cdot T}{778} \cdot \ln \frac{V_2}{V_1}$$

ENG

(15) SI System

$$Q = R \cdot T \cdot \ln \frac{V_2}{V_1}$$

SI

Work: (GASP/TEMP/WORK)

(16) With P and V

$$W = P_1 \cdot V_1 \cdot \ln \frac{V_2}{V_1}$$

P . V

(17) With R, T, and V

$$W = R \cdot T \cdot \ln \frac{V_2}{V_1}$$

R . T . V

CONSTANT VOLUME: (GASP/VOLM)

$dv=0, W=0, Q=du, c=cv$

(18) Pressure change

$$P_2 = P_1 \frac{T_2}{T_1}$$

ΔP

(19) Temperature change

$$T_2 = T_1 \frac{P_2}{P_1}$$

ΔT

(20) Enthalpy change

$$dh = c_p (T_2 - T_1)$$

ΔH

(21) Entropy change

$$ds = c_v \cdot \ln \frac{T_2}{T_1}$$

ΔS

(22) Internal energy change

$$du = c_v (T_2 - T_1)$$

ΔU

(23) Heat

$$Q = c_v (T_2 - T_1)$$

Q

GAS PROPERTY CHANGE (IDEAL GAS)

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|---|----------------|
| <u>ISENTROPIC PROCESS: (GASP/ISENT)</u> | | |
| $ds=0, Q=0$ | | |
| (24) Pressure change (change in volume) | $P_2 = P_1 \left(\frac{V_1}{V_2} \right)^k$ | $\Delta P / V$ |
| (25) Pressure change (change in temperature) | $P_2 = P_1 \left(\frac{T_2}{T_1} \right)^{\frac{k}{k-1}}$ | $\Delta P / T$ |
| (26) Temperature change (change in volume) | $T_2 = T_1 \left(\frac{V_1}{V_2} \right)^{k-1}$ | $\Delta T / V$ |
| (27) Temperature change (change in pressure) | $T_2 = T_1 \left(\frac{P_2}{P_1} \right)^{\frac{k-1}{k}}$ | $\Delta T / P$ |
| (28) Volume change (change in pressure) | $V_2 = V_1 \left(\frac{P_1}{P_2} \right)^{\frac{1}{k}}$ | $\Delta V / P$ |
| (29) Volume change (change in temperature) | $V_2 = V_1 \left(\frac{T_1}{T_2} \right)^{\frac{1}{k-1}}$ | $\Delta V / T$ |
| (30) Enthalpy change | $dh = c_p (T_2 - T_1)$ | ΔH |
| (31) Internal energy change | $du = c_v (T_2 - T_1)$ | ΔU |
| <u>Work: (GASP/ISENT/WORK)</u> | | |
| <u>Closed System: (GASP/ISENT/WORK/CLOSE)</u> | | |
| (32) With P and V | $W = \frac{P_1 * V_1 - P_2 * V_2}{k-1}$ | $P \cdot V$ |
| <u>With CV and T: (GASP/ISENT/WORK/CLOSE/CV.T)</u> | | |
| (33) English System | $W = 778 * c_v (T_1 - T_2)$ | ENG |
| (34) English System | $W = c_v (T_1 - T_2)$ | SI |
| <u>Steady Flow System: (GASP/ISENT/WORK/FLOW)</u> | | |
| <u>With CP and T: (GASP/ISENT/WORK/FLOW/CP.T)</u> | | |
| (35) English System | $W = 778 * c_p * T_1 \left(1 - \left(\frac{P_2}{P_1} \right)^{\frac{k-1}{k}} \right)$ | ENG |
| (36) SI System | $W = c_p * T_1 \left(1 - \left(\frac{P_2}{P_1} \right)^{\frac{k-1}{k}} \right)$ | SI |

GAS PROPERTY CHANGE (IDEAL GAS)

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|--|----------------|
| <u>ISENTROPIC PROCESS: (GASP/ISENT)</u> | | |
| <u>Work: (GASP/ISENT/WORK)</u> | | |
| <u>Steady Flow System (continued): (GASP/ISENT/WORK/FLOW)</u> | | |
| (37) With P and V | $W = \frac{k}{k-1} (P_2 v_2 - P_1 v_1)$ | P . V |
| <u>Specific Heat Ratio: (GASP/ISENT/K)</u> | | |
| (38) With P and V | $k = \frac{\ln \frac{P_2}{P_1}}{\ln \frac{v_1}{v_2}}$ | P . V |
| (39) With P and T | $k = \frac{\ln (P_2/P_1)}{\ln (P_2/P_1) - \ln (T_2/T_1)}$ | P . T |
| <hr/> | | |
| <u>POLYTROPIC PROCESS: (GASP/POLYT)</u> | | |
| (40) Pressure change (change in volume) | $P_2 = P_1 \left(\frac{v_1}{v_2} \right)^n$ | $\Delta P / V$ |
| (41) Pressure change (change in temperature) | $P_2 = P_1 \left(\frac{T_2}{T_1} \right)^{\frac{n}{n-1}}$ | $\Delta P / T$ |
| (42) Temperature change (change in volume) | $T_2 = T_1 \left(\frac{v_1}{v_2} \right)^{n-1}$ | $\Delta T / V$ |
| (43) Temperature change (change in pressure) | $T_2 = T_1 \left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}}$ | $\Delta T / P$ |
| (44) Volume change (change in pressure) | $v_2 = v_1 \left(\frac{P_1}{P_2} \right)^{\frac{1}{n}}$ | $\Delta V / P$ |
| (45) Volume change (change in temperature) | $v_2 = v_1 \left(\frac{T_1}{T_2} \right)^{\frac{1}{n-1}}$ | $\Delta V / T$ |
| <u>Enthalpy change: (GASP/POLYT/ ΔH)</u> | | |
| (46) With CP and T | $dh = c_p (T_2 - T_1)$ | CP . T |
| <u>With P and V: (GASP/POLYT/ ΔH /P.V)</u> | | |
| (47) English System | $dh = \frac{n(P_2 * v_2 - P_1 * v_1)}{778(n-1)}$ | ENG |
| (48) SI System | $dh = \frac{n(P_2 * v_2 - P_1 * v_1)}{n-1}$ | SI |

GAS PROPERTY CHANGE (IDEAL GAS)

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|--|-------------|
| <u>POLYTROPIC PROCESS (continued): (GASP/POLYT)</u> | | |
| (49) Entropy change | $ds = \frac{c_v(n-k) \cdot \ln(T_2/T_1)}{n-1}$ | ΔS |
| (50) Internal energy change | $du = c_v(T_2 - T_1)$ | ΔU |
| (51) Heat | $Q = \frac{c_v(n-k)(T_2 - T_1)}{n-1}$ | Q |
| <u>Work: (GASP/POLYT/WORK)</u> | | |
| <u>Closed System: (GASP/POLYT/WORK/CLOSE)</u> | | |
| (52) With P and V | $W = \frac{P_1 \cdot v_1 - P_2 \cdot v_2}{n-1}$ | $P \cdot V$ |
| (53) With R and T | $W = \frac{R \cdot (T_1 - T_2)}{n-1}$ | $R \cdot T$ |
| <u>Steady Flow System: (GASP/POLYT/WORK/FLOW)</u> | | |
| <u>With H: (GASP/POLYT/WORK/FLOW/H)</u> | | |
| (54) English System | $W = 778 \cdot (h_1 - h_2)$ | ENG |
| (55) SI System | $W = (h_1 - h_2)$ | SI |
| (56) With P and V | $W = \frac{n}{n-1} (P_2 \cdot v_2 - P_1 \cdot v_1)$ | $P \cdot V$ |
| <u>Specific Heat Ratio: (GASP/POLYT/N)</u> | | |
| (57) With P and V | $n = \frac{\ln \frac{P_2}{P_1}}{\ln \frac{v_1}{v_2}}$ | $P \cdot V$ |
| (58) With P and T | $n = \frac{\ln(P_2/P_1)}{\ln(P_2/P_1) - \ln(T_2/T_1)}$ | $P \cdot T$ |

GAS PROPERTY CHANGE (IDEAL GAS)

THROTTLING, STEADY FLOW: (GASP/THROT)

$$dP < 0, dv > 0, dT = 0, dh = 0, du = 0, Q = W = 0$$

(59) Pressure change

$$P_2 = P_1 \frac{v_1}{v_2} \quad \Delta P$$

Entropy change: (GASP/THROT/ ΔS)

With R and P: (GASP/THROT/ ΔS /R.P)

(60) English System

$$ds = \frac{R}{778} * \ln \frac{P_1}{P_2} \quad \text{ENG}$$

(61) SI System

$$ds = R * \ln \frac{P_1}{P_2} \quad \text{SI}$$

With R and V: (GASP/THROT/ ΔS /R.V)

(62) English System

$$ds = \frac{R}{778} * \ln \frac{v_2}{v_1} \quad \text{ENG}$$

(63) SI System

$$ds = R * \ln \frac{v_2}{v_1} \quad \text{SI}$$

(64) Volume change

$$v_2 = v_1 \frac{P_1}{P_2} \quad \Delta V$$

GENERAL: IDEAL GAS, WORK, HP EQUATIONS:

GAS, IDEAL: (GASP/IDEAL)

(65) With the given mass

$$pV = mRT \quad \text{MASS}$$

(66) With the given mole

$$pV = nR'T \quad \text{MOLE}$$

WORK: (GASP/WORK)

(67) English System

$$W = 778 (dh + Q) + Z_1 - Z_2 + \left(\frac{v_1^2 - v_2^2}{2g} \right) \quad \text{ENG}$$

(68) SI System

$$W = dh + Q + (Z_1 - Z_2) * g + \left(\frac{v_1^2 - v_2^2}{2} \right) \quad \text{SI}$$

HORSEPOWER: (GASP/HP)

(69) English System

$$hp = \frac{M}{550} (778 (dh + Q) + Z_1 - Z_2 + \left(\frac{v_1^2 - v_2^2}{2g} \right)) \quad \text{ENG}$$

(70) SI System

$$hp = \frac{M}{745.7} (dh + Q + (Z_1 - Z_2) * g + \left(\frac{v_1^2 - v_2^2}{2} \right)) \quad \text{SI}$$

GAS PROPERTY CHANGE (IDEAL GAS)
VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT (ENG, SI)</u> |
|----------------------|---|
| <u>cp</u> | Specific heat, Constant Pressure; <u>BTU/lbm-oR, J/kg.K</u> (1 BTU/lbm-oR = 4186.8 J/kg.K). |
| <u>cv</u> | Specific Heat, Constant Volume; <u>BTU/lbm-oR, J/kg.K</u> (1 BTU/lbm-oR = 4186.8 J/kg.K). |
| <u>g</u> | Gravitational acceleration; <u>ft/s², m/s²</u> (1 ft/s ² = 0.3048 m/s ²). |
| <u>h</u> | Enthalpy; <u>BTU/lbm, J/kg</u> (1 BTU/lbm = 2326 J/kg, 1 BTU = 1055 J). |
| <u>k</u> | Ratio of Specific Heat; <u>None</u> . |
| <u>M</u> | Mass in flow; <u>lbm/s, kg/s</u> (1 lbm = 0.4536 kg). |
| <u>m</u> | Mass; <u>lbm, kg</u> (1 lbm = 0.4536 kg). |
| <u>n</u> | Polytropic Exponent; <u>None</u> , Number of moles; <u>pmole, kgmole</u> . |
| <u>p</u> | Pressure; <u>lb/ft² Pa</u> (1 lb/ft ² = 47.88 Pa). |
| <u>Q</u> | Heat; <u>BTU/lbm, J/kg</u> (1 BTU/lbm = 2326 J/kg, 1 BTU = 1055 J). |
| <u>R</u> | Specific Heat Constant; <u>ft-lbf/lbm-oR, J/kg.K</u> (1 ft-lbf/lbm-R = 5.3803 J/kg.K, 1 ft.lbf = 1.3558 J). |
| <u>R'</u> | Universal Gas Constant; <u>1545.3 ft-lbf/pmole-oR, 8314 J/kgmole.K</u> . |
| <u>s</u> | Entropy; <u>BTU/lbm-oR, J/kg.K</u> (1 BTU/lbm-oR = 4186.8 J/kg.K). |
| <u>T</u> | Temperature; <u>oR, K</u> . |
| <u>u</u> | Internal energy; <u>BTU/lbm, J/kg</u> (1 BTU/lbm = 2326 J/kg, 1 BTU = 1055 J). |
| <u>V</u> | Volume; <u>ft³, m³</u> (1 ft ³ = 0.0283 m ³). |
| <u>v</u> | Specific volume; <u>ft³/lbm, m³/kg</u> (1 ft ³ /lbm = 0.06243 m ³ /kg). |
| <u>vi</u> | Velocity at inlet; <u>ft/s, m/s</u> (1 ft/s = 0.3048 m/s). |
| <u>vo</u> | Velocity at outlet; <u>ft/s, m/s</u> (1 ft/s = 0.3048 m/s). |
| <u>W</u> | Work; <u>ft-lbf/lbm, J/kg</u> (1 ft-lb/lbm = 2.989 J/kg). |
| <u>z</u> | Elevation; <u>ft, m</u> (1 ft = 0.3048 m). |

MATHEMATICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|---|--------------|
| <u>AREA: (MATH/AREA)</u> | | |
| (01) Circle | $A = \pi * r^2$ | <i>CIRCL</i> |
| <u>Circular segment: (MATH/AREA/SEGM)</u> | | |
| (02) With the given central angle | $A = .5 * r^2 (\pi * \frac{\Omega}{180} - \sin \Omega)$ | <i>ANGL</i> |
| (03) With the given height | $A = .5 * r^2 (\frac{\pi \text{ACOS}(\frac{r-h}{r})}{90} - \sin(2 \text{ACOS}(\frac{r-h}{r})))$ | <i>HGHT</i> |
| (04) Circular sector | $A = \pi * \frac{\Omega}{360} * r^2$ | <i>SECTR</i> |
| (05) Ellipse | $A = \pi * a * b$ | <i>ELIPS</i> |
| (06) Ring section | $A = \pi (r_o^2 - r_i^2)$ | <i>RING</i> |

DETERMINANT: (MATH/DETER)

| | | | |
|-------------------|---|---|------------|
| (07) Second order | $\begin{vmatrix} a_1 & b_1 \\ a_2 & b_2 \end{vmatrix}$ | $DT2 = a_1 b_2 - b_1 a_2$ | <i>DT2</i> |
| (08) Third order | $\begin{vmatrix} a_1 & b_1 & c_1 \\ a_2 & b_2 & c_2 \\ a_3 & b_3 & c_3 \end{vmatrix}$ | $DT3 = a_1 b_2 c_3 + b_1 c_2 a_3 + c_1 a_2 b_3 - a_3 b_2 c_1 - b_3 c_2 a_1 - c_3 a_2 b_1$ | <i>DT3</i> |

HYDRAULIC RADIUS: (MATH/HYD.R)

| | | |
|---|--|--------------|
| (09) General | $HR = \frac{FA \text{ (Flow Area)}}{WP \text{ (Wet Perimeter)}}$ | <i>GENER</i> |
| (10) Pipe, with the given central angle | $HR = \frac{r (.5 * \pi * \Omega - 90 * \sin \Omega)}{\pi * \Omega}$ | <i>ANGL</i> |
| (11) Pipe, with the given height | $HR = .5 * r - \frac{90 (r-h) * \sin(\text{ACOS}(\frac{r-h}{r}))}{\pi * \text{ACOS}(\frac{r-h}{r})}$ | <i>HGHT</i> |

MATHEMATICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|---|--------------|
| (12) Interpolation | $A_n = \frac{A_1 - A_2}{B_1 - B_2} (B_n - B_1) + A_1$ | <i>INTRP</i> |

POLAR/RECTANGULAR COORDINATES: (MATH/PL-RC)

| | | |
|-------------------|--|---------------|
| (13) Angle | $\Omega = \text{ATAN}\left(\frac{Y}{X}\right)$ | <i>ANGL</i> |
| (14) Radius | $R = (x^2 + y^2)^{.5}$ | <i>RDIUS</i> |
| (15) x Coordinate | $x = R * \text{COS}\Omega$ | <i>X. COR</i> |
| (16) y Coordinate | $y = R * \text{SIN}\Omega$ | <i>Y. COR</i> |

| | | |
|-------------------------|--|------------|
| (17) Quadratic equation | $x = \frac{-b \pm (b^2 - 4ac)^{.5}}{2a}$ | <i>QAD</i> |
|-------------------------|--|------------|

| | | |
|-------------------------------------|--|------------|
| (18) Simultaneous (Linear) equation | $x = \frac{c_1 * b_2 - b_1 * c_2}{a_1 * b_2 - a_2 * b_1}, y = \frac{a_2 * c_1 - a_1 * c_2}{a_2 * b_1 - a_1 * b_2}$ | <i>SIM</i> |
|-------------------------------------|--|------------|

SURFACE: (MATH/SURF)

Cones, Circular: (MATH/SURF/CONE)

| | | |
|-------------------------------|--|-------------|
| (19) base included | $S = \pi * r (r^2 + h^2)^{.5} + \pi * r^2$ | <i>FULL</i> |
| (20) Cone, circular, w/o base | $S = \pi * r (r^2 + h^2)^{.5}$ | <i>FACE</i> |

Cylinder: (MATH/SURF/CYLIN)

| | | |
|------------------------------|------------------------------------|--------------|
| (21) Cylinder, ends included | $S = 2 * \pi * r * h + 2\pi * r^2$ | <i>FULL</i> |
| (22) Cylinder, w/o ends | $S = 2 * \pi * r * h$ | <i>FACE</i> |
| (23) Sphere | $S = 4 * \pi * r^2$ | <i>SPHER</i> |

MATHEMATICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

TRIANGLE LAW: (*MATH/ΔLAW*)

Law of Cosine: (*MATH/ΔLAW/COS*)

| | | |
|-----------------------|---|-------------|
| (24) Side of triangle | $a = (b^2 + c^2 - 2 * b * c * \cos A^\circ) \cdot ^5$ | <i>SIDE</i> |
|-----------------------|---|-------------|

| | | |
|------------------------|--|-------------|
| (25) Angle of triangle | $A^\circ = \text{ACOS} \left(\frac{b^2 + c^2 - a^2}{2 * b * c} \right)$ | <i>ANGL</i> |
|------------------------|--|-------------|

Law of Sine: (*MATH/ΔLAW/SIN*)

| | | |
|-----------------------|---|-------------|
| (26) Side of triangle | $a = \frac{b * \sin A^\circ}{\sin B^\circ}$ | <i>SIDE</i> |
|-----------------------|---|-------------|

| | | |
|------------------------|---|-------------|
| (27) Angle of triangle | $A^\circ = \text{ASIN} \left(\frac{a * \sin B^\circ}{b} \right)$ | <i>ANGL</i> |
|------------------------|---|-------------|

VOLUME: (*MATH/VOLM*)

| | | |
|----------------------------|-------------------------------|-------------|
| (28) Cone, right, circular | $V = \frac{\pi * r^2 * h}{3}$ | <i>CONE</i> |
|----------------------------|-------------------------------|-------------|

| | | |
|-------------------------|---------------------|--------------|
| (29) Cylinder, circular | $V = \pi * r^2 * h$ | <i>CYLIN</i> |
|-------------------------|---------------------|--------------|

| | | |
|-------------|-------------------------------|--------------|
| (30) Sphere | $V = \frac{4 * \pi * r^3}{3}$ | <i>SPHER</i> |
|-------------|-------------------------------|--------------|

MATHEMATICS, HP49G BUILT-IN FUNCTIONS

DIFFERENTIATION:

The following is the procedure to differentiate a symbolic expression where:

$f(x)$ = Expression to be differentiated and X = variable of differentiation. Please notice that no variable X is stored in the calculator. Otherwise you will get the numerical value of differential. To ensure:

Key in ' X ENTER TOOL PURGE

* Key in ' $f(x)$ ENTER

* Key in ' X ENTER

* Press ∂ You will get the symbolic answer.

Note 1. The answer may need to be simplified.

Note 2. If you store a value for X and then press NUM, while the differential still located in level 1 of the screen, you will get the numeric value of the differential.

Note 3. You may do the second differentiation:

While the first differential is still in level 1 of the screen key in:

' X ENTER ∂ . Ensure no variable X existed in the calculator.

INTEGRATION:

The following is the procedure to find the value of an integral with numeric limits, where:

$X1$ = lower limit, $X2$ = higher limit, $f(X)$ = Expression to be integrated, and X = variable of integration.

* Key in ' $\int(x_1, x_2, f(x), x)$ ENTER NUM

MATHEMATICS, HP49G BUILT-IN FUNCTIONS

LINEAR (SIMULTANEOUS) EQUATIONS:

The built-in MATRIX Application in HP49G is used to solve the linear equations. Following is the procedure for a three (3) variable linear equation. Same rule applies to others.

Equations format:

$$\begin{array}{l} | a_1x + b_1y + c_1z = d_1 \\ | a_2x + b_2y + c_2z = d_2 \\ | a_3x + b_3y + c_3z = d_3 \end{array}$$

Step 1. Write matrix for **d1, d2, d3**

Press \leftarrow MTRW, key in d1 SPC d2 SPC d3 ENTER ENTER

Step 2. Write matrix for **a1, b1, c1; a2, b2, c2; and a3, b3, c3:**

Press \leftarrow MTRW, F5 (If necessary to make the "GO" right arrow active)

Key in a1 SPC b1 SPC c1 ENTER \blacktriangledown \rightarrow \blacktriangleleft

Key in a2 SPC b2 SPC c2 ENTER

Key in a3 SPC b3 SPC c3 ENTER ENTER

Step 3. Press \div . You will get the answer values in the form of [x y z]

PLOTTING AND CALCULATING ROOTS AND AREAS:

The simplified plotting, root calculation, and area calculation which are performed by the PLOT Application in HP49G, are described below:

Calculator must be in ALG mode.

- * 1. Press \leftarrow Y= CLEAR ADD
- * 2. Key in the expression, f(X) ENTER.
- * 3. Press ERASE (to erase the previous plots.)
- * 4. Press DRAW (to plot the function.)

Press ON ON

MATHEMATICS, HP49G BUILT-IN FUNCTIONS

Calculating Roots:

You should be in the screen with the plotted function.

To find the roots:

- * 1. Press FCN ROOT. Read the first root
- * 2. Press **NXT** **✕** (to locate the cursor).
- * 3. Move the cursor to get close to the point next curve's intersection with **X** axis.
- * 4. Press ROOT. Read the second value.
- * 5. Follow the above steps (2 to 4) for the next root(s), if any.
- * 6. Press **ON ON** (to get back to the normal mode). The roots are on the screen too.

Calculating the Area:

To find the area bounded by the curve, **X** axis, lower limit (**X1**), and the higher limit (**X2**):

- * 1. Plot the expression as described above. But take the following exception for the better vision to the selected area:
- * 2. Press **↶** **Y=** CLEAR ADD
- * 3. Key in the expression, f(X) **ENTER ENTER**.
- * 4. Press **↶** **WIN**
- * 5. Key in value of **X1** **ENTER** and value of **X2**
- * 3. Press AUTO ERASE (to erase the previous plots) DRAW. The curve will appear.
- * 5. Press (x,y)
- * 4. Press **↷** **◀** . X coordinate should read the value of **X1**
- * 4. Press **✕** to set the lower limit.
- * 4. Press **↷** **▶** . X coordinate should read the value of **X2**
- * 6. Press **NXT** FCN AREA. Read the area.
- * 7. When finished, press **ON ON** (to get back to the normal mode.)

NOTE:

If you have to calculate the area between two (2) curves within the **X** limits, you have to calculate the area of each curve and **X** axis and subtract them.

VECTORS:

To perform the vector operations by HP49G, take the following points into consideration:

1. Calculator in **RPN** and = (= or exact answer is located at the top of the screen next to **R**).
2. The functions are built in calculator's Mathematic (**MTH**) section, **MTH/VECTR**.

MATHEMATICS, HP49G BUILT-IN FUNCTIONS

3. Vectors must be entered in the form of [a SPC b] for two (2) dimension and [a SPC b SPC c] for three (3) dimension vectors.

Unit Vector:

To find a Unit Vector, parallel to a given vector:

- * Press MTH VECTR
- * Key in the vector ENTER ENTER (to duplicate the vector on the screen.)
- * Press ABS (to find the magnitude.)
- * Press \div NUM.

Angle Between vectors:

To find the Vectors' angle:

- * Press MTH VECTR
- * Key in the first vector ENTER, key in the second vector ENTER
- * Press DOT (to calculate the dot product.)
- * Press ANS (to bring the two (2) vectors back to the screen.)
- * Press ABS type SWAP, press ENTER ABS (to calculate the magnitude of both vectors.)
- * Press \times (to multiply the magnitudes.)
- * Press \div (to divide the dot product by the products of magnitudes, This is the ACOS of the angle.)
- * Press NUM ACOS (to find the angle.)

Dot Product of vectors:

To find the Dot Product of vectors (V1.V2):

- * Press MTH VECTR
- * Key in the first vector ENTER, key in the second vector
- * Press DOT.

Cross Product of vectors:

To find the Cross Product of vectors (V1xV2):

- * Press MTH VECTR
- * Key in the first vector ENTER, key in the second vector
- * Press CROSS.

Absolute value (magnitude) of vectors:

To find the magnitude of vectors:

- * Press MTH VECTR
- * Key in the vector
- * Press ABS.

MATHEMATICS, HP49G BUILT-IN FUNCTIONS

Addition and subtraction of vectors:

To add or subtract the vectors:

- * Key in the first vector ENTER, key in the second vector ENTER, the third, etc.
- * Apply the arithmetic operation keys ($+$ or $-$) as needed.

MECHANICS OF MATERIALS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|---|-------------------|
| <u>COLUMNS: (MEMA/CLMN)</u> | | |
| <u>Load: (MEMA/CLMN/LOAD)</u> | | |
| (01) Euler load, with given E and I | $F_o = \frac{\pi^2 * E * I}{(C * L)^2}$ | <i>E . I</i> |
| (02) Euler load, with given E , A, and K | $F_o = E * A * \left(\frac{\pi * k}{C * L} \right)^2$ | <i>E . A . K</i> |
| <u>Stress: (MEMA/CLMN/STRES)</u> | | |
| (03) Euler stress, with given F and A | $\sigma_o = \frac{F_o}{A}$ | <i>F . A</i> |
| (04) Euler stress, with given E and K | $\sigma_o = \frac{\pi^2 * E}{\left(L * \frac{C}{k} \right)^2}$ | <i>E . K</i> |
| <hr/> | | |
| <u>SHAFT IN TORSION: (MEMA/SHAFT)</u> | | |
| <u>Angle of twist: (MEMA/SHAFT/ANGL)</u> | | |
| (05) General equation | $\Omega = \frac{180 * T * L}{\pi * G * J}$ | <i>GENER</i> |
| (06) Solid round | $\Omega = \frac{360 * T * L}{\pi^2 * G * r^4}$ | <i>SOLID</i> |
| (07) Hollow round | $\Omega = \frac{360 * T * L}{\pi^2 * G * (r_o^4 - r_i^4)}$ | <i>HOLLO</i> |
| (08) Energy stored | $U = \frac{T^2 * L}{2 * G * J}$ | <i>ENRG</i> |
| (09) Horsepower, English System | $hp = \frac{T * RPM}{63025}$ | <i>HP / ENG</i> |
| (09a) Horsepower, SI System | $hp = \frac{T * RPM}{7120.9}$ | <i>HP / SI</i> |
| <u>Shear Stress: (MEMA/SHAFT/SHEAR)</u> | | |
| (10) General | $\tau = \frac{T * r}{J}$ | <i>GENER</i> |
| (11) Solid round | $\tau = \frac{2 T}{\pi * r^3}$ | <i>SOLID</i> |
| (12) Hollow round | $\tau = \frac{2 * T * r_o}{\pi (r_o^4 - r_i^4)}$ | <i>HOLLO</i> |
| (13) Torque, English System | $T = \frac{63025 * hp}{RPM}$ | <i>TORQ / ENG</i> |
| (13a) Torque, SI System | $T = \frac{7120.9 * hp}{RPM}$ | <i>TORQ / SI</i> |

MECHANICS OF MATERIALS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|--|--------------|
| <u>STRESS: (MEMA/STRES)</u> | | |
| (14) Allowable stress | $\sigma_A = \frac{\sigma_u}{FS}$ | ALLOW |
| <u>Bending stress: (MEMA/STRES/BEND)</u> | | |
| (15) General | $\sigma_b = \frac{M*y}{I_c}$ | GENER |
| (16) Maximum | $\sigma_b = \frac{M*c}{I_c}$ | MAX |
| <u>Bending plus Normal stress: (MEMA/STRES/BND+)</u> | | |
| (17) Maximum | $\sigma = \frac{F}{A} + \frac{M*c}{I_c}$ | MAX |
| (18) Minimum | $\sigma = \frac{F}{A} - \frac{M*c}{I_c}$ | MIN |
| <u>Combined stress: (MEMA/STRES/COMB)</u> | | |
| <u>Normal stress: (MEMA/STRES/COMB/NORM)</u> | | |
| (19) Maximum | $\sigma_{max} = \frac{\sigma_x + \sigma_y}{2} + \sqrt{\left(\frac{\sigma_x - \sigma_y}{2}\right)^2 + \tau_{xy}^2}$ | MAX |
| (20) Minimum | $\sigma_{min} = \frac{\sigma_x + \sigma_y}{2} - \sqrt{\left(\frac{\sigma_x - \sigma_y}{2}\right)^2 + \tau_{xy}^2}$ | MIN |
| <u>Shear stress: (MEMA/STRES/COMB/SHEAR)</u> | | |
| (21) Maximum | $\tau_{max} = \sqrt{\left(\frac{\sigma_x - \sigma_y}{2}\right)^2 + \tau_{xy}^2}$ | MAX |
| (22) Minimum | $\tau_{min} = -\sqrt{\left(\frac{\sigma_x - \sigma_y}{2}\right)^2 + \tau_{xy}^2}$ | MIN |
| (23) Normal | $\sigma = E*\epsilon, \quad \sigma = F/A$ | NRM→ |
| <u>Shear stress: (MEMA/STRES/SHEAR)</u> | | |
| (24) General | $\tau = \frac{M_s * F_s}{I_c * b}$ | GENER |
| <u>Shear stress, Maximum: (MEMA/STRES/SHEAR/MAX)</u> | | |
| (25) In a circular section | $\tau_{max} = \frac{4 * F_s}{3 * \pi * r^2}$ | CIRC |
| (26) In a rectangular section | $\tau_{max} = \frac{3 * F_s}{2 * b * h}$ | RECT |

MECHANICS OF MATERIALS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|--|---------------------------------|
| <u>THERMAL DEFORMATION: (MEMA/DEFOR)</u> | | |
| (27) Linear expansion | $d_L = \alpha * L_o (t_2 - t_1)$ | EXPN |
| <u>Strain: (MEMA/DEFOR/STRN)</u> | | |
| (28) Axial, with elongation | $\epsilon = \frac{d_L}{L_o}$ | ΔL |
| (29) Axial, with change in temperature | $\epsilon = \alpha (t_2 - t_1), \epsilon = \sigma / E$ | AXL→ |
| (30) Lateral, with change in temperature | $\epsilon = \mu \alpha (t_2 - t_1), \epsilon = \mu \sigma / E$ | LAT→ |
| <u>Stress: (MEMA/DEFOR/STRES)</u> | | |
| (31) With the given E and ϵ | $\sigma = E * \epsilon$ | E. ϵ |
| (32) With change in temperature | $\sigma = E * \alpha (t_2 - t_1)$ | ΔT |
| (33) With elongation | $\sigma = dL * E / L$ | ΔL |
| <hr/> | | |
| <u>MISCELLANEOUS (MEMA/MSCL)</u> | | |
| (34) Elongation | $d_L = \frac{F * L}{A * E}$ | ELNG |
| (35) Energy stored in loaded member | $U = \frac{F^2 * L}{2A * E}$ | ENRG |
| <u>Polar moment of inertia (MEMA/MSCL/POLR)</u> | | |
| (36) Round hollow shaft | $J = \frac{\pi (r_o^4 - r_i^4)}{2}$ | HOLLO |
| (37) Round solid shaft | $J = \frac{\pi * r^4}{2}$ | SOLID |
| (38) Radius of Gyration | $k = \left(\frac{I}{A} \right)^{.5}$ | GYRA |
| (39) Shear/Elasticity Modulus | $G = \frac{E}{2(1 + \mu)}$ | MDUL |
| (40) Strain | $\epsilon = \frac{d_L}{L_o}$ | STRN |

MECHANICS OF MATERIALS

VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT (ENG, SI)</u> |
|----------------------|--|
| <u>A</u> | Area; <u>in²</u> , <u>m²</u> (1 in ² =0.000645 m ²). |
| <u>b</u> | Width of section; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>C</u> | End resistant coefficient; <u>None</u> . (Both end built in = 0.5, both end pinned = 1, one end built-in and one end pinned = 0.7, one end built-in and one end free = 2.) |
| <u>c</u> | Distance of extreme fiber from neutral axis; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>dL</u> | Elongation; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>E</u> | Modules of Elasticity; <u>psi</u> , <u>Pa</u> (1 psi=6894.8 Pa). |
| <u>F</u> | Force or load; <u>lbf</u> , <u>N</u> (1 lbf=4.4482 N). |
| <u>Fe</u> | Euler load; <u>lbf</u> , <u>N</u> (1 lbf=4.4482 N). |
| <u>FS</u> | Factor of Safety; <u>None</u> . |
| <u>Fs</u> | Shear force; <u>lbf</u> , <u>N</u> (1 lbf=4.4482 N). |
| <u>G</u> | Shear Modules; <u>psi</u> , <u>Pa</u> (1 psi=6894.8 Pa). |
| <u>h</u> | Height of beam section; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>hp</u> | Horsepower. |
| <u>I</u> | Moment of Inertia; <u>in⁴</u> , <u>m⁴</u> (1 in ⁴ =4.1623EE-7 m ⁴). |
| <u>Ic</u> | Centeroidal Moment of Inertia; <u>in⁴</u> , <u>m⁴</u> (1 in ⁴ =4.1623EE-7 m ⁴). |
| <u>J</u> | Polar Moment of Inertia; <u>in⁴</u> , <u>m⁴</u> (1 in ⁴ =4.1623EE-7 m ⁴). |
| <u>k</u> | Radius of Gyration; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>L</u> | Length; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>M</u> | Moment; <u>in-lbf</u> , <u>N.m</u> (1 in-lbf=0.1129848 N.m). |
| <u>Ms</u> | Statistical Moment; <u>in³</u> , <u>m³</u> (1 in ³ =1.6387EE-5 m ³). |
| <u>P</u> | Pressure; <u>psi</u> , <u>Pa</u> (1 psi=6894.8 Pa). |
| <u>r</u> | Radius; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>ri</u> | Inside radius; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>ro</u> | Outside radius; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>RPM</u> | Revolution Per Minute. |
| <u>T</u> | Torque; <u>in-lbf</u> , <u>N.m</u> (1 in-lbf=0.1129848 N.m). |
| <u>t</u> | Temperature; <u>oF</u> : Thickness; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>U</u> | Energy stored in a load member; <u>in-lbf</u> , <u>N.m</u> (1 in-lbf=0.1129848 N.m). |
| <u>y</u> | Distance of fiber from neutral axis; <u>in</u> , <u>m</u> (1 in=0.0254 m). |
| <u>α</u> | Coefficient of linear thermal deformation; <u>1/oF</u> , <u>1/oC</u> . |
| <u>ε</u> | Strain; <u>None</u> . |
| <u>μ</u> | Poisson's Ratio; <u>None</u> . |
| <u>Ω</u> | Angle of twist; <u>degree</u> . |
| <u>σ</u> | Stress; <u>psi</u> , <u>Pa</u> (1 psi=6894.8 Pa). |
| <u>σ_A</u> | Allowable Stress; <u>psi</u> , <u>Pa</u> (1 psi=6894.8 Pa). |
| <u>σ_b</u> | Bending Stress; <u>psi</u> , <u>Pa</u> (1 psi=6894.8 Pa). |
| <u>σ_e</u> | Euler Stress; <u>psi</u> , <u>Pa</u> (1 psi=6894.8 Pa). |
| <u>σ_u</u> | Ultimate/Yield Stress; <u>psi</u> , <u>Pa</u> (1 psi=6894.8 Pa). |
| <u>τ</u> | Shear Stress; <u>psi</u> , <u>Pa</u> (1 psi=6894.8 Pa). |

THERMODYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|---|---------------|
| <u>ATMOSPHERIC AIR: (THER/ATM.A)</u> | | |
| (01) Pressure, dry air | $P_{da} = P_{at} - P_{vv}$ | <i>P. DRY</i> |
| (02) Pressure, total | $P_{at} = P_{da} + P_{vv}$ | <i>P. TOT</i> |
| <u>Pressure, water vapor: (THER/ATM.A/P.WV)</u> | | |
| (03) With the given H_s and P | $P_{vv} = \frac{H_s * P_{at}}{.621 + H_s}$ | <i>HS. P</i> |
| (04) With the given RH and P | $P_{vv} = RH * P_{svv}$ | <i>RH. P</i> |
| <u>Relative Humidity: (THER/ATM.A/REL.H)</u> | | |
| (05) With the given P_{vv} | $RH = \frac{P_{vv}}{P_{svv}}$ | <i>PWV</i> |
| (06) With the given P_{da} | $RH = \frac{1.61 * H_s * P_{da}}{P_{svv}}$ | <i>PDA</i> |
| <u>Specific Humidity: (THER/ATM.A/SPC.H)</u> | | |
| (07) With the given P_{da} | $H_s = \frac{.621 * P_{vv}}{P_{da}}$ | <i>PDA</i> |
| (08) With the given P_{at} | $H_s = \frac{.621 * P_{vv}}{P_{at} - P_{vv}}$ | <i>PAT</i> |

COMPRESSORS: (THER/COMP)

Enthalpy: (THER/COMP/ENTH)

Compression Enthalpy: (THER/COMP/ENTH/COMP)

| | | |
|--------------------------------|--|--------------|
| (09) English System | $h = \frac{v_f (P_2 - P_1)}{778}$ | <i>ENG</i> |
| (10) SI System | $h = v_f (P_2 - P_1)$ | <i>SI</i> |
| (11) Actual discharge enthalpy | $h_{2A} = h_1 + \frac{h_{2I} - h_1}{\eta}$ | <i>ACTU</i> |
| (12) Ideal discharge enthalpy | $h_{2I} = \eta (h_{2A} - h_1) + h_1$ | <i>IDEAL</i> |
| (13) Efficiency | $\eta = \frac{h_{2I} - h_1}{h_{2A} - h_1}$ | <i>EFFI</i> |

THERMODYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|---|-------------|
| <u>EFFICIENCY: (THER/EFFI)</u> | | |
| <u>Carnot (THER/EFFI/CARN)</u> | | |
| (14) With the given heats | $\eta = \frac{Q_{in} - Q_{out}}{Q_{in}}$ | HEAT |
| (15) With the given temperatures | $\eta = \frac{T_b - T_l}{T_h}$ | TEMP |
| <u>Rankin (THER/EFFI/RANK)</u> | | |
| (16) With the given heats | $\eta = \frac{Q_{in} - Q_{out}}{Q_{in}}$ | HEAT |
| <u>With the given works: (THER/EFFI/RANK/WORK)</u> | | |
| (17) English System | $\eta = \frac{W_{turb} - W_{pump}}{778 Q_{in}}$ | ENG |
| (18) SI System | $\eta = \frac{W_{turb} - W_{pump}}{Q_{in}}$ | SI |

GAS: (THER/GAS)

Enthalpy: (THER/GAS/H)

With the given P and V: (THER/GAS/H/P.V)

| | | |
|---------------------|---------------------------------|------------|
| (19) English System | $h = u + \frac{P \cdot v}{778}$ | ENG |
|---------------------|---------------------------------|------------|

| | | |
|----------------|---------------------|-----------|
| (20) SI System | $h = u + p \cdot v$ | SI |
|----------------|---------------------|-----------|

With the given R and T: (THER/GAS/H/R.T)

| | | |
|---------------------|---------------------------------|------------|
| (21) English System | $h = u + \frac{R \cdot T}{778}$ | ENG |
|---------------------|---------------------------------|------------|

| | | |
|----------------|---------------------|-----------|
| (22) SI System | $h = u + R \cdot T$ | SI |
|----------------|---------------------|-----------|

Ratio of Specific Heat (THER/GAS/K)

| | | |
|-------------------------------|-----------------------|---------------|
| (23) With the given cp and cv | $k = \frac{C_p}{C_v}$ | CP, CV |
|-------------------------------|-----------------------|---------------|

With the given R and cv: (THER/GAS/K/R.CV)

| | | |
|---------------------|-----------------------------------|------------|
| (24) English System | $k = \frac{R}{778 \cdot C_v} + 1$ | ENG |
|---------------------|-----------------------------------|------------|

| | | |
|----------------|-------------------------|-----------|
| (25) SI System | $k = \frac{R}{C_v} + 1$ | SI |
|----------------|-------------------------|-----------|

THERMODYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

GAS (continued): (THER/GAS)

With the given R and cp: (THER/GAS/K/R.CP)

(26) English System

$$k = \frac{c_p}{c_p - \frac{R}{778}} \quad \text{ENG}$$

(27) SI System

$$k = \frac{c_p}{c_p - R} \quad \text{SI}$$

Specific Heat Constant: (THER/GAS/R)

With the given cp and cv: (THER/GAS/R/CP.CV)

(28) English System

$$R = 778 (c_p - c_v) \quad \text{ENG}$$

(29) SI System

$$R = c_p - c_v \quad \text{SI}$$

With the given Molecular Weight MW: (THER/GAS/R/MW)

(30) English System

$$R = \frac{1545.3}{MW} \quad \text{ENG}$$

(31) SI System

$$R = \frac{8314}{MW} \quad \text{SI}$$

Specific Heat, Constant Pressure: (THER/GAS/CP)

(32) With the given k and cv

$$c_p = k * c_v \quad \text{K. CV}$$

With the given k and R: (THER/GAS/CP/K.R)

(33) English System

$$c_p = \frac{k * R}{778 (k - 1)} \quad \text{ENG}$$

(34) SI System

$$c_p = \frac{k * R}{(k - 1)} \quad \text{SI}$$

Specific Heat, Constant Volume: (THER/GAS/CV)

(35) With the given k and cp

$$c_v = \frac{c_p}{k} \quad \text{K. CP}$$

With the given k and R: (THER/GAS/CV/K.R)

(36) English System

$$c_v = \frac{R}{778 (k - 1)} \quad \text{ENG}$$

(37) SI System

$$c_v = \frac{R}{k - 1} \quad \text{SI}$$

THERMODYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|-------------------------------------|----------------|-------------|
| <u>Gas, Ideal: (THER/GAS/IDEAL)</u> | | |
| (38) With the given mass | $pV = mRT$ | MASS |
| (39) With the given mole | $pV = nR'T$ | MOLE |
| (40) Gas, Real | $pV = mRTZ$ | REAL |

HEAT EXCHANGER: (THER/HTEXC)

Heat Flow: (THER/HTEXC/HTFLO)

| | | |
|--|--------------------------------------|---------------|
| (41) Multiple pass | $q = F_c \cdot U \cdot A \cdot LMTD$ | MULTI |
| <u>Single pass: (THER/HTEXC/HTFLO/SINGL)</u> | | |
| (42) With the given U and A | $q = U \cdot A \cdot LMTD$ | U . A |
| (43) With the given m and cp | $q = m \cdot c_p \cdot (t_2 - t_1)$ | M . CP |

Logarithmic Mean Temperature Difference: (THER/HTEXC/LMTD)

Counter flow: (THER/HTEXC/LMTD/COUNT)

| | | |
|---------------------|--|------------|
| (44) English System | $LMTD = \frac{(T_1 - t_o) - (T_o - t_1)}{\ln \frac{T_1 - t_o}{T_o - t_1}}$ | ENG |
|---------------------|--|------------|

| | | |
|----------------|--|-----------|
| (45) SI System | $LMTD = \frac{(T_1 - t_o) - (T_o - t_1)}{\ln \frac{T_1 - t_o}{T_o - t_1}}$ | SI |
|----------------|--|-----------|

Parallel flow: (THER/HTEXC/LMTD/PARAL)

| | | |
|---------------------|--|------------|
| (46) English System | $LMTD = \frac{(T_o - t_o) - (T_1 - t_1)}{\ln \frac{T_o - t_o}{T_1 - t_1}}$ | ENG |
|---------------------|--|------------|

| | | |
|----------------|--|-----------|
| (47) SI System | $LMTD = \frac{(T_o - t_o) - (T_1 - t_1)}{\ln \frac{T_o - t_o}{T_1 - t_1}}$ | SI |
|----------------|--|-----------|

THERMODYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|---|---|--------------|
| HEAT FLOW THROUGH: (THER/HTFLO) | | |
| (48) A film | $q = h \cdot A (t_1 - t_2)$ | FILM |
| <u>Pipe: (THER/HTFLO/PIPE)</u> | | |
| (49) Un-insulated w/o film | $q = \frac{2\pi \cdot K \cdot l \cdot (t_1 - t_2)}{\ln \frac{r_o}{r_i}}$ | BARE |
| (50) Insulated w/o film | $q = \frac{2\pi \cdot l \cdot (t_1 - t_2)}{\frac{\ln(\frac{r_o}{r_i})}{K_{pipe}} + \frac{\ln(\frac{r_{ins}}{r_o})}{K_{ins}}}$ | INSUL |
| <u>Slab: (THER/HTFLO/SLAB)</u> | | |
| <u>Single Section, no film: (THER/HTFLO/SLAB/SINGL)</u> | | |
| (51) With the given K and L | $q = \frac{K \cdot A (t_1 - t_2)}{L}$ | K.L |
| (52) With the given U | $q = U \cdot A (t_1 - t_2)$ | U |
| <u>Composite Sections: (THER/HTFLO/SLAB/COMP)</u> | | |
| (53) With up to 3 sections, no film, 3K | $q = \frac{A (t_1 - t_2)}{\frac{L_1}{K_1} + \frac{L_2}{K_2} + \frac{L_3}{K_3}}$ | 3K |
| (54) With 1 film and 1 section, 1h + 1K | $q = \frac{A (t_1 - t_2)}{\frac{L_1}{K_1} + \frac{1}{h_1}}$ | 1H1K |
| (55) With 2 film and 2 sections, 2h + 2K | $q = \frac{A (t_1 - t_2)}{\frac{1}{h_1} + \frac{L_1}{K_1} + \frac{L_2}{K_2} + \frac{1}{h_2}}$ | 2H2K |
| (56) With 2 film and 3 sections, 2h + 3K | $q = \frac{A (t_1 - t_2)}{\frac{1}{h_1} + \frac{L_1}{K_1} + \frac{L_2}{K_2} + \frac{L_3}{K_3} + \frac{1}{h_2}}$ | 2H3K |
| <u>Radiation: (THER/HTFLO/RADIA)</u> | | |
| (57) English System | $q_r = .1713 \text{EE-}8 \cdot A \cdot F_o \cdot F_a (T_1^4 - T_2^4)$ | ENG |
| (58) SI System | $q_r = 5.6724 \text{EE-}8 \cdot A \cdot F_o \cdot F_a (T_1^4 - T_2^4)$ | SI |

THERMODYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|---|-------------|
| <u>INTERNAL COMBUSTION ENGINES: (THER/NGIN)</u> | | |
| <u>Engine displacement: (THER/NGIN/DISP)</u> | | |
| (59) English System | $disp = \frac{\pi * BORE^2 * STRK * NCYL}{4}$ | ENG |
| (60) SI System | $disp = \frac{\pi * BORE^2 * STRK * NCYL}{4 * EE3}$ | SI |
| <u>Indicated horsepower: (THER/NGIN/HP)</u> | | |
| <u>With the given power strokes, NPST: (THER/NGIN/HP/NPST)</u> | | |
| (61) English System | $hp = \frac{\pi * P_m * BORE^2 * STRK * NPST}{1.584 * EE6}$ | ENG |
| (62) SI System | $hp = \frac{\pi * P_m * BORE^2 * STRK * NPST}{1.82496 * EE6}$ | SI |
| <u>With the given cycle strokes, NCST: (THER/NGIN/HP/NCST)</u> | | |
| (63) English System | $hp = \frac{\pi * P_m * BORE^2 * STRK * RPM * NCYL}{7.92 * EE5 * NCST}$ | ENG |
| (64) SI System | $hp = \frac{\pi * P_m * BORE^2 * STRK * RPM * NCYL}{9.1248 * EE5 * NCST}$ | SI |
| (65) Number of power strokes/min | $NPST = \frac{2 * RPM * NCYL}{NCST}$ | NPST |
| <u>Thermal efficiency: (THER/NGIN/ η_{TH})</u> | | |
| <u>With the given fuel consumption, FC: (THER/NGIN/ η_{TH} /FC)</u> | | |
| (66) English System | $\eta_{th} = \frac{2545 * hp}{FC * HV}$ | ENG |
| (67) SI System | $\eta_{th} = \frac{2684975 * hp}{FC * HV}$ | SI |
| <u>With the given fuel consumption, SFC: (THER/NGIN/ η_{TH} /SFC)</u> | | |
| (68) English System | $\eta_{th} = \frac{2545}{SFC * HV}$ | ENG |
| (69) SI System | $\eta_{th} = \frac{2684975}{SFC * HV}$ | SI |

THERMODYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

INTERNAL COMBUSTION ENGINES: (THER/NGIN)

Volumetric efficiency: (THER/NGIN/ η_v)

With the given engine displacement, DISP: (THER/NGIN/ η_v /DISP)

| | | |
|---------------------|---|------------|
| (70) English System | $\eta_v = \frac{3456 * I_{NAIR}}{RPM * disp}$ | ENG |
|---------------------|---|------------|

| | | |
|----------------|--|-----------|
| (71) SI System | $\eta_v = \frac{120 * I_{NAIR}}{RPM * disp}$ | SI |
|----------------|--|-----------|

With the given engine bore and stroke: (THER/NGIN/ η_v /BR.ST)

| | | |
|---------------------|--|------------|
| (72) English System | $\eta_v = \frac{13824 * I_{NAIR}}{\pi * RPM * BORE^2 * STRK * NCYL}$ | ENG |
|---------------------|--|------------|

| | | |
|----------------|---|-----------|
| (73) SI System | $\eta_v = \frac{4.8885 * I_{NAIR}}{\pi * RPM * BORE^2 * STRK * NCYL}$ | SI |
|----------------|---|-----------|

REFRIGERATION: (THER/REFRI)

Coefficient Of Performance: (THER/REFRI/COP)

| | | |
|--|----------------------------------|-------------|
| (74) With the given tons of refrigeration, tonR: | $COP = \frac{4.715 * ton_R}{hp}$ | TONR |
|--|----------------------------------|-------------|

| | | |
|---------------------------|---|-------------|
| (75) With the given heats | $COP = \frac{Q_{in}}{Q_{out} - Q_{in}}$ | HEAT |
|---------------------------|---|-------------|

| | | |
|----------------------------------|--|-------------|
| (76) With the given temperatures | $COP = \frac{T_{low}}{T_{high} - T_{low}}$ | TEMP |
|----------------------------------|--|-------------|

Energy Efficiency Ratio: (THER/REFRI/EER)

| | | |
|------------------------|--|-----------|
| (77) With the given hp | $EER = \frac{12000 * ton_R}{745.7 * hp}$ | HP |
|------------------------|--|-----------|

| | | |
|--------------------------|------------------------------------|-------------|
| (78) With the given watt | $EER = \frac{12000 * ton_R}{watt}$ | WATT |
|--------------------------|------------------------------------|-------------|

Horsepower: (THER/REFRI/HP)

| | | |
|-------------------------|----------------------------------|------------|
| (79) With the given COP | $hp = \frac{4.715 * ton_R}{COP}$ | COP |
|-------------------------|----------------------------------|------------|

| | | |
|-------------------------|----------------------------------|------------|
| (80) With the given EER | $hp = \frac{16.09 * ton_R}{EER}$ | EER |
|-------------------------|----------------------------------|------------|

THERMODYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--------------------|----------------|-------------|
|--------------------|----------------|-------------|

REFRIGERATION: (THER/REFRI)

Refrigerant rate: (THER/REFRI/RATE)

| | | |
|---------------------|---|------------|
| (81) English System | $M = \frac{10 * \text{ton}_R}{3 (h_2 - h_1)}$ | <i>ENG</i> |
|---------------------|---|------------|

| | | |
|----------------|---|-----------|
| (82) SI System | $M = \frac{3517.2 * \text{ton}_R}{h_2 - h_1}$ | <i>SI</i> |
|----------------|---|-----------|

STEAM: (THER/STIM)

| | | |
|------------------|------------------------|----------|
| (83) Enthalpy, h | $h = h_f + X * h_{fg}$ | <i>H</i> |
|------------------|------------------------|----------|

| | | |
|-----------------|------------------------|----------|
| (84) Entropy, s | $s = s_f + X * s_{fg}$ | <i>S</i> |
|-----------------|------------------------|----------|

Quality (THER/STIM/X)

| | | |
|-----------------------|------------------------------|----------|
| (85) With the given h | $X = \frac{h - h_f}{h_{fg}}$ | <i>H</i> |
|-----------------------|------------------------------|----------|

| | | |
|-----------------------|------------------------------|----------|
| (86) With the given s | $X = \frac{s - s_f}{s_{fg}}$ | <i>S</i> |
|-----------------------|------------------------------|----------|

| | | |
|-------------------------|------------------------|----------|
| (87) Specific volume, v | $v = v_f + X * v_{fg}$ | <i>V</i> |
|-------------------------|------------------------|----------|

Steam rate: (THER/STIM/RATE)

| | | |
|---------------------|----------------------------------|------------|
| (88) English System | $M = \frac{Q}{3600 (h_1 - h_2)}$ | <i>ENG</i> |
|---------------------|----------------------------------|------------|

| | | |
|----------------|-----------------------------|-----------|
| (89) SI System | $M = \frac{W}{(h_1 - h_2)}$ | <i>SI</i> |
|----------------|-----------------------------|-----------|

TURBINE: (THER/TURB)

Enthalpy at Discharge: (THER/TURB/ENTH)

| | | |
|--------------------------------|--------------------------------------|-------------|
| (90) Actual discharge enthalpy | $h_{2A} = h_1 - \eta (h_1 - h_{2I})$ | <i>ACTU</i> |
|--------------------------------|--------------------------------------|-------------|

| | | |
|-------------------------------|--|--------------|
| (91) Ideal discharge enthalpy | $h_{2I} = h_1 + \frac{h_{2A} - h_1}{\eta}$ | <i>IDEAL</i> |
|-------------------------------|--|--------------|

| | | |
|-----------------|--|-------------|
| (92) Efficiency | $\eta = \frac{h_1 - h_{2A}}{h_1 - h_{2I}}$ | <i>EFFI</i> |
|-----------------|--|-------------|

THERMODYNAMICS

| <u>DESCRIPTION</u> | <u>FORMULA</u> | <u>NAME</u> |
|--|--|-------------|
| <u>TURBINE: (THER/TURB)</u> | | |
| <u>Horsepower: (THER/TURB/HP)</u> | | |
| (93) English System | $hp = \frac{M \cdot \eta}{550} \left(778(h_1 - h_o) + \frac{v_1^2 - v_o^2}{2g} \right)$ | ENG |
| (94) SI System | $hp = \frac{M \cdot \eta}{745.7} \left(h_1 - h_o + \frac{v_1^2 - v_o^2}{2} \right)$ | SI |
| <u>Specific Steam Rate: (THER/TURB/RATE)</u> | | |
| (95) English System | $SSR = \frac{3413}{3600(h_1 - h_o)}$ | ENG |
| (96) SI System | $SSR = \frac{1000}{h_1 - h_o}$ | SI |

THERMODYNAMICS

VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT (ENG, SI)</u> |
|---------------|---|
| <u>A</u> | Surface area; <u>ft²</u> , <u>m²</u> (1 ft ² =0.0929 m ²). |
| <u>BORE</u> | Piston's bore; <u>in</u> , <u>cm</u> (1 in=2.54 cm). |
| <u>COP</u> | Coefficient Of Performance; <u>None</u> . |
| <u>cp</u> | Specific heat, Constant Pressure; <u>BTU/lbm-oR</u> , <u>J/kg.K</u> (1 BTU/lbm.oR=4186.8 J/kg.K). |
| <u>cv</u> | Specific Heat, Constant Volume; <u>BTU/lbm-oR</u> , <u>J/kg.K</u> (1 BTU/lbm.oR=4186.8 J/kg.K). |
| <u>disp</u> | Engine's displacement; <u>in³/cyc</u> , <u>L/cyc</u> (1 in ³ /cyc=0.01639 L/cyc). |
| <u>EER</u> | Energy Efficiency Ratio; <u>BTU/watt</u> . |
| <u>Fa</u> | Shape Factor; <u>None</u> . |
| <u>Fc</u> | Correction Factor; <u>None</u> . |
| <u>FC</u> | Fuel Consumption; <u>lbm</u> , <u>kg</u> (1 lbm=0.4536 kg). |
| <u>Fe</u> | Emissivity Factor; <u>None</u> . |
| <u>g</u> | Gravitational acceleration; <u>ft/s²</u> , <u>m/s²</u> (1 ft/s ² =0.3048 m/s ²). |
| <u>h</u> | Enthalpy; <u>BTU/lbm</u> , <u>J/kg</u> (1 BTU/lbm=2326 J/kg, 1 BTU=1055 J). |
| <u>h</u> | Film coefficient; <u>BTU/hr-ft².oR</u> , <u>W/m².K</u> (1 BTU/hr-ft ² .oR=5.68 W/m ² .K). |
| <u>hf</u> | Enthalpy of Saturated liquid; <u>BTU/lbm</u> , <u>J/kg</u> (1 BTU/lbm=2326 J/kg, 1 BTU=1055 J). |
| <u>hfg</u> | Enthalpy of vaporization; <u>BTU/lbm</u> , <u>J/kg</u> (1 BTU/lbm=2326 J/kg, 1 BTU=1055 J). |
| <u>hg</u> | Enthalpy of Saturated vapor; <u>BTU/lbm</u> , <u>J/kg</u> (1 BTU/lbm=2326 J/kg, 1 BTU=1055 J). |
| <u>hp</u> | Horsepower. |
| <u>Hs</u> | Specific Humidity; <u>None</u> ; <u>lbw/lbda</u> , <u>kgw/kgda</u> (1 lbm=0.4536 kg). |
| <u>HV</u> | Heating Value; <u>BTU/lbm</u> , <u>J/kg</u> (1 BTU/lbm=2326 J/kg, 1 BTU=1055 J). |
| <u>h2A</u> | Discharge Actual Enthalpy; <u>BTU/lbm</u> , <u>J/kg</u> (1 BTU/lbm=2326 J/kg, 1 BTU=1055 J). |
| <u>h2I</u> | Discharge Ideal Enthalpy; <u>BTU/lbm</u> , <u>J/kg</u> (1 BTU/lbm=2326 J/kg, 1 BTU=1055 J). |
| <u>INAIR</u> | Intake air quantity; <u>cfm</u> , <u>L/s</u> (1 cfm=0.47195 L/s). |
| <u>K</u> | Thermal Conductivity; <u>BTU/hr-ft-oR</u> , <u>W/m.K</u> (1 BTU/hr-ft-oR=1.731 W/m.K). |
| <u>k</u> | Ratio of Specific Heat; <u>None</u> . |
| <u>L</u> | Thickness; <u>ft</u> , <u>m</u> (1 ft=0.3048 m). |
| <u>l</u> | Length; <u>ft</u> , <u>m</u> (1 ft=0.3048 m). |
| <u>LMTD</u> | Logarithmic Mean Temperature Difference; <u>oF</u> , <u>oC</u> . |
| <u>M</u> | Mass in flow; <u>lbm/s</u> , <u>kg/s</u> (1 lbm=0.4536 kg). |
| <u>MW</u> | Molecular Weight. |
| <u>NCST</u> | Number of strokes per each cycle; <u>stroke/cycle</u> . |
| <u>NCYL</u> | Number of Cylinders; <u>None</u> . |
| <u>NPST</u> | Number of engine's power strokes per minute; <u>stroke/minute</u> . |
| <u>m</u> | Mass; <u>lbm</u> , <u>kg</u> (1 lbm=0.4536 kg). |
| <u>n</u> | Polytropic Exponent; <u>None</u> , Number of moles; <u>pmole</u> , <u>kgmole</u> . |
| <u>p</u> | Pressure; <u>lbf/ft²</u> , <u>Pa</u> (1 lbf/ft ² =47.88 Pa). |
| <u>Pat</u> | Atmospheric Pressure; <u>psi</u> , <u>Pa</u> (1 psi=6894.76 Pa). |
| <u>Pda</u> | Dry Air Partial Pressure; <u>psi</u> , <u>Pa</u> (1 psi=6894.76 Pa). |

THERMODYNAMICS

VARIABLES IDENTIFICATION

| <u>SYMBOL</u> | <u>DESCRIPTION; UNIT (ENG, SI)</u> |
|------------------------|---|
| <u>P_m</u> | Engine's Mean Effective Pressure; <u>psi</u> , <u>kg/cm²</u> (1 psi=0.07031 kg/cm ²). |
| <u>P_{swv}</u> | Saturated Water Vapor Pressure; <u>psi</u> , <u>Pa</u> (1 psi=6894.76 Pa). |
| <u>P_{wv}</u> | Water Vapor Pressure; <u>psi</u> (1 psi=6894.76 Pa). |
| <u>Q</u> | Heat/unit of weight; <u>BTU/lbm</u> , <u>J/kg</u> (1 BTU/lbm=2326 J/kg, 1 BTU=1055 J). |
| <u>q</u> | Heat flow quantity; <u>BTU/hr</u> , <u>W</u> (1 BTU/hr=0.2931 W=0.252 kcal/hr). |
| <u>q_r</u> | Radiation Heat flow; <u>BTU/hr</u> , <u>W</u> (1 BTU/hr=0.2931 W=0.252 kcal/hr). |
| <u>R</u> | Specific Heat Constant; <u>ft-lbf/lbm-oR</u> , <u>J/kg.K</u> (1 ft-lbf/lbm.oR=5.3803 J/kg.K, 1 ft.lbf=1.3558 J). |
| <u>R'</u> | Universal Gas Constant; <u>1545.3 ft-lbf/pmole-oR</u> , <u>8314 J/kgmole.K</u> . |
| <u>r</u> | Radius; <u>ft</u> , <u>m</u> subscript i = inside, o = outside (1 ft=0.3048 m). |
| <u>RH</u> | Relative Humidity; <u>decimal</u> . |
| <u>RPM</u> | Revolutions Per Minute. |
| <u>s</u> | Entropy; <u>BTU/lbm-oR</u> , <u>J/kg.K</u> (1 BTU/lbm-oR=4186.8 J/kg.K). |
| <u>sf</u> | Entropy of Saturated Liquid; <u>BTU/lbm-oR</u> , <u>J/kg.K</u> (1 BTU/lbm-oR=4186.8 J/kg.K). |
| <u>SFC</u> | Specific Fuel Consumption; <u>lbm/hp</u> , <u>kg/hp</u> (1 lbm=0.4536 k). |
| <u>sfg</u> | Entropy of vaporization; <u>BTU/lbm-oR</u> , <u>J/kg.K</u> (1 BTU/lbm-oR=4186.8 J/kg.K). |
| <u>sg</u> | Entropy of Saturated Vapor; <u>BTU/lbm-oR</u> , <u>J/kg.K</u> (1 BTU/lbm-R=4186.8 J/kg.K). |
| <u>SSR</u> | Specific Steam Rate; <u>lbm/kw</u> , <u>kg/kw</u> (1 lbm=0.4536 kg). |
| <u>STRK</u> | Piston's stroke; <u>in</u> , <u>cm</u> (1 in=2.54 cm). |
| <u>T</u> | Temperature; <u>oR</u> , <u>K</u> . |
| <u>T_i</u> | Hot fluid inlet temperature; <u>oF</u> , <u>oC</u> . |
| <u>t_i</u> | Cold fluid inlet temperature; <u>oF</u> , <u>oC</u> . |
| <u>T_o</u> | Hot fluid outlet temperature; <u>oF</u> , <u>oC</u> . |
| <u>t_o</u> | Cold fluid inlet temperature; <u>oF</u> , <u>oC</u> . |
| <u>tonR</u> | Ton of refrigeration; <u>12,000 BTU/hr</u> , <u>3517 W</u> , <u>3024 kcal/hr</u> . |
| <u>U</u> | Overall coefficient of heat transfer; <u>BTU/hr-sf-oR</u> , <u>W/m².K</u> (1 BTU/hr-ft ² -oR=5.68 W/m ² .K). |
| <u>u</u> | Internal energy; <u>BTU/lbm</u> , <u>J/kg</u> (1 BTU/lbm=2326 J/kg, 1 BTU=1055 J). |
| <u>V</u> | Volume; <u>ft³</u> , <u>m³</u> (1 ft ³ =0.02832 m ³). |
| <u>v</u> | Specific volume; <u>ft³/lbm</u> , <u>m³/kg</u> (1 ft ³ /lbm=0.06243 m ³ /kg). |
| <u>vf</u> | Specific volume of saturated liquid; <u>ft³/lbm</u> , <u>m³/kg</u> (1 ft ³ /lbm=0.06243 m ³ /kg). |
| <u>vfg</u> | Specific volume of vaporization; <u>ft³/lbm</u> , <u>m³/kg</u> (1 ft ³ /lbm=0.06243 m ³ /kg). |
| <u>vg</u> | Specific volume of saturated vapor; <u>ft³/lbm</u> , <u>m³/kg</u> (1 ft ³ /lbm=0.06243 m ³ /kg). |
| <u>v_i</u> | Velocity at inlet; <u>ft/s</u> , <u>m/s</u> (1 ft/s=0.3048 m/s). |
| <u>v_o</u> | Velocity at outlet; <u>ft/s</u> , <u>m/s</u> (1 ft/s=0.3048 m/s). |
| <u>W</u> | Work; <u>ft-lbf/lbm</u> , <u>J/kg</u> (1 ft-lbf/lbm=2.9891 J/kg). |
| <u>X</u> | Quality of steam; <u>decimal</u> . |
| <u>Z</u> | Compressibility Factor; <u>None</u> . |
| <u>η</u> | Efficiency; <u>decimal</u> . |
| <u>ρ</u> | Density; <u>lbm/ft³</u> , <u>kg/m³</u> (1 lbm/ft ³ =16.0185 kg/m ³). |

QUICK REFERENCE TO NCEES FE REFERENCE HANDBOOK

This part is prepared to summarize and highlight the more common, useful, and calculator accepted equations in NCEES FE Reference Handbook (January 1996 issue). Subject equations are programmed in ROM card.

By learning the overall concept, the user may retrieve the selected equation and solve it for an unknown variable in a faster and more accurate way without even any need to refer to this part of the manual.

Read the following notes and memorize the naming procedure for an easy access to stored equations:

1. Acquaint yourself with the subjects, equations, and the nomenclature of variables and their units in NCEES FE Reference Handbook. Ensure to use the proper unit to get the proper answer.
2. Following are the general rules for naming and retrieving the equations, except for Chemical, Civil, and Mechanical Engineering Sections, which are named by the subjects:
 - a. The main directories are representing the following sections in NCEES FE Reference Handbook:

| | |
|--|-------|
| <u>D</u> YNAMICS | DY |
| <u>E</u> LECTRICITY | EL |
| <u>E</u> NGINEERING <u>E</u> CONOMICS | EE |
| <u>F</u> LUID <u>M</u> ECHANICS | FM |
| <u>H</u> EAT <u>T</u> RANSFER | HT |
| <u>M</u> ATHEMATICS | MA |
| <u>M</u> ECHANICS OF <u>M</u> ATERIALS | MM |
| <u>T</u> HERMODYNAMICS | TH |
| | |
| <u>C</u> HEMICAL ENGINEERING | CHEM |
| <u>C</u> IVIL ENGINEERING | CIVIL |
| <u>M</u> ECHANICAL ENGINEERING | MECH |

- b. The subdirectories are representing the main subjects covered in the Handbook.
 - c. The NAME of the equation which will appear on the screen menu, generally, is either the variable's (at the left side of the equation) symbol or other sub-directories recognizable abbreviation.

DYNAMICS

DIRECTORY (*DY*)

| TO FIND | SUB DIR. | SYMB | NAME |
|--|------------|--------------|-------------------------------|
| <u>Circular motion:</u> | | | |
| (01) Tangential velocity | CIRCU | vt | VT |
| (02) Tangential acceleration | | at | AT |
| (03) Normal acceleration (2 equations) | | an | AN→ |
| <u>Linear motion:</u> | | | |
| (04) Distance | LINER | s | S |
| (05) Velocity | | v | V |
| (06) Velocity | | v | V² |
| <u>Projectile:</u> | | | |
| (07) Horizontal velocity | PROJ | vx | VX |
| (08) Vertical velocity (2 equations) | | vy | VY→ |
| (09) Horizontal distance (2 equations) | | x | X→ |
| (10) Vertical distance (2 equations) | | y | Y→ |
| (11) Weight | -- | W | WGHT |
| (12) Newton's 2nd law (2 equations) | -- | ΣF | ΣF→ |
| <u>Energy:</u> | | | |
| (13) Kinetic Energy | ENRG | KE | KE |
| (14) Kinetic Energy Change | | any | ΔKE |
| (15) Potential Energy | ENRG/SPRIN | PE | PE |
| (16) Spring/Potential Energy Stored | | PE | PE |
| (17) Spring/Change in Potential Energy | | any | ΔPE |
| (18) Centrifugal Force (2 equations) | -- | Fc | FC→ |
| (19) Tangent of Banking angle | -- | tan θ | TANθ |

ELECTRICITY

DIRECTORY (*EL*)

| TO FIND | SUB DIR. | SYMB | NAME |
|---|----------|------------------------------------|--|
| <p><u>Resistivity and Resistors:</u></p> <p>(01) Resistance</p> <p>(02) Resistivity, change in temperature</p> <p>(03) Resistance, change in temperature</p> <p>(04) Resistance (total), 3 in series</p> <p>(05) Resistance (total), 3 in parallel</p> <p>(06) Resistance (total), 2 in parallel</p> | RESIS | R ρ R RT RT RT | GENER $\rho \cdot \Delta T$ $R \cdot \Delta T$ SERI PAR3 PAR2 |
| <p><u>Power in Resistive element</u></p> <p>(07) With V and I</p> <p>(08) With V and R</p> <p>(09) With I and R</p> | POWR | P P P | V.I V.R I.R |
| <p><u>Capacitors in series and parallel:</u></p> <p>(10) Capacitance, 3 in parallel</p> <p>(11) Capacitance, 2 in series</p> <p>(12) Capacitance, 3 in series</p> | CAPAC | Ceq Ceq Ceq | PARA SER2 SER3 |
| <p><u>Inductors in series and parallel:</u></p> <p>(13) Inductance, 2 in parallel</p> <p>(14) Inductance, 3 in parallel</p> <p>(15) Inductance, 3 in series</p> | INDUC | Leq Leq Leq | PAR2 PAR3 SERI |

ELECTRICITY

DIRECTORY (*EL*)

| TO FIND | SUB DIR. | SYMB | NAME |
|--|----------|------------------------------------|---|
| <p><u>RC Transients:</u></p> <p>(16) Voltage across capacitor</p> <p>(17) Current</p> <p>(18) Voltage across resistor (2 equations)</p> | TRNSI/RC | Vct it VRt | VCT IT <i>VRT→</i> |
| <p><u>RL Transients:</u></p> <p>(19) Current</p> <p>(20) Voltage across resistor</p> <p>(21) Voltage across inductor</p> | TRNSI/RL | it VRt VLt | IT <i>VRT→</i> <i>VLt→</i> |
| <p><u>Amplifiers:</u></p> <p>(22) Output voltage</p> | -- | vo | AMPLI |
| <p><u>Reactance:</u></p> <p>(23) Capacitive reactance (2 equations)</p> <p>(24) Inductive reactance (2 equations)</p> | REAC | Xc XL | <i>XC→</i> <i>XL→</i> |
| <p><u>Resonance:</u></p> <p>(25) Radiant resonance frequency (2 equations)</p> <p>(26) Series Resonance</p> <p>(27) Quality Factor, Series (2 equations)</p> <p>(28) Quality Factor, Parallel (2 equations)</p> | RESO | ω_o ω_o Q Q | <i>ω_o→</i> <i>$\omega_o L$</i> <i>QS→</i> <i>QP→</i> |

ENGINEERING ECONOMICS

DIRECTORY (EE)

| TO FIND | SUB DIR. | SYMB | NAME |
|---|----------|------|--------------|
| <u>Discount Factor, Discrete Compound:</u> | | | |
| (01) F/P Factor | FCTR | F | F/P |
| (02) P/F Factor | | P | P/F |
| (03) A/F Factor | | A | A/F |
| (04) A/P Factor | | A | A/P |
| (05) F/A Factor | | F | F/A |
| (06) P/A Factor | | P | P/A |
| (07) P/G Factor | | P | P/G |
| (08) F/G Factor | | F | F/G |
| (09) A/G Factor | | A | A/G |
| (10) Non-Annual Compounding | -- | ie | COMP |
| <u>Discount Factor, Continuous Compound:</u> | | | |
| (11) Continuous Compounding F/P | CONTI | F | F/P |
| (12) Continuous Compounding P/F | | P | P/F |
| (13) Continuous Compounding A/F | | A | A/F |
| (14) Continuous Compounding F/A | | F | F/A |
| (15) Continuous Compounding A/P | | A | A/P |
| (16) Continuous Compounding P/A | | P | P/A |
| <u>Depreciation:</u> | | | |
| (17) Depreciation, Straight Line | -- | Dj | DEPRI |
| <u>Inflation:</u> | | | |
| (18) Combined interest and inflation rate | -- | d | INFLA |

FLUID MECHANICS
DIRECTORY (FM)

| TO FIND | SUB DIR. | SYMB | NAME |
|--|------------|----------|--------------|
| <u>Surface Tension:</u> | | | |
| (01) General | CAPIL/TENS | σ | GENE |
| (02) In bulb surrounded by air | | σ | AIR |
| (03) In a droplet or bubble in liquid | | σ | LIQID |
| (04) Capillary rise | CAPIL | h | RISE |
| <u>Pressure Field in a Static Liquid:</u> | | | |
| (05) Simple manometer equation | PRESS | P_o | PO |
| (06) Atmospheric pressure (2 equations) | | Patm | PA-2 |
| <u>Forces on submerged Surfaces:</u> | | | |
| (07) Pressure on submerged surface | FORCE | p | P |
| (08) y coord. of Center of Pressure | | y | Y1 |
| (09) z coord. of Center of Pressure | | z | Z1 |
| (10) y coord. of Center of Pressure | | y | Y2 |
| (11) z coord. of Center of Pressure | | z | Z2 |
| (12) Force on the plate | | F | F |
| (13) Mass flow rate (2 equations) | MASS | m | M-2 |
| (14) Bernoulli equation, no friction | BERN | any | NO.HF |
| (15) Bernoulli equation, + hf | | any | W.HF |
| (16) Bernoulli equation, + hf | | any | HF+ |

FLUID MECHANICS

DIRECTORY (FM)

| TO FIND | SUB DIR. | SYMB | NAME |
|---|-------------|--------|--------------------------|
| <u>Fluid flow:</u> | | | |
| (17) Velocity distribution for laminar flow | FLOW | v | V |
| (18) Shear stress distribution | | τ | τ |
| (19) Drag force | | FD | FD |
| (20) Drag coefficient (2 equations) | | CD | CD |
| <u>Reynolds Number:</u> | | | |
| (21) Newtonian fluid | REYN | Re | RE |
| (22) Power law fluid | | Re' | RE' |
| (23) Friction head (Darcy equation) | FRIC.H | hf | DARCY |
| (24) Minor loss, with the given C | FRIC.H/MINO | hf | C |
| (25) Minor loss, with C = .04 | | hf | C = .04 |
| (26) Pump power equation | - | W | pump |
| <u>Jet Propulsion:</u> | | | |
| (27) Flow quantity | JET | Q | Q |
| (28) Velocity | | V2 | V2 |
| <u>Deflection Blades:</u> | | | |
| <u>Fixed blades:</u> | | | |
| (29) x component | BLADE | Fx | FX |
| (30) y component | | Fy | FY |

FLUID MECHANICS

DIRECTORY (FM)

| TO FIND | SUB DIR. | SYMB | NAME |
|---|---------------|------------------|--|
| <u>Deflection Blades:</u> | | | |
| <u>Moving blades:</u> | | | |
| (31) x component (2 equations) | BLADE | F _x | <i>F_X</i> |
| (32) y component (2 equations) | | F _y | <i>F_Y</i> |
| <u>Impulse Turbine:</u> | | | |
| (33) Power of turbine | TURB | W | W |
| (34) Maximum power of turbine | | W _{max} | WMX |
| <u>Open Channel Flow:</u> | | | |
| (35) Manning's equations English System | CHAN/MANI | V | ENG |
| (36) Manning's equations SI System | | V | SI |
| (37) Hazen-Williams equation English System | CHAN/HAZN | V | ENG |
| (38) Hazen-Williams equation SI System | | V | SI |
| (39) Speed of sound | SOUND | c | C |
| (40) Velocity, Pitot Tube (2 equations) | <i>PITO</i> → | V | <i>V</i> -2 |
| (41) Venturi meter, Flow quantity | - | Q | VENT |
| <u>Orifice:</u> | | | |
| (42) Flow quantity | ORIF | Q | Q |
| (43) Coefficient of orifice | | C | C |
| (44) Submerged flow quantity (2 equations) | | Q | SUB → |
| (45) Free discharge flow | | Q | FREE |

HEAT TRANSFER

DIRECTORY (HT)

| TO FIND | SUB DIR. | NAME |
|--|-------------------|----------------|
| <p><u>RADIATION:</u> (15) Radiation emitted by a body</p> | RADIA | Q |
| <p><u>Radiation heat transfer between two bodies:</u> (16) Small to a large body (17) Two (2) black bodies</p> | RADIA/Q12 | SMAL BLAK |
| <p><u>HEAT EXCHANGERS:</u></p> <p><u>Shell and Tube:</u> (18) Overall heat transfer coefficient</p> | HTEX HTEX/SHEL | U |
| <p><u>Log Mean Temperature Difference:</u> (19) Counter current flow in tubular (20) Parallel flow in tubular</p> | HTEX/LMTD | CONTR PARAL |
| <p>(21) Heat Transfer/Section Area equation</p> | HTEX | Q/A |
| <p><u>Tubular Heat Exchanger:</u> (22) Rate of Heat Transfer</p> | HTEX/TUBUL | Q |

HEAT TRANSFER

DIRECTORY (*HT*)

| TO FIND | SUB DIR. | NAME |
|---|--|--|
| <p><u>HEAT EXCHANGERS:</u></p> <p><u>Tubular Heat Exchanger:</u></p> <p><u>Nusselt number:</u></p> <p>(23) Laminar flow</p> <p>(24) Turbulent flow (2 equations)</p> <p><u>Liquid Metals:</u></p> <p>(25) Constant heat flux</p> <p>(26) Constant wall temperature</p> <p>(27) Condensation of pure vapor</p> | <p>HTEX</p> <p>HTEX/TUBUL</p> <p>HTEX/TUBUL/NU</p> <p>HTEX/TUBUL</p> <p>/LIQID</p> <p>HTEX/TUBUL</p> | <p>LAMI</p> <p>TUR→</p> <p>HEAT</p> <p>TEMP</p> <p>VAPR</p> |
| <p><u>HEAT TRANSFER TO/FROM</u></p> <p><u>IMMERSED BODY:</u></p> <p><u>Nusselt Number:</u></p> <p><u>Flow parallel to constant temp. flat plate:</u></p> <p>(28) For $Re < 10^5$</p> <p>(29) For $Re > 10^5$</p> <p>(30) Of a constant temperature of cylinder</p> <p>(31) Of a constant temperature of sphere</p> | <p>IMERS</p> <p>IMERS/NU</p> <p>IMERS/NU/PLATE</p> <p>IMERS/NU</p> | <p>RE < .1M</p> <p>RE > .1M</p> <p>CYLN</p> <p>SPHER</p> |

HEAT TRANSFER

DIRECTORY (*HT*)

| TO FIND | SUB DIR. | NAME |
|---|--|---|
| <p><u>CONDUCTIVE HEAT TRANSFER:</u></p> <p><u>Steady Conduction With Internal Energy</u></p> <p><u>Generation:</u></p> <p><u>Plane wall:</u></p> <p>(32) Intermediate temperature at point x</p> <p><u>Long Circular Cylinder:</u></p> <p>(33) Temperature</p> <p>(34) Heat transfer per unit length</p> <p><u>Transient Conduction, Lump Capacitance</u></p> <p><u>Method:</u></p> <p>(35) Heat transfer</p> <p>(36) Temperature variation</p> <p>(37) Total temperature transferred up to time t</p> <p>(38) Biot number</p> | <p>COND'</p> <p>COND'/ENRG</p> <p>COND'/ENRG</p> <p>/WALL</p> <p>COND'/ENRG</p> <p>/CYLIN</p> <p>COND'/TRNSI</p> | <p>TX</p> <p>T</p> <p>Q</p> <p>Q</p> <p>T</p> <p>QTTL</p> <p>BI</p> |
| <p><u>NATURAL (FREE) CONVECTION:</u></p> <p><u>Vertical flat plate/cylinder:</u></p> <p>(39) Heat transfer coefficient</p> <p>(40) Raleigh Number</p> <p><u>Long Horizontal Cylinder and large body:</u></p> <p>(41) Heat transfer coefficient</p> <p>(42) Raleigh Number</p> | <p>CONV'</p> <p>CONV'/VERTI</p> <p>CONV'/HORIZ</p> | <p>H</p> <p>RAL</p> <p>H</p> <p>RAD</p> |

HEAT TRANSFER

DIRECTORY (*HT*)

| TO FIND | SUB DIR. | NAME |
|--|----------|--|
| <p><u>RADIATION:</u></p> <p>(43) Two-body problem</p> <p>(44) Radiation Shields</p> <p>(45) Reradiating surface</p> | RADI' | <p>2BODY</p> <p>SHILD</p> <p>SURF</p> |

MATHEMATICS

DIRECTORY (MA)

| TO FIND | SUB DIR. | SYMB | NAME |
|---|---------------|--------------------------|---|
| <u>Straight Line:</u> (01) Slope between two (2) points (02) Angle between two (2) lines (03) Distance between two (2) points | LINE | m α d | SLOP ANGL DIST |
| <u>Quadratic Equations:</u> (04) Root 1, x_1 (05) Root 2, x_2 | QUAD | x_1 x_2 | X1 X2 |
| <u>Conic Sections:</u> (06) Parabola (07) Ellipse, equation and eccentricity (2 equ.) (08) Hyperbola, equation and eccentricity (2 equ.) (09) Circle, equation | CONIC | any any any any | PARAB ELIP HYP CIRCL |
| <u>Trigonometry:</u> (10) Law of Sines (3 equations) (11) Law of Cosines (3 equations) | TRIGO | any any | SIN COS |
| (12) Determinant, 2nd order | DETER | DT | DT2 |
| (13) Determinant, 3rd order | | DT | DT3 |
| (14) Probability, Permutation | PROB | Pnr | PERM |
| (15) Probability, Combination | | Cnr | COMB |
| <u>Ellipse:</u> (16) Area (17) Perimeter | ELIPS | A p | AREA PERI |
| <u>Circular Segment:</u> (18) Area (19) Angle | CIRCL SEGM | A ϕ | AREA ANGL |

MATHEMATICS

DIRECTORY (MA)

| TO FIND | SUB DIR. | SYMB | NAME |
|--|---------------|-----------------------------------|--|
| <u>Circular Sector:</u> (20) Area (21) Angle | CIRCL SECT | A ϕ | AREA ANGL |
| <u>Sphere:</u> (22) Volume (23) Area | SPHER | V A | VOLM AREA |
| <u>Parallelogram:</u> (24) Periphery (25) d1 (26) d2 (27) d1d2/ab (28) Area (2 equations) | PARAL | p d1 d2 d1d2 A | PERI D1 D2 D1D2 AREA→ |
| <u>Regular Polygon (n equal sides):</u> (29) Angle (30) Angle (31) Side (32) Perimeter (33) Area | POLIG | ϕ θ s p A | ϕ θ S P A |
| (34) Prismoid Volume | PRISM | V | VOLM |
| <u>Right Circular Cone:</u> (35) Volume (36) Area (37) Ax/Ab ratio | CONE | V A Ax/Ab | VOLM AREA AXAB |
| <u>Right Circular Cylinder:</u> (38) Volume (39) Area | CYLIN | V A | VOLM AREA |
| <u>Parabola of Revolution:</u> (40) Area of parabola (2 equations) (41) Volume | PARAB | A V | AREA VOLM |

MECHANICS OF MATERIALS

DIRECTORY (MM)

| TO FIND | SUB DIR. | SYMB | NAME |
|--|------------|------------|------------------------------|
| <u>Engineering strain:</u> | | | |
| (01) Engineering strain | STRN/ENGI | ϵ | ϵ |
| (02) Force/Deformation equation | | F | F |
| <u>Shear stress strain:</u> | | | |
| (03) Shear Strain | STRN/SHEAR | γ | γ |
| (04) Shear Modulus | | G | G |
| <u>Loading and Deformation:</u> | | | |
| (05) Stress | DEFOR/LOAD | σ | σ |
| (06) Strain | | ϵ | ϵ |
| (07) Modulus of Elasticity (2 equations) | | E | <i>E</i> |
| (08) Elongation | | δ | δ |
| <u>Thermal deformations:</u> | | | |
| (09) Deformation caused by temp. difference | DEFOR/THER | δt | δT |
| <u>Cylindrical Pressure, Stress:</u> | | | |
| <u>Stress in Wall, internal pressure:</u> | | | |
| (10) Tangential (Hoop) stress | WALL/INSID | σt | σT |
| (11) Radial stress | | σr | σR |
| <u>Stress in Wall, external pressure:</u> | | | |
| (12) Tangential (Hoop) stress | WALL/OUTSI | σt | σT |
| (13) Radial stress | | σr | σR |
| (14) Stress in caps | -- | σa | <i>CAPS</i> |
| (15) Stress in thin wall cylinders | -- | σt | <i>THIN</i> |

MECHANICS OF MATERIALS

DIRECTORY (MM)

| TO FIND | SUB DIR. | SYMB | NAME |
|---|-----------|--|---|
| <p><u>Mohr's Circle, Stress:</u></p> <p>(16) Principle, maximum</p> <p>(17) Principle, minimum</p> <p>(18) Shear stress, maximum</p> | MOHR | $\sigma_{1,2}$ $\sigma_{1,2}$ τ_{max} | σ_{MAX} σ_{MIN} τ_{MAX} |
| <p><u>Hook's Law:</u></p> <p><u>Three dimensional stress case:</u></p> <p>(19) Strain, x axis</p> <p>(20) Strain, y axis</p> <p>(21) Strain, z axis</p> <p><u>Plane stress case:</u></p> <p>(22) Strain, x axis</p> <p>(23) Strain, y axis</p> <p>(24) Strain, z axis</p> | HOOK/3DIM | ϵ_x ϵ_y ϵ_z | ϵ_x ϵ_y ϵ_z |
| <p><u>Torsion:</u></p> <p>(25) Twisting moment per radian of twist</p> <p>(26) Shear stress, hollow thin wall shaft</p> | TORS | T/ϕ τ | T/ϕ τ |
| <p><u>Stresses in Beams</u></p> <p>(27) Radius of curvature, deflected shaft</p> <p>(28) Normal Stress in beam, at y distance</p> <p>(29) Stress in beam, at c distance (2 equations)</p> <p>(30) Stress in beam, with S (2 equations)</p> <p>(31) Shear flow</p> <p>(32) Shear stress</p> | BEAM | ρ σ_x σ_x σ_x q τ_{xy} | $1/\rho$ σ_{x1} $\sigma_{x2} \rightarrow$ $\sigma_{x3} \rightarrow$ Q τ_{xy} |

MECHANICS OF MATERIALS

DIRECTORY (MM)

| TO FIND | SUB DIR. | SYMB | NAME |
|--|----------|------------|---------------------------|
| <u>Columns/Beams:</u> (33) Euler's critical load, equation 1 (34) Euler's critical load, equation 2 | CLMN | Pcr Pcr | PCR1 PCR2 |
| <u>Elastic Strain Energy:</u> (35) Energy stored in beam (36) Strain energy/unit vol.(2 equations) | ENRG | U u | U $\sigma \rightarrow$ |

THERMODYNAMICS

DIRECTORY (TH)

| TO FIND | SUB DIR. | SYMB | NAME |
|--|--------------|------------|-----------------------|
| <u>Properties of Single component systems:</u> | | | |
| (01) Quality of vapor | | x | X |
| (02) Specific volume (2 equations) | | v | V→ |
| (03) Internal energy | | u | U |
| (04) Enthalpy | PROP | h | H |
| (05) Entropy | | s | S |
| <u>Ideal gas:</u> | | | |
| (06) P, V equations | PROP/IDEAL | any | PV |
| (07) P, V, T equations | | any | PVT |
| (08) Gas constant | PROP | R | R |
| <u>For cold air standard, constant heat capacity:</u> | | | |
| (09) Change in internal energy | AIR | Δu | ΔU |
| (10) Change in enthalpy | | Δh | ΔH |
| (11) Change in entropy (T & P) (2 equations) | | Δs | $\Delta S\rightarrow$ |
| <u>For constant entropy process:</u> | | | |
| (12) P1, v1, P2, v2 equation | | any | P/V |
| (13) T1, P1, T2, P2 equation | $\Delta S=0$ | any | T/P |
| (14) T1, v1, T2, v2 equation | | any | T/V |
| (15) Ratio of Specific Heat | | k | K |
| <u>Closed Thermodynamic Systems:</u> | | | |
| <u>Work performed, ideal gas:</u> | | | |
| (16) Constant Pressure | CLOSE | w | $\Delta P=0$ |
| (17) Constant Volume, w=0 | | - | -- |
| (18) Constant Temperature (2 equations) | | w | $\Delta T=0$ |

THERMODYNAMICS

DIRECTORY (TH)

| TO FIND | SUB DIR. | SYMB | NAME |
|---|----------|----------|---------------------------------|
| <u>Closed Thermodynamic Systems:</u> | | | |
| <u>Work performed, ideal gas:</u> | | | |
| (19) Isentropic (2 equations) | CLOSE | w | <i>ISEN→</i> |
| (20) Polytropic | | w | <i>POLY</i> |
| <u>Open Thermodynamic Systems:</u> | | | |
| <u>Work performed, ideal gas:</u> | | | |
| (21) Constant Pressure, w=0 | OPEN | - | - |
| (22) Constant Volume | | w | $\Delta V=0$ |
| (23) Constant Temperature (2 equations) | | w | $\Delta T=0→$ |
| (24) Isentropic (2 equations) | | w | <i>ISEN→</i> |
| (25) Isentropic, steady flow | | Wis | <i>WIS</i> |
| (26) Polytropic | | w | <i>POLY</i> |
| <u>Nozzles, Diffusors:</u> | | | |
| (27) Velocity term | NOZL | any | HI |
| (28) Efficiency of nozzle | | η | EFFI |
| <u>Turbines:</u> | | | |
| (29) Efficiency | TURB | η | EFFI |
| <u>Pump:</u> | | | |
| (30) Efficiency | PUMP | η | EFFI |
| <u>Compressor:</u> | | | |
| (31) Efficiency | COMP | η | EFFI |
| <u>Heat Exchanegrs:</u> | | | |
| (32) m1,h1,m2,h2 equation | HTEX | any | HTEX |
| <u>Heat Engines:</u> | | | |
| (33) Efficiency | H.ENG | η | $\eta→$ |
| (34) Efficiency of Carnot Cycle. | | η_c | η_c |

THERMODYNAMICS

DIRECTORY (*TH*)

| TO FIND | SUB DIR. | SYMB | NAME |
|---|----------|--------------------------------------|--|
| <u>Coefficient Of Performance:</u> (35) Heat Pump (36) Refrigerator | COP | COP _c COP _c | HPMP REFR |
| <u>Ideal Gas Mixture:</u> (37) Partial Pressure (38) Partial Volume | MIXT | P _i V _i | PRES VOLM |
| <u>Psychometric:</u> (39) Total air pressure (40) Specific Humidity, mv, ma (41) Specific Humidity, P _v , P _a (2 equations) (42) Relative Humidity, P _v , P _g (43) Enthalpy | PSYC | P ω ω φ h | P ω ω→ φ→ H |

CHEMICAL ENGINEERING

DIRECTORY (*CHEM*)

| TO FIND | SUB DIR. | NAME |
|--|--|--|
| <p><u>Chemical Thermodynamics:</u> (01) Activity Coefficients</p> <p><u>Ideal solutions, Fugacities Coefficients:</u> (02) In term of pressure (03) mixture</p> <p><u>Chemical Equilibrium:</u> <u>For Reaction:</u> (04) (05)</p> <p><u>For mixtures:</u> (06) (07)</p> | <p style="text-align: center;">THER THER/ACTIV</p> <p style="text-align: center;">THER/IDEAL</p> <p style="text-align: center;">THER/EQUIL THER/EQUIL/REACT</p> <p style="text-align: center;">THER/EQUIL/MIXTR</p> | <p style="text-align: center;">γ_{IV}</p> <p style="text-align: center;">FI VIV</p> <p style="text-align: center;">ΔG KA</p> <p style="text-align: center;">KA KP</p> |
| <p><u>Chemical Reaction Engineering:</u> <u>Rate of Reaction:</u> (08) Rate (2 equations) (09) Rate Constant (10) Moles of A, reacted/fed</p> <p><u>Reaction Order:</u> <u>Zero Order Reaction:</u> (11) Rate (12) Concentration of Component A (13) Moles of A, reacted/fed</p> <p><u>First Order Reaction:</u> (14) Rate (15) Concentration of Component A (16) Moles of A, reacted/fed</p> <p><u>Second Order Reaction:</u> (17) Rate (18) Concentration of Component A (19) Moles of A, reacted/fed</p> | <p style="text-align: center;">REACT REACT/RATE</p> <p style="text-align: center;">REACT/ORDER REACT/ORDER/ZERO</p> <p style="text-align: center;">REACT/ORDER/FIRST</p> <p style="text-align: center;">REACT/ORDER/SCND</p> | <p style="text-align: center;">RA→ K XA</p> <p style="text-align: center;">RA CA XA</p> <p style="text-align: center;">RA CA XA</p> <p style="text-align: center;">RA CA XA</p> |

CHEMICAL ENGINEERING

DIRECTORY (*CHEM*)

| TO FIND | SUB DIR. | NAME |
|--|---|---|
| <p><u>Reactors:</u></p> <p><u>Batch:</u> (20) Rate (21) Volume</p> <p><u>Flow:</u> (22) Plug-Flow Reactor</p> <p><u>Continuous:</u> (23) Continuous Stirred Tank Reactor (CSTR) (24) Stirred Tank Reactors in series (2 equations)</p> | <p style="text-align: center;">RACTR RACTR/BATCH</p> <p style="text-align: center;">RACTR/FLOW</p> <p style="text-align: center;">RACTR/FLOW/CONTI</p> | <p style="text-align: center;">RA V</p> <p style="text-align: center;">PLUG</p> <p style="text-align: center;">CSTR <i>SER</i>→</p> |
| <p><u>Distillation:</u></p> <p><u>Flash (or equilibrium) Distillation:</u> (25) Component material balance (26) Overall material Balance</p> <p><u>Differential (simple or Rayleigh) Distillation:</u> (27) y, when relative volatility is constant (28) Differential Distillation equation</p> <p><u>Continuous (binary system) Distillation:</u></p> <p><u>Total Material Balance:</u> (29) (30)</p> <p><u>Operating Lines:</u></p> <p><u>Rectifying Section:</u> (31) Total Material (32) Component A (2 equations)</p> <p><u>Stripping Section:</u> (33) Total Material (34) Component A (2 equations)</p> <p><u>Reflux Ratio:</u> (35) Ratio of Reflux to overhead product (36) Feed condition line (37) Murphree Plate Efficiency</p> | <p style="text-align: center;">DISTIL DISTIL/FLASH</p> <p style="text-align: center;">DISTIL/DIFER</p> <p style="text-align: center;">DISTIL/CONTI DISTIL/CONTI/T.MAT</p> <p style="text-align: center;">DISTIL/CONTI/OPER DISTIL/CONTI/OPER/RECTI</p> <p style="text-align: center;">DISTIL/CONTI/OPER/STRIP</p> <p style="text-align: center;">DISTIL/CONTI/OPER/RFLUX</p> | <p style="text-align: center;">FZF F</p> <p style="text-align: center;">Y W/W₀</p> <p style="text-align: center;">F FZF</p> <p style="text-align: center;">T.MAT <i>CMP. A</i>→</p> <p style="text-align: center;">T.MAT <i>CMP. A</i>→</p> <p style="text-align: center;"><i>RD</i>→ SLOPE EME</p> |

CHEMICAL ENGINEERING

DIRECTORY (*CHEM*)

| TO FIND | SUB DIR. | NAME |
|---|---|---|
| <p><u>Diffusors:</u> <u>Molecular Diffusion:</u> (38) Gas (39) Liquid (40) Unidirectional of a Gas: (41) Equimolar Counter Diffusion</p> | <p>DIFFU DIFFU/MOLEC DIFFU</p> | <p>GAS LIQID UNIDI EQUI</p> |
| <p><u>Convection:</u> <u>Two Film Theory (for equimolar Counter-Diffusion):</u> (42) First Equation (43) Second Equation (44) Third Equation (45) Fourth Equation <u>Overall Coefficient:</u> (46) (47) <u>Transfer Unit:</u> (48) Height of Transfer Unit (49) Height of Transfer Unit (50) Height of Tower (2 equations) (51) Dimension-less Group Equation</p> | <p>CONV CONV/2FILM CONV/COEF CONV/TRNS CONV</p> | <p>EQ1 EQ2 EQ3 EQ4 K'G K'L HOG HOL Z→ KM</p> |

CIVIL ENGINEERING

DIRECTORY (CIVIL)

| TO FIND | SUB DIR. | NAME |
|---|---|---|
| <p><u>GEOTECHNICAL DEFINITIONS:</u></p> <p>(01) Coefficient of Curvature or Gradation</p> <p>(02) Uniformity Coefficient</p> <p>(03) Void Ratio</p> <p>(04) Water Content (%)</p> <p>(05) Compression Index</p> <p>(06) Relative Density (%) (2 equations)</p> <p>(07) Specific Gravity</p> <p>(08) Settlement</p> <p>(09) Plasticity Index</p> <p>(10) Degree of Saturation (%)</p> <p>(11) Shrinkage Index</p> <p>(12) For flow nets</p> <p>(13) Total Unit Weight of Soil</p> <p>(14) Dry Unit Weight of Soil (2 equations)</p> <p>(15) Unit Weight of Solids</p> <p>(16) Prosperity (2 equations)</p> <p>(17) Normal Stress</p> <p>(18) General Shear Stress</p> <p>(19) Coefficient of Active Earth Pressure</p> <p>(20) Coefficient of Passive Earth Pressure</p> <p>(21) Active Resultant Force</p> <p>(22) Bearing Capacity Equation</p> <p>(23) Factor of Safety (Slope Stability)</p> <p>(24) Coefficient of Consolidation</p> <p>(25) Effective Stress</p> | <p>GEOT/DEFIN</p> | <p>CC</p> <p>CU</p> <p>E</p> <p>W</p> <p>CC</p> <p>DD</p> <p>G</p> <p>ΔH</p> <p>PI</p> <p>S</p> <p>SI</p> <p>Q</p> <p>γ</p> <p>γD</p> <p>γS</p> <p>η</p> <p>σ</p> <p>τ</p> <p>KA</p> <p>KP</p> <p>PA</p> <p>QULT</p> <p>FS</p> <p>CV</p> <p>σ'</p> |
| <p><u>STRUCTURAL ANALYSIS:</u></p> <p><u>Deflection of Trusses and Frames:</u></p> <p><u>Deflection of Trusses:</u></p> <p>(26) General Equation</p> <p>(27) For temperature</p> <p>(28) For Load</p> | <p>STRUC</p> <p>STRUC/DFLEC</p> <p>STRUC/DFLEC/TRUS</p> | <p>GNRL</p> <p>TEMP</p> <p>LOAD</p> |

CIVIL ENGINEERING

DIRECTORY (CIVIL)

| TO FIND | SUB DIR. | NAME |
|---|------------------------|-----------------|
| <u>TRANSPORTATION:</u> | | |
| <u>Distance:</u> | | |
| (29) Braking Distance: | TRANS TRANS/DIST | BRAKE |
| <u>Sight Distance:</u> | TRANS/DIST/SIGHT | |
| <u>Crest, Vertical Curve:</u> | TRANS/DIST/SIGHT/CREST | |
| (30) $S < L$ | | S < L |
| (31) $S > L$ | | S > L |
| <u>Sag, Vertical Curve:</u> | TRANS/DIST/SIGHT/SAG | |
| (32) $S < L$ | | S < L |
| (33) $S > L$ | | S > L |
| (34) Riding Comfort on sag vertical curve | TRANS/DIST | COMF |
| <u>Adequate Sight Distance:</u> | TRANS/DIST/ADEQ | |
| (35) $S < L$ | | S < L |
| (36) $S > L$ | | S > L |
| (37) Horizontal Curve | TRANS/DIST | HORIZ |
| <u>Super elevation:</u> | | |
| (38) Highways (General and SI system) | TRANS/SUPER/H.WAY | GEN,SI |
| (39) Railroads | TRANS/SUPER | RAIL |
| <u>Spirals:</u> | | |
| (40) Highways | TRANS/SPIRA/H.WAY | ENG,SI |
| (41) Railroads (2 equations) | TRANS/SPIRA | RAIL→ |
| <u>Modified Davis Equation:</u> | | |
| (42) Level tangent Resistance | | R |
| (43) Tractive Effort | TRANS/DAVIS | TE |

CIVIL ENGINEERING

DIRECTORY (CIVIL)

| TO FIND | SUB DIR. | NAME |
|---|--|---|
| <p><u>STRUCTURAL STEEL DESIGN:</u></p> <p><u>Tension Members:</u></p> <p><u>Allowable Stress Design (ASD):</u></p> <p>(58) For yielding</p> <p>(59) For fracture</p> <p><u>Load Resistance Factor Design (LRFD):</u></p> <p>(60) For yielding</p> <p>(61) For fracture</p> <p><u>Member Connections:</u></p> <p><u>Allowable Stress Design (ASD):</u></p> <p>(62) Shear Stress</p> <p>(63) Allowable Stress</p> <p><u>Load Resistance Factor Design (LRFD):</u></p> <p>(64) Nominal Strength</p> <p><u>Compression Members:</u></p> <p>(65) Maximum stress</p> <p>(65a) Minimum stress</p> <p>(65b) Euler formula (1)</p> <p>(65c) Euler formula (2)</p> <p>(65d) Slenderness Ratio</p> <p>(66) Cc value</p> <p><u>Allowable Stress Design (ASD):</u></p> <p><u>Allowable Axial Compressive Stress (Fa):</u></p> <p>(67) If $SR > Cc$</p> <p>(68) If $SR \leq Cc$</p> <p><u>Load Resistance Factor Design (LRFD):</u></p> <p><u>Critical Stress (Fcr):</u></p> <p>(69) If $0 \leq \lambda_c \leq 1.5$</p> <p>(70) If $\lambda_c > 1.5$</p> <p>(71) Column Slenderness parameter</p> <p>(72) Required Axial Strength</p> | <p style="text-align: center;">STEEL</p> <p style="text-align: center;">STEEL/TENS</p> <p style="text-align: center;">STEEL/TENS/ASD</p> <p style="text-align: center;">STEEL/TENS/LRFD</p> <p style="text-align: center;">STEEL/CONEC</p> <p style="text-align: center;">STEEL/CONEC/ASD</p> <p style="text-align: center;">STEEL/CONEC/LRFD</p> <p style="text-align: center;">STEEL/COMP</p> <p style="text-align: center;">STEEL/COMP/ASD</p> <p style="text-align: center;">STEEL/COMP/LRFD</p> | <p style="text-align: center;">YIELD</p> <p style="text-align: center;">FRACT</p> <p style="text-align: center;">YIELD</p> <p style="text-align: center;">FRACT</p> <p style="text-align: center;">FV</p> <p style="text-align: center;">FT</p> <p style="text-align: center;">ϕR_N</p> <p style="text-align: center;">σ_{MAX}</p> <p style="text-align: center;">σ_{MIN}</p> <p style="text-align: center;">PCR1</p> <p style="text-align: center;">PCR2</p> <p style="text-align: center;">SR</p> <p style="text-align: center;">CC</p> <p style="text-align: center;">$SR > CC$</p> <p style="text-align: center;">$SR \leq CC$</p> <p style="text-align: center;">$\lambda \leq 1.5$</p> <p style="text-align: center;">$\lambda > 1.5$</p> <p style="text-align: center;">λC</p> <p style="text-align: center;">PU</p> |

CIVIL ENGINEERING

DIRECTORY (CIVIL)

| TO FIND | SUB DIR. | NAME |
|--|--|---|
| <p><u>CURVE FORMULAS:</u> <u>Vertical Curves:</u> (73) Horiz. Distance to min/max Elev. on Curve (3 eq.) <u>Elevation:</u> (74) Tangent Elevation (2 equations) (75) Curve Elevation (2 equations)</p> <p>(76) Tangent offset (77) Parabola Constant (78) Tangent offset at PVI (79) Rate of change of grade</p> <p><u>Horizontal Curves:</u> (80) Radius (81) Length of curve from P.C. to P.T. (2 equations) (82) Radius (2 equations) (83) Length of curve from P.C. to P.T. (84) Length of Middle Ordinate (85) Angle between two Tangents (2 equations) (86) Length of curve from P.C. to P.T. (2 equations) (87) Length of Sub-Chord (88) Angle of Sub-Chord (89) External Distance</p> | <p style="text-align: center;">CURVE CURVE/VERTI</p> <p style="text-align: center;">CURVE/VERTI/ELEV</p> <p style="text-align: center;">CURVE/VERTI</p> <p style="text-align: center;">CURVE/HORIZ</p> | <p style="text-align: center;"><i><u>X</u></i><i><u>M</u></i><i><u>→</u></i></p> <p style="text-align: center;">TANG CURV</p> <p style="text-align: center;">Y A E R</p> <p style="text-align: center;">R <i>T</i><i>→</i> <i>R</i><i>→</i> L M <i>I/2</i><i>→</i> <i>L</i><i>→</i> C D <i>E</i></p> |
| <p><u>BEAM FIXED-END MOMENT:</u> <u>Situation 1:</u> (90) AB moment (91) BA moment</p> <p><u>Situation 2:</u> (92) AB moment (93) BA moment</p> <p><u>Situation 3:</u> (94) AB moment (95) BA moment</p> | <p style="text-align: center;">BEAM BEAM/SITU1</p> <p style="text-align: center;">BEAM/SITU2</p> <p style="text-align: center;">BEAM/SITU3</p> | <p style="text-align: center;">MAB MBA</p> <p style="text-align: center;">MAB MBA</p> <p style="text-align: center;">MAB MBA</p> |

MECHANICAL ENGINEERING

DIRECTORY (*MECH*)

| TO FIND | SUB DIR. | NAME |
|--|---|--|
| <p><u>HVAC</u> <u>Heating Load:</u> (15) Heat loss (R is given) (16) Thermal Resistance (17) Heat loss (U is given)</p> <p><u>Cooling Load:</u> (18) Heat gain</p> <p><u>Infiltration:</u> (19) Heat loss, Air Change Method (20) Heat loss, Crack Method</p> | <p style="text-align: center;">HVAC HVAC/LOAD/HEAT</p> <p style="text-align: center;">HVAC/LOAD/COOL</p> <p style="text-align: center;">HVAC/INFIL</p> | <p style="text-align: center;">Q R" Q</p> <p style="text-align: center;">Q</p> <p style="text-align: center;">CHNG CRAK</p> |
| <p><u>FANS:</u> (21) Power</p> | FAN | POWR |
| <p><u>PUMPS:</u> (22) Net Positive Suction Head (23) Power</p> | PUMP | NPSH POWR |
| <p><u>COMPRESSORS:</u> (24) Input Power (2 equations) (25) Exit enthalpy (26) Exit temperature</p> | COMP | W→ HE TE |
| <p><u>ENERGY CONSERVATION:</u> <u>Internal Combustion Engines:</u> <u>DIESEL cycle:</u> (27) Compression Ratio (28) Cut-Off Ratio (29) Efficiency (30) Ratio of Specific Heat</p> | INTER INTER/DISEL | R RC η K |

MECHANICAL ENGINEERING

DIRECTORY (MECH)

| TO FIND | SUB DIR. | NAME |
|--|--|---|
| <p><u>GAS TURBINE, Brayton Cycle:</u> <u>With Regenerator:</u> (48) h3 (49) T3 (50) q34 (51) q56 (52) Efficiency (53) Regenerated efficiency</p> | <p>TURB TURB/RGEN</p> | <p>H3 T3 Q34→ Q56→ η ηRG→</p> |
| <p><u>STEAM POWER PLANTS:</u> <u>Feed Water Heater:</u> (54) Open system (55) Closed system (56) Junction <u>Pump:</u> (57) Work (58) h2s (59) Work</p> | <p>STIM STIM/HETER STIM STIM/PUMP</p> | <p>OPEN CLOSE JUNC W H2S W</p> |
| <p><u>SHAFT AND AXLES:</u> <u>Static Loading:</u> (60) Maximum Shear stress (61) Von Mises stress <u>Fatigue Loading:</u> (62) Shaft diameter</p> | <p>SHAFT SHAFT/STAT SHAFT/FATIG</p> | <p>τ_{MX} σ' D</p> |

MECHANICAL ENGINEERING

DIRECTORY (MECH)

| TO FIND | SUB DIR. | NAME |
|--|--|---|
| <p><u>SCREWS:</u></p> <p>(63) Torque required to raise</p> <p>(64) Torque required to lower</p> <p>(65) Efficiency of power screw</p> <p>(66) Total bolt load</p> <p>(67) Total material load</p> <p>(68) Bolt stiffness</p> <p>(69) Member stiffness</p> | SCRW | <p>TR</p> <p>TL</p> <p>η</p> <p>FB</p> <p>FM</p> <p>KB</p> <p>KM</p> |
| <p><u>FASTENERS:</u></p> <p>(70) Bolt load factor</p> <p>(71) Factor of safety</p> <p>(72) Alternating stress</p> <p>(73) Mean stress</p> | FASTE | <p>NB</p> <p>NS</p> <p>σ_A</p> <p>σ_M</p> |
| <p><u>SPRINGS:</u></p> <p><u>Helical Linear Springs:</u></p> <p>(74) Shear stress</p> <p>(75) Correction factor</p> <p>(76) Spring rate (spring factor)</p> <p><u>Helical Torsion Springs:</u></p> <p>(77) Bending stress</p> <p>(78) Correction factor</p> <p>(79) Deflection, Moment equation</p> <p>(80) Spring rate (spring factor)</p> <p>(81) Endurance limit</p> | <p>SPRIN</p> <p>SPRIN/LINER</p> <p>SPRIN/TORS</p> <p>SPRIN</p> | <p>τ</p> <p>KS</p> <p>K</p> <p>σ</p> <p>KI</p> <p>FR</p> <p>K</p> <p>SE</p> |

MECHANICAL ENGINEERING

DIRECTORY (*MECH*)

| TO FIND | SUB DIR. | NAME |
|---|--------------------|----------------------------------|
| <p><u>PRESS/SHRINK FITS:</u> (82) Interface induced pressure (83) Torque, maximum by press/shrink fits</p> | FITS | PRESS TORQ |
| <p><u>COLUMNS:</u> <u>Intermediate columns:</u> (84) Slenderness ratio (85) Critical Load</p> <p><u>Long columns:</u> (86) Critical Load</p> | CLMN CLMN/INTER | SRD PCR |
| <p><u>GEARS, STRAIGHT SPUR:</u> (87) Radial Force</p> <p><u>Transmitted Load (Tangential Force):</u> (88) With the given torque (2 equations) (89) With the given power (2 equations)</p> <p>(90) Bending stress (91) Surface stress</p> | GEAR | WR |
| | GEAR/WT | TRQ PWR |
| | GEAR | σ_B σ_C |

