

Pocket Professional[™] OWNER'S MANUAL



The Pocket Professional[™]

Mechanical Engineering Application Pac

Owner's Manual

SPARCOM[®]

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Notice

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Mechanical Engineering Application Pac Changes

The following changes were made to the Mechanical Engineering Application Pac for version 2.5:

- ✔ Browser: Cursor movement and scrolling speed have been increased.
- ✔ Constant Library: Constants have been updated to conform to latest accepted values.

HP 48GX USERS ONLY: You should install the application card in Port 1 for two reasons:

1. Application cards installed in Port 1 will execute ~ 20% faster than those installed in Port 2.

2. Application cards installed in Port 2 may experience long pauses (~ 5-10 seconds or more) intermittently during operation. This is not a software defect. It is caused by the new memory architecture of the extended HP 48GX Port 2, which is different from the HP 48SX Port 2. Such pauses will not occur if the application card is operated from Port 1 of the HP 48GX or if it is operated from either port of the HP 48SX.

Mechanical Engineering Application Pac Manual Changes

These changes apply to the Mechanical Engineering Application Pac Manual, Edition 2, August 1991.

Changes for the HP 48GX

General: To display all libraries on the HP 48GX, press Further instead of

General: On the HP 48GX, the Im key has been replaced by CANCEL.

General: To perform a screen dump on the HP 48GX, press ON - 10 instead of ON-UTH.

General: To display an item too wide for the display on the HP 48GX, press instead of I was

Page 3-3: Using the Constants Library: On the HP 48GX, press Frid TYPE Full DTAG instead of Frid TOBUT FULL For The State of the Tobus Full State of the State of Frid Tobus Full State of Frid Tobu

Changes for Version 2.5

General: Because the constants have been updated, some of the examples may differ slightly from the manual.

Page 1-3: Accessing the Mechanical Engineering Application Pac: Picture menu keys should read MEAP MOON ABOUT instead of MEAP ECON DEREC DERUB ABOUT.

Page 1-6: Using the Search Mode: The search mode is now case-insensitive.

Page 1-9: Viewing Variable Definitions: Picture should be:



- Page 1-16: Finding and Selecting the Equation: If you are continuing the previous example, move the pointer to the second equation in the list and press SELECT. to deselect the second equation.
- Page 1-16: Tagging and Entering the Variables: If you are continuing the previous example, after entering the other values at the solver screen, move the pointer to V and press [3009] to unmark V as known (required for plotting); then, press [30101] to turn units off (for faster plotting). This results in the following screen:

Pac and Manual Changes

June 6, 1994



Page 1-20: Loading Values from the Stack: First Method: Stark should be USUK.

- Page 2-5: Cantilever Beam Point Load: Example: Solve equations 1, 3, and 4.
- Page 2-6: Cantilever Beam Uniform Load: Example: Solve equations 3 and 4.
- Page 2-7: Cantilever Beam Moment: Example: Solve equations 3 and 4.
- Page 2-9: Simple Beam Uniform Load: Equation 1 should contain +x³ instead of -x³
- Page 2-9: Simple Beam Uniform Load: Equation 2 should contain +4x³ instead of -4x³.
- Page 2-11: Simple Beam Moment: Example: Solve equations 3 and 4.

Page 2-24: Manometers: Example: Solve equations 2 and 4 instead of 3 and 4.

Page 2-26: Immersed Bodies: Example: Solve equations 1 and 3.

- Page 2-32: Thermodynamics/Ideal Gas Law: Variable description for Vs1 should be "specific volume state 1."
- Page 2-33: Thermodynamics/Ideal Gas Law: Example: RG=6.8479_Btu/(lb*°R).
- Page 2-49: Semi-Infinite Solid: Example: Solve equations 1, 2, 3, and 4.
- Page 2-50: Blackbody Radiation: Example: Solve equations 1 and 3 for first part of example and equation 2 for second part of example.
- Page 2-56: Inclined Planes: Equation 5 should be deleted.
- Page 2-57: Inclined Planes: Example: Solve equations 1 and 2.
- Page 2-59: Axial Load: Example 2: Solve equations 4 and 5.
- Page 2-62: Torsion: Variable γ should have angle units instead of no units.
- Page 2-62: Torsion: Example 1: t=418.8790_MPa, γ=0.4_*.
- Page 2-64: Principal Stresses: Equation 2 should contain $COS(2 \cdot \Theta) \tau_{XY} \cdot SIN(2 \cdot \Theta)$ instead of $COS(2 \cdot \Theta) + \tau_{XY} \cdot SIN(2 \cdot \Theta)$.
- Page 2-65: Principal Stresses: Example: Solve equations 1 and 2; oy1=-60705.081_Pa.
- Page 2-67: Mohr's Circle: Example: Solve equations 1, 2, and 4.
- Page 2-68: Simple and Compound Pendulums: Example 2: Solve equation 2.
- Page 2-72: Natural Frequency Beams: Example: Solve equation 1; fn1=1.5381_Hz.

Page 2-74: Helical Springs: Equation 7 should be $\frac{4 \cdot C - 1}{4 \cdot C - 4} + \frac{.615}{C}$ instead of $\frac{2 \cdot C + 1}{2 \cdot C}$.

Pac and Manual Changes

June 6, 1994

Page 3-3: Using the ECON Function: ECON should be MCON.

Page 3-3: Using the ECON Function: Picture menu keys should read MEAP MEON ABOUN instead of MEAP BEON DEFICE DEFIUE ABOUT.

Table of Contents

Chapter 1: Getting Started

Welcome
Installing and Removing the Card
To Install the Application Card
To Remove an Application Card
Accessing the Mechanical Engineering Application Pac 1-3
Using the Main Menu1-4
Applications in the Main Menu
Moving Around the Screen
Viewing Items Too Wide for the Display
Changing the Font Size
Using the Search Mode
Using the Equation Library
Accessing Equations
Selecting and Displaying Equations
Viewing Variable Definitions
Using the Solver Function
Converting Data to Different Units
Options After Solving the Equation
Managing Units
Solving Multiple Equations
Plotting One Equation
Multiple Plots
What You Should Know About the Solver
Speeding Up Computing Time
"Bad Guess" Message
Loading Values from the Stack
Memory Requirements
Sparcom's "MEAPPD" Directory
MEpar
Summary of Softkeys
Summary of Functions
Chapter 2: Equation Library
Beams
Hollow Rectangle/I/C Beams
L/T/U Beams

0	
/T/U Beams	-3
Cantilever Beam-Point Load	-4
Cantilever Beam-Uniform Load	-5
Cantilever Beam-Moment	-7

Simple Beam-Point Load	2-8
Simple Beam-Uniform Load	2-9
Simple Beam-Moment	2-10
Simple Beam-Linear Load	2-12
Fluid Mechanics	2-14
Fluid Statics	2-14
Bernoulli's Equation	2-16
Mechanical Energy Balance	2-17
Discharge from Tanks	2-19
Horizontal Jet on Vertical Plate	2-21
Vertical Jet on Horizontal Plate	2-22
Manometers	2-23
Friction Loss	2-24
Immersed Bodies	2-26
Gas Laws	2-27
Ideal Gas Laws	2-27
Gas-Constant Pressure	2-28
Gas-Constant Volume	2-29
Gas-Constant Temperature	2-30
Thermodynamics/Ideal Gas Law	2-31
Real Gas Law	2-33
Polytropic Process	2-34
Heat Transfer	2-36
Steady State - Conduction & Convection	2-36
Heat Conduction-Cylindrical, Spherical Wall	2-39
Forced Convection-Flat Plate (Heat)	2-40
Forced Convection-Flat Plate (Drag)	2-42
Lumped Cap Analysis	2-44
Negligible Surface Resistance	2-45
Semi-Infinite Solid	2-48
Blackbody Radiation	2-49
Radiant Heat Exchange	2-50
Mechanics	2-52
Linear Motion	2-52
Angular Motion	2-53
Force, Work, Power	2-54
Forces in Angular Motion	2-55
Elastic Collisions (1D)	2-56
Inclined Planes	2-56
Stress Analysis	2-57
Normal Stress/Strain	2-57
Axial Load	2-59

Dynamic Load	2-60
Torsion	2-61
Pure Shear	2-62
Principal Stresses	2-64
Mohr's Circle	2-65
Vibrations	2-68
Simple and Compound Pendulums	2-68
Damped and Free Vibration	2-69
Natural Frequency-Spring System	2-70
Natural Frequency-Beams	2-71
Vibration Isolation	2-73
Machine Design	2-74
Helical Springs	2-74
Frequency of Helical Springs	2-76
Viscosity & Petroff's Law	2-77
Chapter 3: Constants Library	
Types of Constants	3-1
Universal Constants	3-1
Magnetic Properties	3_2
Mechanical Thermal	3-2
Using the Constants Library	3-2
Using the ECON Function	3_3
Constants Library Softkeys	3-4
Chapter 4: Applycic	
Steam Tables	4-1
Saturated Steam Properties	4-2
Superheated Steam Properties	4-2
Using Steam Tables	4-2
Vector Analysis	4-4
Specifying Vectors	4-4
Thermocouples	4-6
Using the Thermocouples Function	4-6
Basis for Temperature/Voltage Conversions	4-6
Summary of Softkeys	4-7
Chapter 5: Reference Library	
Reference Library Topics	5-1
Using the Reference Library	5-2
Reference Library Softkeys	5-2

Appendix A: Warranty and Service

Pocket Professional Support		. A-1
Limited One-Year Warranty		. A-1
What Is Covered		. A-1
What Is Not Covered		. A-1
If the Card Requires Service		. A-2
Service Charge		. A-2
Shipping Instructions		. A-2
Environmental Limits	•••	. A-3
Appendix B: Bibliography Mechanical Engineering References		. B-1
Appendix C: Questions and Answers		
Questions Commonly Asked	•••	. C-1

Chapter 1 Getting Started

In This Chapter

- □ Welcome
- Installing and Removing the Card
- Using the Main Menu
- Using the Equation Library
- □ What You Should Know About the Solver
- □ Summary of Functions
- □ Summary of Softkeys

Welcome

Sparcom's Pocket Professional[™] software is the first of its kind, developed to provide speed, efficiency and portability to students and professionals in the technical fields. When you slide the Pocket Professional[™] Mechanical Engineering Application Pac into your HP 48SX, your calculator is instantly transformed into an electronic "textbook," ready to efficiently solve your mechanical engineering problems. The software is organized into six sections: Equation Library, Steam Tables, Vector Analysis, Thermocouples, Constants Library and Reference Library. . . all available in an efficient, menu-driven format.

Installing and Removing the Card

The HP 48SX has two ports for installing plug-in cards. You can install your Mechanical Engineering Application Pac card in either port. Be sure to **turn off the calculator** while installing or removing the card. Otherwise, user memory may be erased.

To Install the Application Card

1. Turn off the calculator. Do not press (IN) until you have completed the installation procedure.

2. Remove the port cover. Press against the grip lines and push forward. Lift the cover to expose the two plug-in ports.



- 3. Select either empty port for the Pocket Professional card.
- 4. Position the card just outside the slot. Point the triangular arrow on the card toward the calculator port opening, as shown.
- 5. Slide the card firmly into the slot. After you first feel resistance, push the card about 1/4 inch further, until it is fully seated.



6. Replace the port cover.

To Remove an Application Card

- 1. Turn the calculator off. Do not press (N) until you have completed the procedure.
- 2. Remove the port cover. Press against the card's grip and slide the card out of the port.



3. Replace the port cover. If you want to remove a RAM card that contains merged memory, you must free the merged memory before removing the card. Otherwise, you are likely to lose data stored in user memory. See the *HP 48SX Owner's Manual* for instructions.

Accessing the Mechanical Engineering Application Pac

After you turn on your calculator by pressing \bigcirc , there are three ways to start the software.

First Method: Press **C LERARY** to display all libraries available to the HP 48SX. Find and press **MEAP** to enter the Mechanical Engineering Application Pac library directory. The screen displays new menu keys or "softkeys" along the bottom, as shown:

ł	HOME	MEAPPD	}
4	:		
3 2	:		
1	:		
۲	IEAP E	CON DERI	EC DERUB ABOUT

Press the **MEAP** softkey again to start the application. The **ECON** softkey accesses the Constants Library function, described in Chapter 3.

The **DERME** and **DERUB** are functions required by the software, but are not available to the user.

Pressing the **ABOUT** softkey displays a screen containing the revision number of the Mechanical Engineering Application Pac. (Press **ATR** to exit the revision screen).

Second Method: Type in COM MEAPP ENTER.

Third Method: Add the command "MEAPP" to the CST (custom) menu (for more information, refer to Chapter 15 of the *HP 48SX Owner's Manual*, "Customizing the Calculator"). After the command has been added, press [ST], then press MEAP to start the application.

Using the Main Menu

After you start the application, the main menu screen appears:



The main menu lists the six major areas of application in a menu-driven format. Menu-driven means that the information is selected by moving the pointer to an item in the menu and pressing **ENTER**.

Applications in the Main Menu

Each application in the main menu is briefly described below and is discussed in detail in the next four chapters of this manual.

Equation Library	Allows you to solve, plot and analyze over 300 equations commonly used by mechanical engi-
	neers.
Constants Library	Lists over 20 constants in three categories: uni-
	versal constants, magnetic properties, and me-
	chanical/thermal properties.
Steam Tables	Calculates entropy, enthalpy, internal energy
	and specific volume of saturated and super-
	heated steam.
Vector Analysis	Adds, computes cross and dot products of
	vectors specified by magnitude and direction.
Thermocouples	Computes thermocouple data (emf or tempera-
	ture) for standard thermocouples.

Reference Library	Includes reference data for the physical proper-
	ties of water, orifice coefficients of water, valve
	and fitting loss coefficients, and relative rough-
	ness of various materials.

The "softkeys" located along the bottom of each screen give you options that relate to the information displayed on any given screen. The following softkeys appear along the bottom of the main menu. A summary of common softkeys used throughout the software is given at the end of this chapter.

- **FONT** Toggles between the large (case-sensitive) and small (uppercase) fonts for easier viewing of results.
- **UP** Moves up one level in the menu structure.

Moving Around the Screen

Use the **A** and **Y** keys to move the pointer up and down in the menu list. Pressing **FY** moves the pointer to the bottom of the screen, or pages down (one screen at a time) if the pointer is already at the bottom of the screen. Pressing **FA** moves the pointer to the top of the screen, or pages up. Pressing **FY** moves the pointer to the bottom of the list and **FA** moves the pointer to the bottom of the list and **FA**

Viewing Items Too Wide for the Display

If the text of a menu item is too wide to fit within the display, an ellipsis (...) appears at the end of the line. Press regime to display the rest of the text. Press ATM or ENTER to return to the original display of the item.

Changing the Font Size

The default font for the Mechanical Engineering Application Pac displays information in the small font with uppercase letters only. Pressing **FONT** displays the information in a larger font, which is case-sensitive. The font size remains (shown below) until you press **FONT** again:



Using the Search Mode

When menu lists are long, it is faster to locate an item using the search mode. To initiate a search, press the \square key to display the following screen:

PRG { Home Meappd }		
Search for:		
(+SKIP SKIP→] +DEL DEL→ INS ■		

The calculator is now in *alpha* entry mode, as indicated by the alpha (α) annunciator at the very top of the screen. Alpha entry mode overrides the function of the standard keyboard. This means that each key that has a white capital letter printed to its lower right loses its original function and types that letter onto the command line when pressed. (See the *HP 48SX Owner's Manual*, "The Keyboard and Display", for a complete description of how the alpha mode operates). Type the first letter or letters of the name you want to search for, to create the *search string*, and press ENTER. The search function is case-sensitive. To enter a lower case letter in the alpha entry mode, precede the letter with the \subseteq key.

Press I to return to the main menu.

Editing Text Entries

The search mode softkeys, shown on the screen above, are command line editing keys. They are built into the HP 48SX and allow you to edit the search string. Their functions are summarized below:

SKIP Moves the cursor to the beginning of the current word.

SKIP Moves the cursor to the beginning of the next word.

- Deletes all the characters in the current word to the left of the cursor.
- **DEL** Deletes all the characters from the cursor's current position to the first character of the next word.
- **INS** Toggles between insert and typeover modes.

Using the Equation Library

The Equation Library contains over 300 equations commonly used by today's mechanical engineering professionals and students. The Equation Library enables you to:

- Select the equation category and topic from the main menu.
- List all the equations in a topic.
- Solve a specific equation or set of equations.
- View a description of the variables, and show a figure if available.
- Plot the equation.

The next few pages show you how to solve a single equation. Solving multiple equations systematically is discussed later in chapter. For example, let's suppose you want to calculate the pressure of a fluid with a density of 1.05g/cm³ at point 2, 125 feet below point 1. Assume that pressure at point 1 is 1_atm.

Accessing Equations

The first step in solving this problem is to locate the necessary equation in the Equation Library. At the main menu, move the pointer to EQUATION LIBRARY and press ENTER. This displays the list of six main categories:

Equation	Library
→BEAMS/COLUMNS	-
I GAS LAWS	
HEAT TRANSFER	
I MECHANICS I STRESS ANALYSIS	
VIERATIONS	
MACHINE DESIGN	EDNT UD

Move the pointer to FLUID MECHANICS, and press **ENTER** to display the list of topics in this category:



Selecting and Displaying Equations

Move the pointer to the topic FLUID STATICS and press [ENTER], or press the softkey **EQNS**, to display the equation set for fluid statics:



This screen lists all the equations in the current topic. In this case, there are two. For this example, the static pressure P2 at depth h2 is given by the first equation in the set:

 $P2 = P1 + \rho \cdot g \cdot (h1 - h2)$

where ρ is the density of fluid, P1 is the pressure at height h1, and P2 is the pressure at height h2, and g is the acceleration of gravity constant and is automatically entered from the constants library; no user entry is needed.

Commonly recognizable symbols such as R, the universal gas constant, or k the Boltzmann's constant are automatically extracted from the constants library and no user entry is required. Such variables do not appear in the variable list.

You can solve both of the equations of this set sequentially, iteratively and systematically, or solve only the equation that you select. To select an equation, move the pointer to it and press **SELECT**. This places a triangular tag in front of the equation. If no equations are selected, all the equations in the set are solved sequentially:



Solving multiple equations is discussed later in this chapter.

If you want to view an equation in its full "textbook" form, move the pointer to the equation and press **ENTER**:

```
HP HESE EQUATION WRITER
P2=P1+p·9·(h1-h2)
Press centers to return to list...
```

Press ENTER or ATN to return to the equation list.

When displaying a lengthy equation from the Equation Library, pressing or scrolls the screen to the left or to the right revealing the entire equation. Pressing > moves the display window to the end of the equation, and pressing > moves the display window to the beginning of the equation.

Viewing Variable Definitions

You can view a list that defines all the variables in the selected equation, or set of equations, by pressing the **WARS** softkey at the equations screen. The screen below displays the definitions screen for the first equation of the FLUID STATICS topic:

Fluid Statics +P1: (PA) PRES PT 1 P2: (PA) PRES PT 2 P: (KG/M'3) DENSITY OF FLUID H1: (M) HT AT PT 1 H2: (M) HT AT PT 2
MAIN EQNS VIEW (FICURE)SOLVE UP

To continue solving the problem, you need to use the solver function.

Using the Solver Function

The Sparcom "solver" is a software function that simplifies the job of setting up equations to be calculated by the HP 48SX. The solver function is discussed in more detail later in this chapter, under "What You Need to Know About the Solver."

Enter the solver function of the software by pressing **SOLVE**. At the solver screen, the units key becomes available. To work with units for this example, press the **UNITS** toggle key until it reads **UNITE** The variables for the selected equation(s) now appear on the screen, with units, waiting for you to enter values:

÷	P1: P2: P2: P2: P2: P2: P2: H1:	Fluid '0_PA' '0_PA' '0_KG/M^3' '0_M' '0_M'	Statics
C	ALC	EQNS VARS	UNIT= >STK UP

To enter the density, move the pointer to ρ and press ENTER. This displays the following screen:

{ HOME MEAPPD }	PRG
Set P, density of fluid:	
♦ EKGZ EGZMI EGZC ELBZF ELBZII	

Enter the value for density at the prompt:

{ HOME MEAPPD }	PRG
Set P, density of fluid:	
1.05 _kgz_gzm_gzc_lbzf_lbzt	

After the density is entered, there are two ways to assign units to your entry. The easiest way is by selecting one of the unit softkeys provided on the menu line. If you choose **not** to add units, just press **ENTER** at the prompt, and the software will assign SI units. In some cases, more units are available than the six softkeys displayed in the first screen. In these cases, press **NUT** to display the additional units. For a complete description of units supported by the HP 48SX and their respective symbols, see the HP 48SX Owner's Manual. For this example, press **CC** to add units of g/cm³ to your entry:



Press **ENTER** This returns you to the solver screen with 1.05 g/cm^3 stored into the variable, ρ :



The triangular tag indicates that ρ is a known variable. Repeat this procedure for the other known variables, P1, h1 and h2. This results in the following screen:



With four of the five variables known in this equation, you may now solve the equation for the density by pressing **CALC**. After a few moments, the calculator returns to this screen with the calculated value of P2:



The * by P2 indicates that this value was calculated and was not initially specified.

Converting Data to Different Units.

Suppose you want to convert the pressure at point 2 (P2) from Pascals to atmospheres. First press the key to reveal the next page of softkeys available for this display:



Move the pointer to the variable P2 and press **CONV**. This lists a select set of possible units for P2:



Move the pointer to _atm and press ENTER:



This converts the pressure in Pascals to atmospheres. If you want to use the data for further calculations, move the pointer to the data item and press **STK** and then press **STK** to place it on the calculator stack.

Options After Solving the Equation

Pressing All exits the software and places you in the calculator operating environment. Pressing **CLEAR** resets all entries in the current topic to zero. **Pressing PURGE** deletes the global copies of each variable in the currently selected set of equations that reside in the MEAPPD directory. To return to the main menu screen press **UP** multiple times. At the main menu, a new RESUME SOLVING entry will have been added to the list, as shown:

MECHANICAL →RESUME SOLVING EQUATION LIBERARY STEAM TABLES VECTOR ANALYSIS THERMOCOUPLES CONSTANTS LIBERARY REFERENCE LIBERARY	ENG	APP
	FD	NT QUIT

Selecting the RESUME SOLVING function returns you directly to the equation set you were working with, with all previous entries still intact.

Managing Units

When solving an equation, **UNITS** (a toggle key) controls whether the calculations are performed in your choice of units, or in *Systeme Internationale d'Unites* (SI) units. When the **UNITS** softkey appears, it means that all entries are converted to SI units and the unit designations are removed. **UNITS** indicates that the software is managing units, and that all values will contain the unit designations that you specify. *All values entered without unit designations are assumed to be in (SI) units.*

Note: Using designated units usually increases processing time.

Solving Multiple Equations

For many problems, the result of one calculation acts as the input to another. The Mechanical Engineering Application Pac is capable of solving multiple equations systematically.

Selecting the Equation Set

This example shows how to calculate the forces on an object moving in a fluid. From the Equation Library menu screen, move the pointer to FLUID MECHANICS and press ENTER. This category contains nine topics. Move the pointer to IMMERSED BODIES and press ENTER.

The equations for this topic are displayed on the screen:



These are the three equations in their written form:

$$Fd = \frac{Cd \cdot \rho \cdot V^2 \cdot A}{2} \qquad Fl = \frac{Cl \cdot \rho \cdot V^2 \cdot A}{2}$$
$$P = Fd \cdot V$$

To view the variables for this equation set, press **VARS**. All the variables for the IMMERSED BODIES topic are listed in the following table:

Variable	Description	Eqn Units
Fd	drag force	1 N
FI	lift force	1 [¯] N
Cd	drag coefficient	1
CI	lift coefficient	1
ρ	fluid density	1_kg/m ^ 3
V	fluid velocity	1_m/s
Α	area normal to flow	1_m^2
Р	power	1_W

Solving the Equation Set

At the equations screen, move the pointer to the first two equations and press the **SELECT** softkey to "tag" these equations to be solved. The following screen displays these two selected equations indicated by the triangular tags:

Immersed ▶FD=CD%/%V^2%A/2 ▶FL=CL%/%V^2%A/2 → P=FD%V	bodies	
MAIN SELECT VARS PI	OT SOLVE	UP

Press **SOLVE** to enter the solver function for these two equations. Enter all the information pertaining to the problem at one time, using the procedure described previously. Press **CALC** to start the solver. The solver then steps through each equation in the list, solving those equations that contain sufficient data to calculate an unknown variable. When all known variables are found, or all remaining equations have more than one unknown variable, the solver stops. It then lists the variables it can't find, and returns to the solver screen. The given variables and calculated results for both selected equations are shown below:

Tagging Variables

If you want to solve for only one variable in the list, you can tag it as "wanted." Move the pointer to the variable you want to tag, press with to display the additional softkeys for this screen, and press want. This places a "?" tag in front of the variable you want to solve for:

C EQNS VARS UNIT= >STK UP



If you tag Fl and press **CALC**, the solver stops when it finds a value for Fl, rather than solving for the entire set. It is possible to tag more than one variable in the list as "wanted."

Plotting One Equation

Any equation in the Equation Library that is of the form y = f(a,b,c...) can be easily plotted using the Mechanical Engineering Application Pac. To plot an equation, the dependent variable on the left (y) and the desired independent variable (a or b or c...) on the right side must be unknown (no triangular tag). However, all other variables must be known.

Finding and Selecting the Equation

As an example, plot the variation of drag force as a function of velocity. The equations that describe drag force are filed in the FLUID MECHANICS category, under the topic IMMERSED BODIES. Move the pointer to the first equation in the list and press **SELECT**. Press **ENTER** to view the written out form of the equation, or **VARS** to view the subset of variables for this equation. The equation and a table of its variables are shown below:

$$Fd = \frac{Cd \cdot \rho \cdot V^2 \cdot A}{2}$$

Variable	Description	Eqn Units
Fd	drag force	1 N
Cd	drag coefficient	1
ρ	fluid density	1_kg/m ^ 3
V	fluid velocity	1_m/s
A	area normal to flow	1_m ^ 2

Tagging and Entering the Variables

To plot the drag force curve (Fd versus V), Cd, ρ , and A must be tagged as known variables. Press **SOLVE** to specify values for the following known variables:

Cd = 0.4 ρ = 1.20_kg/m³ A = 1430.7068 ft²

With these three variables entered, return to the equations screen by pressing **ECNS**. Position the pointer at the first equation and press **PLOT**. Since this equation is of the proper form, and all but Fd and V have been specified, it may be plotted.

Entering the X and Y Coordinates

The first prompt asks whether you want to erase the previous plot and reset the axes, **YES**, or whether you want the new plot drawn over any existing graphics already on the screen, **NO**. To continue with this example, at the prompt enter **YES** to clear all previous plots from the screen.

Now enter the minimum and maximum values for the x coordinate for the graph. Type the coordinates for the plot on the same line, separated by a space (use the relation). For this example plot, select the no units option (**UNITS**), then enter 1 100 for V (the assumed units are _m/s). This results in the following screen:

{ HOME MEAPPD }	PRG
Enter horizontal m for V (m/s): <min> <max></max></min>	range
1 100♦ €skipiskip∋ €del (del⇒ (ins	D ASTK

The plot function now prompts for the limits of the y-axis (in this case, Fd, the drag force in _N units). You can either enter the lower and upper limits for y, or allow the system to auto range when ENTER is pressed. For this example, press ENTER to auto range a plot of Fd versus V over the range of 1 to 100_m/s, shown below:



Plotting Speed

If units are on (the **WNITE** key is displayed at the solver screen) a plot can take up to 10 minutes to display. If you turn the units off (i.e., toggle the units key to remove the box) the plot function performs in approximately one tenth of the time.

However, as described earlier in this chapter under "Managing Units," when you turn off units, all values are converted to SI units. Therefore, when you enter the x-axis coordinates, you need to enter them as low limit and upper limit. The plot will also be displayed in SI units.

Softkeys for the Plot Function

The softkeys shown in the above plot are plot function keys in the HP 48SX. For example, pressing **COCHD** displays the (x,y) coordinates of any point on the screen indicated by the cursor. For a description of the behavior of the plot function softkeys, see Chapter 18 of the HP 48SX Owner's Manual.

Note that the **SLOPE** and **F** keys, inside the HP 48SX **FCN** submenu, are supported by the Mechanical Engineering Application Pac only when units are off. You can remove the softkeys from the plot to expose more of the graph by pressing **MXT** and **KEYS**. Press **ATH** to interrupt the plotting of an equation or to return to the equation screen.

Multiple Plots

In some cases, you may want to graph several versions of an equation on the same axes. To do this, simply answer **NO** to the "Clear plot first?" prompt after you have pressed **PLOT**.

For example, suppose you are interested in plotting a new drag force curve for a higher density (e.g., $\rho = 2.4 \text{ kg/m}^3$). Return to the solver screen by pressing **SOLVE** and enter the new value for Fd. Then go to the equations screen, move the pointer to the drag force equation, and press **PLOT**. At the prompt, press **NO**. The new graph will plot over the previous one, as shown:



There is no limit to the number of graphs that may be plotted on a given axis. However, the HP 48SX plot/graphics function keys support only the most recent plot.

What You Should Know About the Solver

The examples in this chapter show how the Sparcom's solver makes it easy to specify values and units for equation variables. The solver screen displays the status of each variable in the selected equation set:

- Unknown value (no triangular tag)
- Known value (triangular tag)
- Wanted value ("?" tag)
- Calculated value ("*" tag)

Equation variables show units used by the user.

Once you set these parameters, pressing **CALC** activates the HP 48SX root-finder to calculate the solution(s). The root-finder requires an initial value on which to base its search. You can provide a "guess" for the calculator to use, or the solver will provide a "guess" value of 1. The root-finder then generates pairs of intermediate values and interpolates between them to find the solution. The time required to find the root depends on how close the initial guess is to the actual solution.

Speeding Up Computing Time

You can speed up computing time by providing the calculator a "guess" value close to the expected solution. At the variables screen, enter your guess value into the "unknown" variable. The variable will then be tagged as "known" (triangle). Press the **KNOW** softkey to toggle the variable back to "unknown" (no tag). Now press **CALC**.

"Bad Guess" Message

If the calculator displays the message, "Bad Guess(es)," after you press the **CALC** softkey, it indicates an error has been made in setting up the problem. Go back through the set up process and check for errors in the data specification.

We urge you to read Chapter 17 of the *HP 48SX Owner's Manual* for a detailed discussion on using the HP 48SX root finder function.

Loading Values from the Stack

There are two ways to enter a value into the Sparcom solver directly from the calculator stack:

First Method: Make sure the value you want is on the stack. Press MEAP, then choose an equation set to solve, or select RESUME SOLVING to return to the equation set you're working with. At the variables screen, move the pointer to the variable that will incorporate the value currently on the stack and press ENTER. A prompt message asks you to enter the value. Press for $\frac{1}{\sqrt{2}}$ to reveal the command line editing keys. Press the STK softkey to invoke a limited version of the HP 48SX Interactive Stack. Move the pointer to the appropriate stack level and press ECHO then ENTER. This takes you back to the "Enter value" prompt message. Press ENTER again to store the echoed value into the current variable and return to the solver screen.

Second Method: Alternatively, store the desired value into a global variable in the MEAPPD directory under the same name as the equation variable. When the solver is entered, it will automatically recall the value and load it into the selected equation variable. Remember to use the **KNOW** softkey to tag the variable as known.

Memory Requirements

The Mechanical Engineeering Application Pac requires some RAM memory in order to work. This memory is used for temporary storage, and for saving variables such as equations to be plotted later. You may encounter errors if the available memory is less than about 4000 bytes.

Sparcom's "MEAPPD" Directory

When you plug in the Mechanical Engineering Application Pac for the first time, the software creates its own directory, MEAPPD, in the HOME directory of the HP 48SX. ALL operations performed by the software take place in the MEAPPD directory. It is, therefore, the only place where global variables are created or purged by the solver. If you purge this directory by mistake, it will be recreated in its entirety, but all the values that you previously stored will be lost.

MEpar

The variable MEpar is created in the MEAPPD directory and is utilized to provide a direct path from the main menu to the solver level. MEpar is

created (or rewritten) whenever the equation, solver, or variable levels of the the Equation Library are exited.

There are three possible exit routes that trigger an MEpar update:

- 1) Pressing I to quit the software and exit to the calculator stack.
- 2) Pressing UP to return to the topic level.
- 3) Pressing MAIN to return to the main menu level.

Summary of Softkeys

- **CALC** Stores all variable values and iterates through the set of selected equations in an attempt to find values for all wanted variables. After completion of the solver process, the user is returned to the solver level, where newly found variables are marked with "*".
- **CLEAR** Resets the values of the current variable set to zero.
- **EONS** Enters the equation level of the current topic.
- FIGURE Displays a figure for the currently selected topic or displays "No figure".
- FONT Toggles between small and large display font.
- **KNOW** Toggles the currently selected variable between known and unknown, adding or removing the triangular tag.
- MAIN Returns to the main menu.
- **PLOT** Prompts the user for x-axis and y-axis values (with option for autoscale y). This feature only works for equations of the form y = f(a, b,) where y and one variable on the right are unknown.
- **PURGE** Purges the global copies (in the MEAPPD directory) of the current variable set displayed in the solver level.
- **QUIT** Exits the Mechanical Engineering Application Pac.

Getting Started

- **SELECT** Marks or unmarks the currently selected equation with the triangular tag. Only variables in the marked equations will appear in the solver and variable levels (with the exception of constants). If no equations are selected, all will be used.
- **SOLVE** Enters the solver level of the currrent topic, and executes SOLVE function on the tagged equations, or if none are tagged all equations are solved systematically
- **STK** Copies selected entry to calculator stack.
- **UNIT** Toggle key. Indicates that units are on.
- **UNITS** Toggle key. Indicates units are off. When off, all variables are assumed to be SI, if entered with no units, and are converted to SI units even if entered in other units.
- **UP** Moves up one level in the menu structure.
- VARS Enters the variable level for the current topic.
- **VIEW** Displays the full text entry for a variable description or value if the description is too wide to fit on the screen.
- **WANT** Toggles the currently selected variable between wanted and not wanted, adding or removing the symbol "?". If no variables are marked "wanted," all variables are assumed to be wanted.
- ENTERPrompts for the value of the currently selected variable. If
the selected variable already contains a value, that value is
copied to the command line for editing. PressingImage: Image: Image:
- This key is generally used to exit the current operation or application.
Summary of Functions

The following figure diagrams the basic flow and function of each level of the Equation Library and Sparcom solver. On the following page, the softkeys available at each level are explained in more detail.



Notes:

Chapter 2 Equation Library

In This Chapter

The Equation Library contains over 300 equations organized into eight main categories. Each category contains several topics. Each topic includes an equation set, a complete list of all variables, a full set of units for these variables. In addition to listing what is in the software, this chapter provides illustrations for several topics and at least one example for each equation set.

- Beams
- Fluid Mechanics
- Gas Laws
- Heat Transfer

Mechanics
Stress Analysis

□ Vibrations

Machine Design

Beams

The first two topics in this category focus on the computing properties of beams. The remaining topics cover load effects of simple and cantilever beams.

- Hollow Rectangle/I/C Beams
- L/T/U Beams
- Cantilever Beam-Point Load
- Cantilever Beam-Uniform Load
- Cantilever Beam-Moment
- Simple Beam-Point Load
- Simple Beam-Uniform Load
- Simple Beam-Moment
- Simple Beam-Linear Load

Hollow Rectangle/I/C Beams

This topic describes the cross-sectional properties of rectangular I and C sections. Properties computed include area of cross section, moment of

Equation Library

inertia, gyration radius, section modulus and distance of center of gravity from the top. The illustration below (not available in the software) shows the dimensional details.

1)
$$A = B \cdot H - bi \cdot hi$$

2) $y_1 = \frac{H}{2}$
3) $|x| = \frac{B \cdot H^3 - bi \cdot hi^3}{12}$
4) $r = \left(\frac{B \cdot H^3 - bi \cdot hi^3}{12 \cdot (B \cdot H - bi \cdot hi)}\right)^{v_2}$
5) $SM = \frac{B \cdot H^3 - bi \cdot hi^3}{6 \cdot H}$
Variable Description Eqn Units
A area of cross section 1 m^2
B outer width 1 m
bi inner width 1 m
H outer height 1 m
hi inner height 1 m
y1 distance/center of mass 1 m^2
 $|x|$ area moment 1 m^2
SM section modulus 1 m^3



Example: A hollow rectangular beam has an outer height of 6_in and an inner height of 12.5_cm. The inner and outer widths are 8_in and 24_cm. Find its section properties. Solve for all equations to get the results.

Given	Result
$B = 24$ _cm	$y1 = 0.07620_m$

.

L/T/U Beams

This equation set describes the cross-sectional properties of L, T and U beams. Properties include cross-sectional area, coordinates of the center of mass, area moment of inertia and the radius of gyration. The picture below illustrates the dimensional conventions for these beams.

1) Area =
$$B \cdot H - bi \cdot (H - d)$$
 2) $C1 = \frac{1}{2} \cdot \left(\frac{a \cdot H^2 + bi \cdot d^2}{a \cdot H + bi \cdot d}\right)$

3) C2 = H - C1
4)
$$Ix = \frac{1}{3} \cdot (B \cdot C1^3 - bi \cdot hi^3 + a \cdot C2^3)$$

5)
$$r = \left(\frac{lx}{B \cdot d + a \cdot (H - d)}\right)^{v_2}$$

Variable	Description	Eqn Units
Area	area of cross section	1_m^2
В	overall width	1_m
bi	inner width	1_m
Н	overall height	1_m
hi	CM distance from flange top	1_m
d	flange thickness	1_m
C1	CM distance from top	1_m
C2	CM distance from bottom	1_m
а	side thickness	1_m
lx	area moment of cross section	1_m^4
r	gyration radius	1_m



Example: A U beam has an outer width of 8_in, an inner width of 6_in, an outer height of 6_in and a flange thickness of 4_cm. The center of mass line is located 1_cm away from the inner flange plane. Find the section properties. Using all the equations in the set we get:

Given	Result
$B = 8_{in}$	Area = 0.0138_m^2
bi = 6_in	C1 = 0.04183 m
$H = 6_{in}$	C2 = 0.1106 m
$hi = 1_cm$	$lx = 1.6352E-5_m^4$
a = 1_in	r = 3.859E-2_m
$d = 4_cm$	

Cantilever Beam-Point Load

The four equations listed here describe deflection, slope at any point along the beam, and specifically, deflection and slope at the free end of a cantilever beam with a point load.

These equations assume that the beam weight is negligible. Only one point load is allowed in the equation set, and the superposition principle should be applied if more than one point load is to be considered. The illustration shows details of the problem set up.

1)
$$v = \frac{P \cdot x^2}{6 \cdot E \cdot I} \cdot (3 \cdot a - x)$$
 2) $v_1 = \frac{P \cdot x}{2 \cdot E \cdot I} \cdot (2 \cdot a - x)$

3) <i>δb</i>	$= \frac{P \cdot a^2}{6 \cdot E \cdot I} \cdot (3 \cdot L - a)$	$4) \Theta b = \frac{P}{2 \cdot i}$	a² E · I
Variable	Description		Eqn Units
v	deflection at x		1_m
v1	slope at x		1
Р	load		1_N
x	distance from fixed end		1_m
a	load location from fixed e	nd	1_m
L	beam length		1_m
E	Young's modulus		1 Pa
I	area moment of inertia		1_m^4
δb	displacement at free end		1_m
Θb	angle at free end		1_°

Example: A 25-foot-long cantilever beam has a point load of 10000_lbf at a distance of 17_ft from the fixed end. Find the deflection at the load point, and the deflection and slope at the free end. Assume $E = 30 \times 10^{6}$ psi and I = 1880 in ^ 4.

Given	Result
$P = 10000_lbf$	$v = 1.2745E-2_m$
a = 17_ft	$\delta b = 2.1741 E_{-2}m$
$L = 25_{ft}$	$\Theta b = 0.2114^{\circ}$
E = 30E6_psi	
l = 1880_in ^ 4	
$x = 17_{ft}$	

Cantilever Beam-Uniform Load

The four equations listed here describe deflection, slope at any point along the beam, and specifically deflection and slope at the free end of a cantilever beam with a uniform load.

Beam weight can be included in the uniformly distributed load. The illustration below shows details of the beam for this load condition.

1)
$$v = \frac{w \cdot x^2}{24 \cdot E \cdot l} \cdot (6 \cdot L^2 - 4 \cdot L \cdot x + x^2)$$

2) $v_1 = \frac{w \cdot x}{6 \cdot E \cdot l} \cdot (3 \cdot L^2 - 3 \cdot L \cdot x + x^2)$
3) $\delta b = \frac{w \cdot L^4}{8 \cdot E \cdot l}$
4) $\Theta b = \frac{w \cdot L^3}{6 \cdot E \cdot l}$
Variable Description Eqn Units
v deflection at x 1_m
v1 slope at x 1
w uniform load 1_m
L beam length 1_m
E Young's modulus 1_Pa
I area moment 1_m^4

angle at free end Θb



Example: A 25-foot-long cantilever beam has a uniformly distributed load of 200_lb/m. The Young's modulus for the beam material is 10×10^{6} psi, and has an area moment of 180 in ^4. Find the maximum deflection and slope at the free end.

Given	Result
w = 200 lbf/m	$\delta b = 0.0726 m$
L = 25 ft	$\Theta b = 0.7277^{\circ}$
$E = 10\overline{E}6_{psi}$	_
$l = 180 \text{ in } ^4$	

1⁻°

L

L

Cantilever Beam-Moment

These equations describe deflection, slope at any point along the beam, and specifically deflection and slope at the free end of a cantilever beam for a moment applied at a distance a from the clamped end. These equations assume that the beam weight is negligible.

1) $v = \frac{M0 \cdot a}{2 \cdot E \cdot I} \cdot (2 \cdot x - a)$	2) $v1 = \frac{M0 \cdot x}{E \cdot I}$
---	--

2١	sh	_	$M0 \cdot a$	2)	۸)	Qh	_	<i>M</i> 0	•	а
3)	00	_	$2 \cdot E \cdot 1$	- a)	4)	90	-	Ε	•	I

Variable	Description	Eqn Units
v	deflection at x	1_m
v1	slope at x	1
MO	moment	1_N∙m
x	distance from fixed end	1_m
а	location of M0 from fixed end	1_m
L	length of beam	1_m
E	Young's modulus	1_Pa
1	area moment	1_m^4
δb	displacement at free end	1_m
Θb	angle at free end	1_°



Example: Using the cantilever beam described in the previous example, suppose you have a moment M0 at a distance of 16_ft from the free end with a value of $17600_N \cdot m$. Find the deflection and slope at the free end.

Given	Result
$M0 = 17600 N \cdot m$	$\delta b = 8.6096E-2_m$
a = 16_ft	$\Theta b = 0.9520^{\circ}$
L = 25_ft	
E = 10E6_psi	
$I = 180 \text{ in}^{4}$	

Simple Beam-Point Load

The seven equations in this set describe deflection slope at any location along the beam, slope at either end of the beam, location maximum deflection, and value of maximum deflection. The assumed load condition is a point load. Additional assumptions include negligible weight contribution from the beam.

1)	$v = \frac{P \cdot b \cdot x}{6 \cdot E \cdot L \cdot I} \cdot \left(L^2 - b^2 - x^2\right)$)	
2)	$v1 = \frac{P \cdot b}{6 \cdot E \cdot L \cdot I} \cdot \left(L^2 - b^2 - 3\right)$	$\cdot x^2$	
3)	$\Theta a = \frac{P \cdot a \cdot b \cdot (L + b)}{6 \cdot L \cdot E \cdot 1}$	4) $\Theta b = \frac{P \cdot a \cdot b}{6 \cdot L}$	· (L + a) · E · I
5)	$\delta c = \frac{P \cdot b \cdot (3 \cdot L^2 - 4 \cdot b^2)}{48 \cdot E \cdot 1}$	$6) x1 = \left(\frac{L^2 - b^2}{3}\right)$) ^{1⁄2}
7)	$\delta \max = \frac{P \cdot b \cdot (L^2 - b^2)^{3/2}}{9 \cdot \sqrt{3} \cdot L \cdot E \cdot 1}$		
Variat	ble Description	Eq	n Units
Variat ∨	ble Description deflection at x	Eq 1 r	n Units m
Variat v v1	ble Description deflection at x slope at x	Eq 1_r 1	n Units m
Variat v v1 P	ble Description deflection at x slope at x uniform load	Eq 1_r 1	n Units m N
Variat v v1 P x	ble Description deflection at x slope at x uniform load distance from fixed end	Eq 1_r 1 1_1 1_1	n Units m N
Variat v v1 P x a	ble Description deflection at x slope at x uniform load distance from fixed end location from end	Eq 1_r 1_ 1_1 1_r 1_r	n Units m N m m
Variat V V1 P X a L	ble Description deflection at x slope at x uniform load distance from fixed end location from end beam length	Eq 1_r 1_ 1_1 1_r 1_r 1_r	n Units ກ N ກ ກ
Variat V V1 P X a L E	ble Description deflection at x slope at x uniform load distance from fixed end location from end beam length Young's modulus	Eq 1_r 1 1_1 1_r 1_r 1_r 1_r	n Units n N n n n Pa
Variat V V1 P X a L E I	ble Description deflection at x slope at x uniform load distance from fixed end location from end beam length Young's modulus area moment	Eq 1_r 1 1_! 1_! 1_r 1_r 1_r 1_r	n Units m N m m Pa m^4
Variat V V1 P x a L E I Øa	ble Description deflection at x slope at x uniform load distance from fixed end location from end beam length Young's modulus area moment angle at left end	Eq 1_r 1 1_1 1_r 1_r 1_r 1_r 1_r 1_r	n Units m N m n Pa m ^ 4
Variat ∨ V1 P X a L E I Øa Øb	ble Description deflection at x slope at x uniform load distance from fixed end location from end beam length Young's modulus area moment angle at left end angle at right end	Eq 1_r 1 1_1 1_r 1_r 1_r 1_r 1_r 1_° 1_°	n Units m M m m a n^4
Variat ∨ V1 P x a L E I Ø b x1	ble Description deflection at x slope at x uniform load distance from fixed end location from end beam length Young's modulus area moment angle at left end angle at right end distance to maximum de	Eq 1_r 1_1 1_1 1_r 1_r 1_r 1_r 1_° 1_° 1_°	n Units m m m n Pa m ^ 4 m
Variat v v1 P x a L E I Θa Θb x1 δc	ble Description deflection at x slope at x uniform load distance from fixed end location from end beam length Young's modulus area moment angle at left end angle at right end distance to maximum de deflection at center	Eq 1_r 1 1_1 1_r 1_r 1_r 1_r 1_r 1_° 1_° 1_° 1_r 1_° 1_° 1_r 1_r 1_°	n Units n N n n Pa n ^ 4 n n
Variat V V1 P x a L E I Θa Θb x1 δc δmax	ble Description deflection at x slope at x uniform load distance from fixed end location from end beam length Young's modulus area moment angle at left end angle at right end distance to maximum de deflection at center maximum deflection	Eq 1_r 1 1_1 1_r 1_r 1_r 1_r 1_r 1_° 1_° 1_r 1_r 1_r 1_r 1_r 1_r	n Units n N n n Pa n^4 n n n



Example: A simple beam 20_ft long has a point load of 2500_lbf at a distance of 12_ft from the left support. Compute deflection at center, maximum deflection, and end slopes. Use 30_GPa for E and 140_in ^4 for I. Use equations 3, 4, 5, 6 and 7 to solve the problem.

Given	Result
$P = 2500$ _lbf	δc = 2.83401E-2_m
a = 12_ft	$\delta max = 2.8468E-2_m$
L = 20 ft	$\Theta a = 0.7585^{\circ}$
E = 30 GPa	$\Theta b = 0.8668^{\circ}$
$I = 140_{in}^{4}$	x1 = 3.2257 m
b = 8 ft	

Simple Beam-Uniform Load

These five equations describe deflection, slope along any location along the beam, slope at either end of the beam, and value of maximum deflection. The assumed load condition is a uniformly distributed load. Effect of beam weight can be included in the load conditions if necessary.

1)
$$v = \frac{w \cdot x}{24 \cdot E \cdot 1} \cdot (L^3 - 2 \cdot L \cdot x^2 - x^3)$$

2) $v_1 = \frac{w}{24 \cdot E \cdot 1} \cdot (L^3 - 6 \cdot L \cdot x^2 - 4 \cdot x^3)$
3) $\Theta a = \frac{w \cdot L^3}{24 \cdot E \cdot 1}$
4) $\Theta b = \Theta a$
5) $\delta \max = \frac{5 \cdot w \cdot L^4}{384 \cdot E \cdot 1}$

Mechanical Engr. Pac

Variable	Description	Eqn Units
v	deflection at x	1_m
v1	slope at x	1
w	distributed load	1_N/m
x	distance from fixed end	1_m
L	beam length	1_m
E	Young's modulus	1_Pa
1	area moment	1_m^4
Θa	angle at left end	1_°
Θb	angle at right end	1_°
δmax	deflection at center	1_m



Example: A 20_ft simple beam is subjected to a uniformly distributed load of 100_N/ft. The beam is made of a material with an elastic modulus of 30 x 10^6_psi and has a moment of inertia of 210_in^4. Find the maximum deflection and slope at either end. Use equations 3-5 to solve the problem.

Given	Result
w = 100 N/ft	∂max = 3.2629E-4_m
L = 20 ft	Θa = 0.0098_°
$E = 30E6_{psi}$	$\Theta b = 0.0098^{\circ}$
$I = 210_{in}^{-4}$	_

Simple Beam-Moment

This equation set describes deflection, slope along any location along the beam, and slope at either end of the beam. The load condition assumed here is a moment located at a distance a from the fixed end of the beam. The calculations are made assuming contributions from the load. No other loads are considered in this computation.

Equation Library

1)
$$v = \frac{M0 \cdot x}{6 \cdot L \cdot E \cdot 1} \cdot (6 \cdot a \cdot L - 3 \cdot a^2 - 2 \cdot L^2 - x^2)$$

2) $v_1 = \frac{M0}{6 \cdot L \cdot E \cdot 1} \cdot (6 \cdot a \cdot L - 3 \cdot a^2 - 2 \cdot L^2 - 3 \cdot x^2)$

3)
$$\Theta a = \frac{M0}{6 \cdot L \cdot E \cdot I} \cdot (6 \cdot a \cdot L - 3 \cdot a^2 - 2 \cdot L^2)$$

4)
$$\Theta b = \frac{M0}{6 \cdot L \cdot E \cdot I} \cdot (3 \cdot a^2 - L^2)$$

Variable	Description	Eqn Units
v	deflection at x	1_m
v1	slope at x	1
MO	moment	1_N∙m
x	distance from fixed end	1_m
а	location of load from left end	1_m
L	beam length	1_m
E	Young's modulus	1_Pa
1	area moment	1_m^4
Θa	angle at left end	1_°
Θb	angle at right end	1_°



Example: A 20_ft long simple beam has a moment of $2600_N \cdot m$ applied 11_ft from the left end. The beam has a moment of inertia of 210_in^4 and an elastic modulus of 30_GPa. Find the slopes at either end.

Given
$M0 = 2600 N \cdot m$
a = 11_ft
L = 20 ft

Result $\Theta a = 2.2654E-2_{O}^{\circ}$ $\Theta b = -5.339E-3_{O}^{\circ}$

$$E = 30_GPa$$
$$I = 210_in^4$$

Simple Beam-Linear Load

The seven equations in this set focus on deflection, slope at any location along the beam, slope at either end of the beam, and the location and value of maximum deflection. The assumed load is uniformly increasing from 0 at the fixed end to a value w0 at the freely supported end.

1)
$$v = \frac{w0 \cdot x}{360 \cdot E \cdot L \cdot 1} \cdot (7 \cdot L^4 - 10 \cdot L^2 \cdot x^2 + 3 \cdot x^4)$$

2) $v1 = \frac{w0}{360 \cdot E \cdot L \cdot 1} \cdot (7 \cdot L^4 - 30 \cdot L^2 \cdot x^2 + 15 \cdot x^4)$
3) $\delta c = \frac{5 \cdot w0 \cdot L^4}{768 \cdot E \cdot 1}$
4) $\delta \max = .00652 \cdot \left(\frac{w0 \cdot L^4}{E \cdot 1}\right)$
5) $\Theta a = \frac{7 \cdot w0 \cdot L^3}{360 \cdot E \cdot 1}$
6) $\Theta b = \frac{w0 \cdot L^3}{45 \cdot E \cdot 1}$

7) $x_1 = .5193 \cdot L$

Variable	Description	Eqn Units
v	deflection at x	1_m
v1	slope at x	1
w0	load rate at free end	1_N/m
x	distance from fixed end	1_m
L	beam length	1_m
E	Young's modulus	1_Pa
1	area moment	1_m^4
Θa	angle at left end	1_°
Θb	angle at right end	1_°
x1	distance to maximum deflection	1_m
δς	deflection at center	1_m
δmax	maximum deflection	1_m



Example: A 20_ft long simple beam has a linear load increasing from 0 at one end to 1000_lbf/m at the other. Find the maximum slope at either end, given an elastic modulus of 30_GPa and an area moment of 210_in ^4. Use equations 4-6 to solve the problem.

Given

 $w0 = 1000_lbf/m$ $L = 20_ft$ $E = 30_GPa$ $I = 210_in ^ 4$

Result

 $\Theta a = 0.4281_{\circ}$ $\Theta b = 0.4893_{\circ}$ $\delta max = 0.01527_{m}$

Fluid Mechanics

In this category, fundamental fluid flow equations are contained in the following topics:

- Fluid Statics
- Bernoulli's Equation
- Mechanical Energy Balance
- Discharge from Tanks
- Horizontal Jet on Vertical Plate
- Vertical Jet on Horizontal Plate
- Manometers
- Friction Loss
- Immersed Bodies

Fluid Statics

These equations describe static fluids when in equilibrium, $\Sigma F = 0$. The pressure-at-depth equation (1) is for constant density (incompressible) fluids. The barometric equation (2) is used for an isothermal perfect gas.

1)
$$P2 = P1 + \rho \cdot g \cdot (h1 - h2)$$

2)
$$P = Patm \cdot e^{-\left(\frac{MWT \cdot g \cdot h}{R \cdot T}\right)}$$

Variable	Description	Eqn Units
Р	pressure	1 Pa
P1	pressure at point 1	1 [¯] Pa
P2	pressure at point 2	1_Pa
Patm	pressure at reference level	1 Pa
ρ	density of fluid	1_kg/m ^ 3
ĥ	height above reference level	1_m
h1	height at point 1	1_m
h2	height at point 2	1_m
т	temperature	1_K
MWT	molecular weight of gas	1_kg/mol



Example 1: Use equation 1 to find the pressure at the bottom of a full, 5-foot-high tank of ethylene glycol.

GivenResultP1 = 14.7_psiP2 = 17.1125_psi $\rho = 69.48_lb/ft^3$ h1 = 5_fth2 = 0_fth2 = 0_ft

Example 2: What is the pressure of air (average molecular weight = $29_g/mol$) at a height of 1.0 mile above sea level? Plot the pressure of air versus height above sea level. (Assume T = 59 °F, neglect temperature gradient). Use second equation.

Given Patm = 14.696_psi T = 59_°F MWT = 29_g/mol h = 1.0_mi **Result** P = 12.1419_psi

Plotting the barometric equation yields: (be sure to unmark the variable "h" prior to generating this plot)

x1 = 0x2 = 20y1 = -2y2 = 16



Bernoulli's Equation

A frictionless, streamlined flow of an incompressible fluid obeys Bernoulli's equation if no shaft work is performed.

1)
$$\frac{\Delta P}{\rho} + \frac{V2^2 - V1^2}{2} + g \cdot \Delta h = 0$$

2)
$$V1^2 \cdot \left(1 - \left(\frac{A1}{A2}\right)^2\right) = 2 \cdot \left(\frac{\Delta P}{\rho} + g \cdot \Delta h\right)$$

3)
$$V2^2 \cdot \left(\left(\frac{A2}{A1}\right)^2 - 1\right) = 2 \cdot \left(\frac{\Delta P}{\rho} + g \cdot \Delta h\right)$$

4)
$$\Delta h = h2 - h1 \quad 5) \quad \Delta P = P2 - P1 \quad 6) \quad Q = A1 \cdot V1$$

7)
$$Q = A2 \cdot V2 \quad 8) \quad M = \rho \cdot Q \quad 9) \quad A1 = \frac{\pi \cdot D1^2}{4}$$

10) A2 =
$$\frac{\pi \cdot D2^2}{4}$$

Variable	Description	Eqn Units
ΔP	pressure difference	1 Pa
P1	pressure at point 1	1_Pa
P2	pressure at point 2	1_Pa
ρ	density of fluid	1_kg/m ^ 3
V1	velocity at point 1	1_m/s
V2	velocity at point 2	1_m/s
Δh	height difference	1_m
h1	height at point 1	1_m
h2	height at point 2	1_m
A1	cross section area at point 1	1_m^2

A2	cross section area at point 2	1 m^2
Q	volumetric flow rate	1 m ^ 3/s
М	mass flow rate	1 kg/s
D1	pipe diameter at point 1	1 m
D2	pipe diameter at point 2	1 ⁻ m

Example: A Venturi meter reading gives a pressure drop in a pipe 12.3_psi from point (1) to point (2).



The throat's (point 2) cross sectional area is known to be .0513_ft ^2 and the volumetric flow rate at point 1 is 1000_gal/min. What is the cross sectional area of the pipe at point 1? (ρ H₂O = 62.43_lb/ft ^3). Use equations 1 and 2, and 6-10.

Given	Result
A2 = .0513_ft ^ 2	$A1 = 0.2861_{ft}^{2}$
∆P = -12.3_psi	V1 = 7.7866 ft/s
$\rho = 62.43 _ lb/ft^3$	V2 = 43.4309 ft/s
$\Delta h = 0_m$	D1 = 7.2430_in
$Q = 1000_gal/min$	$D2 = 3.067$ _in
	M = 139.0946 lb/s

Mechanical Energy Balance

The mechanical energy balance equation is valid for flow of an incompressible fluid where friction from fluid movement is included. Heat loss and internal energy changes from non-friction sources are neglected.

1)
$$\frac{\Delta P}{\rho} + \frac{V2^2 - V1^2}{2} + g \cdot \Delta h + F = \frac{Ws}{M}$$

2)
$$V1^2 \cdot \left(1 - \left(\frac{A1}{A2}\right)^2\right) = 2 \cdot \left(\frac{\Delta P}{\rho} + g \cdot \Delta h + F - \frac{Ws}{M}\right)$$

Mechanical Engr. Pac

3)
$$V2^2 \cdot \left(\left(\frac{A2}{A1}\right)^2 - 1\right) = 2 \cdot \left(\frac{\Delta P}{\rho} + g \cdot \Delta h + F - \frac{Ws}{M}\right)$$

4) $\Delta h = h2 - h1$ 5) $\Delta P = P2 - P1$ 6) $Q = A1 \cdot V1$
7) $Q = A2 \cdot V2$ 8) $M = \rho \cdot Q$ 9) $A1 = \frac{\pi \cdot D1^2}{4}$

10) A2 =
$$\frac{\pi \cdot D2^2}{4}$$

Variable	Description	Eqn Units
ΔP	pressure difference	1 Pa
P1	pressure at point 1	1_Pa
P2	pressure at point 2	1_Pa
ρ	density of fluid	1_kg/m^3
V1	velocity at point 1	1_m/s
V2	velocity at point 2	1_m/s
Δh	height difference	1_m
h1	height at point 1	1_m
h2	height at point 2	1_m
A1	cross section area at point 1	1_m^2
A2	cross section area at point 2	1_m^2
Q	volumetric flow rate	1_m^3/s
М	mass flow rate	1_kg/s
D1	pipe diameter at point 1	1_m
D2	pipe diameter at point 2	1_m
F	friction loss from pipe (head loss)	1_m^2/s^2
Ws	shaft work	1_W

Example: A lake supplies water for a turbine to generate energy. The same diameter pipe is used from lake to discharge (V1 = V2). At 400 feet above the turbine, the pressure is 37_psi, and at the discharge point the pressure is 16_psi. The discharge point is 20_ft below the turbine. ρ H₂O = 62.3_lb/ft^3.



What is the friction loss from the pipe? Choose an arbitrary value for V1 and set V2 to V1. Use equations 1, 4 and 5.

Given V1 = 10 m/sV2 = 10 m/sP2 = 16 psiP1 = 37 psi $\rho = 62.3 \text{ lb/ft}^3$ h2 = -420 fth1 = 0 ft Ws = -987 hpM = 1521 lb/s

Result $F = 111.6353 \text{ ft} \cdot \text{lbf/lb}$ $\Delta P = -21 \text{ psi}$ $\Delta h = -420 \text{ ft}$

Discharge from Tanks

The configuration and area of an orifice determine water discharge parameters, such as velocity, volumetric flow rate and time to empty. The equations for this section assume a constant area tank filled with water with only one nozzle and no influx of water during discharge.

- 2) $Cv = \frac{Cd}{Cc}$ 1) $V = Cv \cdot \sqrt{2 \cdot q \cdot h}$
- 3) $Q = Cc \cdot A0 \cdot Cv \cdot \sqrt{2 \cdot q \cdot h}$
- 4) $Q = Cd \cdot A0 \cdot \sqrt{2 \cdot q \cdot h}$ 5

6)
$$t = \frac{2 \cdot At \cdot (\sqrt{h10} - \sqrt{h20})}{Cd \cdot A0 \cdot \sqrt{2 \cdot g}}$$

5) ghead =
$$\frac{Pgage}{\rho \cdot g}$$

7)
$$h10 = h1 + ghead$$

8) h20 = h2 + ghead

Variable	Description	Eqn Units
V	orifice velocity	1_m/s
ghead	gauge pressure head	1_m
h1	tank water height 1	1_m
h2	tank water height 2	1_m
h10	tank static head 1	1_m
h20	tank static head 2	1_m
A0	orifice area	1_m^2
At	tank cross section area	1_m^2
Cv	velocity coefficient	1
Cd	discharge coefficient	1
Cc	contraction coefficient	1
t	discharge time	1_s
h	fluid height	1_m
Q	volumetric flow rate	1_m^3/s
Pgage	gauge pressure	1_Pa
ρ	density of fluid	1_kg/m^3



Example: A constant gauge pressure of 30_psi is used to empty a tank of water. The tank has a smooth, well-tapered nozzle, a height of 10_ft and a constant cross sectional area of 37.5_{ft}^2 . The density of H₂O is 62.43_lb/ft^3. How long will it take to empty the tank? The orifice cross sectional area is .00351_ft^2. Use the entire equation set.

Appropriate discharge coefficients can be found in the reference section of this software. See Chapter 5.

Given	Result
At = 37.5_ft^2	h10 = 79.1976_ft
$A0 = .00351_{ft}^{2}$	$h20 = 69.1976_{ft}$
$\rho = 62.43 \text{ lb/ft}^3$	ghead = 69.1976_ft
Pgage = 30_psi	t = 1562.7_sec

Horizontal Jet on Vertical Plate

This equation adapts the linear momentum equation:

$$F = \frac{d (M \cdot V)}{dt}$$

for a horizontal jet hitting a vertical plate. The horizontal jet is assumed to have a uniform velocity distribution and hits the surface of the plate normally. Thus, there is no y direction force, only x direction.

$$Fx = -\rho \cdot (Vjet + Vplate)^2 \cdot A$$

Variable	Description	Eqn Units
Fx	plate force	1_N
ρ	fluid density	1_kg/m^3
Vjet	jet velocity	1_m/s
Vplate	plate velocity	1_m/s
Α	area normal to flow	1_m^2



Example: Beaver Cleaver sticks his hand out of the window of Ward's souped-up '57 Bel Air. The velocity of the Bel Air is 110_mph. Assuming Beaver holds his hand normal to the flow of the air, what is the force on Beaver's hand? The area of Beaver's hand is 15_{in}^{2} , ρ of air at 20_{c}° = 1.204 kg/m³ and the air is static.

Given

 $\rho = 1.204 kg/m^3$ Vjet = 0_mph Vplate = 110_mph **Result** Fx = -6.334 [bf

 $A = 15 \text{ in } ^2$

Vertical Jet on Horizontal Plate

The equations below adapt the linear motion equation,

$$F = \frac{d (M \cdot V)}{dt}$$

for a vertical jet hitting a horizontal plate. In the case of an equilibrium height of a plate with a weight, the Bernoulli, momentum, and continuity equations are combined to define "heq" in terms of initial nozzle velocity.

1)
$$Fy = -\rho \cdot V0 \cdot A0 \cdot \sqrt{V0^2 - 2 \cdot g \cdot h}$$

2) $heq = \frac{V0^2}{2 \cdot g} - \frac{1}{2 \cdot g} \cdot \left(\left(\frac{M \cdot g}{\rho \cdot A0 \cdot V0} \right)^2 \right)$

3)
$$A0 = \frac{\pi}{4} \cdot D0^2$$

Variable	Description	Eqn Units
Fy	Y direction force	1 N
ρ	fluid density	1_kg/m ^ 3
V0	initial fluid velocity	1_m/s
A0	fluid area	1_m^2
h	height from nozzle	1_m
heq	height at equilibrium	1_m
M	mass of plate and weight	1_kg
D0	nozzle diameter	1_m



Example: A plate weighs 50 pounds and is supported by a vertical jet of water. The exit diameter of the nozzle is 4 inches and the velocity at the nozzle is $30_{ff/sec}$. The water density is $998.3_{kg/m}^3$. What is the equilibrium height of the board? Use equations 2 and 3.

Given $V0 = 30_{ft/sec}$ $D0 = 4_{in}$ $M = 50_{lb}$ $\rho = 998.3_{kg/m}^{3}$ Result heq = 12.4757_ft A0 = 12.5663_in ^2

Manometers

This topic includes equations 1 and 2 for general manaometers, and equations 3 and 4 for differential manaometers.

1) $\Delta p = \rho \mathbf{1} \cdot g \cdot d\mathbf{1} - \rho \mathbf{2} \cdot g \cdot d\mathbf{2} - \rho f \cdot g \cdot h$ 2) $\Delta p = (\rho - \rho f) \cdot g \cdot h$ 3) $\Delta p = p\mathbf{2} - p\mathbf{1}$

4))	ρf	=	SP	GR	•	ρ H2O
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Variable	Description	Eqn Units
p1	point 1 pressure	1_Pa
p2	point 2 pressure	1_Pa
Δр	pressure difference	1_Pa
ρ1	fluid density point 1	1_kg/m^3
ρ2	fluid density point 2	1_kg/m^3
ρf	manometer fluid density	1_kg/m^3
d1	manometer fluid depression 1	1_m
d2	manometer fluid depression 2	1_m
h	manometer fluid height difference	1_m
SPGR	specific gravity ratio	1
ρ	fluid density $1 = 2$	1_kg/m^3





Example: A differential manometer is used to measure pressure drop in a pipe line. Mercury is used as the manometer fluid has a SPGR = 13.546. The relative difference between the first and second arm is 3.0 inches. What is the pressure drop if water at 20_°C is flowing through the pipe? Use equations 3 and 4.

Given	Result
SPGR = 13.546	Δp = -1.36_psi
h = 3.0_in	$\rho f = 845.67 \text{ [b/ft}^3$
$\rho = 62.19 \text{ lb/ft}^3$	

Friction Loss

The following equations allow for the measurement of kinetic or potential energy that is converted to thermal energy. The equations apply to a round pipe that is in full flow. The fluid must be incompressible and heat losses and internal energy change due to anything but friction are negligible. (This equation set uses the DARCY friction factor function).

1)
$$FL = \frac{f \cdot L \cdot Vavg^2}{2 \cdot D} + \frac{Ksum \cdot Vavg^2}{2}$$

2) $Le = \frac{2 \cdot FL \cdot D}{f \cdot Vavg^2}$
3) $Re = \frac{\rho \cdot Vavg \cdot D}{\mu}$
4) $J = \frac{\mu}{\rho}$
5) $Q = Vavg \cdot A$
6) $Re = \frac{Vavg \cdot D}{J}$
7) $D = \sqrt{(4 \cdot A)/\pi}$

8) $f = DARCY(Re, \varepsilon, D)$

Variable	Description	Eqn Units
FL	friction loss	1_m^2/s^2
f	DARCY friction factor	1
L	pipe length	1_m
Vavg	average velocity	1_m/s
D	pipe internal diameter	1_m
ε	pipe roughness	1_m
Re	Reynold's number	1
Le	equivalent length	1_m
Ksum	summation of minor loss items	1
Q	volumetric flow rate	1_m^3/s
ρ	fluid density	1_kg/m ^ 3
J	kinematic viscosity	1_m^2/s
Α	cross section area	1_m^2
μ	dynamic viscosity	1_Pa ⋅ s



Example: Given the picture above, what is the equivalent length of a straight pipe with the same flow rate, friction factor and heat loss? Use all the equations to solve the problem.

Appropriate minor loss values are listed in the reference section of this software. See Chapter 5.

GivenResultL = 105_ftLe = 220.Ksum = 9FL = 103.Q = 80_gal/minf = .01990D = 3.068_in Re = 824 ρ = $62.3_lb/ft^3$ A = 4.769 ε = .020_mmJ = $1.00 \times 10^{-}6_m^{-}2/s$

Result Le = 220.5985_{ft} FL = $103.5144_{ft}^2/s^2$ f = .019905Re = 82465.6171A = $4.769 E-3_{m}^2$

Immersed Bodies

Lift and drag forces act upon an object as it moves through a fluid such as air. The equations below assume that the fluid flow behind the object is turbulent.

1) <i>Fd</i> =	$\frac{Cd \cdot \rho \cdot V^2 \cdot A}{2}$	2) $Fl = \frac{Cl \cdot \rho \cdot V^2 \cdot A}{2}$
3) P =	Fd·V	
Variable	Description	Eqn Units
Fd	drag force	1 N
FI	lift force	1 ⁻ N
Cd	drag coefficient	1
CI	lift coefficient	1
ρ	fluid density	1 kg/m^3
v	fluid velocity	1_m/s
Α	area normal to flow	1 ⁻ m^2
Р	power	1 [¯] W

Example: John J. Gorilla, golf's long drive champion, wants to know the amount of power needed for his standard long drive. Calculate the drag force and power needed to overcome aerodynamic drag just after impact.

Given

 $\rho = 1.204_kg/m^3$ Cd = 0.40 A = 0.01539_ft^2 V = 100_mph **Result** Fd = .1547_lbf P = 0.0412 hp

Gas Laws

The equations in this topic describe the pressure, volume, temperature and thermodynamic relationships of ideal gases. Z-factor equations for a real gas are also included. Note that all equations in this section presume values for work and heat on a mass basis, thus: W = 3.4 Btu/lb or Q = 5 J/kg. These equations are included under the following seven topics:

- Ideal Gas Laws
- Gas-Constant Pressure
- Gas-Constant Volume
- Gas-Constant Temperature
- Thermodymanics/Ideal Gas Law
- Real Gas Law
- Polytropic Process

Ideal Gas Laws

The behavior of an ideal gas can be described by the equations below.

2) $p \cdot V = n \cdot R \cdot T$ 1) $p \cdot Vs = RG \cdot T$ 3) $RG = \frac{R}{MWT}$ 4) $V = Vs \cdot m$ 5) $m = n \cdot MWT$ 6) Cp - Cv = RG7) $Cp = \frac{k \cdot RG}{k-1}$ 8) $Cv = \frac{RG}{k-1}$ 9) $k = \frac{Cp}{Cv}$ Egn Units Variable Description 1 Pa pressure p $1 \text{ m}^3/\text{kg}$ Vs specific volume 1_J/(kg ⋅ K) RG specific gas constant temperature 1 K

volume

Т

v

1 m^3

n	number of moles	1_mol
MWT	molecular weight	1_kg/mol
m	mass of gas	1_kg
Ср	specific heat constant pressure	1_J/(kg⋅K)
Cv	specific heat constant volume	1_J/(kg⋅K)
k	specific heat ratio	1

Example: Calculate the mass of CO₂ in a 500_ft 3 tank, if the pressure is 14.696_psi and the temperature is 68_°F. The molecular weight of CO₂ is 44.01. Use equations 2-5.

Given	Result
$V = 500_{ft}^{3}$	$RG = .0451_Btu/(lb \cdot R)$
p = 14.696_psi	Vs = 8.7612_ft ^ 3/lb
$T = 68_{F}$	$m = 57.0699$ _lb
MWT = 44.01 g/mol	n = 588.1952_mol

Gas-Constant Pressure

volume 1

For a closed system, an ideal gas that is subjected to an isobaric process is described by the following equations.

1) $\frac{Vs2}{Vs1}$ =	<u>T2</u> T1	2) V1 = $m \cdot V$	/s1
3) V2 = r	m · Vs2	4) $m = MWT$	· n
5) ΔVs =	Vs2 – Vs1	6) $RG = \frac{R}{MW}$	T
7) W12 =	$p \cdot \Delta Vs$	8) $W12 = RG$	· (<i>T</i> 2 - <i>T</i> 1)
9) Q = C	¢p · (T2 − T1)		
10) Q =	$Cv \cdot (T2 - T1) + p \cdot \Delta Vs$		
Variable	Description		Eqn Units
Vs2	specific volume, state 2		1_m^3/kg
Vs1	specific volume, state 1		1_m^3/kg
T2	temperature, state 2		1_K
T1	temperature, state 1		1 K

1 m^3

V1

V2	volume 2	1_m^3
m	mass	1 [–] kg
MWT	molecular weight	1_kg/mol
n	number of moles	1 mol
ΔVs	specific volume diff	1 [_] m^3/kg
RG	gas specific constant	1_J/(kg ⋅ K)
W12	work to change 1 to 2	1_J/kg
р	pressure	1_Pa
Q	heat	1_J/kg
Ср	specific heat, constant pressure	1 J/(kg⋅K)
Cv	specific heat, constant volume	1_J/(kg⋅K)

Example: The temperature rise of nitrogen (N_2) for a constant pressure process is 48 _K. What is the amount of work performed, heat generated, and specific volume after the process is completed? At the beginning of the process, the chamber has a volume of 10_l with .75_mol of N₂ present. The initial temperature is 400_K. Specific heat at constant volume is 1.041_kJ/(kg·K). Use equations 1-9.

Given	Result
$V1 = 10_{I}$	$W12 = 6.1290$ _Btu/lb
T2 = 448 K	Q = 21.4824 Btu/lb
T1 = 400 K	Vs1 = 0.4760_l/g
n = .75_mol	Vs2 = .5331_l/g
MWT = 28.0134 g/mol	$RG = 55.2 \text{ ft} \cdot \text{lbf}/(\text{lb} \cdot \text{°R})$
$Cp = 1.041 kJ/(kg \cdot K)$	$m = .0463$ _lb
	$Cv = .744 kJ/(kg \cdot K)$
	V2 = 11.2
	$\Delta Vs = .05712 l/g$
	p = 249599.0127_Pa

Gas-Constant Volume

For a closed system, an ideal gas that is subjected to a constant volume process is described by the following equations.

1) $\frac{p2}{p1} = \frac{T2}{T1}$ 2) $RG = \frac{R}{MWT}$ 3) $V = Vs \cdot m$ 4) $m = MWT \cdot n$ 5) $Q = Cv \cdot (T2 - T1)$

Mechanical Engr. Pac

6) Q =	$\frac{Cv \cdot Vs \cdot \Delta p}{RG} $ 7)	$\Delta p = p2 - p1$
Variable	Description	Eqn Units
p2	pressure, state 2	1_Pa
p1	pressure, state 1	1_Pa
T2	temperature, state 2	1_K
T1	temperature, state 1	1_K
RG	specific gas constant	1_J/(kg ⋅ K)
MWT	molecular weight	1_kg/mol
V	volume	1_m^3
Vs	specific volume	1_m^3/kg
m	mass	1_kg
n	number of moles	1_mol
Q	quantity of heat	1_J/kg
Cv	specific heat constant volu	me 1_J/(kg⋅K)
Δр	pressure difference	1_Pa

Example: What amount of heat is used when Argon, at a constant volume, is heated from $0^{\circ}C$ to $100^{\circ}C$? Cv is $3.199_{kJ}/(kg \cdot K)$. Use equation 5.

 Given
 Result

 $Cv = 3.199_k J/(kg \cdot K)$ $Q = 319.9_k J/kg$
 $T2 = 100_{\circ}C$ $T1 = 0_{\circ}C$

Gas-Constant Temperature

For a closed system, an ideal gas that is subjected to an isothermal process is described by the following equations.

1) $\frac{p2}{p1} = \frac{Vs1}{Vs2}$ 2) $RG = \frac{R}{MWT}$ 3) $V1 = Vs1 \cdot m$ 4) $V2 = Vs2 \cdot m$ 5) $m = MWT \cdot n$ 6) Q = W7) $W = RG \cdot T \cdot LN\left(\frac{Vs2}{Vs1}\right)$ 8) $W = RG \cdot T \cdot LN\left(\frac{p1}{p2}\right)$

Variable	Description	Eqn Units
p2	pressure at state 2	1_Pa
p1	pressure at state 1	1_Pa
Vs1	specific volume, state 1	1_m^3/kg
Vs2	specific volume, state 2	1_m^3/kg
RG	specific gas constant	1_J/(kg⋅K)
MWT	molecular weight	1_kg/mol
V1	volume, state 1	1_m^3
m	mass	1_kg
n	number of moles	1_mol
Q	quantity of heat	1_J/kg
W	work	1_J/kg
Т	temperature	1_K
V2	volume, state 2	1_m^3

Example: Air, with a molecular weight of 29_g/mol, undergoes a constant temperature process. Assuming 10 pounds of air at 1_atm is compressed to 3_atm. What is the amount of heat given off by the system? The ambient temperature is 59_°F. Use equations 2, 5, 6 and 8.

Given	Result
p1 = 1_atm	$RG = .28689 kJ/kg \cdot K$
$p2 = 3_atm$	$n = 156.41$ _mol
m = 10 lb	Q = -39.046 Btu/lb
$MWT = 29_g/mol$	$W = -39.046$ _Btu/lb
$T = 59 {}^{\circ}F$	_

Thermodynamics/Ideal Gas Law

These equations describe thermodynamic properties of an ideal gas with constant specific heats and no internal heat sources.

1) $\Delta u = Cv \cdot (T2 - T1)$) 2) $\Delta u = u^2 - u^1$
3) $\Delta h = Cp \cdot (T2 - T1)$	4) $\Delta h = h2 - h1$
5) $Cp - Cv = RG$	6) $RG = \frac{R}{MWT}$
7) $\Delta s = Cv \cdot LN\left(\frac{T2}{T1}\right)$	+ $RG \cdot LN\left(\frac{Vs2}{Vs1}\right)$

Mechanical Engr. Pac

8)
$$\Delta s = Cp \cdot LN\left(\frac{T2}{T1}\right) - RG \cdot LN\left(\frac{p2}{p1}\right)$$

9) $\Delta s = Cp \cdot LN\left(\frac{Vs2}{Vs1}\right) + Cv \cdot LN\left(\frac{p2}{p1}\right)$
10) $\Delta s = s2 - s1$
11) $V1 = Vs1 \cdot MWT \cdot n1$

12) $V2 = Vs2 \cdot MWT \cdot n2$

Variable	Description	Eqn Units
p1	pressure state 1	1_Pa
p2	pressure state 2	1_Pa
T2	temperature state 2	1_K
T1	temperature state 1	1_K
Cv	specific heat at constant volume	1_J/(kg ⋅ K)
Ср	specific heat at contant pressure	1_J/(kg ⋅ K)
RG	specific gas constant	1_J/(kg ⋅ K)
MWT	molecular weight	1_kg/mol
Δu	Δ specific internal energy	1_J/kg
u2	internal energy state 2	1_J/kg
u1	internal energy state 1	1_J/kg
∆h	specific enthalpy	1_J/kg
h2	specific enthalpy state 2	1_J/kg
h1	specific enthalpy state 1	1_J/kg
Δs	Δ entropy	1_J/(kg ⋅ K)
s2	specific entropy state 2	1_J/(kg ⋅ K)
s1	specific entropy state 1	1_J/(kg ⋅ K)
V1	volume state 1	1_m^3
Vs1	specific volume state 2	1_m^3/kg
n1	number of moles state 1	1_mol
n2	number of moles state 2	1_mol
V2	volume state 2	1_m^3
Vs2	specific volume state 2	1_m^3/kg

Example: Calculate the temperature drop for an isentropic expansion of air from 821_°R at 5_atm to 1_atm. Assume that the molecular weight of air is 29_g/mol and Cp = .240_Btu/(lb.°R). Use equations 6 and 8.

Given

Result

 $RG = .0685 Btu/(lb \cdot R)$

T2 = 518.5327 °R

 $\Delta s = 0$ $T1 = 821 \ ^{\circ}R$ p1 = 5 atm $p2 = 1_atm$ MWT = 29 g/mol $Cp = .240 \text{ Btu/(lb} \cdot ^{\circ}\text{R})$

Real Gas Law

The real gas law equations below are based upon the principle of corresponding states. The compressibility factor, Z, is calculated from the reduced temperature and reduced volume and is used to "correct" for non-ideal behavior. Z factor can be computed based on what is known, such as T, Tc, pc, Vm, Vs, MWT, and n. Choose Z factors ZF1, ZF2, ZF3 or ZF4 accordingly. The functions used to calculate Z are valid in low and medium pressures, that is for pR < 6.0, and are unavailable for use outside the scope of this topic.

1) p · Vs =	= Z · RG · T	2) $RG = \frac{R}{MW}$	T
3) <i>m</i> = <i>n</i>	· MWT	4) $p \cdot V = n$	$\cdot Z \cdot R \cdot T$
5) $V = m$	· Vs	6) $pR = \frac{p}{pc}$	
7) TR = -	<u>T</u> Tc	8) $Z = ZF 1$ (Т, Тс, рс, Vm)
9) $Z = ZF$	2 (T, Tc, pc, Vs, MWT)	10) $Z = ZF$ 3	(T, Tc, pc, V, n)
11) $Z = Z$	F 4 (T, Tc, pc, Vs, RG)		
Variable p Vs V T RG MWT m n Z	Description pressure specific volume volume temperature specific gas constant molecular weight mass number of moles		Eqn Units 1_Pa 1_m^3/kg 1_M^3 1_K 1_K 1_J/(kg·K) 1_kg/mol 1_kg

Equation Library

pR	reduced pressure	1
pc	critical pressure	1_Pa
TR	reduced temperature	1
Тс	critical temperature	1_K
Vm	molar volume	1_m ^ 3/mol

Example: 25 moles of oxygen (O_2) is contained in a 10 liter cylinder at -10 °C. Estimate the pressure in the cylinder. Use equations 4 and 10.

Given	Result
Tc = 154.4_K	Z = 0.9539
$pc = 49.7_atm$	p = 51.528_atm
T = -10 °C	
V = 10	
n = 25 mol	

Polytropic Process

Useful equations for analyzing ideal gases are those derived from the polytropic process where $Pv^{\gamma} = \text{constant}$. Several different process states can be analyzed by assigning γ its particular value.

γ equals (w	vhen)	Type of State Change
0		isobaric
1		isothermal
к	-	isentropic
∞		constant volume process

1) $\frac{\rho 2}{\rho 1} = \left(\frac{Vs1}{Vs2}\right)^{\gamma}$	2) $\frac{T2}{T1} = \left(\frac{Vs1}{Vs2}\right)^{\gamma-1}$
3) $V1 = Vs1 \cdot m$	4) V2 = Vs2 \cdot m

5)
$$m = n \cdot MWT$$

Variable	Description	Eqn Units
p2	pressure state 2	1_Pa
p1	pressure state 1	1_Pa
Vs1	specific volume state 1	1_m^3/kg
Vs2	specific volume state 2	1_m ^ 3/kg
Equation Library

V1	volume state 1	1_m^3
V2	volume state 2	1 ⁻ m^3
T2	temperature state 2	1_K
T1	temperature state 1	1 K
n	number of moles	1_mol
γ	polytropic constant	1
MWT	molecular weight	1_kg/mol
m	mass of gas	1_kg

Example: During an isothermal process the pressure goes from 1_atm to 2_atm. If the specific volume initially was $1_{ft}^3/lb$, what is the final specific volume? Use equation 1.

Given

 $p1 = 1_atm$ $p2 = 2_atm$ $Vs1 = 1_ft^3/lb$ $\gamma = 1$

Result

 $Vs2 = .5_ft^3/lb$

Heat Transfer

In this category, conductive, convective, and radiative forms of heat transfer are described in the following topics:

- Steady State Conduction & Convection
- Heat Conduction-Cylindrical, Spherical Wall
- Forced Convection-Flat Plate (Heat)
- Forced Convection-Flat Plate (Drag)
- Lumped Cap Analysis
- Negligible Surface Resistance
- Semi-Infinite Solid
- Blackbody Radiation
- Radiant Heat Exchange

Steady State - Conduction & Convection

The equation below uses the resistance analog to solve for steady-state conduction and convection. The resistance analog means that more than one wall configuration can be solved by the equation set. Up to a three-layer wall with convection on both sides can be solved for in this topic.

Wall Configuration



Resistance Analog



In the first example, a three-layer wall with convection on both sides is used. Thus:

SUMR = RV1 + RD1 + RD2 + RD3 + RV2

is the appropriate equation. In example 2, a two-layer wall with no convection is used. Thus:

SUMR = RD1 + RD2

is the appropriate equation. In order to solve example 2, RV1, RD3 and RV2 must be "known" to be zero:



1)
$$qx = \frac{Th - Tc}{SUMR}$$
 2) $SUMR = RV1 + RD1 + RD2 + RD3 + RV2$

- 3) $RV1 = \frac{1}{h1 \cdot A}$ 4) $RV2 = \frac{1}{h2 \cdot A}$ 5) $RD1 = \frac{L1}{K1 \cdot A}$
- 6) $RD2 = \frac{L2}{K2 \cdot A}$ 7) $RD3 = \frac{L3}{K3 \cdot A}$ 8) $U = \frac{1}{SUMR}$

Variable	Description	Eqn Units
qx	energy transfer rate	1_W
Th	hot temperature	1_K
Тс	cold temperature	1_K
SUMR	summation of resistances	1_K/W
RV1	convective resistance at 1	1_K/W
RV2	convective resistance at 2	1_K/W
RD1	conductive resistance at 1	1_K/W
RD2	conductive resistance at 2	1_K/W
RD3	conductive resistance at 3	1 ⁻ K/W
L1,L2,L3	length of conduction at 1, 2, 3	1 ⁻ m
K1,K2,K3	thermal conductivity at 1, 2, 3	1 [¯] W/(m⋅K)
h1,h2	convective heat transfer coefficient	1_W/(m ^ 2 · K)
Α	area	1 m^2
U	overall heat transfer coefficient	1_W/K

Example 1: A 75_m^2 wall is constructed of 15_cm thick concrete $k1 = 1.21_W/(m \cdot K)$, 5_cm thick rock wool $k2 = .040_W/(m \cdot K)$, and 1.25_cm thick plaster board $k3 = .51_W/(m \cdot K)$. The outside wind (-2_°C) blows 20_m/s (h1 = 34.0_W/(m^2 \cdot K)). The inside air at 20_°C is nearly still (h2 = 9.36_W/(m^2 \cdot K)). What is the energy transfer rate, qx?

Given	Result
$A = 75_m^2$	$RV1 = 3.921 \times 10^{-4} K/W$
$K1 = 1.21 W/(m \cdot K)$	$RV2 = 1.4245 \times 10^{-3} K/W$
$K2 = .040 W/(m \cdot K)$	$RD1 = 1.652 \times 10^{-3} K/W$
$K3 = .51 W/(m \cdot K)$	$RD2 = 1.667 \times 10^{-2} K/W$
h1 = 34.0_W/(m^2·K)	$RD3 = 3.2679 \times 10^{-4} K/W$
$h2 = 9.36 W/(m^2 \cdot K)$	$SUMR = 2.0463 \times 10^{-2} K/W$
Th = 20°C	qx = 1075.11_W
$Tc = -2_{C}$	U = 48.87 W/K
$L1 = 15_cm$	
$L2 = 5_cm$	
L3 = 1.25 cm	

Example 2: An insulated rod is composed of a 20 inch section of iron



 $(K=44.1_Btu/(h \cdot ft \cdot {}^{\circ}F))$, and lead $(K=20.3_Btu/(h \cdot ft \cdot {}^{\circ}F))$. Calculate the energy transfer rate if one end is at 450_ ${}^{\circ}F$ and the other end is at 100_ ${}^{\circ}F$. The cross-sectional area is 3.14_in ^2. Select equations 1, 2, 5, 6 and 8 for this problem.

Given	Result
$A = 3.14 in^{2}$	$RD1 = .8665 \text{°F} \cdot \text{h/Btu}$
$Th = 450^{\circ}F$	$RD2 = 1.8825 \text{ °F} \cdot \text{h/Btu}$
Tc = 100°F	$SUMR = 2.7491^{\circ}F \cdot h/Btu$
K1 = 44.1 Btu/(h·ft·°F)	qx = 127.31_Btu/h
K2 = 20.3 Btu/(h·ft·°F)	$U = .3637 \text{Btu}/(h \cdot \text{°F})$
$L1 = 10_{in}$	
$L2 = 10$ _in	
$*RV1 = 0_K/W$	
*RV2 = 0 K/W	
*RD3 = $0_K/W$	
*In order for SUMR equation to work, RV1,	RV2, and RD3 must be set ("known'
zero.	

Heat Conduction-Cylindrical, Spherical Wall

The equations below solve heat conduction problems through a single layer cylinder, a two-layer cylinder and a spherical wall.

Single layer cylinder
$$qr1 = \frac{2 \cdot \pi \cdot k1 \cdot L \cdot (T1 - T2)}{LN\left(\frac{r2}{r1}\right)}$$

2-layer cylinder $qr2 = \frac{2 \cdot \pi \cdot L \cdot (T1 - T3)}{\frac{1}{k1} \cdot LN\left(\frac{r2}{r1}\right) + \frac{1}{k2} \cdot LN\left(\frac{r3}{r2}\right)}$
Spherical wall $qs = \frac{4 \cdot \pi \cdot k \cdot (T1 - T2)}{\frac{1}{r1} - \frac{1}{r2}}$

) to

Variable	Description	Eqn Units
qr1	energy transfer rate	1_W
qr2	energy transfer rate	1_W
qs	energy transfer rate	1_W
k	thermal conductivity of sphere	1_W/(m ⋅ K)
k1	thermal conductivity, layer 1	1_W/(m ⋅ K)
k2	thermal conductivity, layer 2	1_W/(m ⋅ K)
L	length of cylinder	1_m
T1	temperature at 1	1_K
T2	temperature at 2	1_K
ТЗ	temperature at 3	1_K
r1	radius at 1	1_m
r2	radius at 2	1_m
r3	radius at 3	1_m

Example: A one inch, schedule 160, pipe is subjected to outside and inside surface temperatures of $150_{\text{°}}F$ and $250_{\text{°}}F$, respectively. Calculate the heat flow per foot of pipe. Internal radius = .407 inches, external radius = .657 inches. Use the single layer equation.

 Given
 Result

 k1 = 22.9_Btu/(h·ft·°R)
 qr1 = 30046.7_Btu/h

 $r1 = .407_{in}$ $r2 = .657_{in}$
 $r1 = 250_{°}F$ $T2 = 150_{°}F$
 $L = 1_{ft}$ r1

Forced Convection-Flat Plate (Heat)

Equations for analyzing heat transfer from laminar flow on a two-dimensional plate are listed below. The fluid has a constant viscosity and is considered incompressible. (Rex.L < 5×10^{5} , .6 < Pr < 15).

1)
$$Nux = .332 \cdot \sqrt{Rex} \cdot Pr^{\frac{1}{3}}$$

2) $NuL = .664 \cdot \sqrt{ReL} \cdot Pr^{\frac{1}{3}}$
3) $Rex = \frac{V \cdot x}{\eta}$
4) $ReL = \frac{V \cdot L}{\eta}$

5) <i>Nux</i> = $\frac{1}{2}$	$\frac{k \cdot x}{k}$	6) $NuL = \frac{hL}{k}$	L
7) <i>hL</i> = 2	· hx	8) $\Delta T = Ts -$	T∞
9) $qL = hL$	$\cdot \Delta T$	10) $qx = hx \cdot x$	ΔT
11) $Pr = \frac{\eta}{\alpha}$	12) $\eta = \frac{\mu}{\rho}$	$13) \alpha = \frac{k}{\rho \cdot C\rho}$	-
Variable	Description		Eqn Units
Nux	Nusselt number at x		1
NuL	Nusselt number at L		1
Rex	Reynold's number at x		1
ReL	Reynold's number at L		1
V∞	velocity of fluid		1_m/s
Pr	Prandtl number		1
hx	location convection heat	transfer coeff	1_W/(m^2·K)
hL	mean convection heat tra	anfer coeff	1_W/(m^2·K)
x	distance from edge		1_m
L	mean distance		1_m
k	thermal conductivity		1_W/(m⋅K)
ΔT	temperature difference		1_K
Ts	surface temperature		1_K
T∞	final temperature		1_K
qL	mean heat transfer rate		1_W/m^2
qx	local heat transfer rate		1_W/m^2
η	kinematic viscosity		1_m^2/s
μ	dynamic viscosity		1_Pa·s
α	thermal diffusivity		1_m^2/s
ρ	density		1_kg/m ^ 3
Ср	neat capacity		1_J/(kg⋅K)

Example: Air at 70_°F with a uniform free stream velocity ($V \propto = 50_{\text{ft/s}}$) is moving parallel to a smooth flat plate heated to a uniform surface temperature of 212 °F. $\eta = 0.21 \times 10^{-3}$ ft ^2/s, k = 0.0164 Btu/(h · ft · °F) and Pr = 0.72. What is the length of the laminar boundary layer? Use equation 3.

Given

Result

 $\eta = 0.21 \times 10^{-3} \text{ft}^2/\text{s}$ x = 2.10 ft (critical length) $V \infty = 50 \text{ft/s}$ Rex = 5 x 10^5 (transition)

What is the local heat-transfer coefficient at the critical length? Use equations 1 and 5.

Given Rex = 5 E5 $x = 2.1_{ft}$ $k = 0.0164_{Btu}/(h \cdot ft \cdot F)$ Pr = 0.72 **Result** hx = 1.643_Btu/(h·ft^2·°F) Nux = 210.4

What is the mean heat capacity coefficient over the portion of the plate covered by the laminar boundary layer? Use equations 2 and 6.

Given	Result
ReL = 5 x 10 ^ 5	$hL = 3.286 Btu/(h \cdot ft ^ 2 \cdot ^{\circ}F)$
Pr = 0.72	NuL = 420.8
L = 2.1_ft	
$k = 0.0\overline{1}64_Btu/(h \cdot ft \cdot {}^{\circ}F)$	

Forced Convection-Flat Plate (Drag)

Equations for analyzing skin-friction drag and boundary layer thickness for laminar flow over a two-dimensional plate are given below.

1) $Cfx = \frac{.664 \cdot 1}{\sqrt{Rex}}$ 2) $CfL = \frac{1.328}{\sqrt{ReL}}$ 3) $CfL = 2 \cdot Cfx$ 4) $\delta t = \frac{\delta}{Pr^{\frac{1}{3}}}$ 5) $\delta = \frac{5 \cdot x}{\sqrt{Rex}}$ 6) $Ff = \frac{CfL \cdot \rho \cdot V\infty^2}{2} \cdot A$ 7) $Rex = \frac{V\infty \cdot x}{\eta}$ 8) $ReL = \frac{V\infty \cdot L}{\eta}$

9)
$$\eta = \frac{\mu}{\rho}$$

Variable	Description	Eqn Units
Cfx	location skin friction coefficient	1
CfL	mean skin friction coefficient	1
Rex	location Reynold's number	1
ReL	mean Reynold's number	1
δt	thermal thickness	1_m
δ	boundary layer thickness	1_m
Pr	Prandtl number	1
x	distance from edge	1_m
L	mean distance	1_m
Ff	skin friction drag	1_N
V∞	fluid velocity	1_m/s
Α	area	1_m^2
η	kinematic viscosity	1_m^2/s
μ	dynamic viscosity	1_Pa∙s
ρ	density	1_kg/m ^ 3

Example: Air at 70_°F with a uniform free-stream velocity ($V \infty = 50_{ft/s}$) is moving parallel to a smooth flat plate heated to a uniform surface temperature of 212_°F. What is the thickness of the hydrodynamic and thermal boundary layers at the critical length? Use equations 4 and 5.

Given	Result
$x = 2.10_{ft}$	$\delta = 0.0148$ _ft
$Rex = 5 \times 10^{5}$	$\delta t = 0.0166 ft$
Pr = .72	_

What is the force from skin-friction if the area of the plate is $10_{ft} \sim 2$? Use equations 2 and 6.

Given	Result
$A = 10_{ft}^2$	$CfL = 1.878 \times 10^{-3}$
$V \infty = 50 \text{ ft/s}$	$Ff = 0.04750 \ Ibf$
$\rho = 0.0651$ lb/ft ^ 3	_
$ReL = 5 \times 10^{5}$	

Lumped Cap Analysis

In unsteady-state conduction, if there is an extremely small internal temperature gradient, then lumped analysis can be performed, Bi < 0.1.

1)	$\frac{T-T\infty}{Ti-T\infty}$	2)	Bi	=	$\frac{h \cdot L}{k}$
3)	e ^{-Bi · Fo}	4)	Fo	=	$\frac{\alpha \cdot t}{L^2}$

5)
$$\alpha = \frac{k}{\rho \cdot c\rho}$$

Variable	Description	Eqn Units
Θ	normalized temperature	1
т	body temperature	1_K
T∞	constant surface temperature	1_K
Ті	initial body temperature	1_K
Bi	Biot modulus	1
α	thermal diffusivity	1_m^2/s
t	time	1_s
L	length parameter	1_m
k	thermal conductivity	1_W/(m ⋅ K)
ρ	density	1_kg/m ^ 3
ср	specific heat	1_J/(kg ⋅ K)
Fo	Fourier modulus	1
h	convective heat transfer coefficient	1_W/(m ^ 2 · K)

Note: L is the ratio of body volume divided by the surface area.

Geometry	L equals
long cylinder	D/4
sphere	D/6
cube	S/6
long parallelpiped	S/4
Where: $D = diameter and S = length of sid$	e of square

Example: A 1_cm diameter steel sphere at 600_°C is cooled to 90_°C in an air stream. The air stream's temperature is 25_°C. How much time does this take?

Step 1: Check for Biot modulus < 0.1. Use equation 2.

Step 2: Solve for all equations.

 Given
 Result

 Bi = .00448 $\Theta = .11304$
 $T\infty = 25_^{\circ}C$ $\alpha = 1.16 \times 10^{-5}_m^{-2/s}$
 $Ti = 600_^{\circ}C$ $t = 116.1_s$
 $T = 90_^{\circ}C$ Fo = 486

 $L = .16667_cm$ $k = 42_W/(m \cdot K)$
 $\rho = 7865.5_kg/m^{-3}3$ $cp = .459_kJ/(kg \cdot K)$

Negligible Surface Resistance

Temperatures at the center of objects of typical geometrical shapes are covered by the following set of equations. It is assumed that there is an initial uniform temperature and a constant surface temperature. The functions are valid from $0.12 < \tau < 1.2$.

1) $\Theta = \frac{Tc - T\infty}{Ti - T\infty}$ 2) $\tau = \frac{\alpha \cdot t}{x^2}$ 3) $\alpha = \frac{k}{\rho \cdot c\rho}$ 4) $\Theta = \text{TSPH}(\tau)$ Sphere (TSPH) 5) $\Theta = \text{TCYL}(\tau)$



6) Θ = TCUB (τ)



7) Θ = TCYLINF (τ)



8) Θ = TPARINF (τ)



9) Θ = TSLAB (τ)



Slab (Infinite) (TSLAB)

Variable	Description	Eqn Units
Θ	normalized temperature	1
Тс	centerline temperature	1_K
T∞	final temperature	1_K
Ti	initial uniform temperature	1_K
α	thermal diffusivity	1_m ^ 2/s
t	time	1_s
x	centerline to surface length	1_m
k	thermal conductivity	1_W/(m⋅K)
ρ	density	1_kg/m^3
ср	specific heat	1_J/(kg ⋅ K)
τ	Fourier modulus	1

Example: A sphere of lead $(x = .1_ft)$, initially at a temperature of 98_°C, is dropped into a vigorously agitated tank of water maintained at 0_°C by an external refrigerator unit. The average properties of the lead sphere during cooling are given as: $\rho = 708_{lb}/ft^3$, $cp = 0.03_{Btu}/(lb \cdot °F)$ and $K = 20.3_{Btu}/(h \cdot ft \cdot °F)$. How many seconds will it take for the center of the sphere to attain a temperature of 18.3_°C? Use equations 1, 2, 3 and 4.

Given	Result
$\rho = 708 \text{lb/ft}^3$	$\alpha = 0.956_{ft} ^ 2/h$
$cp = 0.03$ _Btu/(lb·°R)	$\Theta = 0.187$
$k = 20.3$ _Btu/(h·ft·°F)	t = 9.06 s
Ti = 98°C	$\tau = .24$
$Tc = 18.3 \ ^{\circ}C$	

 $T \infty = 0_{C}$ x = .1 ft

Semi-Infinite Solid

The six equations in this topic describe transient heat conduction solution for a semi-infinite solid. Error function and complementary error function are computed using an internal program that is not available for use in other topics.

1) $\eta =$	$\frac{x}{2 \cdot \sqrt{\alpha \cdot t}}$	2) $\Theta = \frac{T-T}{Ti-T}$	- <u>T∞</u> - <u>T∞</u>
3) $\lambda = -$	$\frac{h \cdot \sqrt{\alpha \cdot t}}{k}$		
4)	ERF (η) + e $\left(2 \cdot \lambda \cdot \left(\eta + \frac{\lambda}{2}\right)\right)$) . ERFC ($\eta + \lambda$.)
5) $\frac{q}{A} =$	$\frac{k\cdot(T\infty-Ti)}{\sqrt{\pi}\cdot\alpha\cdot t}\cdot e^{-x^2/(4\cdot$	$\alpha \cdot t$)	
6) α =	$\frac{k}{\rho \cdot cp}$		
Variable	Description		Eqn Units
η	similarity parameter		1
х	distance		1_m
α	thermal diffusivity		1_m ^ 2/s
t	time		1_s
Θ -	normalized temperatur	re -	1
T	temperature		1_K

T∞ final temperature

- Ti initial temperature lambda parameter λ h
- convective heat transfer coefficient k thermal conductivity
- 1 W/($m \cdot K$) heat flow rate 1 W q Α area 1_m^2 density 1 kg/m^3 ρ specific heat $1 J/(kg \cdot K)$ ср

1 K

1 K

1 W/(m^ $2 \cdot K$)

1

Example: Assume that the Alaskan tundra has a constant and uniform temperature of -7_°C to a depth of several meters. On a very particular spring day, a Hawaiian air mass ($T \propto = 20_{\circ}C$) moves over the tundra for a period of eight hours. The convective coefficient between air and surface is 13.14_W/(m^2·K). Assume tundra properties of $\alpha = 4.65 \times 10^{\circ}-7_{m}^{2}/s$ and $k = 0.865_W/(m \cdot K)$. Calculate (a) surface temperature at 5 hours and (b) depth at which $T = 0_{\circ}C$ after 8 hours.

A. Surface temperature at 5 hours:

GivenResult $x = 0_m$ $\Theta = .34059$ $T^{\infty} = 20_{\ }^{\circ}C$ $\eta = 0$ $Ti = -7_{\ }^{\circ}C$ $\lambda = 1.3897$ $\alpha = 4.65 \times 10^{-7} \text{ m}^{2}/\text{s}$ $T = 10.80_{\ }^{\circ}C$ $k = 0.865_{\ }W/(m \cdot K)$ $T = 13.14_{\ }W/(m^{2} \cdot K)$

B. Depth at which T = 0 °C after 8 hours:

 Given
 Result

 $T = 0_{\circ}C$ $x = .1314_{\circ}m$
 $T\infty = 20_{\circ}C$ $\Theta = .74074$
 $Ti = -7_{\circ}C$ $\lambda = 1.7579$
 $\alpha = 4.65 \times 10^{-7} \text{-m}^2/\text{s}$ $\eta = .56787$
 $k = 0.865_{\circ}W/(m \cdot K)$ $t = 8_{\circ}h$
 $h = 13.14_{\circ}W/(m^22 \cdot K)$ Note: Problem B takes over three minutes to calculate.

Blackbody Radiation

A blackbody is one which neither reflects nor transmits any thermal energy. The following equations describe this behavior. PLAM21 computes the normalized fraction of emitted radiation in the wavelength range $\lambda 1$ to $\lambda 2$ for the blackbody temperature of T.

1)
$$Eb = \sigma \cdot T^4$$
 2) $Eb\lambda = \frac{c1 \cdot \lambda^{-5}}{e^{c2/(\lambda \cdot T)} - 1}$

3)	$lmax \cdot T = c3$	4) frac =	PLAM21 (λ2, λ1, Τ)
5)	$Eb12 = frac \cdot Eb$	6) $q = Eb$	· A
Varia	ble Description		Eqn Units
Eb	total emissive powe	r	1_W/m^2
Ebl	monochromatic em	issive power	1_W/m^2·µm
Т	temperature		1_K
λ	wavelength		1_m
λmax	maximum emissivity	y wavelength	1_m
frac	total energy fractior	า	1
Eb12	emissive power $\lambda 1$,	λ2	1_W/m ^ 2
q	heat flux		1_W
A	area		1_m^2
λ1	wavelength 1		1_m
λ2	wavelength 2		1_m

The PLAM21 function takes over 6 minutes to converge on an answer.

Example: A blackbody has a temperature of 450_°C. At what wavelength does maximum monochromatic emissive power occur? What is the total emissive power? (use equations 1 and 2)

Given	Result
T = 450 °C	$\lambda max = 4.0069 \mu m$
_	$Eb = 15505.1 \text{ W/m}^2$

What is the maximum monochromatic emission power?

Given	Result
$T = 450 ^{\circ}C$	$Eb\lambda = 2545.404 W/(m^2 \cdot \mu m)$
$\lambda = 4.00 \mu m$	

Radiant Heat Exchange

When the heat transfer rate is at equilibrium between two gray and opaque surfaces, the following equations can be used.

1)
$$q12 = \frac{Eb1 - Eb2}{\frac{1 - \varepsilon 1}{\varepsilon 1 \cdot A1} + \frac{1}{A1 \cdot F12} + \frac{1 - \varepsilon 2}{\varepsilon 2 \cdot A2}}$$

2)	$Eb1 = \sigma \cdot T1^4$	3) Eb2 = σ ·	T2 ⁴
4)	$A1 \cdot F12 = A2 \cdot F21$		
5)	$q12 = A1 \cdot \epsilon 1 \cdot \sigma \cdot \left(T1^4 - T2^4\right)$	when A2 > >A1	
Varia	ble Description		Eqn Units
q12	heat flow rate		1 W
Eb1	emissive power at 1		1_W/m^2
Eb2	emissive power at 2		1_W/m^2
T1	temperature 1		1_K
T2	temperature 2		1_K
A1	area 1		1_m^2
A2	area 2		1_m^2
ε1	emissivity 1		1
ε2	emissivity 2		1
F12	view factor 1		1
F21	view factor 2		1

Example: The equilibrium temperature of a chromnickel ($\varepsilon = .68$) cannonball is 700_°F. The temperature of the furnace walls is 1200_°F. What is the heat transfer rate? The surface area of the cannonball is 1.40_ft ^2. Use equation 5.

Given	Result
$T1 = 700_{F}$	q12 =-9418.7935 Btu/h
T2 = 1200°F	· _
$A1 = 1.40 \text{ ft}^2$	
$\varepsilon 1 = .68$	

Mechanics

This category covers six topics of interest to mechanical engineers concerning laws of motion.

- Linear Motion
- Angular Motion
- Force, Work, Power
- Forces in Angular Motion
- Elastic Collisions (1D)
- Inclined Planes

Linear Motion

Five equations describe the relationships between initial and final velocity, distance travelled, acceleration and time of travel. These equations assume that the linear motion is characterized by constant acceleration.

1) <i>x</i> = <i>x</i>	$xo + vo \cdot t + \frac{1}{2} \cdot a \cdot t^2$	2) $x = xo + v \cdot t - \frac{1}{2} \cdot a \cdot t^2$
3) $x = x$	$xo + \frac{1}{2} \cdot (v + vo) \cdot t$	4) $v = vo + a \cdot t$
5) v ² =	$vo^2 + 2 \cdot a \cdot (x - xo)$	
Variable	Description	Eqn Units
x	distance at t	1 m
хо	distance at $t=0$	1 ⁻ m
vo	initial velocity	1 [_] m/s
t	time of travel	1 ⁻ s
а	acceleration	1 [¯] m/s ^ 2
v	velocity at t	1 [_] m/s

Example 1: You brake your Mazda RX7 from 80 mph to 45 mph over a displacement of 100 yards. What is the decceleration, assuming it to be

constant, and the elapsed time? Select equations 4 and 5 to solve the problem.

GivenResult $x = 100_yd$ $a = -4.7808_m/s^2$ $xo = 0_m$ $t = 3.2727_s$ $vo = 80_mph$ $v = 45_mph$

Example 2: If you continue to decelerate at the rate from Example 1, how much further distance will the car travel before coming to a halt? Using equation 4, you can find time t and use it to solve for x using equations 1, 2 or 3.

GivenResult $xo = 0_m$ $x = 42.3237_m$ $vo = 45_mph$ $t = 4.2078_s$ $v = 0_mph$ $a = -4.7808_m/s^2$

Angular Motion

Three equations in this topic cover the relationships between angular displacement, initial and final angular velocity, angular acceleration, and time.

- 1) $\Theta = \Theta o + \omega o \cdot t + \frac{1}{2} \cdot \alpha \cdot t^2$
- 2) $\Theta = \Theta o + \omega \cdot t \frac{1}{2} \cdot \alpha \cdot t^2$
- 3) $\omega = \omega o + \alpha \cdot t$

Variable	Description	Eqn Units
Θ	final angular displacement	1_°
Θο	initial angular displacement	1_°
ωο	initial angular velocity	1_r/s
ω	final angular velocity	1_r/s
t	time	1_s
α	angular acceleration	1_r/s ^ 2

Example: A rotating shift spinning at an initial angular velocity of 10_r/s changes its angular velocity at a constant rate to a final velocity of 125_r/min in 30 seconds. Find the angular displacement and angular acceleration.

 Given
 Result

 $\Theta o = 0$ $\alpha = -.2639 r/s^2$
 $\omega o = 10 r/s$ $\Theta = 181.25 r$
 $\omega = 125 r/min$ t = 30 s

Force, Work, Power

The five equations in this set focus on Newton's second law; power, force and velocity relationships; and initial and final kinetic energy for linear motion.

1) $F = m \cdot a$ 2) $P = F \cdot v$

3)
$$v = \frac{1}{2} \cdot (vi + vf)$$
 4) $vf = vi + a \cdot t$

5)
$$Ki = \frac{1}{2} \cdot m \cdot vi^2$$
 6) $Kf = \frac{1}{2} \cdot m \cdot vf^2$

Variable	Description	Eqn Units
F	force	1_N
m	mass	1_kg
а	acceleration	1_m/s^2
Р	power	1_W
v	avg velocity	1_ m/s
vf	final velocity	1_m/s
vi	initial velocity	1_m/s
t	time	1_s
Ki	initial kinetic energy	1_J
Kf	final kinetic energy	1_J

Example: You are starting a Porsche 911 from rest to a velocity of 100_mph in 15_seconds. What is the force required to move this 2600_lb vehicle? What is the average power required during this time interval and find its initial and final energy.

Given m = 2600_lb vf = 100_mph vi = 0_mph t = 15_s **Result** $F = 790.1468_lbf$ $a = 35200_ft/min^2$ $P = 105.3529_hp$ $Ki = 0_Btu$ $Kf = 869161.5044_ft \cdot lbf$ v = 50 mph

Forces in Angular Motion

Five equations under this topic define relationships between radial forces, acceleration and power.

1) $F = m \cdot \omega^2 \cdot r$ 2) $v = \omega \cdot r$ 3) $ar = \frac{v^2}{r}$ 4) $\omega = 2 \cdot \pi \cdot n$ 5) $P = \tau \cdot \omega$ Variable Description Egn Units F 1 N force 1 kg m mass angular velocity 1 r/s ω 1 m radius r 1 m/s velocity v radial acceleration 1 m/s^2 ar 1 N·m τ torque 1 W Ρ power rotational speed 1 1/s n

Example 1: A drum with a radius 1.5_ft is spinning at a speed of 240 revolutions per minute. Find the centripetal force on a 1_oz mass on the circumference. Find the radial acceleration and tangential velocity. Use the first four equations to solve the problem.

Given	Result
m = 1_oz	$\omega = 25.1327 \text{ r/s}$
$r = 1.5_{ft}$	F = 8.1871
n = 240_1/min	v = 11.4907_m/s
_	ar = 288.7925_m/s^2

Elastic Collisions (1D)

These two equations cover one-dimensional elastic collisions for a mass m1, with an initial velocity, v1i, colliding with a mass, m2, initially at rest.

1) $v1f = \frac{m1 - m2}{m1 + m2} \cdot v1i$		2) $v2f = \frac{2 \cdot m1}{m1 + m2} \cdot v1i$	
Variable	Description		Eqn Units
v1f	final velocity of m1		1 m/s
m1	mass m1		1_kg
m2	mass m2		1_kg
v1i	initial velocity of m1		1_m/s
∨2f	final velocity of m2		1_m/s

Example: A 10_oz billiard ball travelling at 25_ft/s strikes a 12_oz billiard ball at rest. Find the velocities of the two balls after collision.

Given	Result
m1 = 10_oz	v1f = -2.2728_ft/s
$m2 = 12_{oz}$	v2f = 22.7272_ft/s
v1i = 25_ft/s	_

Inclined Planes

There are six equations in this topic describing the forces of a mass, m1, sliding down an inclined plane subject to a friction. The mass, m1, is being held by a suspended mass, m2.

2) $Fp = \frac{m1 \cdot g \cdot SIN(\Theta + \Theta f)}{COS(\Theta f)}$ 1) $\mu = TAN(\Theta f)$ 3) $Fh = m1 \cdot g \cdot TAN (\Theta + \Theta f)$ 4) $F = m2 \cdot g$ 5) Fp = F6) $Fh \cdot COS(\Theta) = m2 \cdot g$ Variable Description Eqn Units friction coefficient μ 1 1° Θf angle friction 1[°] Θ angle plane Fp force along plane 1 N Fh horizontal force 1 N

m1	mass sliding down	1_kg
m2	mass	1_kg
F	force due gravity	1_N



Example: A 1.25_kg mass slides down a 30_° inclined plane with a coefficient of friction of 0.1. What is the angle of friction and force parallel to the inclined plane?

Given	Result
$\mu = 0.1$	Fp = 7.1907_N
$\Theta = 30^{\circ}$	$\Theta f = 5.7106^{\circ}$
m1 = 1.25 kg	_

Stress Analysis

The seven topics in this category focus on analytical expressions for stress analysis under a variety of conditions, including shear stress analysis, principal stresses and Mohr's circle.

- Normal Stress/Strain
- Axial Load
- Dynamic Load
- Torsion
- Pure Shear
- Principal Stresses
- Mohr's Circle

Normal Stress/Strain

The six equations in this set give the basic relationships between stress, force, area, elongation, and shear stress.

1)
$$\sigma = \frac{P}{A}$$
 2) $\varepsilon = \frac{\delta}{L}$ 3) $\sigma = E \cdot \varepsilon$
4) $ecc = \frac{\sigma}{E} \cdot (1 - 2 \cdot v)$ 5) $\tau = G \cdot \gamma$
6) $G = \frac{E}{2 \cdot (1 + v)}$
Variable Description Equ Units
 σ normal stress 1_Pa
force 1_N
A area 1_m^2
E Young's modulus 1_Pa
 ε normal strain 1
ecc eccentricity 1
 τ shear stress 1_Pa
G shear modulus 1_Pa
G shear modulus 1_Pa
 φ shear strain 1
 V Poisson's ratio 1
L length 1_m

Example: A prismatic bar has a cross section of 800_{mm}^2 and a length of 2.8_m subject to an axial force of 125_{kN} . The measured elongation is 1.4_mm, and has a Young's modulus of 75_GPa. If the shear modulus is 40 GPa, find the Poisson's ratio and eccentricity.

Given	Result
$P = 125_kN$	$\sigma = 156250000$ _Pa
$A = 800 \text{mm}^{2}$	$\varepsilon = 0.0005$
E = 75_GPa	v = -0.0625
G = 40 GPa	ecc = 0.002344
$\gamma = 0.0\overline{5}$	$\tau = 2000$ _MPa
L = 2.8 m	
$\delta = 1.4$ mm	

Axial Load

These five equations describe properties of an axially loaded member and thermal strain.

1) $\delta = \frac{P}{E}$	• <u>L</u> • A	2) $k = \frac{E \cdot A}{L}$	3) f =	$\frac{L}{E \cdot A}$
4) $\varepsilon t = \alpha$	$\cdot \Delta t$	5) $\delta t = \varepsilon t \cdot L$		
Variable	Descrip	tion		Eqn Units
δ	displace	ement		1_m
Р	load			1_N
L	length			1_m
E	Young's	s modulus		1_Pa
A	area			1_m^2
k	stiffness	6		1_N/m
f	complia	ince		1_m/N
εt	thermal	strain		1
α	coeffici	ent of thermal expansion		1_1/K
Δt	tempera	ature change		1_K
δt	thermal	elongation		1_m

Example 1: An axially-loaded member, with an area of 500_mm² and 20_ft long, is subjected to an axial load of 12_klbf. The modulus of elasticity is 155_GPa. Find the elongation, spring constant, and compliance. Use equations 1, 2, and 3 to solve this problem.

Given	Result
$P = 12_klbf$	δ = 4.1987E-3_m
L = 20 ft	$k = 12713254.5932$ _N/m
$E = 155$ _GPa	f = 7.8658E-8_m/N
$A = 500 mm^{2}$	_

Example 2: A 100-foot-long bar has an expansion coefficient of 0.00005_1/°F. Find the thermal strain and thermal elongation for a temperature change of 45_°C.

Given	Result
$L = 100_{ft}$	$\delta t = 0.12344 \text{_m}$

$$\alpha = 0.00005_{1}^{\circ}F$$
 $\varepsilon t = 0.00405_{\Delta t} = 45_{C}^{\circ}C$

Dynamic Load

A sliding collar on a prismatic bar represents a simple case of a dynamic load. The equations below show some basic relationships.

1)
$$\delta \max = \frac{W \cdot L}{E \cdot A} + \left(\left(\frac{W \cdot L}{E \cdot A} \right)^2 + \frac{2 \cdot W \cdot L \cdot h}{E \cdot A} \right)^{\frac{1}{2}}$$

2) $\sigma \max = \frac{E \cdot \delta \max}{L}$
3) $\sigma st = \frac{W}{A}$
4) $\sigma \max = \sigma st + \left(\sigma st^2 + \frac{2 \cdot h \cdot E \cdot \sigma st}{L} \right)^{\frac{1}{2}}$

Variable	Description	Eqn Units
δ max	maximum elongation	1_m
σ max	maximum tensile stress	1 Pa
W	load	1 [¯] N
L	length of bar	1_m
E	Young's modulus	1_Pa
Α	area	1_m^2
h	elevation of flange	1_m
σ st	static stress	1_Pa



Example: A 10_m prismatic bar has a 1_kN load lifted 786_mm from the bottom. The bar has a cross sectional area of 0.00025_{ft}^2 and an elastic modulus of 256_GPa. Find the maximum elongation, maximum stress, and static stress.

GivenResult $W = 1_kN$ $\delta max = 5.3128E-2_m$ $L = 10_m$ $\sigma max = 1360079023.01_Pa$ $E = 256_GPa$ $\sigma st = 43055641.6668_Pa$ $A = 0.00025_ft^2$ h = 786 mm

Torsion

Torsion refers to the twisting of a structural member when loaded by couples that produce rotation about its longitudinal axis. The following equations describe this phenomenon.

1) $\tau = \mathbf{G} \cdot \boldsymbol{\gamma}$ 2) $\boldsymbol{\gamma} = \boldsymbol{r} \cdot \boldsymbol{\Theta}$ 3) $\boldsymbol{\varphi} = \frac{\boldsymbol{T} \cdot \boldsymbol{L}}{\boldsymbol{G} \cdot \boldsymbol{l} \boldsymbol{p}}$

4)
$$lp = \frac{\pi \cdot d^4}{32}$$
 5) $\tau max = \frac{T \cdot r}{lp}$

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Equation Library

Variable	Description	Eqn Units
τ	shear stress	1_Pa
G	shear modulus	1_Pa
γ	shear strain	1
r	radius	1_m
Θ	twist angle per unit length	1_°/m
φ	angle of twist	1_°
Т	torque	1_N ⋅ m
L	length	1_m
lp	polar moment of inertia, circular bar	1_m^4
d	diameter	1_m
τ max	maximum shear stress	1_Pa

Example 1: A shaft with a radius of 5_cm experiences a twist of 8_°/m. The shear modulus of elasticity is 60_GPa. What is the shear stress experienced by the shaft? Use equations 1 and 2.

Given	Result
$G = 60_GPa$	$\tau = 66666666.67$ _Pa
r = 5 cm	$\gamma = 1.1111E-3$
$\Theta = 8_{m}/m$	

Example 2: For the shaft in Example 1, find the total twist and maximum shear stress, if the shaft is 10_ft long, for an applied torque of $5000_N \cdot m$. Use equations 3, 4 and 5.

Given	Result
$G = 60_GPa$	$\phi = 1.4824_{\circ}$
r = 0.05 m	$\tau \max = 25464790.8947$ Pa
$T = 5000 N \cdot m$	$lp = 9.8175E-6_m^4$
$L = 10_{ft}$	
$d = 0.1_m$	

Pure Shear

When a solid is subjected to torsion, shear stresses are developed over cross sections and on longitudinal planes. These equations describe pure shear.

1)
$$\gamma = \frac{\tau}{G}$$

3)
$$\varepsilon \max = \sqrt{1 + SIN(\gamma)} - 1$$

5)
$$\sigma \Theta = \tau \cdot SIN(2 \cdot \Theta)$$

Variable	Description
γ	shear strain
τ	shear stress
G	shear modulus
εmax	maximum strain
E	Young's modulus
v	Poisson's ratio
$\sigma \Theta$	normal shear stress
τΘ	shear stress
Θ	angle

2)
$$\varepsilon \max = \frac{\tau}{E} \cdot (1 + v)$$

4) G =
$$\frac{E}{2 \cdot (1 + v)}$$

6)
$$\tau \Theta = \tau \cdot COS (2 \cdot \Theta)$$

Eqn Units
1
1_Pa
1_Pa
1
1_Pa
1
1_Pa
1_Pa
1_°



Example: A prismatic bar material has a shear modulus of 50_GPa, and a Young's modulus of 160_GPa. For a shear strain of 1%, find the shear stress,

maximum strain and Poisson's ratio. Use equations 1, 3 and 4 to solve the problem.

Given	Result
$\gamma = 0.01$	$\tau = 500.000$ _MPa
G = 50 GPa	$\varepsilon \max = 5.000 \text{E-3}$
E = 160 GPa	v = 0.600

Example 2: For a shear strain of 1%, what is the maximum strain? Use equation 3.

GivenResult $\gamma = 0.01$ $\varepsilon \max = 0.004987$

Principal Stresses

The four equations in this topic describe the relationship between stresses along x and y axes and stresses along rotated axes.

1)
$$\sigma x = \frac{\sigma x + \sigma y}{2} + \frac{\sigma x - \sigma y}{2} \cdot COS(2 \cdot \Theta) + \tau x y \cdot SIN(2 \cdot \Theta)$$

2)
$$\sigma y = \frac{\sigma x + \sigma y}{2} - \frac{\sigma x - \sigma y}{2} \cdot COS(2 \cdot \Theta) + \tau xy \cdot SIN(2 \cdot \Theta)$$

3)
$$\tau x 1 y 1 = \frac{-(\sigma x - \sigma y)}{2} \cdot SIN (2 \cdot \Theta) + \tau x y \cdot COS (2 \cdot \Theta)$$

4)
$$\sigma x 1 + \sigma y 1 = \sigma x + \sigma y$$

Variable	Description	Eqn Units
<i>o</i> x1	normal stress along rotated x-axis	1_Pa
σy1	normal stress along rotated y-axis	1_Pa
σχ	normal stress along x-axis	1_Pa
σy	normal stress along y-axis	1_Pa
Θ	rotational angle	1_°
τχγ	shear stress	1_Pa
τx1y1	rotated shear stress	1_Pa



Example: Calculate principal stresses along a 30_° rotated axis of a system subject to stress of 150000_Pa along the x-axis and 100000_Pa along the y-axis at a shear stress of 200000_Pa.

GivenResult $\sigma x = 150000_Pa$ $\sigma x1 = 310705.0808_Pa$ $\sigma y = 100000_Pa$ $\sigma y1 = 285705.0808_Pa$ $\Theta = 30_{-}^{\circ}$ $\tau xy = 200000_Pa$

Mohr's Circle

The eight equations in this topic cover interrelationships among principal, normal, maximum and minimum stresses, and angles of rotation.

1)
$$\sigma 1 = \frac{\sigma x + \sigma y}{2} + \left(\left(\frac{\sigma x - \sigma y}{2} \right)^2 + \tau x y^2 \right)^{\nu_2}$$

2)
$$\sigma 2 = \frac{\sigma x + \sigma y}{2} - \left(\left(\frac{\sigma x - \sigma y}{2} \right)^2 + \tau x y^2 \right)^{\nu_2}$$

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3)
$$\sigma 1 + \sigma 2 = \sigma x + \sigma y$$

4) $SIN (2 \cdot \Theta p 1) = \frac{\tau x y}{\left(\left(\frac{\sigma x - \sigma y}{2}\right)^2 + \tau x y^2\right)^{\frac{1}{2}}}$

- 5) $\Theta p2 = \Theta p1 + 90$ 6) $\Theta s = \Theta p1 45$
- 7) $\tau \max = \frac{\sigma 1 \sigma 2}{2}$ 8) $\sigma avg = \frac{\sigma x + \sigma y}{2}$

Variable	Description	Eqn Units
σ1	maximum principal normal stress	1_Pa
σ2	minimum principal normal stress	1_Pa
σavg	normal stress on plane of max shear	1_Pa
σχ	normal stress in x-direction	1_Pa
σy	normal stress in y-direction	1_Pa
τχγ	shear stress	1_Pa
Өр1	angle to plane of max principal normal stress	1_°
Θs	angle to plane of max shear stress	1_°
Өр2	angle to plane of min principal normal stress	1_°
τmax	max principal normal stress	1_Pa



Example: For a beam system, the normal x and y stresses are 120_kPa and 90_kPa, respectively. If the system experiences a 75_kPa shear stress, find the maximum and minimum principal normal stresses.

Given $\sigma x = 120_k Pa$ $\sigma y = 90_k Pa$ $\tau xy = 75_k Pa$

Result $\sigma 1 = 181485.2927$ Pa $\sigma 2 = 28514.7073$ Pa $\Theta p1 = 39.3450^{\circ}$

Vibrations

The five topics in this category describe oscillation/frequency relationships in typical mechanical engineering applications.

- Simple and Compound Pendulums
- Damped and Free Vibration
- Natural Frequency-Spring System
- Natural Frequency-Beams
- Vibration Isolation

Simple and Compound Pendulums

These two equations define the period of oscillations of a simple or compound pendulum.

$2 \cdot \pi \cdot \sqrt{\ln g }$ 2) to	$c = 2 \cdot \pi \cdot \sqrt{1/(m \cdot g \cdot h)}$
Description	Eqn Units
simple pendulum period	1_s
compound pendulum period	1_s
simple pendulum length	1_m
moment of intertia	1_kg m.^2
compound pendulum mass	1_kg
distance of center of mass	1_m
	$2 \cdot \pi \cdot \sqrt{len / g}$ 2) to Description simple pendulum period compound pendulum period simple pendulum length moment of intertia compound pendulum mass distance of center of mass

Example 1: A simple pendulum has a period of 1.25_s. Find its length, using equation 1.

Given	Result
ts = 1.25_s	$len = 0.3881_m$

Example 2: A compound pendulum has a moment of inertia of $50 \text{ kg} \cdot \text{m}^2$, and a mass of 75 kg. The center of mass is 8 in away from the point of oscillation. Find its period.

Given	Result
$I = 50_{kg} \cdot m^2$	tc = 3.6343 s
m = 75_kg	

h = 8 in

Damped and Free Vibration

The six equations in this topic focus on the basics of damped oscillation of a spring system. Equations 1 and 6 show the relationship between natural radian frequency and cyclical frequency. Equations 2-5 describe the impact of viscous damping on natural frequency, including conditions for critical damping.

1)
$$\omega = \sqrt{k/m}$$

2) $\alpha = \frac{C}{2 \cdot m}$
3) $\omega d = \sqrt{\omega^2 - \alpha^2}$
4) $\omega d = \omega \cdot \left(1 - \left(\frac{C}{Cc}\right)^2\right)^{\frac{1}{2}}$

5) $Cc = 2 \cdot \sqrt{k \cdot m}$	6) $\omega = 2 \cdot \pi \cdot t$
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Variable	Description	Eqn Units
ω	natural radian frequency	1_r/s
f	frequency	1_Hz
α	damping component	1_1/s
С	coefficient of viscous damping	1_kg/s
Cc	critical damping coefficient	1_kg/s
ωd	damped radian frequency	1_r/s
m	mass	1_kg
k	spring constant	1_N/m

Example 1: A spring has a spring constant of 18_N/m. A mass of 4_oz is suspended. What is the radian and cyclical frequency? Use equations 1 and 6.

Given	Result
$m = 4_{oz}$	$\omega = 12.5989 \text{ r/s}$
k = 18 N/m	f = 2.0052 Hz

Example 2: Design a damped spring system with a vibration frequency of 10_Hz and a damped radian frequency of 50_r/s for a 4_oz mass. Find the

critical damping parameter. Use equations 1 and 6 to find the natural frequency and spring constant. Use equation 3 to find damping component α . Find the coefficient of damping from equation 2, and round off the design using equation 5.

Given	Result
f = 10_Hz	$\omega = 62.8319 r/s$
$\omega d = 50_r/s$	$k = 447.6772$ _N/m
m = 4_oz	$\alpha = 38.0505 \text{ r/s}$
	C = 8.6297 kg/s
	Cc = 14.2500 kg/s

Natural Frequency-Spring System

This topic describes the natural radian frequency of four simple spring systems.

1) ωn =	$\left(\frac{k}{m+\frac{1}{3}\cdot ms}\right)^{\nu_2}$	2) $\omega s = \left(\frac{k \cdot k}{m}\right)$	$\frac{(m1+m2)}{m\cdot m2}\bigg)^{\frac{1}{2}}$
3) $\omega t = v$	(Ks J	4) $\omega t^2 = \left(\frac{\kappa s}{2}\right)^2$	$\frac{(J1+J2)}{J1+J2}\bigg)^{1/2}$
Variable	Description		Eqn Units
k	spring constant		1 N/m
m	mass		1_kg
ms	spring mass		1_kg
m1	mass 1		1_kg
m2	mass 2		1_kg
ωn	natural frequency (sprin	ng + mass)	1_r/s
ωs	natural frequency (sprir	ng + 2 masses)	1_r/s
ωt	natural frequency (torsi	ion)	1_r/s
ωt2	natural frequency (2 to	rsion bars)	1_r/s
Ks	stiffness constant		1_N · m
J	polar moment		1_kg · m ^ 2
J1	polar moment 1		1_kg · m ^ 2
J2	polar moment 2		1_kg · m ^ 2


Example: A spring with a stiffness constant of 275_N/m has a spring mass of 12_oz. If a mass of 8_oz is suspended from this spring, what is its natural frequency? Use the first equation to solve this problem.

Given k = 275_N/m m = 8_oz ms = 12_oz

Result $\omega n = 28.4317 r/s$

Natural Frequency-Beams

These four equations cover the natural frequencies of a cantilever beam, a simple fixed beam, a structured spring and a simple free beam.

1)
$$fn1 = \frac{1}{2 \cdot \pi} \cdot \left(\frac{3 \cdot E \cdot I}{(m + .23 \cdot mb) \cdot len^3} \right)^{\frac{1}{2}}$$

2)
$$fn2 = \frac{1}{2 \cdot \pi} \cdot \left(\frac{48 \cdot E \cdot I}{(m + .5 \cdot mb) \cdot len^3} \right)^{\frac{1}{2}}$$

3)
$$fn3 = \frac{1}{2 \cdot \pi} \cdot \left(\frac{4 \cdot T}{m \cdot len}\right)^{\nu_2}$$

4) $fn4 = \frac{1}{2 \cdot \pi} \cdot \left(\frac{192 \cdot E \cdot I}{(m + .37 \cdot mb) \cdot len^3}\right)^{\nu_2}$

Variable	Description	Eqn Units
fn1	natural frequency cantilever beam	1 Hz
fn2	natural frequency simple fixed beam	1_Hz
fn3	natural frequency structured spring	1_Hz
fn4	natural frequency simple free beam	1_Hz
E	Young's modulus	1_Pa
1	area moment of inertia	1_m^4
m	mass	1_kg
mb	beam mass	1_kg
Т	string tension	1_N
len	length of beam	1_m



Example: A 2600_lb load is placed on a 20_ft cantilever beam weighing 1000_lb. Assuming Young's modulus to be 30_GPa and the area moment of inertia to be 725_in ^4, find the frequency.

Given	Result
$E = 30_GPa$	$fn1 = 1.5381_s$

Equation Library

Vibration Isolation

The equations in this topic describe the basics of how noise vibrations generated by machines (such as motors, turbines, and internal combustion engines) are coupled to their environment, and how to reduce the coupled noise.

1)
$$f = \frac{1}{2 \cdot \pi} \cdot \sqrt{g / \delta}$$

2) $\delta = \frac{meq \cdot g}{k}$
3) $\eta = 1 - \frac{1}{\left(\frac{ff}{f}\right)^2 - 1}$
4) $TR = \beta \cdot \left(1 + \frac{2 \cdot c \cdot ff}{cc \cdot f}\right)^{\frac{1}{2}}$

5)
$$\beta = \frac{1}{\left(\left(1 - \left(\frac{ff}{f}\right)^2\right)^2 + \left(\frac{2 \cdot c \cdot ff}{(cc \cdot f)}\right)^2\right)^{\frac{1}{2}}}$$

Variable	Description	Eqn Units
f	frequency of vibration	1 Hz
ff	forcing frequency	1_Hz
δ	displacement	1_m
k	spring constant	1_N/m
meq	equipment mass	1_kg
η	efficiency of isolation	1
TR	transmissibility ratio	1
β	magnification factor	1
С	coefficient of viscous damping	1_N ⋅ s/m
СС	critical damping	1_N ⋅ s/m

Machine Design

The Equation Library includes three topics involving the design of mechanical elements. No attempt has been made to cover the area of machine design comprehensively.

- Helical Springs
- Frequency of Helical Springs
- Viscosity & Petrof's Law

Helical Springs

These equations describe deflection and stresses in helical springs. A helical spring with a wire diameter, d, and a mean spring diameter, D, is subjected to a force, F. The first equation shows the relationship between the maximum stress in the wire and the applied force. The second equation expresses the stress relationship in terms of a new parameter ks. The last two equations show the relationship between deflection, force, spring parameters and spring rate.

1) $\tau \max = \frac{T \cdot d}{2 \cdot J} + \frac{F}{A}$ 2) $\tau = \frac{Ks \cdot (8 \cdot F \cdot Ds)}{\pi \cdot d^3}$ 3) $T = \frac{F \cdot Ds}{2}$ 4) $J = \frac{\pi \cdot d^4}{32}$ 5) $A = \frac{\pi \cdot d^2}{4}$ 6) $C = \frac{Ds}{d}$ 7) $Ks = \frac{2 \cdot C + 1}{2 \cdot C}$ 8) $y = \frac{8 \cdot F \cdot Ds^3 \cdot N}{d^4 \cdot G} \cdot \left(1 + \frac{1}{2 \cdot C^2}\right)$ 9) $k = \frac{d^4 \cdot G}{8 \cdot Ds^3 \cdot N} \cdot \left(\frac{1}{\left(1 + \frac{1}{(2 \cdot C^2)}\right)}\right)$ Variable Description Eqn Units

F	axial force
Ds	mean spring diameter

Eqn Units 1_N 1_m

d	wire diameter	1_m
А	wire cross section	1_m^2
J	moment of inertia	1_m^4
Т	torsion	1_N∙m
τ	maximum shear stress	1_Pa
τmax	shear stress	1_Pa
С	spring index	1
Ks	shear stress correction factor	1
G	modulus of rigidity	1_Pa
N	no. turns in the spring	1
У	deflection	1_m
k	spring rate	1_N/m



Example: A force of 1000_N is applied to a helical spring with a mean diameter of 1_in and a wire diameter of 0.1_in. Find the spring rate, deflection and stress if the spring has 10 turns. Assume G to be 30_GPa. Using equations 2, 6, 7 and 8 we get:

Given	Result
F = 1000 N	Ks = 1.0508
Ds = 2.5 cm	C = 9.8425

d = 0.1_in	$\tau = 4082244731.6$ _Pa
$N = 10^{-10}$	k = 993.866 N/m
$G = 30_GPa$	y = 1.0062 m

Frequency of Helical Springs

Physical properties of a spring influence the mechanical vibration characteristics of a helical spring. The six equations in this topic identify natural frequencies of vibration based on spring constant and mass.

1)
$$\omega = \pi \cdot \sqrt{k/m}$$

2) $f = \frac{1}{2} \cdot \sqrt{k/m}$
3) $fs = \frac{1}{4} \cdot \sqrt{k/m}$
4) $m = A \cdot L \cdot \rho$

5)
$$m = \frac{\pi^2 \cdot d^2 \cdot Ds \cdot Na \cdot \rho}{4}$$
 6) $A = \frac{\pi \cdot d^2}{4}$

Variable	Description	Eqn Units
ω	natural frequency	1_r/s
k	spring rate	1_N/m
m	spring mass	1_kg
f	frequency	1_Hz
fs	frequency fixed at one end	1_Hz
Α	area of cross section	1_m^2
L	length of spring	1_m
ρ	density	1_kg/m^3
d	wire diameter	1_m
Ds	mean spring diameter	1_m
Na	number of coils	1

Example: A spring with 25 turns is made of a 0.2_in diameter wire, has a mean diameter of 1.65_in and a density of $6_g/cm^3$. The spring constant is 18000_N/m. Find the length of the spring and its natural frequency.

Given	Result
k = 18000 N/m	$\omega = 1332.3799 r/s$
$\rho = 6_g/cm^3$	$f = 212.0548$ _Hz
d = 0.1_in	fs = 106.0274 Hz
$Ds = 1.65_{in}$	A = 5.067E-6_m^2

Na = 25 $L = 3.2916_m$ m = 0.1001 kg

Viscosity & Petroff's Law

These eight equations describe Newton's law of viscosity and Petroff's law, introduce dynamic viscosity, and use the Sommerfeld number to describe force, torque and friction factor, and bearing frictional forces.

1)
$$\tau = \frac{F}{A}$$
 2) $\tau = \frac{2 \cdot \pi \cdot r \cdot \mu \cdot N}{c}$

3)
$$T = \frac{4 \cdot \pi^2 \cdot r^3 \cdot l \cdot \mu \cdot N}{c}$$

4)
$$T = 2 \cdot r^2 \cdot fp \cdot I \cdot P$$

5)
$$fp = \frac{\frac{2 \cdot \pi^2 \cdot \mu \cdot N}{P} \cdot r}{c}$$

6)
$$S = \frac{\left(\frac{r}{c}\right)^2 \cdot \mu \cdot N}{P}$$

7)
$$\frac{fp \cdot r}{c} = 2 \cdot \pi^2 \cdot S$$

Variable	Description	Eqn Units
τ	shear stress	1 Pa
F	force	1 ⁻ N
Α	area of cross section	1_m^2
r	shaft radius	1_m
μ	dynamic viscosity	1 [¯] Pa∙s
N	shaft rotation in rev/s	1 ⁻ 1/s
с	radial clearance	1_m
т	torque	1_N∙m
1	length of bearing	1_m
fp	Petrof's coefficient	1
Р	pressure on projected area	1_Pa
S	Sommerfeld number	1



Example: A force of 1000 N is acting on an area of 12 in 2. Find the stress produced using equation 1.

Given	
F = 1000 N	
A = 12 in^2	

Result $\tau = 129166.925$ _Pa

Chapter 3 Constants Library

In This Chapter

The Constants Library is a collection of physical constants commonly used in mechanical engineering. This chapter covers:

- **Types of Constants**
- □ Using the Constants Library
- □ Using the ECON Function
- □ Constants Library Softkeys

Types of Constants

The Constants Library lists the symbols, descriptions and SI units of three classifications of constants, shown below:

Universal Constants

pi	
R	Universal gas constant
NA	Avogadro's number
Vm	Molar volume
StdT	Standard temperature
StdP	Standard pressure
εO	Permittivity of vacuum
с	Velocity of light in vacuum
h	Planck's constant
k	Boltzmann's constant
σ	Stefan-Boltzmann
c1	Spectral 1
c2	Spectral 2
c3	Wien's displacement

Magnetic Properties

μο	Permeability of vacuum
φo	Magnetic flux quantum
F	Faraday's constant
μe	Electron magnetic moment
μP	Proton magnetic moment

Mechanical, Thermal

G	Gravitational constant
g	Acceleration of gravity
ρH2O	Density of H2O at 20 °C
λH ₂ O	Refractive index of H ₂ O at 20 °C
cpH ₂ O	Heat capacity of H ₂ O at 20 °C
HfH ₂ O	Heat of fusion of H ₂ O
HvH₂O	Heat of vaporization of H ₂ O

Using the Constants Library

Select CONSTANTS LIBRARY from the main menu screen. The Constants Library menu displays three classes of constants:



Example: Suppose you want to find the acceleration of gravity. Use the cursor keys to move the pointer to the MECHANICAL, THERMAL menu item and press **ENTER** to display the following screen:



Move the pointer to ACCELERATION OF GRAVITY. Five softkeys are available at this level and are described at the end of this chapter. To view the value for this constant, press the **VALUE** softkey. This results in the following display:

To place the constant's value on the stack, press ENTER or the STK softkey. The screen flashes a "Value to stack" message, places the value on the stack as a tagged object, then returns to the MECHANICAL, THERMAL menu. The value(s) you entered on the stack become available for calculation when you exit the software. To remove the tag once the value is on the stack press FMG OBJ MAT DTAG.

Using the ECON Function

You can extract the value of any constant without entering the Mechanical Engineering Application Pac with the ECON() function. In all cases, the constant name must be prefixed with a '\$' symbol, accessed by African For example, suppose you want to retrieve the acceleration of gravity:

User Program Method

Inside a user program, use the commands 'g' ECON or 'ECON(g')' EVAL to retrieve the acceleration of gravity in SI units of m/s².

ł	HOME }	
4	:	
2	:	
1	:	9.8066352
Ľ.	IEAP ECON DEREC	DERUB ABOUT

Stack Method

Type '\$g' into level 1 of the stack and press the **ECON** library softkey or type the letters ECON and press **ENTER**.

The constant value will have SI units if units are selected (i.e., if flag 61 is clear); otherwise, the value will have no units.

Constants Library Softkeys

- VALUE Displays the value of the constant with units on the screen. Press ENTER to return to the constants list.
- **STK** Places a copy of the selected constant on the calculator stack. Whether or not the value has units appended is controlled by the units key setting, which can be toggled at the Equation Library screen.
- FONT Toggles between large and small display fonts.
- **UP** Moves up one level in the menu structure.
- MAIN Exits to the main menu.

Chapter 4 Analysis

In This Chapter

This chapter describes three sets of tools used to solve common problems in mechanical engineering.

Steam	Та	bles

Vector Analysis

☐ Thermocouples

The following sections should be read in order, as some information is common to all three topics. These topics are accessed directly from the main menu, shown below:

MERLINA	E110	
I MECHHNICHL	ENG	HPP
RESUME SOLVING		
EQUATION LIBRARY		
→STEAM TABLES		
VECTOR ANALYSIS		
THERMOCOUPLES		
CONSTANTS LIBRARY		
REFERENCE LIBRARY		
	L E N	NTLOUT
		NI VUII

From the main menu, move the pointer to STEAM TABLES and press ENTER.

Steam Tables

Steam Tables is a collection of programs organized as a powerful computational engine designed to calculate thermodynamic properties of steam in a user-friendly environment. Calculations of thermodynamic properties are covered for saturated and superheated steam.

Steam properties are a complex function of temperature, pressure, volume, critical temperature, critical pressure, and molecular weight. The properties listed in this software have been tabulated over a decade. Best fit routines have been developed and agreed upon through the International Formulation

Committee. In cases where it is impossible to get good curve fits, regions of interest have been divided into two or three ranges with separate equation sets. The following tables list all steam properties available in the software.

Saturated Steam Properties

Variable	Description	Units
T(s)	saturation temperature	1_K
P (s)	saturation pressure	1_mPa
V (f)	specific volume - liquid	1_m ^ 3/kg
V (g)	specific volume - vapor	1_m ^ 3/kg
H (f)	enthalpy - liquid	1_KJ/kg
H (fg)	latent heat of vaporization	1_KJ/kg
H (g)	enthalpy - vapor	1_KJ/kg
S(f)	entropy - liquid	1_KJ/(kg ⋅ K)
S (fg)	S (g) - S (f)	1_KJ/(kg⋅K)
S (g)	entropy - vapor	1_KJ/(kg⋅K)
U (f)	internal energy - liquid	1_kJ/kg ⋅ K)
U (g)	internal energy - vapor	1_kJ/kg⋅K)

Superheated Steam Properties

Variable	Description	Units
Temp	given temperature	1_K
Sat Press	given pressure	1_mPa
Sat Temp	corresponding temperature	1_K
Specific Vol	specific volume	1_m ^ 3/kg
Enthalpy	enthalpy	1_KJ/kg
Entropy	entropy	1_KJ/(kg⋅K)

Using Steam Tables

Once you have selected STEAM TABLES at the main menu, the first screen displays two menu items: temperature and pressure. To compute *saturated* steam properties, you can enter a value for either temperature or pressure. Properties of *superheated* steam require you to enter values for both temperature and pressure.



Example: Suppose you want to calculate the properties of saturated steam at 30_°C. First, move the pointer to Temp. and press **ENTER**. At the cursor type in 30. To complete the entry, add the units symbol by pressing the appropriate softkey, in this case **C** and press **ENTER**. The following screen displays:

Saturated Steam TEMP(_K): '30_°C' →PRESSURE(_MPA):
T→ P→ SUPER →STK FONT UP

To view the calculated thermodynamic properties, press

-Saturated Steam Prop.
Tearan area arean in opin
(→T(S): '303.1500000_K'
P(S): '0.0042505 MPA'
U(E) 10 001000E MA3/KG
1077- 0.0010013_FT 3CKG
ACCY: .9592323797W.,95KC.
H(F): '125.0553927_KJ/KG'
N(EG): '2430 5279179 K.1/KG'
M(G): 2556.5663358_KJ/KG
S(F): '0.4341480_KJ/(KGXK)'
ASTV CONT UP
731K[run1] UF

The steam table engine reports all its calculations in SI units. When entering values you may use any compatible units supported by the HP 48SX.

The saturated steam properties can also be computed by allowing a value for pressure and pressing the sofkey \mathbf{P} . The results from this computation are similar to those reported in the screen above.

Ranges of Temperature and Pressure

The computed results are valid only for the following finite ranges of temperature and pressure:

Saturated	Superheated
Temperature: 273.16 - 647.3 K	> Saturated temperature

Pressure: 0.006113 - 22.08 MPa Pressure: 0.006113 - 22.08 MPa

Vector Analysis

Vectors are quantities having both magnitude and direction, such as displacement, force, velocity, momentum and acceleration. This software tool enables you to perform many of the common tasks in vector algebra, such as combining to obtain scalar product, vector product, vector addition and vector subtraction.

After you select VECTOR ANALYSIS at the main menu and press ENTER, the following screen displays:

Vector →MAG A: LOC1 A: [LOC2 A: [MAG B: LOC1 B: [LOC2 B: [Analysis
CROSS DOT	ADD +STK FONT UP

Specifying Vectors

Ususally vectors are specified by a magnitude and a direction. The vector analysis function in the Mechanical Engineering Application Pac is limited to two or three-dimensional vectors.

To specify a vector, you need to enter its magnitude and two points to determine the direction. This procedure is used because in problems such as structural anaylsis, the direction of a vector is inferred by the beginning and end points of a structural member, and magnitude is entered separately. In addition, this approach allows you to enter vectors originating at several points in space. If you choose to specify the direction using only one vector, you need to enter the value in Location 2, and enter $[0\ 0\ 0]$ in Location 1.

Once the computation is complete, the result is displayed as vector B and the system is ready to receive a new vector. This feature allows you continual use of the interface to solve vector analysis problems.

The new softkeys available in the vector analysis function are described below.



Takes the vector product of two vectors and presents a new vector.



Takes the scalar product of two vectors and presents a new scalar quantity.



Adds two vectors specified.

Example: Two force vectors have magnitudes of 100 and 89. The direction of the first vector is specified to be along a line from a $[0\ 0\ 0]$ to $[4\ 5\ 6]$, while the second vector is specified to be along a line from $[10\ 2\ 9]$ to $[3\ 7\ 9]$. Find the scalar product. After the data has been entered you should see the following screen:

Vector Analysis
LOCI A: [0 0 0] LOCZ A: [4 5 6]
MAG 8:89 LOC1 8: (10 2 9 1
LOC2 B: [3 7 9]
CROSS DOT ADD →STK FONT UP

Press **DOT**to reveal the following results:



Thermocouples

This analysis tool is designed to convert a temperature to a thermocouple output in millivolts and vice versa. The software has the ability to handle T, E, J, K and S type thermocouples. The implied assumption for a reference temperature is 0_°C. The thermocouple computations are based on the IPTS-68 standards.

Using the Thermocouples Function

Select THERMOCOUPLES at the main menu. The first screen lists the five types of thermocouple values supported by the software. As an example, suppose you want to find the corresponding temperature of an E type thermocouple showing a 22.13 millivolt reading.

First, move the pointer to TYPE E and press ENTER to display the following screeen:

Type E Thermocouple VOLTAGE(_MV): >TEMP(_=C):
TƏV TEMP. RANGE(®C): -270/1000 Vət Temp. Range(®C): 0/400 Vət Max Dev(®C): 0.25 Təv Vət Ernsejəstk Font up

Press ENTER. At the prompt type 22.13 and press ENTER again. The screen displays this value as voltage in millivolts. Next, press the **V**-T softkey to initiate the voltage-to-temperature conversion calculation (314.059_°C):



Basis for Temperature/Voltage Conversions

The temperature-to-voltage conversion is based on a 12th to 14th order polynomial, ensuring very precise calculations. The voltage-to-temperature

conversion is based on a 5th or 6th order polynomial. A maximum deviation listing or applicable temperature ranges are displayed on each screen.

Summary of Softkeys

ADD	Adds two vectors.
CROSS	Takes the vector product of two vectors and presents a new vector.
DOT	Takes the scalar product of two vectors and presents a new scalar quantity.
FONT	Toggles between small and large display fonts.
⇒STK	Copies selected entry to calculator stack.
UP	Moves up one level in the menu structure.
Т-	Computes saturated steam properties given T.
P→	Computes saturated steam properties given P.
SUPER	Computes superheated steam properties.
Т-У	Converts temperature specified in °C to voltage in mV.
VC-+T	Converts voltage specified in mV to temperature in °C.
ERASE	Clears voltage and temperature values.

Notes

Chapter 5 Reference Library

In This Chapter

The Reference Library is a collection of data, divided into four topics, that are commonly used in fluid mechanics calculations.

□ Reference Library Topics

□ Using the Referency Library

Reference Library Topics

Selecting the REFERENCE LIBRARY from the main menu displays the topics. A description of each topic is listed in the table below:



Water Physical Properties	Lists density, dynamic viscosity,
	and kinematic viscosity for water at
	0 °C to 100 °C.
Orifice Coefficients for Water	Gives the coefficient of discharge,
	contraction, and velocity for 8 differ-
	ent nozzle configurations.
Valve and Fitting Loss Coefficients	Lists K values for 13 different valve
	and fitting configurations.
Relative Roughness	Gives the relative roughness of
	eight types of pipes.

Using the Reference Library

Suppose you need the relative roughness of galvanized iron for a pipe flow calculation. Use the cursor keys to move the pointer to the RELATIVE ROUGHNESS menu item and press **ENTER**. This displays the following screen:



Move the pointer to GALVANIZED IRON and press **ENTER**. This displays the relative roughness of iron:



Press ENTER to copy this value onto the calculator stack. You need to exit the software to continue your calculation on the stack.

Reference Library Softkeys

→STK	Copies selected entry to calculator stack.
PRINT	Allows you to print a data field or the entire list of data to an IR printer.
ALL	Sends all the data in a list to an IR printer.
ONE	Sends the data in the field selected by the pointer to an IR printer.
UNITS	Toggle key. Indicates units are off. When off, all variables are assumed to be SI.
UNITE	Toggle key. Indicates that units are on.

Appendix A Warranty and Service

Pocket Professional Support

You can get answers to your questions about using your Pocket Professional card from Sparcom. If you don't find the information in this manual or in the HP 48SX *Owner's Manual*, contact us in writing, at :

Sparcom Corporation

Attn: Technical Support Dept. 897 NW Grant Avenue, Corvallis, OR 97330, U.S.A. (503) 757-8416

or send E-mail:

from Internet:	support@sparcom.com
from Compuserve:	>Internet:support@sparcom.com
from FidoNet:	To:support@sparcom.com

Limited One-Year Warranty

What Is Covered

The Pocket Professional is warranted by Sparcom Corporation against defects in material and workmanship for one year from the date of original purchase. If you sell your card or give it as a gift, the warranty is automatically transferred to the new owner and remains in effect for the original one-year period. During the warranty period, we will repair or replace (at no charge) a product that proves to be defective, provided you return the product and proof of purchase, shipping prepaid, to Sparcom.

What Is Not Covered

This warranty does not apply if the product has been damaged by accident or misuse or as the result of service or modification by any entity other than Sparcom Corporation. No other warranty is given. The repair or replacement of a product is your exclusive remedy. ANY OTHER IMPLIED WARRANTY OF MERCHANTABILITY OR FITNESS IS LIMITED TO THE ONE-YEAR DURATION OF THIS WRITTEN WARRANTY. IN NO EVENT SHALL SPARCOM CORP. BE LIABLE FOR CONSEQUENTIAL DAMAGES. Products are sold on the basis of specifications applicable at the time of manufacture. Sparcom shall have no obligation to modify or update products, once sold.

If the Card Requires Service

Sparcom will repair a card, or replace it with the same model or one of equal or better functionality, whether it is under warranty or not.

Service Charge

There is a fixed charge for standard out-of-warranty repairs. This charge is subject to the customer's local sales or value-added tax, wherever applicable. Cards damaged by accident or misuse are not covered by fixed charges. These charges are individually determined based on time and material.

Shipping Instructions

If your card requires service, ship it to Sparcom Corporation, 897 NW Grant Avenue, Corvallis, OR 97330, U.S.A.

- Include your return address and a description of the problem.
- Include proof-of-purchase date if the warranty has not expired.
- Include a purchase order, along with a check, or credit card number and expiration date (VISA or MasterCard) to cover the standard repair charge.
- Ship your card, postage prepaid, in adequate protective packaging to prevent damage. Shipping damage is not covered by the warranty, so insuring the shipment is recommended.

Cards are usually serviced and reshipped within five working days.

Environmental Limits

The reliability of the Pocket Professional depends upon the following temperature and humidity limits:

- Operating temperature: 0 to 45 °C (32 to 113 °F).
- Storage temperature: -20 to 60 °C (-4 to 140 °F).
- Operating and storage humidity: 90% relative humidity at 40 °C (104 °F) maximum.

Warranty and Service

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Appendix C Questions and Answers

Questions Commonly Asked

- **Q.** I can't find the MEAPP subdirectory in the Library menu. How can I verify that the card and the calculator are functioning properly?
- A. There are several possibilities:

a. Check to make sure that the card is properly seated in the calculator port.

b. Turn the calculator off and on.

c. The calculator checks the application card when it turns on. If an "Invalid Card Data" or a "Port Not Available" message is displayed, the card may require service.

- **Q**. What do three dots (...) mean at the end of a display line?
- A. The three dots indicate that the object is too long to show on one line. To view the complete object, use the cursor keys to move the arrow to the object and press in the line or area or any returns you to the original display of the item.
- **Q.** I'm using the Equation Library to solve a problem. After selecting the equations and entering values for the variables, the calculator displays "Too many unknowns." What's wrong?
- **A.** Not enough variables were specified to completely solve the problem. You will have to specify more values and solve again.
- **Q.** I'm using the Equation Library to solve a problem. After selecting the equations, I'm ready to enter values for my variables. I find that some of the variables have values already displayed. What's wrong?
- A. The variables with values displayed indicate that these variable names have been used in solving another equation. To start with a clean slate of values, you can use MEAPP to reset the values of all variables to 0.

- **Q**. While using the Equation Library, I turned units off and all the numbers changed. What's wrong?
- A. In no-units mode, the Equation Library assumes that all values are SI in order for the equations to solve correctly. Therefore, when units are turned off, all values are first converted to SI units, then the unit tags are eliminated.
- **Q.** While using the Equation Library to solve an equation set, intermediate answers are given. Why?
- **A.** The Sparcom's equation solver engine has the ability to solve a set of equations in a systematic fashion. The result of computation from each equation is reported, to keep you informed of the solver's progress.
- **Q**. The calculator displays "Bad Guess(es)" while running the Equation Library. What's wrong?
- **A.** The HP 48SX root finder encountered variable values or units that prevented a solution. You may need to start the root finding process by providing a "guess" value. See Chapter 1 for details.
- **Q**. While solving for an angle, I got an answer that was too large: For example, 8752 degrees instead of the expected answer of 112 degrees.
- A. The calculated result may be offset by integer multiples of 360 degrees. By entering a "guess" value, or by solving in no-units mode, you should be able to avoid this problem.
- **Q.** I solved a problem some time ago, and I'm trying to recall those calculated values for a problem I'm working on now. The values from the past calculation have changed. What's wrong?
- **A.** Most likely, the same variable name was used in solving another equation, so you will not be able to recall the old values.
- **Q**. While searching a list of information, I used the alpha key, but the search function didn't work. Why?
- **A.** Since the search function is case-sensitive, it's very possible that you entered the letters in the incorrect case.

Index

A

Accessing Available Libraries, 1-3 Accessing equations, 1-7 Accessing the Application Pac, 1-3 Additional Units Softkeys, 1-11

В

Bad guesses, 1-19 Beams, 2-1 Cantilever-Moment, 2-7 Cantilever-Point Load, 2-4 Cantilever-Uniform Load, 2-5 Hollow Rectangle/I/C, 2-1 L/T/U, 2-3 Simple Beam-Linear Load, 2-12 Simple Beam-Moment, 2-10 Simple Beam-Point Load, 2-8 Simple Beam-Uniform Load, 2-9

С

CONS Command, 3-3 Constants Magnetic Properties, 3-2 Mechanical, Thermal, 3-2 Universal, 3-1 Constants Library, 3-1 Converting Data, 1-12

D

Default units, 1-13 Displaying a constant on the screen, 3-4 Displaying equations, 1-8

Ε

ê, 2-73 ECON Function, 3-3 Editing Text Entries, 1-6 Editing the Browser, 1-6 Ellipsis ..., 1-5 Environmental limits of card, A-3 Equation Library, 1-7

F

Fluid Mechanics, 2-14 Bernoulli's Equation, 2-16 DARCY, 2-24 Discharge from Tanks, 2-19 Fluid Statics, 2-14 Friction Loss, 2-24 Horizontal Jet on Vertical Plate, 2-21 Immersed Bodies, 2-26 Manometers, 2-23 Mechanical Energy Balance, 2-17 Vertical Jet on Horizontal Plate, 2-22 Font Changing font size, 1-5

G

Gas Laws, 2-27 Gas-Constant Temperature, 2-30 Gas-Constant Volume, 2-29 Gas-Contant Pressure, 2-28 Ideal Gas Laws, 2-27 Polytropic Process, 2-34 Real Gas Law, 2-33 Thermodynamics/Ideal Gas Law, 2-31 Z Factor, 2-33

Η

I

Heat Transfer, 2-36 Biot modulus, 2-45 Blackbody Radiation, 2-49 Forced Convection-Flat Plate (Drag), 2-42 Forced Convection-Flat Plate (Heat), 2-40 Fourier modulus, 2-44 Heat Conduction-Cylindrical, Spherical Wall, 2-39 Lumped Cap Analysis, 2-44 Negligible Surface Resistance, 2-45 PLAM21 function, 2-49 Radiant Heat Exchange, 2-50 Resistance Analog, 2-37 Semi-Infinite Solid, 2-48 Steady State-Conduction & Convection, 2-36 TCYL, 2-46 TCYLINF, 2-46 TPARINF, 2-46 **TSLAB**, 2-46 TSPH, 2-45 HP 48SX equationwriter, 1-9

Installing an Application Card, 1-1

Κ

Key ATTN, 1-5, 1-9, 1-22 CST (Custom Menu), 1-4 Library, 1-3 NXT, 1-11 - 1-12 On, 1-3 SPC, 1-17 Visit, 1-5

L

Loading values from stack, 1-19

Μ

Machine Design, 2-74 Frequency of Helical Springs, 2-76 Helical Springs, 2-74 Sommerfeld number, 2-77 Viscosity of Petrof's Law, 2-77 Main Menu, 1-4 - 1-5 Managing Units, 1-13 MEAPPD directory, 1-12, 1-20 Mechanics, 2-52 Angular Motion, 2-53 Elastic Collisions (1D), 2-56 Force, Work, Power, 2-54 Forces in Angular Motion, 2-55 Inclined Planes, 2-56 Linear Motion, 2-52 Memory Requirements, 1-2 MEpar, 1-20 Merged Memory, 1-3 Moving around the screen, 1-5

0

ON key, 1-2 Options after solving equation, 1-12 Orifice Coefficients for Water, 5-1

Ρ

Plotting X, Y coordinates, 1-17 Plotting -Proper form of equations, 1-16 Plotting equations, 1-16 Plotting multiple graphs, 1-18 Plotting speed, 1-17 Putting constants on the stack, 3-4

Q

Questions Commonly Asked, C-1

R

Reference Library, 1-5 Referency Library, 5-1 Relative roughness, 5-1 Removing an Appplication Card, 1-2 Resume Solving, 1-13

S

Saturated Steam Properties, 4-2 Enthalpy - liquid, vapor, 4-2 Entropy - vapor, liquid, 4-2 Internal energy - liquid, vapor, 4-2 Temperature/pressure range, 4-3 Search Mode, 1-6 Search string, 1-6 Seeding the Solver, 1-19 Selecting equations, 1-8 Service Service charge, A-2 Shipping instructions, A-2 Service (if card requires), A-2 SI units, 1-13 Softkey ABOUT, 1-3 ADD, 4-7 ALL, 5-2 CALC, 1-11, 1-15 CLEAR, 1-12 **CONS**, 1-5 CONV, 1-12 COORD, 1-18 CROSS, 4-7 DEL, 1-7 DOT. 4-7 **DTAG**, 3-3 ECHO, 1-20 EQNS, 1-8 ERASE, 4-7 F, 1-18 FNC, 1-18 INS, 1-7 KEY, 1-18 **KEYS**, 1-18 KNOW, 1-19 MAIN, 1-21, 3-4 MCON, 1-3 MEAP, 1-20

MEAPP, 1-3 OBJ, 3-3 ON, 1-1 **ONE**, 5-2 P-, 4-7 PLOT, 1-16 PRINT, 5-2 **PURGE**, 1-12 QUIT, 1-21 SELECT, 1-8, 1-14 SKIP. 1-6 **SLOPE, 1-18** SOLVE, 1-10, 1-15 STK, 1-20 SUPER, 4-7 T-, 4-7 T-V, 4-7 **UNITS. 1-13** UP. 1-13 V-T, 4-7 VALUE, 3-3 VARS, 1-9 **VIEW**, 1-22 WANT, 1-22 Solver function, 1-10, 1-19 Solving equations, 1-10, 1-14 Solving multiple equations, 1-13 Steam tables, 1-4, 4-1 Critical pressure, 4-1 Critical temperature, 4-1 Stress Analysis, 2-57 Axial Load, 2-59 Dynamic Load, 2-60 Mohr's Circle, 2-65 Normal Stress/Strain, 2-57 Principle Stresses, 2-64 Pure Shear, 2-62 Torsion, 2-61 Summary of Functions Equation Library, 1-23 Reference Library, 5-2 Solver, 1-23 Superheated Steam Properties, 4-2 Enthalpy, 4-2 Entropy, 4-2 Specific volume, 4-2 Temperature/pressure range, 4-3

T

Tagging Variables (calculated), 1-12 Tagging variables (knowns), 1-11 Tagging variables (wanted), 1-15 Textbook form of equations, 1-9 Thermocouples, 1-4, 4-6 Basis for temperature/voltage conversions, 4-6 T, E, J, K, S type, 4-6 Time (computational), 1-19

U

Unit conversion, 1-12 Units Managing units, 1-13 Using units, 1-10

V

Valve and Fitting Loss Coefficients, 5-1 Variable Definitions, 1-9 Vector analysis, 1-4, 4-4 Scalar product, 4-4 Vector addition, 4-4 Vector product, 4-4 Vibrations, 2-68 Damped and Free Vibration, 2-69 Natural Frequency-Beams, 2-71 Natural Frequency-Spring System, 2-70 Simple and Compound Pendulums, 2-68 Vibration Isolation, 2-73 Viewing Wide Entries, 1-5

W

Warranty, A-1 Water Physical Properties, 5-1 Notes:



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